

Nanoengineering ABO_3 active sites from low-energy routes (TX100-stabilised water-in-oil microemulsions, surface segregation and surface complexation on colloidal AlOOH /sol–gel Al_2O_3 surfaces) for pollution control catalysis

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It is shown that water-in-oil microemulsions (m/e or μE) can produce BaCeO_3 (BCO) and LaCoO_3 (LCO) precursors. The nanoparticles (NPs) adsorb on AlOOH sols, in much the same way as Turkevich previously immobilised platinum group metal sols. BCO is active in CO and propane oxidation and NO removal under stoichiometric exhaust conditions, but LCO is a better oxidation catalyst. Activity was also seen when Ba,Ce and La,Co are inserted into/segregate at the surface of $\text{AlOOH}/\text{Al}_2\text{O}_3$. However, there is only formation of low levels of BCO, CaAlO_3 (CAO), LCO and LaAlO_3 (LAO) perovskites, along with aluminates and separate oxides. The complexing of cations by AlOOH surface-held oxalate ions, albeit with different efficiencies, has also been explored. All three routes yield active catalysts with micro-domains of crystallinity; microemulsions produce the best defined perovskite NPs, but even those from surface segregation have higher turnover numbers than traditional Pt catalysts. Perovskite NPs may open up green chemistry for air pollution control that is consistent with a circular economy.

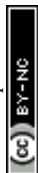
1. Introduction

The authors were intrigued by Turkevich's historic reports of adsorbing and supporting precious metal colloidal particles on AlOOH boehmite,¹ taking advantage of electrostatic attraction, after which transmission electron microscopy (TEM) characterised the surface-held discrete NPs and in parallel catalytic

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activity could be measured directly. They wanted to see whether the approach might be applied to perovskites.²

Routes to perovskites can be high-³ and low-temperature/energy^{4–8} (*e.g.* sol–gel, microwave-assisted sol–gel, electrospinning, hydrothermal synthesis, microemulsion) and mechanochemical.⁹ Some offer opportunities to prepare nanoparticles (NPs; $d < 100$ nm) with different structures: ultrasonics,¹⁰ microwaves (MW)¹¹ and chelators (oxalic acid,¹² citric acid¹³ and tartrate¹⁴), sometimes in one-step preparations.¹⁵ Oxide, halide and oxyhalide perovskite¹⁶ nanoparticles (NPs) can all be produced by such routes. They are used in a wide range of applications:^{17–33} (i) photovoltaic solar cells, (ii) LEDs, photoelectrodes, battery anodes, H₂O and CO₂ electrochemistry, (iii) photocatalysis, (iv) catalysis (*e.g.* combustion of pollutant soot particles with MW regeneration, water gas shift, toluene oxidation, CO methanation and CO oxidation (where activity can be MW-enhanced)), (v) gas sensing, (vi) dielectric heating, (vii) magnetotransport and (viii) biomedicine (*e.g.* hyperthermia and drug delivery). In all these areas perovskite NPs are especially advantageous³⁴ and may be enhanced further by zero-valent NPs,³⁵ supports³⁶ or templates (both inorganic³⁷ or polymeric³⁸).

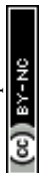
Green catalytic chemistry and resource efficiency are at the heart of a minimum waste circular economy.³⁹ It has long been thought that ABO₃ perovskites⁴⁰ had an advantage in a circular economy over precious metals, provided that their surface areas could be raised above a very modest 1.4 m² g⁻¹ (ref. 41) as reported by Libby, celebrated for his work on 14C radiocarbon dating, and this might be helped by supporting³⁶ or incorporating a polymer or Al₂O₃.

Previously some of the present authors have attempted to nanoengineer catalysts: (a) produced colloidal Pt_xAu_{1-x}Au and Pt–SnO_y alloy sols that were adsorbed on carbon or Al₂O₃ surfaces,⁴² (b) synthesised⁴³ sol–gel Pt–Sn–K/SiO₂–Al₂O₃ hydrocarbon conversion catalysts containing K₂Pt(OH)₆ perovskite precursors⁴⁴ and (c) taken [AlO₄Al₁₂(OH)₂₄(H₂O)₁₂]⁷⁺ Keggin ions (whose formation was followed by ²⁷Al solution NMR in terms of 4-coordinate AlO₄ at about 60 ppm and 6-coordinate AlO₆ at about 2.5 ppm as a function of prevailing OH⁻/Al³⁺ ratios) and partially replaced Al³⁺ with Fe³⁺ or Au³⁺ (ref. 45). These were adsorbed to a 5% loading on SiO₂ surfaces. They showed a similar light-off temperature (LOT) for CO oxidation (870 K) to commercial platinum-group metal three-way catalysts (TWCs) (812 K) in a stoichiometric gas stream. Maximum% conversion of CO at 633 K was seen at Au : Fe = 25 : 75, but these were thermally unstable.

Now we have investigated whether the BaCeO₃ (BCO) and LaAl_{1-x}Co_xO₃ (LACO) perovskite active sites and the sol–gel host could be designed simultaneously to form intriguing environmental catalysts by:

(i) forming these as NPs in aqueous droplets in water-in-oil microemulsions and harvesting by a phase inversion step at 273 K (appreciating that these might be unstable during calcination),

(ii) causing them to form at the surface of colloidal AlOOH or sol–gel Al₂O₃ as the component concentrations were progressively raised beyond the point of maximum solubility in the supporting sol–gel matrix. Alumina was chosen because it is a frequent catalyst support that comes in γ , δ and θ forms.⁴⁶ In the latter, nanowires can be seen in high resolution TEM (HRTEM). Boehmite AlOOH converts to γ -alumina at 723 K, then δ , then θ and finally the α -phase at 1473 K. It can form a defective cubic O²⁻ close-packing spinel structure with 16 possible octahedral sites and 8 tetrahedral sites for Al³⁺ and other stabilising cations. One



knows that there is a maximum solubility of such stabilising cations ($\text{La}^{3+}/\text{Fe}^{2+}$, $\text{Ba}^{2+}/\text{Ce}^{4+}$, and $\text{La}^{3+}/\text{Co}^{2+}$, *etc.*) beyond which phases are formed at the alumina surface. Alumina can be stabilised by $\text{Ce}^{3+/4+}$ or Ba^{2+} ,⁴⁷ the authors appreciated that dispersed CeO_2 NPs (including octapods⁴⁸) could be formed and M^{x+} -alumina reactions could produce spinel BaAl_2O_4 ,⁴⁹ barium hexaluminates, $\text{Ce}^{3+/4+}\text{AlO}_y$ phases⁵⁰ or perovskite CeAlO_3 (CAO)⁵¹ phases, and

(iii) adsorbing oxalate ions on the surface of peptized ALOOH needles and reacting these with the perovskite cations in aqueous solution to give an insoluble surface oxalate that decomposes on calcination.

