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Microdroplet photofuel cells to harvest high-density energy and dye degradation†

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In this study, a membraneless photofuel cell, namely, μ -DropFC, was designed and developed to harvest chemical and solar energies simultaneously. The prototypes can also perform environmental remediation to demonstrate their multitasking potential as a sustainable hybrid device in a single embodiment. A hydrogen peroxide (H_2O_2) microdroplet at optimal pH and salt loading was utilized as a fuel integrated with Al as an anode and zinc phthalocyanine (ZnPC)-coated Cu as a cathode. The presence of n-type semiconductor ZnPC in between the electrolyte and metal enabled the formation of a photo-active Schottky junction suitable for power generation under light. Concurrently, the oxidation and reduction of H_2O_2 on the electrodes helped in the conversion of chemical energy into the electrical one in the same membraneless setup. The suspension of Au nanoparticles (Au NPs) in the droplet helped in enhancing the overall power density under photonic illumination through the effects of localized surface plasmon resonance (LSPR). Furthermore, the presence of photo-active n-type CdS NPs enabled the catalytic photo-degradation of dyes under light in the same embodiment. A 40 μL μ -DropFC could show a significantly high open circuit potential of ~ 0.58 V along with a power density of 0.72 mW cm^{-2} . Under the same condition, the integration of ten such μ -DropFCs could produce a power density of $\sim 7 \text{ mW cm}^{-2}$ at an efficiency of 3.4%, showing the potential of the prototype for a very large scale integration (VLSI). The μ -DropFC could also degrade $\sim 85\%$ of an industrial pollutant, rhodamine 6G, in 1 h while generating a power density of $\sim 0.6 \text{ mW cm}^{-2}$. The performance parameters of μ -DropFCs were found to be either comparable or superior to the existing prototypes. In a way, the affordable, portable, membraneless, and high-performance μ -DropFC could harvest energy from multiple resources while engaging in environmental remediation.

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1. Introduction

Infusing the efficacies of nanoscale science^{1,2} in microfluidic devices for the development of affordable and portable energy harvesters with a significantly high power density has attracted major research attention in the recent years. The inventions of state-of-the-art thermoelectric, triboelectric, piezo-acoustic, electrokinetic, or Marangoni energy harvesters are directed towards this end.^{3–9} Interestingly, the traditional renewable¹⁰ or non-renewable¹¹ energy-harvesting technologies have also been

undergoing a paradigm shift from the regime of macroscopic to the very large scale integration (e.g. VLSI) of micro or nanoscopic prototypes for enhanced efficiency, higher throughput, and escalated power density.¹² Thus, it is not very surprising that a flurry of research activities has also been observed in the miniaturization along with process intensification¹³ of more widely employed commercial energy harvesters such as batteries,^{14,15} photovoltaic cells,¹⁶ or fuel cells^{17,18} for better efficiency.

In particular, since the path-breaking invention by Sir William Grove in the 18th century¹⁹ to convert chemical energy into the electrical one, fuel cells (FCs) have shown remarkable progress²⁰ despite numerous setbacks.²¹ For example, the utility of the FCs as isolated or distributed power resources has now been translated into a few megawatt plants for power supply.¹⁷ A large varieties of FCs composed of polymer electrolyte membranes, phosphoric acid, methanol or alkali have made appearance at different lengths and performance scales not only to power energy-intensive rockets but also to run miniaturized micro-transmitters or biomedical devices.^{22–25} Presently, the fuels utilized in the FCs are either hydrogen (H_2), methanol

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(CH₃OH), methane (CH₄) or their different combinations.²⁶ In particular, H₂ has been the preferred fuel over others owing to its higher energy density and green chemistry to produce water during energy harvesting.^{26,27}

However, as an alternative, hydrogen peroxide (H₂O₂) has lately been employed as an alternative fuel for FCs because of its high energy density and non-toxicity until a concentration of 20 M.²⁸ Much like H₂, peroxide is also a carbon-free and green energy source producing water and oxygen during energy harvesting.²⁹ In short time, the peroxide FCs have evolved from simple oxidizers to standalone energy sources^{28,30} because (i) the existence of peroxide in the liquid state under ambient conditions makes it a better candidate for fuel storage than H₂; (ii) although peroxide possesses a lower gravimetric energy density, it has a significantly higher volumetric energy density; and (iii) they have higher fuel efficiency suitable for the space or underwater applications.^{23,24} However, the peroxide FCs also face limitations associated with the production,³¹ preservation,^{32,33} supply, and storage²⁸ of rather unstable H₂O₂ at industrial scale.

In the recent years, the utilization of membranes in FCs has been found to be slowly waning, which is paving the way to much simpler membraneless single-compartment FCs. The concept was first realized by Yamazaki *et al.*³⁴ who employed H₂O₂ as both an electron acceptor and a fuel with an Ag cathode alongside using Au, Pt, Pd or Ni anodes. Subsequently, various cathodic (*e.g.* metals, inert materials, conducting dyes or their combinations)^{34,35} and anodic (*e.g.* Al, Ni, C, and noble metals)^{30,36,37} materials have been experimented for membraneless FCs over the years. In particular, ferrocyanides along with phthalocyanines and porphyrins³⁸ (PCs) have been found to be excellent candidates for H₂O₂ reduction owing to their low-onset potentials and cost-effectiveness.^{30,36,39–41} Interestingly, an Al (anode)–H₂O₂ (fuel) combination is found to possess a significantly higher specific energy (~17 000 W h kg^{−1}),^{18,42} which is even higher than some of the state-of-the-art Li-ion batteries (~12 000 W h kg^{−1}).⁴³ However, the membraneless peroxide FCs also suffer from the limitations associated with the crossover of reactants and, thus, are suitable for only low-power intensive systems.

In view of this background, we report the design and development of a peroxide microdroplet-based membraneless FC, namely, μ -DropFC, which is capable of converting the combined influences of the chemical and light energies into the electrical one under the same embodiment. In a sense, the droplet-based device is found to be an exception to most of the previous attempts, where film-based approaches were preferred.^{5,8} While the usage of the microdroplet architecture helps in gaining advantages from the confinement effects due to miniaturization, the photo-activity of the droplet helps in improving the open circuit voltage (ψ_{oc}) and current density (J) of the μ -DropFC.¹⁶

The photo-activity^{44,45} inside μ -DropFCs has been facilitated by the localized surface plasmon resonance (LSPR)⁴⁵ of the suspended gold nanoparticles (Au NPs) under light sources. The presence of Au NPs also further enhances the rate of charge transfer between the electrodes by improving the electrical

conductivity of the microdroplet.⁴⁶ To ensure a lower economic footprint, the μ -DropFC is integrated with an Al-foil anode and a Cu–ZnPC cathode, which promotes an augmented catalytic breakdown of H₂O₂ under photonic excitation.^{47,48} Low-work-function Cu also facilitates a stronger adhesion with ZnPC to provide a strong electronic conductivity.^{49–52} Importantly, in such a simple embodiment, a single μ -DropFC can show a significantly high ψ_{oc} of ~0.58 V and a power density of ~0.72 mW cm^{−2} per unit mass of the fuel. Ten such μ -DropFCs show a power density of ~7 mW cm^{−2} at an efficiency of 3.4%, which highlights the potential of such device for μ -VLSI and scale up.

Furthermore, to enhance the overall utility of the prototype, the μ -DropFC setup has been utilized in environmental remediation processes such as dye degradation, while simultaneously being involved in energy harvesting from the peroxide fuel and photonic excitations. For this purpose, we synthesized a nanocomposite of Au NPs embedded in a matrix of cadmium sulfide nanoparticles (CdS NPs) before suspending them in the peroxide fuel to breakdown the “stubborn” organic dyes under photonic excitation.⁵³ As a model system, we show that the Au and CdS NPs with a powerful photocatalytic activity⁵⁴ can break rhodamine 6G dye under light while demonstrating a significantly higher power density of ~0.62 mW cm^{−2}. In some way, the simple and affordable μ -DropFC emulate the state-of-the-art microbial FCs, which have been operated in tandem with dye degradation to simultaneously perform dual objectives.^{55,56}

Concisely, the study showcases the versatility of a droplet⁸ or digital⁵⁷ microfluidic device loaded with the efficacies of nanoscience for efficient energy harvesting from electrochemical and solar resources as well as performing environmental remediation.^{55,56,58}

2. Experimental methods

2.1 Materials

The chemicals 50% (w/v) hydrogen peroxide solution (H₂O₂), cadmium nitrate (Cd(NO₃)), sodium sulfide (Na₂S), hydrochloric acid (37% (w/w), HCl) and sodium hydroxide (NaOH) were purchased from Merck, India. The chemicals zinc phthalocyanine (ZnPC) and rhodamine 6G (Rh6G) were purchased from Sigma Aldrich, India. Copper wires and aluminum foil were purchased from a local vendor. De-ionized water was employed for cleaning, washing and the preparation of the solutions. Gold(III) chloride hydrate, sodium borohydride, trisodium citrate dihydrate, and sodium chloride were purchased from Sigma Aldrich, India. All the chemicals were of analytical grade and were utilized without further purification.

