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## Unlocking nanotubular bismuth oxyiodide toward carbon-neutral electrosynthesis†

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The electrochemical CO<sub>2</sub> reduction reaction (CO<sub>2</sub>RR) to formate is one of the attractive strategies for achieving carbon-neutral sustainability, but synthesizing highly active catalytic materials capable of selectively forming formate, especially under industrially relevant conditions, remains challenging. We herein report ultrathin one-dimensional nanotubular Bi<sub>5</sub>O<sub>7</sub>I with substantial amounts of nanopores and oxygen vacancies for the CO<sub>2</sub>RR. A desirable selectivity of over 93% and high current density for formate are achieved in a potential window of 1000 mV in a flow cell. More importantly, a stable performance of 140 h with faradaic efficiency over 90% in a membrane electrode assembly system demonstrates great potential for industrial CO<sub>2</sub>RR application. The abundant defects within the ultrathin nanotubular structure not only improve the CO<sub>2</sub> adsorption and charge transfer capabilities that facilitate the reaction kinetics, but also modulate the electronic structure and optimize the energy barrier toward formate as revealed by the theoretical calculations. Concurrently, the local high pH caused by the structural defects and hydrophobic surface could remarkably suppress the hydrogen evolution reaction and in turn, accelerate formate formation. These advances demonstrate an effective structure and defect engineering to unlock one-dimensional electrocatalysts to boost the CO<sub>2</sub>RR toward target products.

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### Broader context

The conversion of greenhouse gas CO<sub>2</sub> into value-added chemicals and fuels through electrochemical CO<sub>2</sub> reduction reaction (CO<sub>2</sub>RR) holds promising potential to reduce the CO<sub>2</sub> emission level and simultaneously store renewable energy to achieve sustainable carbon neutrality. Given the commercial viability of different reduced products, reducing CO<sub>2</sub> to formate is one of the most economically viable pathways based on the recent technoeconomic analysis. Nevertheless, achieving high selectivity and current density for formation in a wide potential window still remains challenging when implementing practical CO<sub>2</sub>RR technology applications. In this study, we present an effective strategy by introducing abundant defects into the one-dimensional ultrathin nanotubular structure of Bi<sub>5</sub>O<sub>7</sub>I for efficient CO<sub>2</sub>RR to formate at an industrial-level current density in both flow cell and membrane electrode assembly. The experimental and theoretical studies comprehensively unravel the origins of the enhanced catalytic activity and selectivity resulting from the joint effort of structure and defect merits. These findings underscore the effectiveness of the combination of structure and defect engineering as an attractive strategy for designing advanced electrocatalysts for achieving carbon-neutral sustainability.

## 1. Introduction

The ever-increasing accumulation of CO<sub>2</sub> in the atmosphere has caused severe climate changes that negatively impact the natural environment and sustainable development of human society.<sup>1–3</sup> The electrochemical CO<sub>2</sub> reduction reaction (CO<sub>2</sub>RR) is regarded as an attractive technology to lower the CO<sub>2</sub> emission level when powered by the electricity generated from renewable energy sources (*e.g.*, wind, solar or tidal energy), and it can eventually achieve sustainable carbon neutrality by converting CO<sub>2</sub> to valuable chemicals.<sup>4–6</sup> However, the inertness of CO<sub>2</sub> molecules and multi-electron transfer process during the

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CO<sub>2</sub>RR usually lead to high thermodynamic energy barriers and sluggish reaction kinetics.<sup>7,8</sup> The low solubility of gaseous CO<sub>2</sub> in aqueous media and broad distributions of target products also account for the unsatisfactory CO<sub>2</sub>RR performance.<sup>9</sup> In addition, the hydrogen evolution reaction (HER) always competes with the CO<sub>2</sub>RR in aqueous media and can significantly deteriorate the selectivity for specific products.<sup>10</sup> Thus, it is of great importance to design highly active and selective electrocatalysts for efficient CO<sub>2</sub>RR.