Goldschmidt⁴⁶ in the 1920s explored ABX_3 perovskites. Orthorhombic BCO forms at 1170–1223 K (ref. 52) and LaFeO_3 (LFeO) exhibited its most intense $\{002\}$ X-ray reflections⁵³ at $2\theta = 28.68^\circ$ and $2\theta = 32.20^\circ$. Rhombohedral LCO prepared at 1013 K (ref. 54 and 55) has its most intense $\{110\}$ and $\{104\}$ reflections at $2\theta = 34^\circ$.⁵⁶ But HRTEM is useful in detecting nanoscale perovskite domains (*e.g.* in LCO⁵⁷). Surface titrations ($\text{COT}_{\text{O}}-\text{OT}_{\text{CO}}$)⁵⁸ help probe active sites and oxygen-storage capacity (OSC)⁵⁹ that may be introduced by CeO_2 (ref. 60 and 61) or $\text{Tb}_4\text{O}_7-\text{CeO}_2$,^{62,63} sometimes promoted by platinum-group metals.⁶⁴ Here it is perovskite nanoparticles that are characterised by X-ray diffraction (XRD), Raman, HRTEM, UV/vis, temperature-programmed reduction/oxidation (TPR/TPO) and XPS. It is important that these methods differentiate perovskite NP phases from other by-product phases (*e.g.* aluminates⁶⁵). After characterising these they were evaluated for CO (and hydrocarbon) oxidation (where rates might be different on different facets⁶⁶). 28–118 nm $\text{LaAl}_{1-x}\text{Mn}_x\text{O}_3$ (LAMnO) and $\text{LaAl}_{1-x}\text{Fe}_x\text{O}_3$ (LFeO) perovskites are good catalysts.^{67,68} Cu-doped LaAlO_3 (LAO)⁶⁹ and LaCoO_3 (LCO)⁷⁰ are photocatalysts and electrochemically active.⁷¹ Partial Pd-replacement of Al^{3+} in LAO produces three-way catalytic (TWC) activity in vehicle exhaust conditions.⁷² LCO and LAO are formed at higher La and Co loadings in sol-gel alumina⁷³ (where some say that LAO is an inert perovskite, but others suggest citrate-derived LAO is active in the oxidative-coupling of methane (OCM)⁷⁴), but 42.2 nm $\text{La}_2\text{CoAlO}_6$ double perovskite is more active and has a lower light-off temperature (LOT; 707.1 K) in CH_4 catalysed combustion⁷⁵ than either LCO (763.6 K) or LAO (845.3 K).

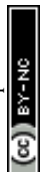
2. Experimental

ALOOH synthesis

0.236 g ALOOH was prepared in 100 cm³ distilled H₂O (initially at 353–358 K) by adding 3.9 mmol aluminium-tri-*sec*-butoxide (ASB, Aldrich, 97%), raising the reflux temperature to 403–413 K, adding 3.9 mmol HCl and refluxing for 48 h to reach a pH of 3.1. One fraction of this ALOOH dispersion was used directly; another was freeze-dried to an ALOOH powder that was calcined at 773 K and then 923 K. Dynamic light scattering (DLS) showed that the average particle size of the ALOOH sol was 60 nm (Fig. 1c); as this was calcined to higher temperatures it would inevitably transform ($\gamma \rightarrow \delta \rightarrow \theta \rightarrow \alpha$).⁴⁶

BCO and LCO synthesis by phase inversion at 273 K in a TX100-stabilised water-in-oil microemulsion

Here two homogenous 0.2 M TX100-stabilised water-in-cyclohexane (90%)/2-methyl-2-propanol (10%) microemulsions were used. In one μE a slight excess of



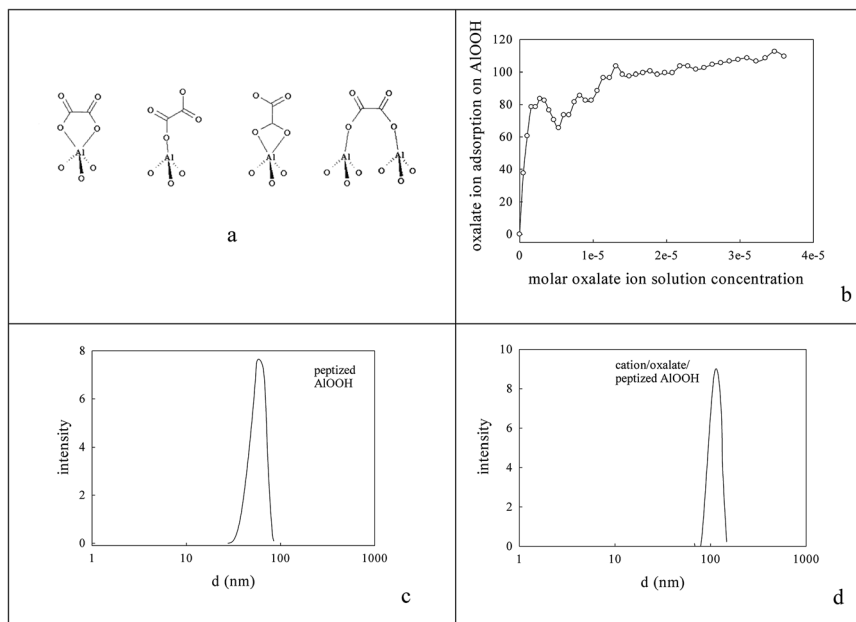


Fig. 1 Nature of oxalate anion adsorption on $\text{AlOOH}^{8,85}$ (a, b). DLS estimate of the average particle size in aqueous dispersions of (c) the peptized AlOOH (60 nm) and (d) after oxalate adsorption and formation of 3.65% cation/oxalate/ AlOOH (114 nm).

ammonium oxalate was introduced to the dispersed water droplets. In another μE mixed 0.02 M La,Co nitrates (or mixed 0.02 M Ba,Ce nitrates) were introduced to the dispersed water droplets.⁷⁶ The two w/o μE s at 298 K were then mixed to produce (as a result of droplet coalescence/re-dispersion mixed 5–10 nm (defined by the diameter of the aqueous droplet size)) Ba-Ce or La-Co oxalate nanoparticles (NPs). The combined microemulsion was then mixed with 50 cm^3 of the pre-prepared AlOOH suspension to give Ba-Ce oxalate/ AlOOH or La-Co oxalate/ AlOOH that were harvested by lowering the combined μE to 273 K (defined by component melting points (280 K, 279.5 K, 273 K and 298–299 K for TX100, cyclohexane, water and 2-methyl-2-propanol)), when two phases appeared. The NP product was found in the upper organic phase. NPs adsorbed on AlOOH , were harvested, washed, dried and calcined (900 K).