2.2 Characterizations

The open circuit voltage (ψ_{oc}) was measured using a digital nanovoltmeter (SES Instruments). The Keithley 2640A source-meter in connection with the Kickstart software was used for potential-amperometry (I – ψ) and chrono-amperometry (J – t) characterizations. The surface morphologies and lattice structures (SAED patterns) of the nanocomposites were detected



using a field emission transmission electron microscope (FETEM, Jeol India). A field emission scanning electron microscope equipped with an energy-dispersive X-ray spectrometer (FESEM-EDX, Zeiss) was used to confirm the elemental composition of different materials. The material characterization of the nanocomposites and electrodes was carried out using a UV-Visible spectrophotometer (SHIMADZU UV-2600 model) and Raman spectrometer (Horiba). A Kelvin Probe Force Microscope (KPFM) was also employed to determine the work function of the electrode after cell operation.

2.3 Methods

(a) Synthesis of Au and CdS NPs. First, Au NPs were prepared by the reduction of the gold chloride salt in the presence of trisodium citrate. For this purpose, 30 mL of HAuCl₄ solution (0.5 mM) in water was prepared and stirred for 30 min. Its temperature was gradually increased, and when the solution started to boil, 3 mL of 38.8 mM trisodium citrate was added drop by drop. Thereafter, the solution was stirred at the boiling temperature for 15–20 min, while it changed its colour from yellow to purple and eventually to red. Thereafter, the solution was allowed to cool down gradually while being stirred, which led to the formation of Au NPs in the size range of 15–20 nm, as confirmed by the FETEM and UV-Vis spectra in Section I of the ESI.†

To prepare the composite of Au and CdS NPs, first, 20 mL of prepared Au NPs solution (20 nM) was added to a beaker, where 10 mL each of aqueous solution of 0.01 M CdNO₃ and 0.01 M Na₂S solution in 0.1 M NaOH were added simultaneously. The reaction temperature was maintained at 60 °C for 12 h while the solution was stirred continuously. The FETEM and UV-Vis spectra in Section I of the ESI† confirmed the formation of the composite of Au and CdS NPs. The sizes of the Au NPs in the composite were around 20 nm, while CdS NPs were around 2–5 nm. This was confirmed by the FETEM images, which have been shown in Fig. S1(a) and (b), Section I of the ESI.† The effect of the harsh peroxide solutions on the characteristic UV spectra of the nanocomposites is also depicted in Fig. S2(a) and (b),

Section I of the ESI.† These plots establish the limited effect of the peroxide moieties on the prepared Au/CdS NPs.

(b) Nomenclature of fuels. To identify the overall characteristics of the μ -DropFCs, different compositions of the fuel were prepared. For this purpose, additives such as the suspensions of Au and/or CdS NPs and Rh6G of different volumes and strengths were added to the primary system of 0.3 M H₂O₂, 0.1 M HCl and 1 M NaCl solution, as tabulated in Table 1. The Fuels 1–6 shown in the table were employed to perform the various parametric studies reported in what follows throughout this work. It may be noted here that the Fuels 2 and 3 had also five variants each based on the volume of the suspension of nanoparticles added, namely, Fuels 2I–2V and Fuels 3I–3V.

(c) μ -DropFC Setup. An overview of the experimental setup for the μ -DropFC and its different components is shown in Fig. 1 and ESI Video 1.† The membraneless energy harvester was composed of a $\sim$ 30 μ L droplet of 0.3 M aqueous hydrogen peroxide (H₂O₂) mixed with 1 M aqueous NaCl electrolyte and 0.1 M HCl. To infuse the photo-activity to the μ -DropFC, an aqueous suspension of 20 nM Au NPs was mixed. The volume of the Au NPs suspension was varied from 10 μ L to 50 μ L to uncover the effects of the LSPR on the performance of the μ -DropFC. A 150 W Xenon (Xe) lamp was used as a light source to excite the plasmonic Au NPs and enhance the output characteristics of the system in terms of ψ_{oc} and P values. The light source was always placed $\sim$ 15 cm from the top of the droplet. The μ -DropFC was integrated with an anode composed of a rectangular aluminum foil (Al) of dimension 2.5 cm $\times$ 2.5 cm and a cylindrical Cu cathode (dia. 1 mm) coated with a layer of ZnPC of thickness 200–300 nm.

3. Results and discussion

3.1 Mechanistic details

Fig. 2 justifies the choices of different materials chosen for the proposed μ -DropFC. Subsequently, the energy band diagrams shown also uncover the working principle of the μ -DropFC, under different conditions.⁵⁹ Fig. 2(a) schematically depicts the

Table 1 Different fuel compositions and their respective abbreviations

Sl. no.	Compositions
Fuel 1	Mixture of 10 μ L 0.3 M aqueous H ₂ O ₂ with 10 μ L of 0.1 M aqueous HCl and 10 μ L of 1 M of aqueous NaCl
Fuels 2I–2V	(I) 10 μ L of Fuel 1 with 10 μ L of 20 nM aqueous Au NPs (II) 10 μ L of Fuel 1 with 20 μ L of 20 nM aqueous Au NPs (III) 10 μ L of Fuel 1 with 30 μ L of 20 nM aqueous Au NPs (IV) 10 μ L of Fuel 1 with 40 μ L of 20 nM aqueous Au NPs (V) 10 μ L of Fuel 1 with 50 μ L of 20 nM aqueous Au NPs
Fuels 3I–3V ^a	(I) 10 μ L of Fuel 1 with 10 μ L of aqueous Au/CdS NPs mixture (II) 10 μ L of Fuel 1 with 20 μ L of aqueous Au/CdS NPs mixture (III) 10 μ L of Fuel 1 with 30 μ L of aqueous Au/CdS NPs mixture (IV) 10 μ L of Fuel 1 with 40 μ L of aqueous Au/CdS NPs mixture (V) 10 μ L of Fuel 1 with 50 μ L of aqueous Au/CdS NPs mixture
Fuel 4	10 μ L of Fuel 1 with 10 μ L of 0.5 mg mL ^{−1} aqueous rhodamine 6G
Fuel 5	10 μ L of Fuel 1 with 10 μ L of 0.5 mg mL ^{−1} aqueous rhodamine 6G + and 10 μ L of 20 nM aqueous Au NPs
Fuel 6 ^a	10 μ L of Fuel 1 with 10 μ L of 0.5 mg mL ^{−1} aqueous rhodamine 6G + and 10 μ L of aqueous Au/CdS NPs mixture

^a Concentration of Au/CdS NP mixture was unknown since they were synthesized *in situ*, as discussed below.



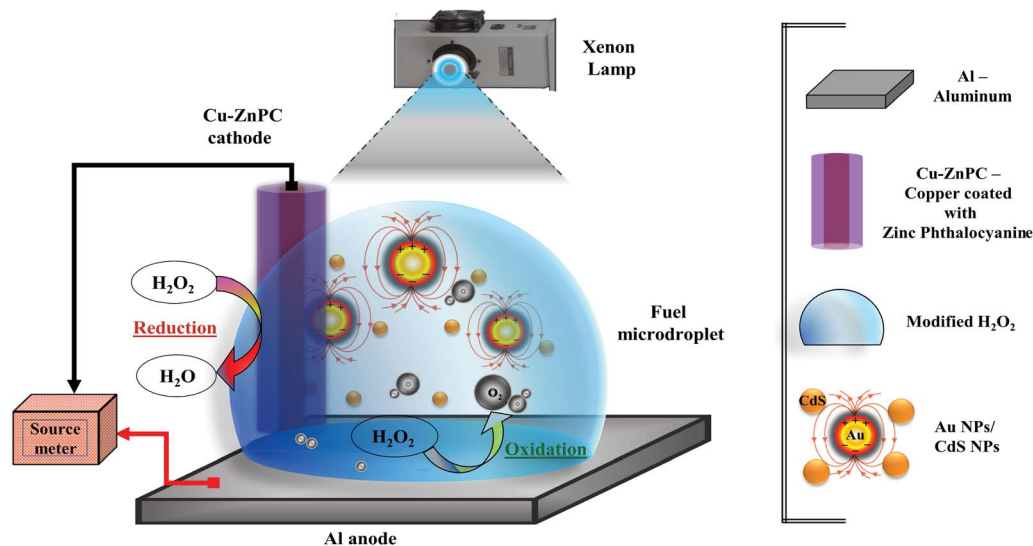


Fig. 1 Schematic of the μ -DropFC setup comprising of a Cu–ZnPC cathode, an Al foil anode, a microdroplet with the fuel (0.3 M H_2O_2 , 0.1 M HCl, 1 M NaCl), additives (Au/CdS NPs) and light source. The image also schematically shows the redox half-reactions at the cathode and anode, $\text{H}_2\text{O}_2 \rightarrow \text{O}_2 + 2\text{H}^+ + 2\text{e}^-$ and $\text{H}_2\text{O}_2 + 2\text{H}^+ + 2\text{e}^- \rightarrow 2\text{H}_2\text{O}$, respectively. The legends aid in the identification of the different components and their placements.