As one of the typical liquid products with two-electron reduction of CO<sub>2</sub>, formate can be utilized in fuel cells as hydrogen carriers, and in the textile and pharmaceutical industries.<sup>11,12</sup> So far, various metal-based electrocatalysts (*e.g.*, Pd,<sup>13,14</sup> Sn,<sup>15,16</sup> In,<sup>17,18</sup> Pb<sup>19,20</sup> and Bi<sup>21–24</sup>) have been demonstrated to form formate, among which Bi-based materials show great potential due to their low toxicity and earth abundance. Various studies on Bi-based electrocatalysts, including Bi nanoparticles,<sup>25</sup> Bi dendrites<sup>26</sup> and two-dimensional Bi nanosheets,<sup>27–30</sup> have demonstrated the effectiveness of structure engineering in improving CO<sub>2</sub>RR performance toward formate formation, but still fail to meet the requirements of industrial applications, *e.g.*, high current densities (*j*) and wide potential window with high faradaic efficiencies (FEs) to lower the capital investment for the desired production rate.<sup>31,32</sup> However, most of the reported formate faradaic efficiencies (FE<sub>formate</sub>) on Bi-based materials show an increased peak of over 90% at moderate potential, while such high selectivity could only be maintained in a narrow potential window.<sup>33</sup> Although some reported electrocatalysts demonstrated wider potential windows with higher FE<sub>formate</sub>, the achieved *j* is still far from the one for practical implementations. Therefore, it is imperative to develop efficient electrocatalysts for CO<sub>2</sub>RR-to-formate conversion with high *j* and FE over a wide potential window to realize practical applications at an industrial scale.

It has been well recognized that the structure modulation of electrocatalysts is an effective approach to improving CO<sub>2</sub>RR performance. Among numerous nanomaterials with various morphologies and structures, one-dimensional nanomaterials are regarded as promising candidates for the CO<sub>2</sub>RR.<sup>34,35</sup> The large surface area guarantees a substantial amount of active sites for the CO<sub>2</sub>RR, while the unique channel structure of the nanotubes could significantly improve the charge transfer ability and the mass transport in aqueous media. Nonetheless, electrocatalysts with nanotubular structures are challenging the position to address the issues of low CO<sub>2</sub> solubility and sluggish multi-electron transfer kinetics. As another critical factor, defects on as-prepared electrocatalysts can introduce massive uncoordinated sites, thereby ensuring desirable CO<sub>2</sub>RR performance. Zhang *et al.*<sup>36</sup> demonstrated that defects could enrich the reaction intermediates and OH<sup>−</sup>, which could consequently prompt the C–C bond formation and improve the selectivity of the target product. This is further confirmed by Yang *et al.*<sup>37</sup> who showed that defective indium/indium oxide heterostructures exhibit a high selectivity for C<sub>1</sub> products with FE approaching 100% in a broad potential range. Presently, among various electrocatalysts, defects are mostly introduced on bulk or two-dimensional materials but there are almost no

studies on one-dimensional materials.<sup>38,39</sup> In light of the advantages of low-dimensional materials and structure defects, introducing defects into the nanotubular Bi-based architecture holds great potential to drive highly active and selective CO<sub>2</sub>RR to formate.

In this work, ultrathin Bi<sub>5</sub>O<sub>7</sub>I nanotubes (NTs) with nanopores and abundant oxygen vacancies are synthesized and demonstrated as a highly active, selective and stable electrocatalyst for the CO<sub>2</sub>RR toward formate formation. The as-obtained Bi<sub>5</sub>O<sub>7</sub>I NTs show a desirable FE<sub>formate</sub> within a wide potential range as well as a high formate formation rate of 1145 μmol h<sup>−1</sup> cm<sup>−2</sup> at a moderate potential. Moreover, the CO<sub>2</sub>RR performance is boosted in a flow cell that delivers a high current density of 225 mA cm<sup>−2</sup> at −1.0 V *versus* reversible hydrogen electrode (*vs.* RHE) and achieves a good stability of 7 h with negligible degradation. The Bi<sub>5</sub>O<sub>7</sub>I NTs are further evaluated in a membrane electrode assembly system at a current density of 200 mA cm<sup>−2</sup> and show negligible changes of cell voltage and FE over 140 h for CO<sub>2</sub>RR. Benefitting from the nanotubular morphology and defective structure, the massive uncoordinated active sites can not only strengthen the CO<sub>2</sub> adsorption and charge transfer, thereby speeding up the CO<sub>2</sub>RR reaction kinetics, but also provide a hydrophobic surface with a higher local pH to effectively inhibit the competing HER. Density functional theory (DFT) calculations reveal that the defective structure of the electrocatalyst can effectively modulate the electronic structure and optimize the adsorption of the reaction intermediate, thereby promoting CO<sub>2</sub>RR performance. All of the above merits collectively contribute to the enhanced electrocatalytic performance for CO<sub>2</sub>-to-formate conversion.