Surface segregation using $\text{AlOOH}/\text{Al}_2\text{O}_3$, Ce- $\text{AlOOH}/\text{Al}_2\text{O}_3$ and Ba,Ce- $\text{AlOOH}/\text{Al}_2\text{O}_3$

Surface segregation was attempted using dispersed colloidal AlOOH , where mixed metal cation pairs ($\text{Ba}^{2+}, \text{Ce}^{4+}$ or $\text{La}^{3+}, \text{Co}^{3+}$) were present in the AlOOH forming/peptizing solution/suspension sufficient to cause 25% Ba,Ce- $\text{AlOOH}/\text{Al}_2\text{O}_3$ and 25% La,Co- $\text{AlOOH}/\text{Al}_2\text{O}_3$ to form after calcination at 1173 K. Sol-gel- $\text{AlOOH}/\text{Al}_2\text{O}_3$ derived Ce- and Ba,Ce-containing catalysts^{77,78} were prepared from ASB, 2-methylpentane-2,4-diol (MPD, Aldrich, 99%), $\text{Ba}(\text{NO}_3)_2$ - $\text{Ce}(\text{NO}_3)_3$ (Aldrich, 99.999%; dissolved in MPD) and deionised H_2O ^{78,79} as reported previously.⁴⁵ For Ba,Ce- $\text{AlOOH}/\text{Al}_2\text{O}_3$ the Ba and Ce nitrates were dissolved in MPD at 360 K, followed by ASB and refluxing at 393 K for 6 h under N_2 . After cooling to 363 K, H_2O



was added dropwise over 25 min and refluxing was continued (2 h), followed by ageing at 373 K for 7 days, vacuum-drying (353 K) and then calcining (1173 K; 2 h; static air). Citrates, tartrates or acetates^{80,81} could have been used but nitrates were preferred. MPD was both a solvent^{82,83} and complexing agent⁸⁰/pore templating agent. Fuentes⁸³ derived La₂O₃-Al₂O₃ using MPD; here the metal : MPD : H₂O ratio was 1 : 5 : 25. Sol-gel ALOOH/Al₂O₃ (BET surface area 179 m² g⁻¹) had a higher surface area than when Ce was added (*e.g.* 16.6% (ICP-MS derived) Ce-ALOOH/Al₂O₃ (BET surface area 168 m² g⁻¹)).

Surface complexation

The peptized ALOOH dispersion had a final pH of 3.1 (below its isoelectric point/point of zero charge (7.8–8.6)) and so it adsorbed oxalate anions⁸⁴ on its surface *e.g.* see Fig. 1a and b; the % adsorption was deduced from the % differential change in suspension conductivity ($100\% \times (\sigma_{\text{H}_2\text{O}} - \sigma_{\text{ALO}(\text{aq})})/\sigma_{\text{H}_2\text{O}}$) on sequential addition of 1 cm³ portions of 10 mM oxalic acid to 50 cm³ H₂O or ALOOH_(aq) respectively). After Ba²⁺, Ce⁴⁺ or La³⁺, Co³⁺ addition the average DLS particle size rose, almost doubling to 114 nm (Fig. 1c and d). This pre-adsorbed oxalate was titrated with Ba²⁺, Ce⁴⁺ or La³⁺, Co³⁺ forming a surface layer of low solubility mixed oxalates⁸⁴ at an intended 5% loading. However, XPS (using Ba (780.7 eV), Ce (897.7 eV), La (834.7 eV) and Co (781.6 eV) peaks) and FAAS suggested that only a 3.65% metal loading on the oxalate/ALOOH was achieved with Ba : Ce and La : Co ratios on oxalate/ALOOH of 25 : 75 and 30 : 70. This was equivalent to the formation of 0.91% Ba, 2.74% Ce-ALOOH/Al₂O₃ and 1.095% La, 2.56% Co-ALOOH/Al₂O₃.

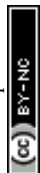
Characterization

Malvern DLS, Jeol HRTEM, X'Pert Pro XRD, Supra SEM-EDX and XPS characterization was carried out. TPR,⁸⁵ titration and catalysis was followed as now described. Setaram and Thermo Scientific DSC profiles were used for CO (40 μmol) and O₂ (47 μmol) titrations of catalysts in a flowing N₂ (50 cm³ min⁻¹) inert gas stream held isothermally at a selected temperature. Catalytic measurements were carried out as described previously.⁵⁹ Samples (200 mg) were placed in a silica reactor (6 mm diameter) and heated in flowing N₂ to 773 K for 20 min. Then after cooling to 298 K the stoichiometric reactant stream (NO + O₂ oxidant/CO + propane reductant (*R*) ratio = 1.13, where the reactant stream contained 1000 ppm NO, 5890 ppm O₂, 6000 ppm CO, 520 ppm propane, 10% CO₂ in a N₂ balance) was introduced at 500 cm³ min⁻¹ (equivalent to a 60 000 h⁻¹ space velocity in a gasoline-fuelled engine exhaust) at 101 kPa under Brooks smart 5850S mass flow controllers. NDIR, FID-GC and CLD analysers were used for CO/CO₂, propane and NO_x concentrations in real time during heating from 300 K to 900 K at 10 K min⁻¹.