basic state of the μ -DropFC before any reaction started or light illumination took place.⁵⁹ The schematic diagram shows the Fermi levels (E_F) of Cu, ZnPC, peroxide solution, and Al alongside showing the band-gap for the p-type semiconductor ZnPC with the conduction and valence bands at $E_C = -3.8$ eV and $E_V = -5.8$ eV.^{59,60} The presence of ZnPC ensured the formation of a Schottky junction between metallic Cu, p-type SC ZnPC, and electrolyte. Furthermore, the peroxide electrolyte was reactive at room temperature and the typical energy levels D_{ox} (e.g. -5.3 eV)^{30,61} and D_{R} (e.g. -6.4 eV)^{30,61} denote their oxidation and reduction potentials.

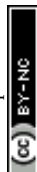
It may be noted here that once the droplet was integrated with the electrodes, the setup started harvesting energy even under dark conditions and the energy band diagram after such equilibration is shown in Fig. 2(b). The electrolyte loaded with H_2O_2 underwent oxidation at the Al-foil-anode to release O_2 gas in the atmosphere and produce H^+ ions in the solution following the half-reaction, $\text{H}_2\text{O}_2 \rightarrow \text{O}_2 + 2\text{H}^+ + 2\text{e}^-$.³⁶ The peroxide decomposition in the bulk under acidic and basic conditions is elucidated in detail in Section II of ESI.† The oxidation of the anode led to a progressive deposition of oxides at the Al-foil-anode when Al combined with hydroxyl ions of the droplet. This was confirmed by the Raman and KPFM characterization of the electrodes before and after the analysis, as shown in Fig. S4b, c, and S5 of Section III of ESI.†⁶² The reduction of H_2O_2 occurred at the ZnPC–Cu cathode, which eventually formed water, following the half-reaction, $\text{H}_2\text{O}_2 + 2\text{H}^+ + 2\text{e}^- \rightarrow 2\text{H}_2\text{O}$.³⁶

Interestingly, the KPFM helped in identifying the work function of the Al anode before the reaction to be ~ 4.577 eV, as depicted in Fig. 2(a). The schematic diagram in Fig. 2(b) shows that these redox reactions initiate a charge transport across the electrodes, which was the initiation of the conversion of

chemical energy into electrical energy. Since the circuit was complete, the different components of the μ -DropFC strived to equilibrate their Fermi level. However, upon contact with the low-work-function Cu, an electron flow occurred from the metal to ZnPC *via* the formation of mixed states,^{51,52} which led to the balancing of the potentials at these two surfaces, as shown in Fig. 2(b). Further, during equilibration of the Fermi level, the conduction and valence bands of the p-type SC ZnPC underwent a band bending near the SC–electrolyte and metal–SC interfaces, as shown in Fig. 2(b).^{59,60}

The band diagram under dark conditions also helped the charge transfer at the mixed-molecule ZnPC–Cu interface. Previous studies have shown that interfacial dipoles could be created at the metal–SC junctions, which influenced the Schottky barrier height.^{51,52} Especially when the SC layer is physisorbed on a metal surface, charge redistribution might take place across the junction to affect the interface dipoles. In such a scenario, to maintain the Pauli exclusion principle valid, the charges present around the interface are pushed back into the metal, leading to a slight reduction in its work-function. Importantly, the interactions between the ZnPC and Cu in the proposed μ -DropFC could be explained along the similar lines. The physisorbed ZnPC on Cu created interfacial states at the junction, and the ZnPC molecules were “pulled” towards the Cu core owing to the lower work function of the metal.⁵² This made the interaction between SC and metal surfaces result in a stronger bond, and subsequently, the charge transfer from Cu to the HOMO of ZnPC facilitated the reduction of peroxide into water near the SC–electrolyte interface.⁵²

Fig. 2(c) shows the effect of the illumination of a Xe lamp on the μ -DropFC, wherein the photonic excitation pumps in more electrons into the system due to the electron transfer from valence to conduction bands of ZnPC molecules.⁶⁰



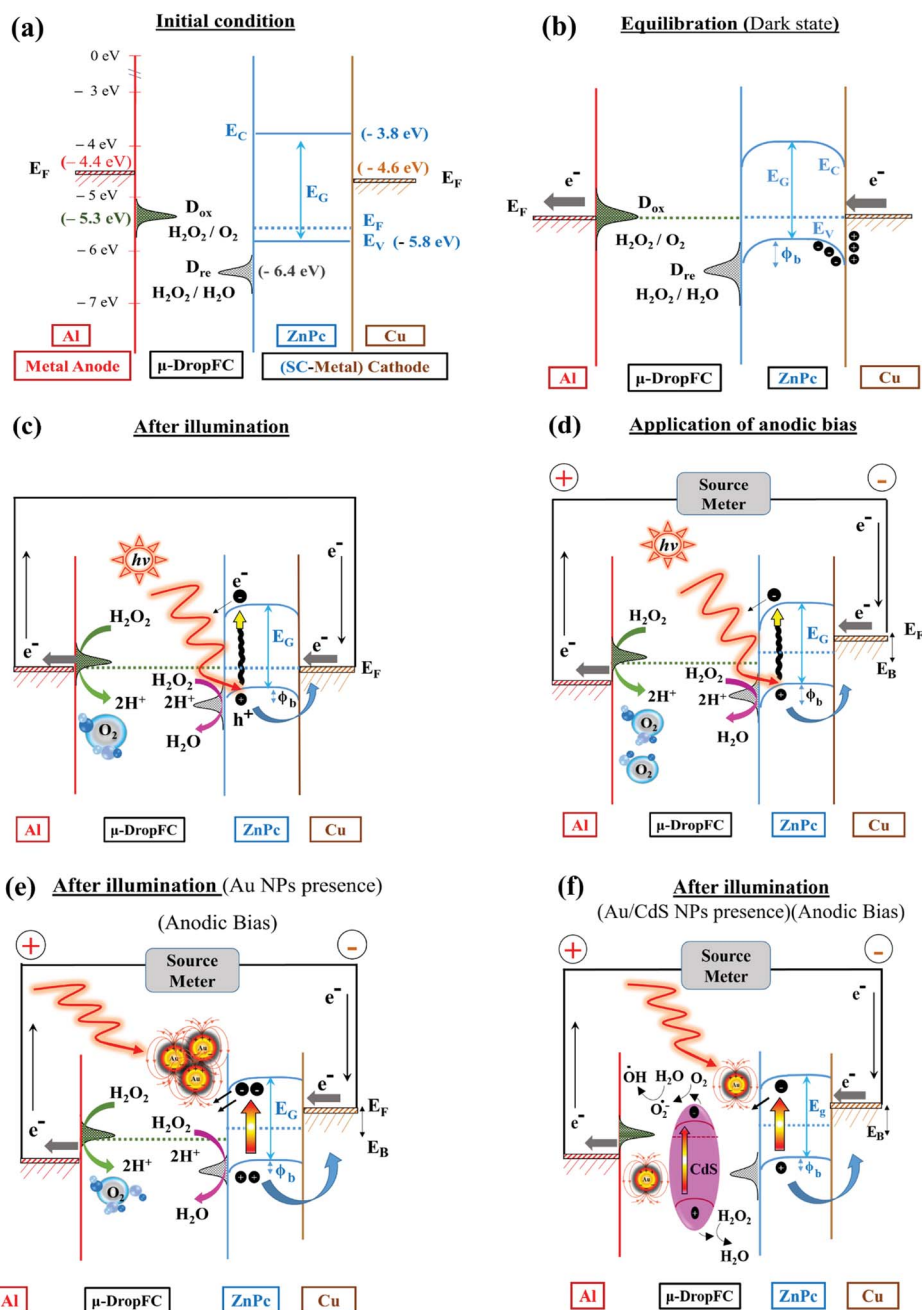


Fig. 2 Schematics of the energy band diagrams displaying the various stages of the operation of the μ -DropFC. (a) Initial condition, even before equilibration, when the contact has just been established between the components. (b) Equilibrium under the dark condition when the Fermi levels of different materials equilibrated before photonic illumination. (c) Effects after the illumination using the Xe lamp. (d) The situation when an anodic bias has been applied to the setup shown in (c). (e) Influence of the LSPR of the Au NPs under illumination. (f) Influence of the Au/CdS NPs. The images also depict the overviews of redox reactions occurring at the anode and cathode.