## 2. Results and discussion

### 2.1 Structural characterizations of Bi<sub>5</sub>O<sub>7</sub>I nanotubes

The Bi<sub>5</sub>O<sub>7</sub>I NTs were synthesized *via* the hydrothermal method. As characterized by the high-angle annular dark-field scanning transmission electron microscopy (HAADF-STEM), the prepared catalyst shows an ultrathin nanotubular structure with a uniform diameter of about 5 nm, where a substantial amount of nanopores can be observed on the side wall (Fig. 1a and b). The magnified HAADF-STEM image further clearly shows the wall thickness of about 1 nm with the distribution of nanopores along the wall (Fig. 1c). It is expected that the abundant defects on ultrathin porous nanotubes are beneficial for gas adsorption and charge transfer during the electrochemical reactions. Energy dispersive X-ray spectroscopy (EDS) elemental mapping (Fig. 1d–g) confirms the uniform distribution of Bi, O and I along the nanotubes, indicating a successful preparation of the Bi<sub>5</sub>O<sub>7</sub>I NTs. Moreover, Bi<sub>5</sub>O<sub>7</sub>I NTs were further characterized by powder X-ray diffraction (XRD), as shown in Fig. 1h. The three peaks of the XRD patterns ranging from 25 to 35° are assigned to the (312), (004) and (600) planes of Bi<sub>5</sub>O<sub>7</sub>I (JCPDS 40-0548), suggesting a high purity of the prepared Bi<sub>5</sub>O<sub>7</sub>I NTs. For comparison, Bi<sub>5</sub>O<sub>7</sub>I nanobelts (NBs) were obtained under the same conditions except that the pH was increased to 12.5.



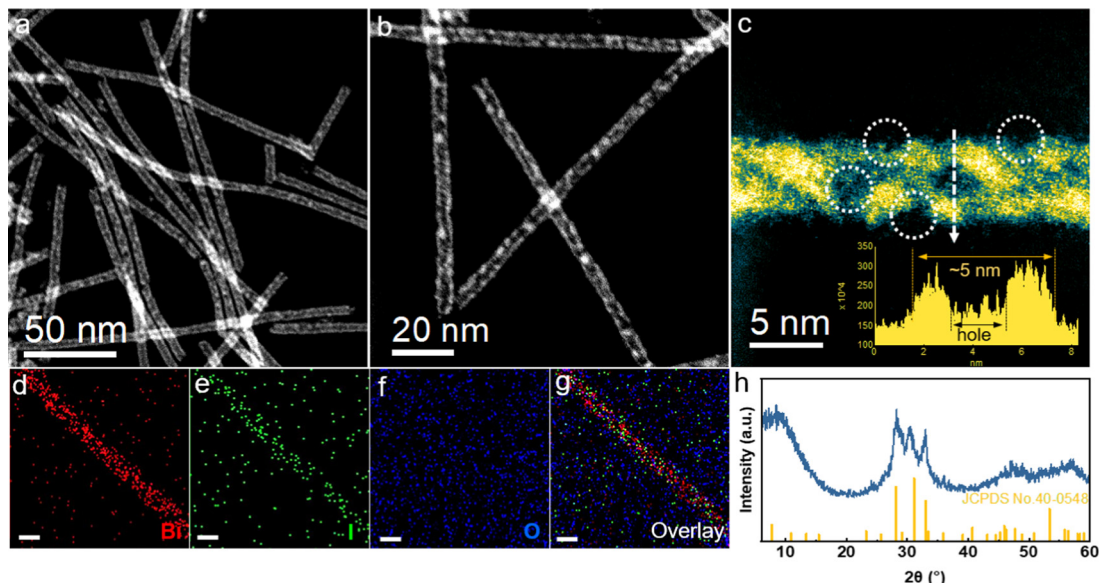


Fig. 1 Catalyst characterizations. (a–c) HADDF-STEM images of  $\text{Bi}_5\text{O}_7\text{I}$  NTs (inset is the line scan of the depth); (d–g) the corresponding EDS elemental mappings and overlay image of  $\text{Bi}_5\text{O}_7\text{I}$  NTs (scale bar: 5 nm); (h) XRD pattern of  $\text{Bi}_5\text{O}_7\text{I}$  NTs.