3. Results

BCO and LCO microemulsion precipitation

Fig. 2a shows the effect of the water content of TX100-stabilised water-in-cyclohexane/2-methyl-2-propanol μE on the partitioning of the surfactant between the water and hydrocarbon phases. There is continuous coalescence and



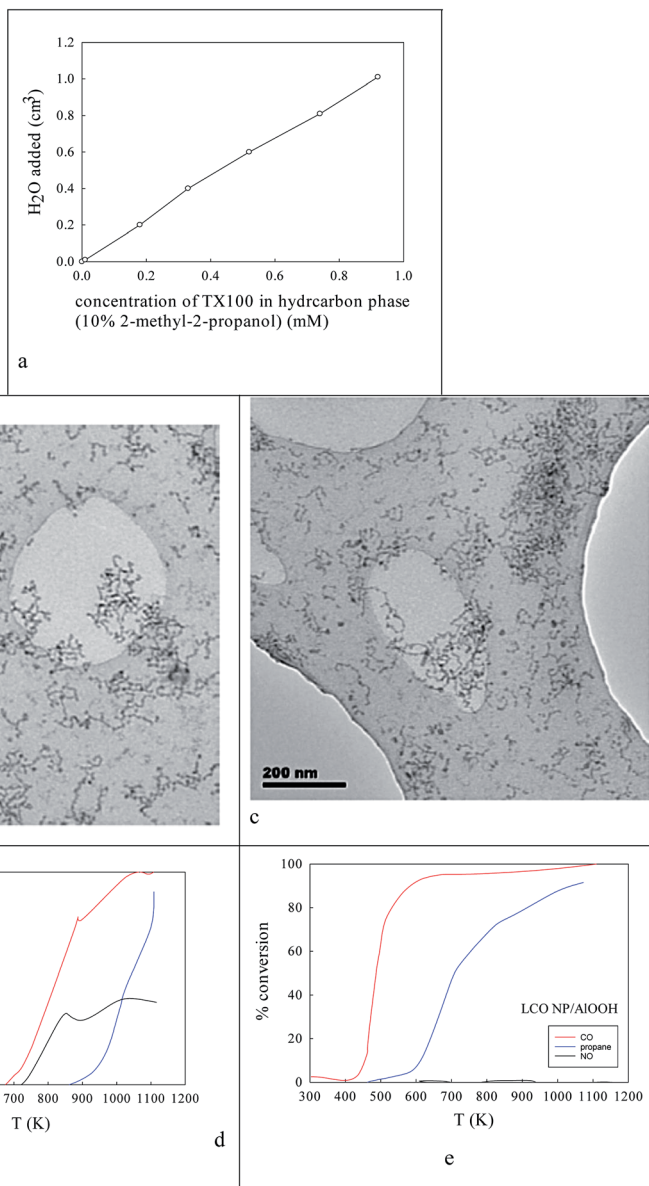


Fig. 2 (a) Effect of H₂O content on TX100 in the oil phase of a H₂O-in-cyclohexane/2-methyl-2-propanol *m/z*. (b, c) TEM of *m/z*-derived BCO and LCO NPs and fractal aggregates. (d, e) The activity of such NPs adsorbed onto AIOOH.

separation of nm-sized water droplets, some containing a slight excess of ammonium oxalate and some metal cations. Fig. 2b and c show TEM evidence of the sizes of microemulsion-derived 10–20 nm BCO NPs (with 40–121 nm fractal nanothreads) and 10–21 nm LCO NPs (with and 43–108 nm fractal nano-chains) after phase inversion at 273 K. In Fig. 2d and e one sees the activity of such AIOOH-supported perovskite NPs under stoichiometric conditions as a function



of temperature. Clearly BCO has activity in CO and propane oxidation and more surprisingly in NO conversion (under stoichiometric conditions), but LCO has higher CO and propane activity, but no NO reduction activity. This is promising.

Ba,Ce and La,Co surface segregation⁵⁹ on ALOOH/Al₂O₃

Clearly the ionic radius of Ce^{4+/3+} (87/101 pm) relative to O²⁻ and Al³⁺ in part defines its solubility in ALOOH/Al₂O₃. Fig. 3 shows some characterization data before and after introduction of 20% Ce to the ALOOH/Al₂O₃. The sample surface area dropped by 6.1% on this Ce introduction, but HRTEM (Fig. 3a) saw 5 nm nano-crystallites with lattice spacings of 0.19 nm. XRD found after calcination the presence of θ -Al₂O₃, low levels of 10–12 nm γ -Al₂O₃ and CeO₂, but there was no evidence of CAO. Interestingly, in H₂-TPR a 720 K peak (α ; H/CeO₂ ratio = 0.156) was associated with alumina-dispersed CeO₂,^{85,86} while a 900 K + (β) peak was thought to relate to CAO⁸⁸ (that was too fine to be seen XRD) or Ce₂O₃. Fig. 3c shows that CeO₂ addition raises the activity in CO conversion modestly above that

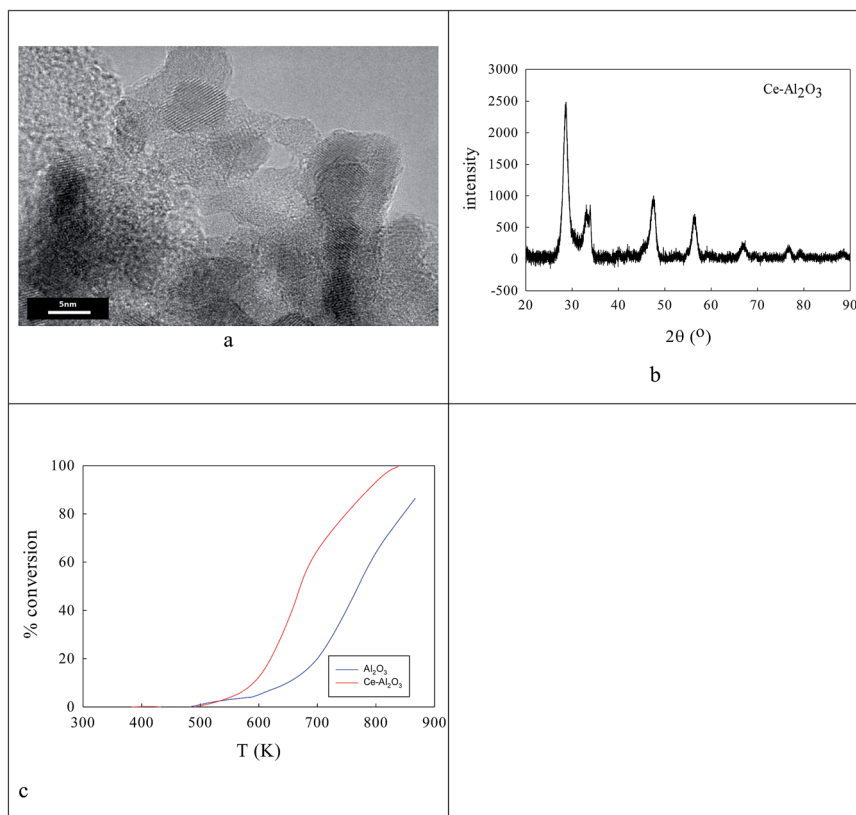
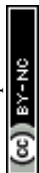


Fig. 3 Well-dispersed sol-gel 20% CeO₂-ALOHH (before calcination)/Al₂O₃ (after calcination) (168 m² g⁻¹) seen in (a) HRTEM and (b) XRD was slightly more active in CO oxidation under stoichiometric conditions (c) than the pure Al₂O₃ despite a 6.1% loss of surface area. HRTEM (a) shows 5 nm nano-crystallites (b). XRD (c) shows θ -Al₂O₃ and CeO₂ (but not CAO). H₂-TPR did, however, provide evidence in terms of a 900 K + β -peak for CAO.



of the alumina support only, despite the loss of surface area, but there is no HC or NO conversion.