Subsequently, the influence of anodic bias to the pattern of band bending of the p-type ZnPC is shown in Fig. 2(d) under the illumination of a Xe lamp. The image also suggests a redistribution of the Fermi levels with the application of the anodic bias. It can be seen that at the anode, the Fermi level went down due to the introduction of positive charges, which facilitated the reaction further as more electron transfer could take place from the oxidation reaction of H_2O_2 . Subsequently, on the cathode side, the Fermi level increased due to injection of negative

charges, which further increased the rate of reduction reaction. In a way, at the electrode interfaces, charges were either introduced (cathode) or removed (anode), which influenced the rate of reaction. This led to higher electron transfer from the metal to the p-type SC. Furthermore, since the inherent charge density over the p-type SC increased under light, this facilitated higher rate of charge transfer to the adjacent electrolyte due to the Fermi energy difference. The effect of the addition of the Au NPs to the μ -DropFC and the subsequent effect of LSPR are

schematically shown in Fig. 2(e). The photonic excitation on the Au NPs promoted LSPR on the same, which, in turn, improved the photoactivity of the μ -DropFC. The presence of Au NPs also increased the electrical conductivity of the microdroplet, which improved the rate of electron transfer through the circuit.

Concisely, Fig. 2 helps in understanding that the usage of each and every component contributed to the increased performance of the μ -DropFC. Importantly, the μ -DropFC setup was found to be rather robust because the output characteristics did not alter much when the experiments were repeated on the same system. This was shown by reporting the small reduction in ψ_{oc} measured for the duration of a single operation cycle when the same set of electrodes were operated 3 times, as shown in Fig. S4a of Section III of the ESI.[†] However, the change in the ψ_{oc} values changed significantly after three cycles, owing to the electrode degradation. Again, the KPFM analysis revealed a significant change in the surface potentials upon exposure of the Al-foil-anode to peroxide in the presence of an anodic bias, as shown in Fig. S5 in Section III of the ESI.[†]

Fig. 2(f) depicts the variations in the band configurations upon the addition of n-type CdS NPs in the solution in the form of Au/CdS NPs. This facilitated the formation of a p-n junction when some of the n-type CdS NPs got adsorbed at the p-type ZnPC. Thus, in dark condition and in the presence of forward bias, the flow of electrons could take place from CdS to ZnPC. However, under light, the electronic transitions of both the ZnPC and CdS molecules changed the scenario. The transition in the n-type CdS facilitated its oxidation into CdSO_4 in the presence of peroxide fuels⁶³ while the electron in the

conduction band of ZnPC after transition due to photonic excitation was transferred to CdS for further oxidation of the same. In this manner, the configuration ensured that the addition of CdS did not disturb the mainstream flow of electrons in the μ -DropFC. It may be noted here that the major purpose of addition of CdS NPs were to degrade the dyes under light. However, to ensure such activity, we did not compromise much with the power density of the μ -DropFC owing to the photoactivity of the CdS NPs, as shown in Fig. 2(f). It may also be noted here that the Au/CdS NPs were mostly suspended in the bulk rather than adsorbed on the electrodes, which influenced the kinetics of the electron flow rather than the thermodynamics. Furthermore, these nanoparticles increased the rate of decomposition of the peroxide fuel due to catalytic activity. The charge transfer in the electrolyte was also facilitated by the presence of Na^+ and Cl^- ions in the electrolyte.⁸

3.2 μ -DropFC characterization

The ESI Video 2[†] shows the performances of the μ -DropFCs under dark and illuminated conditions. Clearly, the setup generated a higher output under light following the mechanism mentioned previously. The electrical characterization of the μ -DropFCs was performed using a set of nanovoltmeter and sourcemeter. For this purpose, linear sweep voltammetry (LSV) was employed with a voltage scan from 0 V to the open circuit voltage (ψ_{oc}) of the system. The testing parameters were kept the same for all experiments reported unless mentioned otherwise. In what follows, we discuss the results associated with the μ -DropFCs under the light. The results thus obtained were shown

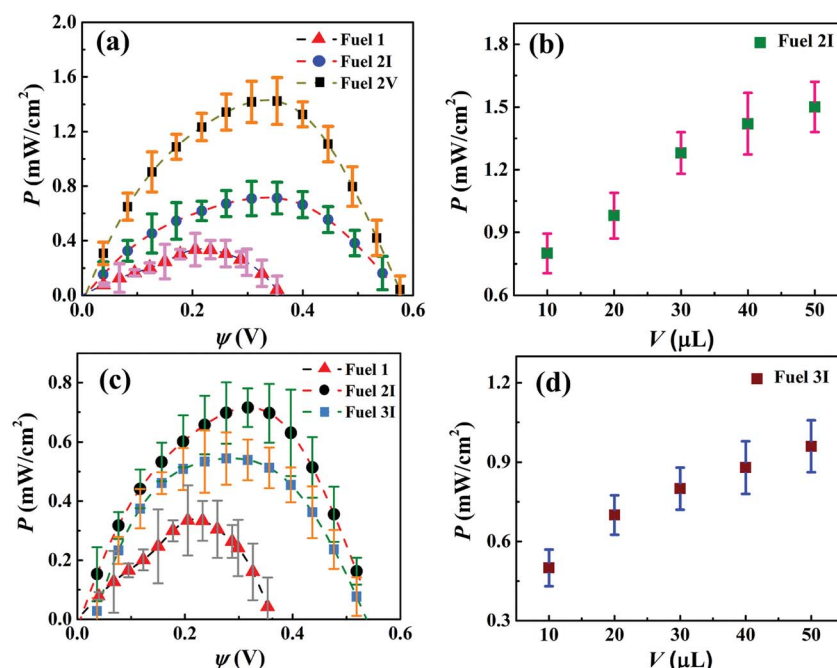
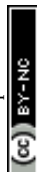


Fig. 3 Power-potential (P - ψ) curves for the different μ -DropFCs containing different volumes of additives – Au NPs and Au/CdS NPs, respectively. (a) Performance curves indicating the variation in power density (P) with ψ of three different fuels: 1, 2I and 2V. (b) Effect of changing the volume (V) of the Au NPs suspension on the overall power generation (P). (c) Power-potential (P - ψ) curves for Fuels 1, 2I and 3I. (d) Effect of changing the volume (V) of the Au/CdS NPs suspension on the overall power generation, P . All the results were obtained under the application of a voltage sweep from 0 V to ψ_{oc} , and then by measuring the resulting output currents. Details of Fuels 1–6 are provided in Table 1.



as the P - ψ characteristics in Fig. 3. It may be noted here that all the P - ψ plots show a progressive increase in P with ψ until they reach a maximum value of $P_{\max}$ before they decrease with a further increase in ψ to a zero value at ψ_{oc} . It may also be noted here that, initially, we optimized the loading of salt and acid in the native μ -DropFCs before we performed the experiments with the NPs. Fig. S3 in Section II of ESI† show the characteristics of a few native μ -DropFCs when the salt and acid/alkali loadings were varied. Fig. S3 in Section II of ESI† also shows that although the alkalinity of the solution improved the power density of the energy harvester, it reduced the life time and ψ_{oc} . In contrast, at an acidic pH 1, steady and continuous degradation of peroxide for a longer duration led to a better performing and long-lasting μ -DropFC. These experiments uncovered that Fuel 1 in Table 1, a mixture of 10 μL 0.3 M aqueous H_2O_2 with 10 μL of 0.1 M aqueous HCl and 10 μL of 1 M of aqueous NaCl was the near-optimal native system, which led to $P_{\max} \sim 0.35 \text{ mW cm}^{-2}$ at $\psi_{\text{oc}} = 0.38 \text{ V}$, as shown in plot (a) of Fig. 3.