The scanning electron microscopy (SEM) and TEM images (Fig. S1, ESI<sup>†</sup>) clearly show the structure of belts with the width of around a micrometer, and the lattice fringe of 0.32 nm is assigned to the (312) plane of  $\text{Bi}_5\text{O}_7\text{I}$ , in agreement with the XRD result (Fig. S2, ESI<sup>†</sup>).

## 2.2 Electrocatalytic performance for the $\text{CO}_2\text{RR}$

The  $\text{CO}_2\text{RR}$  electrocatalytic activities of  $\text{Bi}_5\text{O}_7\text{I}$  NTs and NBs were first evaluated in an H-type cell containing 0.5 M  $\text{CO}_2$ -

saturated  $\text{KHCO}_3$  with all the potentials referred to the reversible hydrogen electrode (RHE) unless specified otherwise. Firstly, linear sweep voltammetry (LSV) curves were measured in Ar- and  $\text{CO}_2$ -saturated electrolytes, respectively, to evaluate the electrocatalytic activities toward the  $\text{CO}_2\text{RR}$ . As shown in Fig. 2a, the  $\text{Bi}_5\text{O}_7\text{I}$  NTs deliver a comparably higher total current density ( $j$ ) in  $\text{CO}_2$ -saturated electrolyte than that in Ar, implying the higher preference to the  $\text{CO}_2\text{RR}$ . A similar result is also obtained on  $\text{Bi}_5\text{O}_7\text{I}$  NBs, while the higher  $j$  and more positive