The ionic radius of Ba^{2+} (135 pm) is larger than that of Ce^{4+} . As the Ba^{2+} and Ce^{4+} contents inserted into the $\text{AlOOH}/\text{Al}_2\text{O}_3$ each rise from 0 to 25%, it was expected that BaAl_2O_4 would appear, that CeO_2 would segregate, but also that CAO or BCO might form in or at the surface of the host sol-gel matrix more strongly. It was found (see Fig. 4) that as the Ba,Ce content increased so HRTEM always showed 5–20 nm micro-domains of crystallinity (see Fig. 4a and b) and X-ray diffraction line broadening (XRDLB) (Fig. 4c) revealed unchanging and small average XRDLB crystallite sizes (d_{XRDLB}) while MASNMR saw 6-coordinate Al^{3+} gradually replaced by 4-coordinate (as BaAl_2O_4 appeared), XRD peak intensities

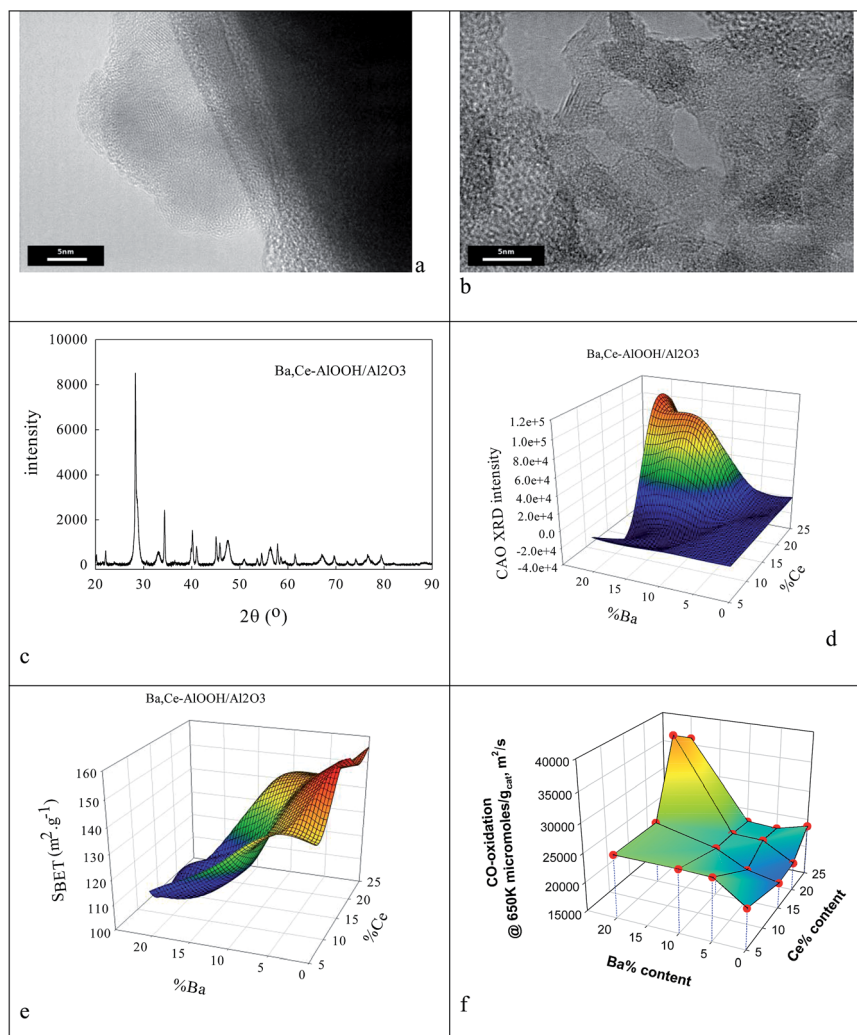


Fig. 4 Effect of Ba,Ce insertions at increasing levels into $\text{AlOOH}/\text{Al}_2\text{O}_3$ after calcination at 1223 K. HRTEM (a, b), XRD structure (c) and CAO level (d), surface area (e) and CO oxidation rate at 650 K in a stoichiometric reactant stream ($R = 1.13$) (f).



for BaAl_2O_4 , CeO_2 and CaO (Fig. 4c and d) increased, surface areas decreased by 8% (Fig. 4e), and total CO (and propane, but not NO) conversion activity at 650 K increased (Fig. 4f).

To understand the nature of the highest CO oxidation catalytic activity (at high Ba,Ce addition levels) $\text{COT}_{\text{O}}\text{-OT}_{\text{CO}}$ titrations of the surface were undertaken on 20% Ba,20% Ce- $\text{AlOOH}/\text{Al}_2\text{O}_3$ at 773 K and compared to EuroPt-1 at 573 K (see DSC profiles in Fig. 5 and integrated peak areas in Table 1) by DSC. Exothermic titration peaks increased in area or were stable with titration cycling, but the authors concentrated on the first CO titrations of surface O (COT_{O1}). On EuroPt-1 at 573 K ($\text{COT}_{\text{O1}} = 126.43 \text{ J g}^{-1}$) COT_{O1} was $4.5\times$ higher than for $88 \text{ m}^2 \text{ g}^{-1}$ 20% Ba,20% Ce- $\text{AlOOH}/\text{Al}_2\text{O}_3$ at 773 K ($\text{COT}_{\text{O1}} = 28.043 \text{ J g}^{-1}$) and these were $57.2\times$ higher than for $170 \text{ m}^2 \text{ g}^{-1}$ undoped- $\text{AlOOH}/\text{Al}_2\text{O}_3$ ($\text{COT}_{\text{O1}} = 0.490 \text{ J g}^{-1}$) at 773 K. Interestingly, COT_{O1} can be converted to a number of active sites (*) adsorbing CO/g catalyst and hence to a turnover frequency (TOF); the TOF for 20% Ba,20% Ce- $\text{AlOOH}/\text{Al}_2\text{O}_3$ was 35% higher than for EuroPt-1 (see Table 1). Furthermore, the 20% Ba,20% Ce- $\text{AlOOH}/\text{Al}_2\text{O}_3$ showed a lower $\text{COT}_{\text{O}}/\text{OT}_{\text{CO}}$ titration ratio than EuroPt-1 (suggesting less potential for CO poisoning). At high CeO_2 and BaO