Interestingly, plot (a) also shows nearly a four-fold increase in $P_{\max}$ when the native system was loaded with a suspension of Au NPs, named as Fuel 2V. The combined influence of the LSPR of the Au NPs under light and enhanced electrical conductivity of the system led to the improvement of the power harvesting parameters, $P_{\max} \sim 1.5 \text{ mW cm}^{-2}$. Plot (b) shows the effect of variation of the volume of Au NPs, Fuel 2I–2V, on the P - ψ values of the μ -DropFCs. The plot suggests that although increasing the volume of the Au NPs led to higher P values, the increment saturated due to diffusional resistance at higher values. The Au NPs improved the output parameters because (i) the LSPR under light improved charge transfer between the electrodes, (ii) under acidic conditions Au NPs catalyzed the degradation of peroxide fuels, (iii) they also acted as electron relays for better charge transfer, and (iv) they reduced the electrical resistance of the composite fuel droplet marginally.^{46,56} Furthermore, the incorporation of the Au NPs or Au/CdS NPs primarily affected the reaction kinetics, as they were suspended in the bulk rather than adsorbed at the electrodes. With the increase in solution volume, the amount of NPs that participated in the charge transfer processes increased, thereby facilitating faster redox reactions at the electrodes, which resulted in higher output. Furthermore, with the increase in solution volume, the area occupied by the composite fuel droplet also increased marginally since the anode surface was partially hydrophilic. This led to an increase in the number of reaction sites available for the redox reaction to occur. Thus, with a progressive increase in the droplet volume, the output cell characteristics were enhanced under external radiation due to the various above-mentioned reasons. Importantly, with the increase in the droplet volume, the resistance to diffusion near the electrodes also decreased; however, a saturation limit was observed beyond the addition of a certain volume of NPs.

The performance of Fuel 3I–3V is summarized in plots (c) and (d). Plot (c) suggests that, in comparison to Fuel 1, they performed better showing $P_{\max} \sim 0.59 \text{ mW cm}^{-2}$; however, the performance was not as good as with Fuel 2. Again, plot (d) shows the increase in the performance characteristics before saturation with the loading of Au/CdS NPs. It may be noted here

that the addition of Au/CdS NPs was intended towards their capability of photocatalytic degradation of dyes, which is to be discussed later. However, from the pure energy harvesting point of view, Fuel 2 with an optimal loading of Au NPs was found to be superlative, as summarized in Fig. 3.

Fig. 4(a) shows the J (current density)- t (time) plot, for Fuels 2I and 3I. The plots suggest that the solution containing only Au NPs displayed an initial higher current density of $\sim 5 \text{ mA cm}^{-2}$ when compared with the solution containing Au/CdS NPs ($\sim 3.5 \text{ mA cm}^{-2}$), upon the application of a bias of 0.1 V. Thereafter, the decay during the initial $\sim 200 \text{ s}$ could be due to the mismatch between the high rate of redox reactions occurring at the interface and the limited charge transfer at the cathode. In such a scenario, the μ -DropFCs with Au NPs showed enhancement due to the higher ionic conductivity, better charge-transfer rates due to the presence of charge mediators, and occurrence of faster chemical kinetics at the electrode interface due to the enhanced plasmonics.^{8,45,56} However, the plot also shows that the μ -DropFCs with Fuel 3I registered a sustained charge density of about 1.7 mA cm^{-2} , which was higher than that of Fuel 2I even after a long period of time. The ratios of J values after 0 s and 1500 s were ~ 0.3 (Fuel 2I) and ~ 0.5 (Fuel 3I), which indicated the slower degradation of the Au/CdS NP system.

Plot (b) in Fig. 4 highlights the difference in ψ_{oc} for Fuels 2I (0.58 V) and 3I (0.52 V). The plots suggest the generation of a high ψ_{oc} upon the addition of the photo-sensitive NPs under a longer duration of light illumination for $\sim 50 \text{ min}$. Herein, the ψ_{oc} values signify the overall driving force of the system, which is a measure of the thermodynamic potential difference between the electrodes.

It may be noted here that for the system containing additional additives in the electrolyte, ψ_{oc} is the difference between the chemical potential (μ) of the electrolyte and the potential of the conduction band of the photo-sensitive electrode (e.g. ZnPC in the present setup), $\psi_{\text{oc}} = E_{\text{C}} - \mu$.^{8,64} The external irradiation might cause intense localized electric field to develop on Au NPs, which effectively could reduce μ to, $\mu' = \mu - qV$, where q represents the charge of the particle and V , the potential developed due to the field around the excited particle.^{8,64} Subsequently, an enhancement in ψ_{oc} could be expected in a μ -

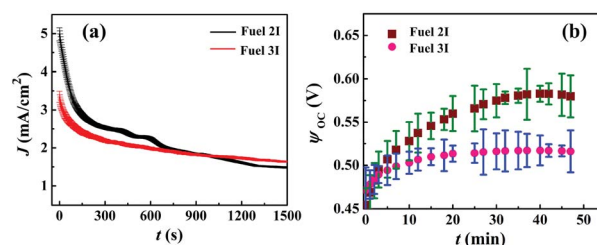


Fig. 4 (a) Chronoamperometric current density (J) versus time (t) studies for different μ -DropFCs with the Fuels 2I and 3I at an applied voltage of 0.1 V. (b) The corresponding open-circuit potential (ψ_{oc}) with t for 50 min. To demonstrate long-term performance of μ -DropFCs, the chronoamperometry test was performed for different systems.

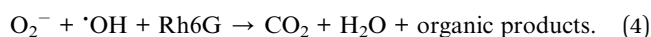
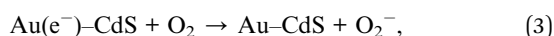
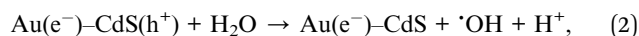
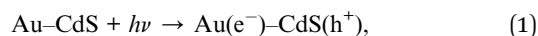


DropFC loaded with Au NPs under a prolonged light exposure, as shown in plot (b). In comparison, for the case of Au/CdS NPs, a lower ψ_{oc} value was observed, which could be attributed to the generation of lower value of potential difference between the electrodes. In the presence of light, the photo-excitation generated the electron-hole pair in CdS NPs in which the conduction band was at a lower potential value. This caused electron transfer from CdS NPs to oxidize the peroxide fuel. In the process, a fraction of the photonic energies was taken up by CdS NPs for peroxide degradation in the bulk rather than at the electrode, which contributed to a reduced ψ_{oc} .

3.3 Energy harvesting with dye degradation

As discussed previously, the μ -DropFC setup could also be utilized as a dye degradation system without much alteration of the components. For this purpose, Au/CdS NPs were involved to exploit their act as superior photo-catalysts under light. The energy harvesting performance involving P - ψ characteristics and J - t curves of such μ -DropFCs is summarized in Fig. S6 of Section IV in the ESI†. These plots concluded that while the addition of Au NPs in the μ -DropFC loaded with Rh6G (Fuel 5) provided an enhanced power density, the addition of Au/CdS NPs in the same (Fuel 6) led to the more efficient dye degradation. This could be because of the catalytic nature of Au/CdS NPs, which degraded some peroxide amount in the bulk of the droplet and thereby lowered the overall energy output. Importantly, Fig. S6 of Section IV in the ESI† also suggest that although the μ -DropFC loaded with Au/CdS NPs and Rh6G (Fuel 6) harvested energy at a lower density, it gave a sustained output of 1.25 mA cm^{-2} , at an applied voltage of $+0.1 \text{ V}$, for a longer period of time.