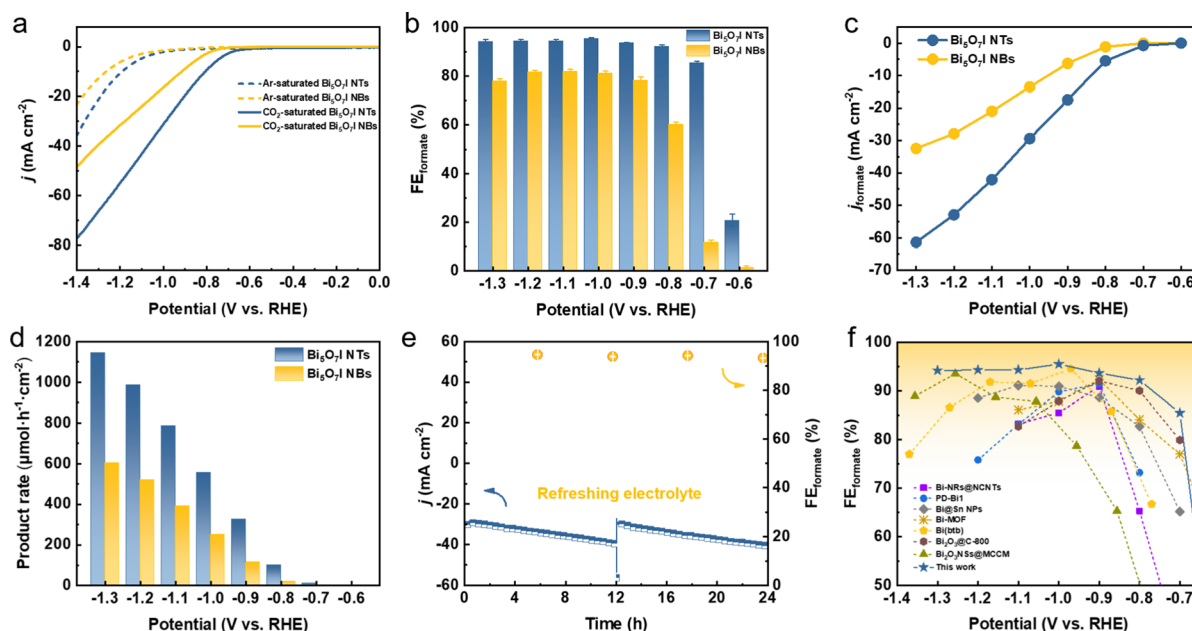


Fig. 2  $\text{CO}_2\text{RR}$  performance in a H-type cell. (a) LSV curves in 0.5 M  $\text{CO}_2$ - or Ar-saturated  $\text{KHCO}_3$  electrolyte, (b) FEs of formate, (c)  $j_{\text{formate}}$  and (d) formate formation rates of  $\text{Bi}_5\text{O}_7\text{I}$  NTs and NBs; (e) stability test of  $\text{Bi}_5\text{O}_7\text{I}$  NTs at  $-1.0$  V in 0.5 M  $\text{CO}_2$ -saturated  $\text{KHCO}_3$  electrolyte; (f) comparison of  $\text{FE}_{\text{formate}}$  of this work with recently reported Bi-based catalysts.



onset potential of the Bi<sub>5</sub>O<sub>7</sub>I NTs suggest their better electrocatalytic activity for CO<sub>2</sub> conversion. To exclude the preferential occurrence of the HER and identify the reduction products of the CO<sub>2</sub>RR, controlled electrolysis was carried out (Fig. S3, ESI†) at different potentials. The gas-phase products were detected by online gas chromatography (GC), and the liquid products were analyzed by ion chromatography (IC). The results show that formate is the dominating product, together with minor amounts of CO and H<sub>2</sub>. As displayed in Fig. 2b, the Bi<sub>5</sub>O<sub>7</sub>I NTs exhibit higher selectivity for formate formation and the FE<sub>formate</sub> maintains over 92% in a wide potential range from −0.8 to −1.3 V, whereas Bi<sub>5</sub>O<sub>7</sub>I NBs show the inferior selectivity with the maximum FE<sub>formate</sub> of about 80% under the same applied potentials. Specifically, the maximum FE<sub>formate</sub> of 95.5% is achieved at −1.0 V where the HER is significantly inhibited with the FE<sub>H<sub>2</sub></sub> of about 1%. Moreover, the FEs for the C<sub>1</sub> products (*i.e.*, formate and CO) are approaching near-unity within a wide potential gap of 500 mV (Fig. S4, ESI†), demonstrating the high preference to the CO<sub>2</sub>RR over the competing HER for Bi<sub>5</sub>O<sub>7</sub>I NTs.

To reveal the electrocatalytic activity for CO<sub>2</sub>RR to formate, the partial current densities of formate ( $j_{\text{formate}}$ ) were derived from the  $j$  and FE<sub>formate</sub>, as shown in Fig. 2c. Clearly, Bi<sub>5</sub>O<sub>7</sub>I NTs possess better electrocatalytic activity for CO<sub>2</sub>-to-formate conversion, where a  $j_{\text{formate}}$  of about 61 mA cm<sup>−2</sup> was reached at a moderate potential of −1.3 V, about two times higher than that of Bi<sub>5</sub>O<sub>7</sub>I NBs (32 mA cm<sup>−2</sup>). Fig. 2d shows the formate formation rate, in which Bi<sub>5</sub>O<sub>7</sub>I NTs exhibit a rate of 1145 μmol h<sup>−1</sup> cm<sup>−2</sup> at −1.3 V, comparably higher than Bi<sub>5</sub>O<sub>7</sub>I NBs (605 μmol h<sup>−1</sup> cm<sup>−2</sup>). Furthermore, a potentiostatic electrolysis measurement was conducted at −1.0 V on Bi<sub>5</sub>O<sub>7</sub>I NTs to evaluate the stability. As shown in Fig. 2e, the  $j$  shows a slight increment after electrolysis for 12 h, which is mainly attributed to the accumulation of products in electrolyte. The  $j$  could go back to the original value after refreshing the electrolyte, indicating the good stability of the electrocatalyst. It is worth noting that the average FE<sub>formate</sub> was maintained at about 92% over 24 h electrolysis, and this further confirms the remarkable durability of Bi<sub>5</sub>O<sub>7</sub>I NTs for formate formation. Further post-catalysis characterizations were performed to identify the structure and composition changes of the catalyst after the CO<sub>2</sub>RR. The Bi<sub>5</sub>O<sub>7</sub>I NTs are fully reduced to metallic Bi after electrolysis as confirmed by the XRD result (Fig. S5, ESI†). It is worth noting that the morphologies of the nanotubular structures with surface defects are well maintained under the reduction conditions, as shown in the TEM images (Fig. S6, ESI†). To better demonstrate the reduction of Bi<sub>5</sub>O<sub>7</sub>I NTs to defective metallic Bi NTs, an electrochemical activation measurement was conducted using fresh electrode at −1.0 V *vs.* RHE in 0.5 M CO<sub>2</sub>-saturated KHCO<sub>3</sub> for 10 min. The XRD results show that Bi<sub>5</sub>O<sub>7</sub>I NTs are already fully reduced to metallic Bi in 10 min (Fig. S7, ESI†). From the HRTEM images, some nanopores can be clearly identified on the nanotube walls. The Fourier transform pattern of the selected area belongs to the zone axis [001] where the lattice fringe of 0.23 nm is well indexed to the (110) facet of metallic Bi (Fig. S8, ESI†). The good structure durability of defective nanotubes