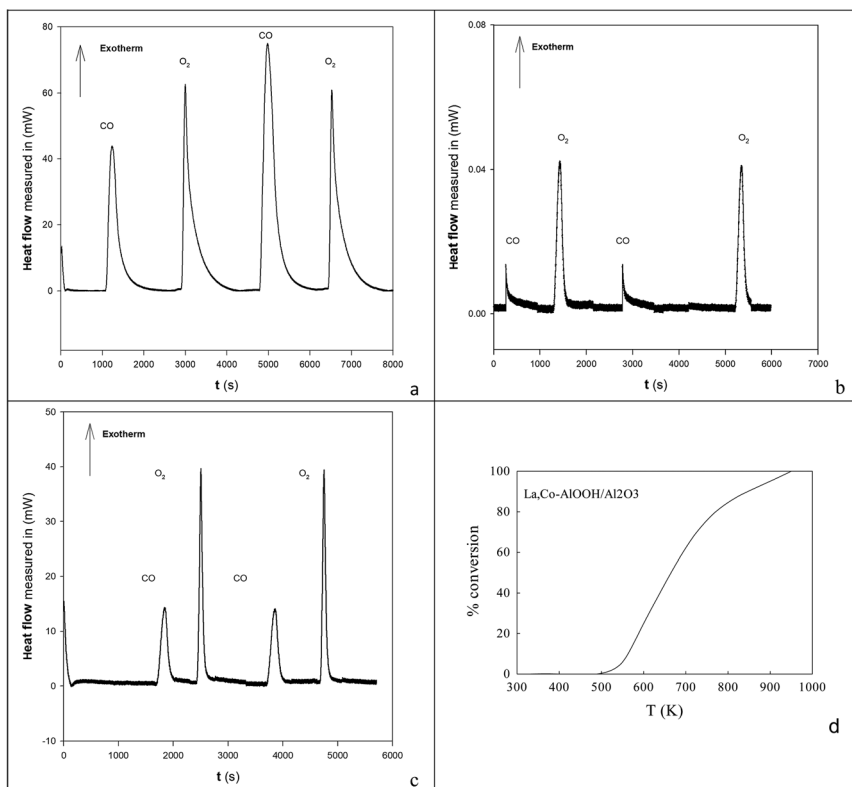


Fig. 5 DSC profiles for CO (40 μmol) and O_2 (47 μmol) titrations on (a) EuroPt-1 6.3% Pt/ SiO_2 at 573 K (where $\text{COT}_{\text{O1}} = 126.43 \text{ J g}^{-1}$; $\text{OT}_{\text{CO1}} = 182.37 \text{ J g}^{-1}$); (b) $\text{AlOOH}/\text{Al}_2\text{O}_3$ ($170 \text{ m}^2 \text{ g}^{-1}$) at 773 K ($\text{COT}_{\text{O1}} = 0.490 \text{ J g}^{-1}$) and (c) 20% Ba,20% Ce- $\text{AlOOH}/\text{Al}_2\text{O}_3$ at 773 K ($88 \text{ m}^2 \text{ g}^{-1}$) at 773 K ($\text{COT}_{\text{O1}} = 28.043 \text{ J g}^{-1}$; $\text{OT}_{\text{CO1}} = 37.886 \text{ J g}^{-1}$). (d) CO oxidation activity profile for 25% La,Co- $\text{AlOOH}/\text{Al}_2\text{O}_3$.

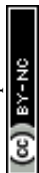


Table 1 Adsorption capacities, rates and TOFs for CO oxidation at 600 K under stoichiometric conditions ($R = 1.13$) for EuroPt-1 6.3% Pt/SiO₂ and 20% Ba,20% Ce–AlOOH/Al₂O₃ (calined at 1223 K)

Catalysts	n_{CO} at ^a 773 K ($\mu\text{mol g}_{\text{cat}}^{-1}$)	Number of active sites ([*])/g _{cat} × 10 ⁻¹⁹	Rate of CO oxidation ^b (molec per g _{cat} per min)	TOF (molec per [*] per s)
EuroPt-1	57	3.4	4.1	0.20
20% Ba,20% Ce–AlOOH/Al ₂ O ₃	41	2.5	4.1	0.27

^a Monolayer CO capacity at 773 K. ^b At 600 K and $R = 1.13$.

concentrations, peaks from low concentrations of CAO and BCO (presumably at the interface between BaAl₂O₄ and CeO₂) appear in low concentration and may be significant contributors to catalytic activity.

La,Co doping was also achieved by replacing the 100 cm³ water for AlOOH by a mixed metal nitrate aqueous solution. This was used to produce 25%La,Co–AlOOH/Al₂O₃. After calcination (923 K) this gave the catalytic profile in Fig. 5d, which is only slightly poorer than Fig. 2e. Hence both Ba,Ce and La,Co cation pairs can be inserted into AlOOH/Al₂O₃ and will produce activity in atmospheric pollution control reactions.

Surface complexation with pre-adsorbed oxalate to give 5% Ba,Ce– and 5% La,Co–AlOOH/Al₂O₃

Fig. 1c gave the average size of AlOOH dispersions seen in DLS (60 nm), on which oxalate anions were adsorbed,⁸⁵ followed by Ba,Ce or La,Co cations to form surface oxalates. Fig. 1d shows that this sequential coating caused the average particle size to rise to 114 nm after drying and calcination at 1223 K that was judged to be necessary to decompose oxalate species. Its oxidation activity was very modest (Fig. 6b).

TGA indicated that AlOOH lost 22% of its mass on heating, but this increased to 36% in 5% Ba,Ce–AlOOH/Al₂O₃ and 37% in 5% La,Co–AlOOH/Al₂O₃. XPS showed that the surface Ba : Ce surface atomic ratio was 25 : 75, while the La : Co XPS ratio on the surface was found to be 85 : 15. XPS-FAAS suggests these samples may be 0.91% Ba, 2.74% Ce–AlOOH/Al₂O₃ or 1.095% La, 2.56% Co–AlOOH/Al₂O₃. Fig. 7a and b show that these samples contain micro-domains of crystallinity 3–5 nm in diameter. Thus XRD (a) and HRTEM (c, d) found 8–20 nm micro-domains of crystallinity. Analysis of HRTEM lattice images for Ba,Ce–AlOOH/Al₂O₃ (0.295 nm and 0.32 nm spacings) and La,Co–AlOOH/Al₂O₃ (0.225 nm and 0.296 nm spacings) gave line spacings after calcination greater than for AlOOH alone (0.19 nm; Fig. 6d). XRD of Ba,Ce–AlOOH/Al₂O₃ (Fig. 7e) shows that the dominant phase is probably 48.3 nm BaAl₂O₄, but there is also evidence from a (311) peak for 14.0 nm CeO₂ and traces of BCO and CeO₂/CAO. XRD for La,Co–AlOOH/Al₂O₃ (Fig. 7f) suggests that the dominant phases are 36–41.5 nm LAO and 17.68 nm Co₃O₄ but with LCO also present in small amounts. This ion preference may relate to oxalate insolubility, but would not help perovskite formation. CO and propane oxidation activity (Fig. 8a and b) was even lower than with sol-gel alumina (Fig. 3c).