Fig. 5(a) schematically shows the energy band diagrams displaying the various stages of the operation of the μ -DropFC when loaded with Fuels 4–6. In the presence of light, the Au NPs catalyzed the formation of OH radicals *via* the degradation of peroxide molecules,⁶⁵ which formed one of the many reactive oxygen species (ROS) engaged in the degradation of the dye, as shown in eqn (1) and (2). The OH radicals were also produced due to the oxidation of water in the presence of holes generated by the n-type CdS NPs under photonic excitations, as shown in eqn (1). Subsequently, the dissolved oxygen accepted the electrons from the LSPR-prone Au NPs to form the superoxide radicals, which subsequently broke down the dye molecules, as shown in eqn (3) and (4). The mechanism for the degradation of dye is summarized as follows:⁵⁶



The Au/CdS nanocomposites are known to have significantly better photocatalytic properties than bare CdS NPs. The

After illumination (Rhodamine 6 G Solution)
(Au/CdS NPs presence) (Anodic Bias)

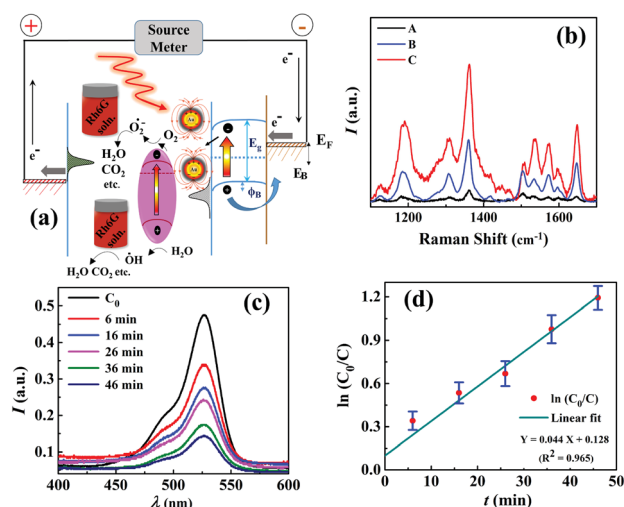


Fig. 5 (a) Schematic of the energy band diagrams displaying the various stages of the operation of the μ -DropFC when loaded with the Fuels 4–6. (b) Plasmonic effect of Au NPs in the form of enhanced Raman spectra of Rh6G molecules. Spectrum A corresponds to a pure Rh6G solution in water (0.5 mg mL^{-1}), spectrum B shows the same when 0.5 mg mL^{-1} of aqueous Rh6G solution was mixed with 0.3 M aqueous H_2O_2 loaded with Au/CdS NPs and spectrum C shows the same when only Au/CdS NPs were added to the Rh6G solution in the absence of peroxide. (c) UV-Visible plots at different time intervals for Fuel 6, measured from 6 min (t_1) to 46 min (t_5). (d) Variation in the normalized concentration of Rh6G ($\ln C_0/C_t$) with time, where the initial concentration is C_0 and the concentration at time t is C_t . The kinetics was found to be similar to a pseudo-first-order reaction with a rate constant of $k \sim 0.044 \text{ min}^{-1}$.

increment in the degradation efficiency was because of the improved charge generation and transfer rates for CdS NPs in the presence of Au NPs.⁶⁶ Importantly, the setup was shown to reduce $\sim 85\%$ of Rh6G in 50 min along with harvesting energy at a decent rate. To confirm the LSPR effect of Au NPs, we performed the surface enhanced Raman spectroscopy (SERS) study, as summarized in Fig. 5(b). The plot shows that, upon irradiation with a 633 nm laser in the Rh6G solution loaded with either Au NPs or Au/CdS NPs, enhanced Raman peaks were observed. We also analyzed the rate of dye degradation of the μ -DropFCs employing UV-Visible spectroscopy. Fig. 5(c) shows the variation in the peak intensity of Rh6G with time for Fuel 6. The plot also shows that the intensity of peaks decreased with time to mark the degradation of the complex dye molecule inside the μ -DropFC. Image (d) shows the variation in the normalized concentration of Rh6G ($\ln C_0/C_t$) with time, where the initial concentration is C_0 and the concentration at time t is C_t . The kinetics for this system was found to be a pseudo first order with a rate constant of $k \sim 0.044 \text{ min}^{-1}$.⁵³

3.4 Performance, VLSI, and efficiency

The μ -DropFC system showed enhanced output characteristics in the presence of additives like Au NPs and Au/CdS NPs. The additives not only played an important role in enhancing the power densities but also aided the transformation of the μ -



DropFC setup to be realized as a dye degradation setup. In what follows, we have analyzed the role of diverse additives in promoting the output characteristics: (i) addition of salt NaCl led to an increase in the electrical conductivity, which further increased when salts like CdSO_4 were formed during the operation due to the oxidation of CdS NPs; (ii) in the presence of high H^+ loading at a lower pH value the controlled breakup of peroxide fuel in the presence of the Au NPs^{56,65} aided high-density-power generation for a longer period; (iii) since the cell operated under a light source, the incident radiation caused LSPR to create plasmonic hot-spots around the Au NPs; (iv) the Au NPs displayed electron relay effect under a large potential difference between the two electrodes to transfer charges at a higher rate. Table 2 provides an overall outlook on the performance of the different fuels utilized for the μ -DropFC. The results presented so far uncovered that the addition of Au NPs in Fuel 1 to generate Fuels 2I–2V helped in enhancing the P_{max} , ψ_{oc} , and ψ_{max} (the voltage corresponding to P_{max}).

Furthermore, the addition of Au/CdS NPs (Fuels 3I–3V) did improve the overall characteristics of the system over native Fuel 1; however, the values were lower compared to Fuels 2I–2V. Importantly, the addition of Rh6G solution did significantly reduce the output values because it hardly contributed to the energy production attributes. To optimize the NPs additives in the fuel, we performed further experiments, which have been summarized in Section V of ESI.† Fig. S7† shows that the addition of $\sim 70 \mu\text{L}$ of Au NPs solution in Fuel 1 can be optimal for harvesting high-density energy for a longer duration. Thus, we chose this fuel to show a pilot-scale μ -VLSI potential of the proposed μ -DropFC setup in Fig. 6.

Fig. 6(a) shows the pilot-scale μ -VLSI setup comprised of 10 μ -DropFCs connected in parallel with each other. Plots (b) and (c) show the corresponding P - ψ analysis for Fuels 2 and 3 with the exception that $70 \mu\text{L}$ Au NPs and Au/CdS NPs were added to prepare each μ -DropFC. Fig. 6(b) shows a 14-fold increase in P_{max} to $\sim 7 \text{ mW cm}^{-2}$ when the number of μ -DropFCs with Fuel 2 was increased from one to ten. It may also be noted that we achieved such power density for the maximum fuel mixture volume of 1 mL ($100 \mu\text{L}$ per cell for 10 cells). Fig. 6(b) shows a 10-fold increase in P_{max} to $\sim 5 \text{ mW cm}^{-2}$ when the number of μ -DropFCs with Fuel 3 was increased from one to ten. Again, the usage of Au NPs led to a better performance than the Au/CdS NPs for the reasons discussed previously.

It may be noted herein that, initially for a single cell, the power density value reached $\sim 0.72 \text{ mW cm}^{-2}$ when it contained $10 \mu\text{L}$ of Au NPs along with other constituents making up the total cell volume to be $\sim 40 \mu\text{L}$. The power density thereafter

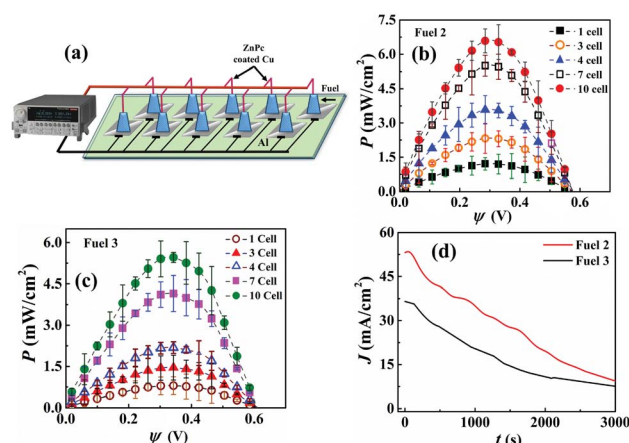


Fig. 6 (a) Schematic of the μ -VLSI setup comprising of 10 μ -DropFCs connected in parallel with each other. Plot (b) and (c) P - ψ curves for the VLSI with the increasing number of μ -DropFCs. In plot (b) for each μ -DropFC, $70 \mu\text{L}$ of Au NPs was added to $10 \mu\text{L}$ of the native system, while in plot (c) $70 \mu\text{L}$ of Au/CdS NPs was added to $10 \mu\text{L}$ of the native system. Plot (d) I - t data for the VLSI setup of 10 μ -DropFCs consisting of the fuels mentioned for plots (b) and (c).

increased to $\sim 1.8 \text{ mW cm}^{-2}$ when the Au NPs volume increased to $\sim 80 \mu\text{L}$. For the large-scale integration experiment, an optimal value of $70 \mu\text{L}$ of Au NPs was chosen, which increased the cell volume to $\sim 100 \mu\text{L}$ after adding all the other additives. Subsequently, different number of cells (3, 4, 7, and 10) were connected and characterized. Due to the parallel connection within the system, the current values added up and resulted in the overall enhancement of the output power values. This circuit design allowed us to harvest high power densities from the setup. There was also a change in the ψ_{oc} values observed; however, the change was not significant when compared with that of the single cell. As the number of cells increased, there was a gradual increase in the maximum power density of the configuration and upon employing linear sweep voltammetry technique, it was observed that the P_{max} value was obtained near 0.36 V. Thereafter, the 10 cells that were connected in parallel to harvest a high power density value from the system eventually resulted in generating $\sim 7 \text{ mW cm}^{-2}$. There was an overall loss in the output efficiency, which could be assigned to various factors, which include the ohmic resistances arising from different cell connections, non-uniform cathode coating (ZnPC) across different cells and time-sensitive system properties like peroxide decomposition.