accounts for the negligible degradation of the electrocatalytic performance as well as the good stability. To the best of our knowledge, the electrocatalytic performance of Bi<sub>5</sub>O<sub>7</sub>I NTs outperforms the recently reported Bi-based electrocatalysts for the CO<sub>2</sub>RR toward formate (Fig. 2f and Table S1, ESI†).<sup>23,28,40–44</sup>

Given the reduction of Bi<sub>5</sub>O<sub>7</sub>I NTs to defective metallic Bi NTs during the CO<sub>2</sub>RR, the similar nanotubular Bi NTs without defects were further prepared to compare the CO<sub>2</sub>RR performance. As shown in Fig. S9 (ESI†), the high purity of metallic Bi is synthesized using the hydrothermal method. The nested Bi NTs can be clearly observed by SEM and TEM images and the lattice distance of 0.33 nm is well indexed to the (012) facet of metallic Bi (Fig. S10, ESI†). The EDS result further confirms the successful preparation of Bi NTs. The CO<sub>2</sub>RR measurement was conducted under the same conditions as Bi<sub>5</sub>O<sub>7</sub>I NTs and NBs. As shown in Fig. S11 (ESI†), the selectivity for formate formation is less than 90% in all measured potentials and the maximum FE<sub>formate</sub> of 86.6% is achieved at −1.3 V *vs.* RHE. In addition, the  $j_{\text{formate}}$  of Bi NTs is much lower compared to that of Bi<sub>5</sub>O<sub>7</sub>I NTs, demonstrating the inferior electrocatalytic activity for formate formation.