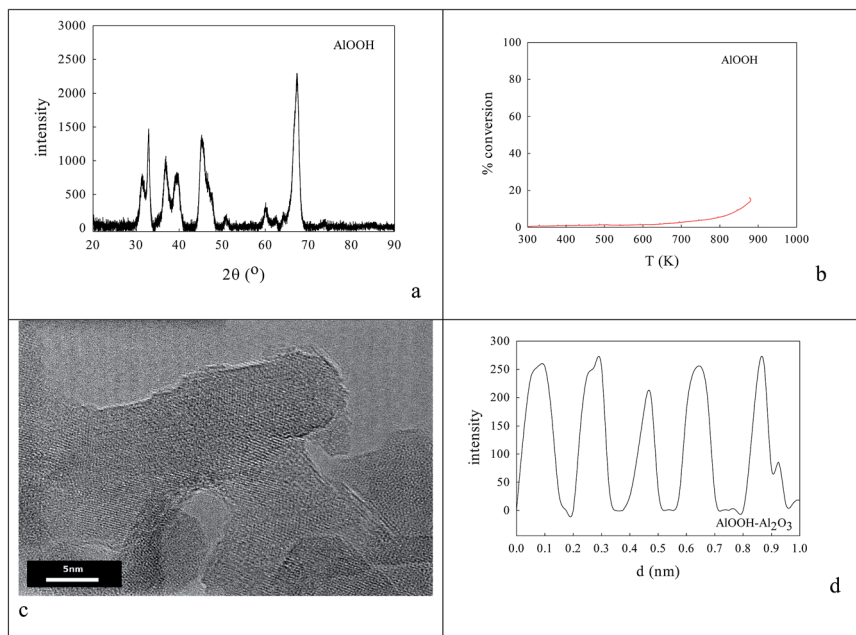


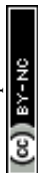
Fig. 6 AIOOH ($d_{\text{DLS}} = 60$ nm; see Fig. 2c)/Al₂O₃ samples onto which oxalate anions had been adsorbed,⁸⁴ then dried and calcined at 1223 K to decompose oxalate species, gave XRD (a) and HRTEM (c, d) evidence of 8–20 nm micro-domains of crystallinity. The most frequent XRD peaks appeared to be 11.70 nm θ -Al₂O₃ (with perhaps low levels of γ -Al₂O₃). The line spacing in micro-crystals was AIOOH (0.19 nm spacing), but activity in CO or propane oxidation or NO reduction (b) was even lower than with sol–gel alumina (Fig. 4f).

DSC measurements of the first COT_{O1} on EuroPt-1 at 423 K (ref. 58) was 143.01 kJ g⁻¹ catalyst (2270 kJ g⁻¹ Pt).⁵⁸ The summed heat flows in the first COT_{O1} from Ba,Ce/AlOOH (1.920 J g⁻¹ catalyst) (and even more so La,Co/AlOOH (660.7 mJ g⁻¹ catalyst)) (see Fig. 8c and d) were much smaller than those for EuroPt-1. That for COT_{O1} from Ba,Ce–AlOOH/Al₂O₃ (1.920 J g⁻¹ catalyst) was a factor of 14 × lower than that for 20% Ba,20% Ce–AlOOH/Al₂O₃ sample (28.04 J g⁻¹ catalyst), but that is not surprising given the imbalance of cations and the lower loading in the surface complexation samples.

4. Discussion and conclusions

It seems from the present work that microemulsion routes to BCO and LCO are effective and that the products adsorb on AIOOH sols, in much the same way as Turkevich immobilised platinum group metal sols.¹ BCO is active in CO and propane oxidation and NO removal under stoichiometric exhaust conditions, but LCO is a better oxidation catalyst. In calcination, the surfactant TX100 is removed, overcoming a frequent impurity disadvantage of μ E routes.

Activity was also seen when Ba,Ce and La,Co are (i) inserted into AIOOH/Al₂O₃ and segregated at the surface, but in addition to formation of low levels of BCO, CAO, LCO and LAO perovskites, one also sees aluminates (*e.g.* BaAl₂O₄) and