Fig. 6(d) shows the chronoamperometry plot for the VLSI system with 10 cells, which confirmed that the overall current density for Fuel 2 was higher than Fuel 3. The tests were performed for 50 min to obtain a variation of j from 55 mA cm^{-2} to 10 mA cm^{-2} (35 mA cm^{-2} to 10 mA cm^{-2}) for Fuel 2 (Fuel 3) with a potential of 0.1 V. The enhanced current density values could be attributed to the inherent electronic and optical properties of the proposed prototype, which substantially improved under the presence of light.

Table 3 shows a comparison of the different performance parameters of the proposed μ -DropFC with the others available

Table 2 Output parameters for the μ -DropFC loaded with Fuels 1–6

Fuels	ψ_{oc} (V)	ψ_{max} (V)	P_{max} (mW cm^{-2})
Fuel 1	0.38	0.24	0.35
Fuel 2I	0.59	0.38	0.72
Fuel 3I	0.55	0.36	0.57
Fuel 4	0.36	0.22	0.39
Fuel 5	0.56	0.44	0.61
Fuel 6	0.54	0.41	0.51



Table 3 Comparison of membraneless H₂O₂ fuel cells with μ -DropFCs

An	Ct	ψ_{oc} (V)	H ₂ O ₂ [M]	P_{max} (mW cm ⁻²)	V_F (mL)	Ref.
Mg	PB	2.3	0.5	4.9	2	18
Ni	PB	0.6	0.5	1.5	50	36
Ni	[Fe ^{II} (H ₂ O) ₂] ₃ [Co ^{III} (CN) ₆] ₂	0.8	0.3	9.9	— ^a	37
Ni	Pedot:PSS	0.5	0.1	0.3	— ^a	41
Ni	FePC	0.5	0.3	0.01	— ^a	47
Al	PB	0.6	0.5	0.8	0.5	61
Al	ZnPC-Cu	0.6	0.3	1.4 – 1 cell, 7.1 – 10 cells	0.07 – 1 cell, 0.1 – 10 cells	This work

^a Not explicitly mentioned. An: anode; Ct: cathode; V_F : volume of fuels utilized per cell; FePC: iron phthalocyanine; PB: Prussian blue.

Table 4 Comparison of the efficiencies of fuels in the μ -DropFC

System	ψ_{oc}	P_{max}	ϵ_{PV}	ϵ_T	ϵ_E	ϵ_O (%)
Fuel 1	0.38	0.35	0.005	0.63	0.35	0.11
Fuel 2I	0.59	0.72	0.01	0.63	0.55	0.36
Fuel 2V	0.62	1.5	0.021	0.63	0.57	0.75
Fuel 3I	0.55	0.57	0.008	0.63	0.51	0.26
Fuel 3V	0.57	0.95	0.014	0.63	0.53	0.47
Fuel 5	0.56	0.61	0.008	0.63	0.52	0.26
Fuel 2 ^a	0.63	7.2	0.102	0.63	0.53	3.54
Fuel 3 ^a	0.61	5.7	0.08	0.63	0.54	2.83

^a 70 μ L of Fuel 2 or 3 was taken for the VLSI system.

in the literature. The values summarized in the table suggest that P_{max} of μ -DropFCs are quite comparable if not better than the others referred with respect to the working volume of the fuel. In a way the proposed setup has its uniqueness in the development of a portable and affordable μ -DropFC for harvesting high density power from both chemical and light energies utilizing significantly low fuel volumes, which can also be simultaneously utilized for dye degradation.

Table 4 shows the efficiency of the different μ -DropFCs reported in this work. The calculations of efficiencies for the different μ -DropFCs are summarized in Section VI of ESI.† The overall efficiency of the μ -DropFC was determined employing the following formula: $\epsilon_O = \epsilon_T \times \epsilon_E \times \epsilon_{PV}$, where ϵ_O denotes the overall efficiency of the system, ϵ_T is the thermodynamic efficiency of the system, ϵ_E is the electrochemical efficiency and ϵ_{PV} is the photovoltaic efficiency of the system.

The data suggest that the efficiency of the Au NP-loaded μ -DropFCs was the best among the proposed systems. The output power density increased by ~ 10 -fold when 10 such units were integrated under the same amount of photonic illumination, which highlighted the scope for improving the overall efficiency of the setup through VLSI. The data reported in Table 4 shows the capacity of the proposed μ -DropFC for harvesting high density power in a very efficient manner, which can be improved further with the help of process intensification and VLSI in the future.

4. Conclusions

A peroxide microdroplet has been designed and developed into a high-performance fuel cell, namely, μ -DropFC, which is also

capable of harvesting solar energy. For this purpose, a peroxide microdroplet at optimal pH and salt loading has been utilized as the native system integrated into an Al-anode and a ZnPC-Cu cathode. The n-type ZnPC enabled the formation of a photoactive Schottky junction at the electrolyte and metal interfaces, which is found to be suitable for power generation under light. Oxidation and reduction of H₂O₂ on the electrodes helped in the conversion of chemical energy into the electrical one in a membraneless setup. The use of suspended Au NPs enhanced the power density under photonic illumination through LSPR. The addition of n-type CdS NPs infuses the capacity of catalytic photo-degradation of dyes under light. The simple, low-cost, portable, and membraneless setup possesses significant power densities of ~ 0.8 mW cm⁻² per cell and 7 mW cm⁻² at an efficiency of 3.5% when a group of 10 cells have been integrated. The single-cell setup requires significantly less working fluid volume and can give a very high power density at a voltage of ~ 0.38 V. The single-cell setup also delivers a current density of ~ 1.5 mA cm⁻² at an applied voltage of 0.1 V for 30 min. Furthermore, the single-cell setup is capable of degrading $\sim 85\%$ of rhodamine 6G dye in 1 h while simultaneously generating energy at a power density of ~ 0.6 mW cm⁻². A comparison with previous works shows the superiority of the proposed μ -DropFC for harvesting high density power, which can be improved further with the help of process intensification and VLSI in the future.

Conflicts of interest

There are no conflicts to declare.

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Notes and references

- 1 K. S. Dhathathreyan, N. Rajalakshmi and R. Balaji, in *Nanotechnology for Energy Sustainability*, Wiley-VCH Verlag GmbH & Co. KGaA, Weinheim, Germany, 2017, pp. 569–596.