### 2.3 High-throughput CO<sub>2</sub>RR performance

It is suggested that the economically compelling application of the CO<sub>2</sub>RR toward formate formation requires a minimum  $j$  of 200 mA cm<sup>−2</sup> with the selectivity of 90% to promote the practical CO<sub>2</sub> electrolysis technology.<sup>32,45</sup> However, the low CO<sub>2</sub> gas solubility in aqueous media (~33 mM) strongly restricts the CO<sub>2</sub> mass transfer, which results in the limited  $j$ . To this end, the CO<sub>2</sub>RR performance of Bi<sub>5</sub>O<sub>7</sub>I NTs on a gas diffusion electrode (GDE) was evaluated in a flow cell with 1.0 M KOH (Fig. S12 and S13, ESI†). As shown in Fig. 3a, the onset potential of −0.3 V was reached in the flow cell, much more positive than −0.6 V in the H-type cell. Notably, the Bi<sub>5</sub>O<sub>7</sub>I NTs show a high  $j$  of 390 mA cm<sup>−2</sup> at −1.4 V that decreases to about 225 mA cm<sup>−2</sup> at −1.0 V, demonstrating the considerably high electrocatalytic activity for CO<sub>2</sub>RR. The shortened gas diffusion pathway on the GDE facilitates the greater access to CO<sub>2</sub>, resulting in better performance than in the H-type cell. In addition, the reduced ohmic resistance and charge transfer resistance (Fig. S14, ESI†) in the flow cell system further promote the enhanced CO<sub>2</sub>RR electrocatalytic performance. The potential controlled electrolysis measurements were also conducted, and the results of product analysis suggest that the FE<sub>formate</sub> exceeds 93% at all the applied potentials from −0.3 to −1.3 V with corresponding  $j_{\text{formate}}$  increasing from 4.0 to 296 mA cm<sup>−2</sup> (Fig. 3b). Meanwhile, the Bi<sub>5</sub>O<sub>7</sub>I NTs also exhibit a good stability with a high  $j$  of over 200 mA cm<sup>−2</sup> and an average FE<sub>formate</sub> of about 94% in the flow cell system for 7 h, as shown in Fig. 3c. The high FE<sub>formate</sub> and  $j$  of Bi<sub>5</sub>O<sub>7</sub>I NTs in a wide potential window make it stand out from the recently reported electrocatalysts for formate production in flow cell systems (Table S2, ESI†).

To evaluate the feasibility of the actual application of Bi<sub>5</sub>O<sub>7</sub>I NTs in the CO<sub>2</sub>RR process, a custom-built two-electrode membrane electrode assembly (MEA) system was used to