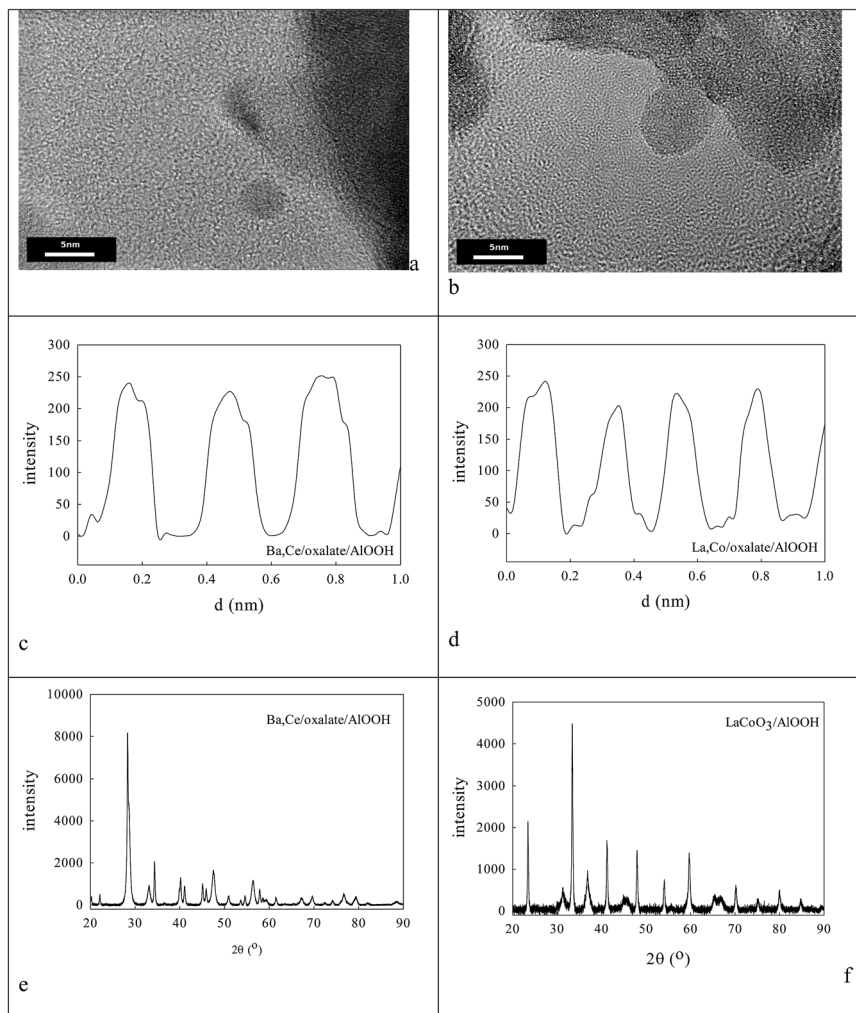


Fig. 7 (a–d) HRTEM of Ba,Ce/oxalate/AlOOH (a, c) and La,Co/oxalate/AlOOH (b, d) produced from Ba^{2+} and Ce^{4+} cations adsorbed on oxalate/AlOOH, drying and then calcination at 1223 K. XRD of Ba,Ce/oxalate/AlOOH (e) and La,Co/oxalate/AlOOH (f) show the dominant and minor phases present.

separate oxide (*e.g.* CeO_2), although this might be minimised by fine tuning of cation loadings and (ii) when the cations were complexed with AlOOH surface-held oxalate ions, albeit with different efficiencies.

Therefore all three routes yield active catalysts with micro-domains of crystallinity.

The longer term aim of the present work was to design and produce nanoparticulate perovskites, with a variety of cations,⁴⁶ stabilised by alumina (*i.e.* where there might be stabilisation by Al^{3+} substitution⁴⁷). Of course one might still wish to use activation by Au nanoparticles/nanocrystals yielding green synergies⁶⁶ in catalysis⁶⁷ and gas sensing.⁶⁸



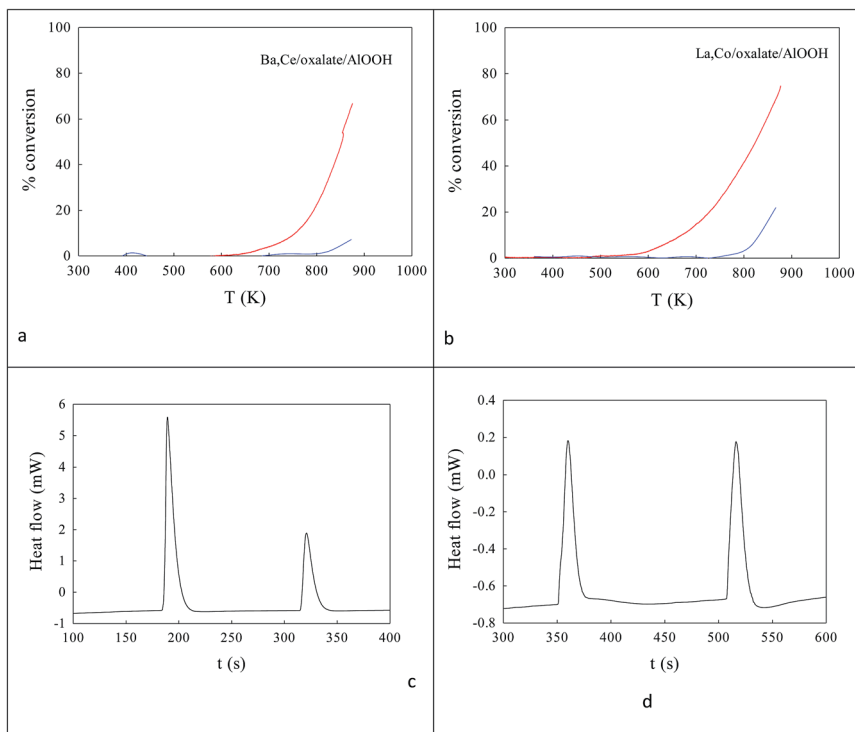
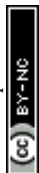


Fig. 8 Catalytic activities (a, b) and DSC analysis of COT_{O_2} and OT_{CO_2} titrations in flowing N_2 (c, d)⁵⁸ of Ba,Ce/oxalate/AlOOH (a, c) and La,Co/oxalate/AlOOH (b, d). Catalytic activities were modest for both these samples. The summed heat flows in the first COT_{O_2} from Ba,Ce/oxalate/AlOOH (1.920 J g^{-1} catalyst) was a factor of $14\times$ lower than that for the 20% Ba,20% Ce–AlOOH/ Al_2O_3 sample (28.043 J g^{-1} catalyst) which is not surprising, given the lower loading in the surface complexation samples. COT_{O_2} was even lower for La,Co/AlOOH (0.661 J g^{-1} catalyst).

Some have seen higher perovskite surface areas (*e.g.* LCO ($22 \text{ m}^2 \text{ g}^{-1}$) than LaMnO_3 (LMnO) ($10 \text{ m}^2 \text{ g}^{-1}$)¹³). Some have compared the propane oxidation activity for $6\text{--}16 \text{ m}^2 \text{ g}^{-1}$ (S_{BET}) and $15\text{--}25 \text{ nm}$ crystallite size ($d_{\text{XRDLB-Scherrer}}$) LMnO perovskites with 1% Pt/ Al_2O_3 (ref. 89) and found that the temperatures of 10%, 50% and 90% oxidation ($T_{10\%}$, $T_{50\%}$ and $T_{90\%}$) were higher for the perovskites than the platinum group metal (PGM). The same authors found the perovskite-like trigonal X-ray diffraction patterns.⁸⁹ Others⁹⁰ have seen primary perovskite particle sizes, shapes, aggregation and structure by high resolution TEM. The present work should be seen against this background.

Here we have explored BaCeO_3 (BCO; that has been used in CO_2 conversion and characterised for structure by XRD⁴⁸ and embedded in hosts⁴⁹) and LCO (that is useful in catalysed phenol removal from water⁵⁰). We believe that the present routes offer an opportunity to develop green nanoparticle perovskite catalysts for a circular economy and a better environment, and that these might ultimately find use for other perovskite applications.²

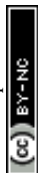


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Notes and references

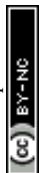
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