- 2 F. Zhu, J. Kim, K.-C. Tsao, J. Zhang and H. Yang, *Curr. Opin. Chem. Eng.*, 2015, **8**, 89–97.
- 3 Z. L. Wang and W. Wu, *Angew. Chem., Int. Ed.*, 2012, **51**, 11700–11721.
- 4 N. Wang, L. Han, H. He, N.-H. Park and K. Koumoto, *Energy Environ. Sci.*, 2011, **4**, 3676–3679.
- 5 M. Bhattacharjee, V. Pasumarthi, J. Chaudhuri, A. K. Singh, H. Nemade and D. Bandyopadhyay, *Nanoscale*, 2016, **8**, 6118–6128.
- 6 S. S. Das, V. M. Pedireddi, A. Bandopadhyay, P. Saha and S. Chakraborty, 2019, arXiv:1907.09999.
- 7 X. Xuan, *Electrophoresis*, 2019, **40**, 2484–2513.
- 8 M. Bhattacharjee, S. Timung, T. K. Mandal and D. Bandyopadhyay, *Nanoscale Adv.*, 2019, **1**, 1155–1164.
- 9 L. Manjakkal, A. Vilouras and R. Dahiya, *IEEE Sens. J.*, 2018, **18**, 7779–7785.
- 10 J. Chen, J.-H. Cui and L. Wang, *IEEE Trans. Very Large Scale Integr. Syst.*, 2015, **23**, 1931–1935.
- 11 R. Vooradi, S. B. Anne, A. K. Tula, M. R. Eden and R. Gani, *BMC Chem. Eng.*, 2019, **1**, 7–24.
- 12 K. V. Selvan and M. S. Mohamed Ali, *Renewable Sustainable Energy Rev.*, 2016, **54**, 1035–1047.
- 13 A. Kundu, J. H. Jang, J. H. Gil, C. R. Jung, H. R. Lee, S.-H. Kim, B. Ku and Y. S. Oh, *J. Power Sources*, 2007, **170**, 67–78.
- 14 T. M. Gür, *Energy Environ. Sci.*, 2018, **11**, 2696–2767.
- 15 S. Mamidi, M. Kakunuri and C. S. Sharma, *ECS Trans.*, 2018, **85**, 21–27.
- 16 S. Thakur, S. Rarotra, M. Bhattacharjee, S. Mitra, G. Natu, T. K. Mandal, A. K. Dasmahapatra and D. Bandyopadhyay, *Phys. Rev. Appl.*, 2018, **10**, 064012–064125.
- 17 S. Hardman, A. Chandan and R. Steinberger-Wilckens, *J. Power Sources*, 2015, **287**, 297–306.
- 18 S. A. Mousavi Shaegh, S. M. Mousavi Ehteshami, S. H. Chan, N.-T. Nguyen and S. N. Tan, *RSC Adv.*, 2014, **4**, 37284–37287.
- 19 W. R. Grove, *London, Edinburgh Dublin Philos. Mag. J. Sci.*, 1839, **14**, 127–130.
- 20 M. L. Perry and T. F. Fuller, *J. Electrochem. Soc.*, 2002, **149**, S59–S67.
- 21 B. C. H. Steele and A. Heinzl, *Nature*, 2001, **414**, 345–352.
- 22 I. Staffell, D. Scamman, A. Velazquez Abad, P. Balcombe, P. E. Dodds, P. Ekins, N. Shah and K. R. Ward, *Energy Environ. Sci.*, 2019, **12**, 463–491.
- 23 N. Luo, G. H. Miley, R. J. Gimlin, R. L. Burton, J. Rusek and F. Holcomb, *J. Propul. Power*, 2008, **24**, 583–589.
- 24 R. German, in *IEEE Proceedings OCEANS*, 1989, vol. 3, pp. 843–848.
- 25 M. A. Modestino, D. Fernandez Rivas, S. M. H. Hashemi, J. G. E. Gardeniers and D. Psaltis, *Energy Environ. Sci.*, 2016, **9**, 3381–3391.
- 26 L. Carrette, K. A. Friedrich and U. Stimming, *Fuel Cells*, 2001, **1**, 5–39.
- 27 R. P. O'Hayre, S.-W. Cha, W. G. Colella and F. B. Prinz, *Fuel Cell Fundamentals*, John Wiley & Sons, 2016.
- 28 R. S. Disselkamp, *Int. J. Hydrogen Energy*, 2010, **35**, 1049–1053.
- 29 L. An, T. Zhao, X. Yan, X. Zhou and P. Tan, *Sci. Bull.*, 2015, **60**, 55–64.
- 30 S. Fukuzumi and Y. Yamada, *ChemElectroChem*, 2016, **3**, 1978–1989.
- 31 J. K. Edwards, S. J. Freakley, R. J. Lewis, J. C. Pritchard and G. J. Hutchings, *Catal. Today*, 2015, **248**, 3–9.
- 32 S. Fukuzumi, Y. Yamada and K. D. Karlin, *Electrochim. Acta*, 2012, **82**, 493–511.
- 33 Y. Yamada, Y. Fukunishi, S. Yamazaki and S. Fukuzumi, *Chem. Commun.*, 2010, **46**, 7334–7336.
- 34 S. Yamazaki, Z. Siroma, H. Senoh, T. Ioroi, N. Fujiwara and K. A. Yasuda, *J. Power Sources*, 2008, **178**, 20–25.
- 35 M. Asadnia, S. M. Mousavi Ehteshami, S. H. Chan and M. E. Warkiani, *RSC Adv.*, 2017, **7**, 40755–40760.
- 36 S. A. Mousavi Shaegh, N.-T. Nguyen, S. M. Mousavi Ehteshami and S. H. Chan, *Energy Environ. Sci.*, 2012, **5**, 8225–8228.
- 37 Y. Yamada, M. Yoneda and S. Fukuzumi, *Energy Environ. Sci.*, 2015, **8**, 1698–1701.
- 38 G. Lisak, T. Tamaki and T. Ogawa, *Anal. Chem.*, 2017, **89**, 3943–3951.
- 39 A. Kozawa, V. E. Zilionis and R. J. Brodd, *J. Electrochem. Soc.*, 1970, **117**, 1470–1474.
- 40 A. A. Karyakin, *Electroanalysis*, 2001, **13**, 813–819.
- 41 E. Miglbauer, P. J. Wójcik and E. D. Głowacki, *Chem. Commun.*, 2018, **54**, 11873–11876.
- 42 A. E. Sanli and A. Aytaç, *Int. J. Hydrogen Energy*, 2011, **36**, 869–875.
- 43 B. Scrosati and J. Garche, *J. Power Sources*, 2010, **195**, 2419–2430.
- 44 M. Haruta, *Gold Bull.*, 2004, **37**, 27–36.
- 45 M.-C. Daniel and D. Astruc, *Chem. Rev.*, 2003, **104**, 293–346.
- 46 K. Mallick, M. J. Witcomb and M. S. Scurrall, *Appl. Phys. A: Mater. Sci. Process.*, 2005, **80**, 797–801.
- 47 Y. Yamada, S. Yoshida, T. Honda and S. Fukuzumi, *Energy Environ. Sci.*, 2011, **4**, 2822–2825.
- 48 I. F. Bohrer, N. C. Colesniuc, J. Park, K. I. Schuller, A. C. Kummel and W. C. Trogler, *J. Am. Chem. Soc.*, 2008, **130**, 3712–3713.
- 49 I.-H. Yeo and D. C. Johnson, *J. Electroanal. Chem.*, 2001, **495**, 110–119.
- 50 A. Maizelis, *J. Electrochem. Energy Convers. Storage*, 2019, **16**, 041003–041009.
- 51 A. Ferretti, C. Baldacchini, A. Calzolari, R. Di Felice, A. Ruini, E. Molinari and M. G. Betti, *Phys. Rev. Lett.*, 2007, **99**, 046802–046805.
- 52 B. Amin, S. Nazir and U. Schwingenschlögl, *Sci. Rep.*, 2013, **3**, 1705–1710.
- 53 C. Chen, W. Ma and J. Zhao, *Chem. Soc. Rev.*, 2010, **39**, 4206–4219.
- 54 Y. Jiao, X.-M. Ma, F.-F. Wang, K. Wang, P.-P. Zhang, Z.-Z. Wang and L. Yang, *Micro Nano Lett.*, 2012, **7**, 631–633.
- 55 S. Kalathil, J. Lee and M. H. Cho, *Bioresour. Technol.*, 2012, **119**, 22–27.
- 56 T. H. Han, M. M. Khan, S. Kalathil, J. Lee and M. H. Cho, *Ind. Eng. Chem. Res.*, 2013, **52**, 8174–8181.



- 57 G. Chen, X. Liu, S. Li, M. Dong and D. Jiang, *Lab Chip*, 2018, **18**, 1026–1034.
- 58 Y. Liu, L. Liu and F. Yang, *RSC Adv.*, 2016, **6**, 12068–12075.
- 59 A. J. Nozik and R. Memming, *J. Phys. Chem.*, 1996, **100**, 13061–13078.
- 60 D. O. Grynko, O. M. Fedoryak, P. S. Smertenko, N. A. Ogurtsov, A. A. Pud, Y. V. Noskov and O. P. Dimitriev, *J. Phys. D: Appl. Phys.*, 2013, **46**, 495114–495122.
- 61 S. M. Mousavi Ehteshami, M. Asadnia, S. N. Tan and S. H. Chan, *J. Power Sources*, 2016, **301**, 392–395.
- 62 D. Tuschel, *Spectroscopy*, 2016, **31**, 14–21.
- 63 W. Lee, H. Kim, D.-R. Jung, J. Kim, C. Nahm, J. Lee, S. Kang, B. Lee and B. Park, *Nanoscale Res. Lett.*, 2012, **7**, 672–676.
- 64 Y.-H. Su, Y.-F. Ke, S.-L. Cai and Q.-Y. Yao, *Light: Sci. Appl.*, 2012, **1**, e14–e18.
- 65 W. He, Y.-T. Zhou, W. G. Wamer, X. Hu, X. Wu, Z. Zheng, M. D. Boudreau and J.-J. Yin, *Biomaterials*, 2013, **34**, 765–773.
- 66 L. Wang, R. Li, J. Liu, J. Han and M. Huang, *J. Mater. Sci.*, 2017, **52**, 1847–1855.