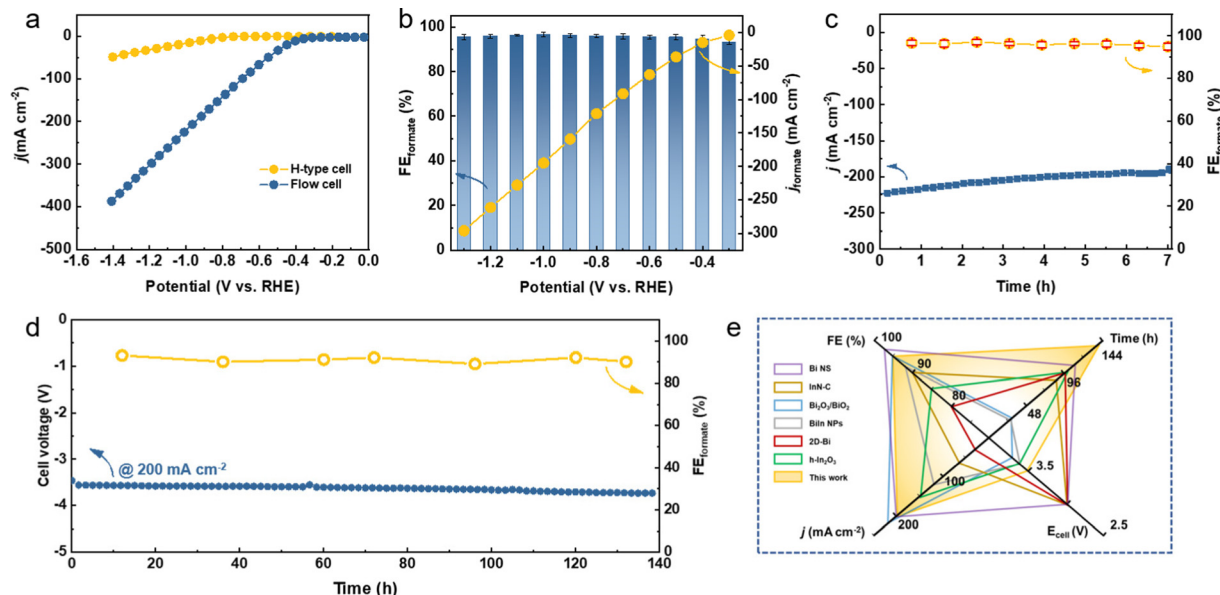


Fig. 3 High-throughput  $\text{CO}_2\text{RR}$  performance. (a) LSV curves of  $\text{Bi}_5\text{O}_7\text{I}$  NTs in the H-type cell and flow cell, (b)  $\text{FE}_{\text{formate}}$  and  $j_{\text{formate}}$  of  $\text{Bi}_5\text{O}_7\text{I}$  NTs at all potentials in the flow cell, (c) stability test of  $\text{Bi}_5\text{O}_7\text{I}$  NTs at  $-1.0$  V vs. RHE in the flow cell, (d) the  $\text{CO}_2\text{RR}$  performance of  $\text{Bi}_5\text{O}_7\text{I}$  NTs at  $200$   $\text{mA cm}^{-2}$  in the MEA system, and (e) comparison of the  $\text{FE}_{\text{formate}}$ ,  $j$ ,  $E_{\text{cell}}$  and stability of recently reported electrocatalysts for the  $\text{CO}_2\text{RR}$  to formate in the MEA system.

perform the stability test (Fig. S15, ESI†). As shown in Fig. 3d, the electrolysis can be stably operated at  $200$   $\text{mA cm}^{-2}$  for  $140$  h with negligible fluctuation of cell voltage, suggesting the good

stability of the electrocatalyst under the MEA working conditions. Moreover, the  $\text{FE}_{\text{formate}}$  was maintained over  $90\%$  in the period of  $140$  h, demonstrating the superb  $\text{CO}_2\text{RR}$  performance

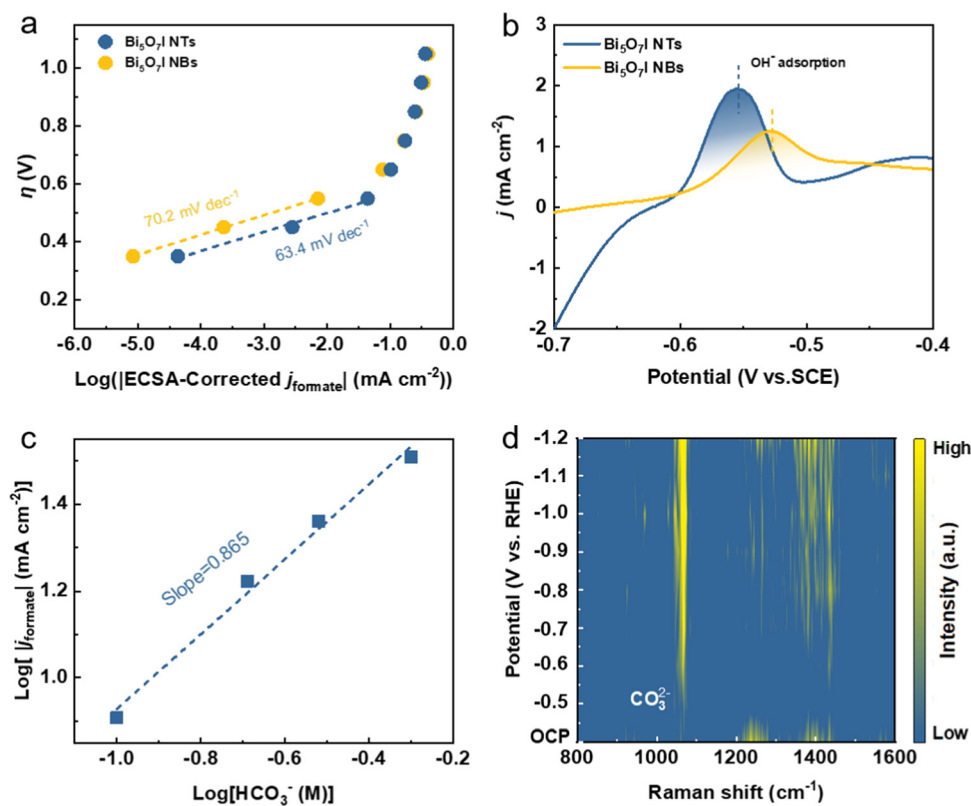


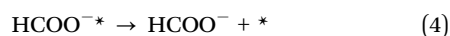
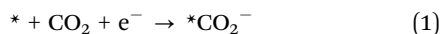
Fig. 4 Kinetic and mechanistic studies. (a) ECSA-corrected Tafel plots for formate production, (b) oxidative LSV curves in  $\text{N}_2$ -saturated  $0.1$  M  $\text{KOH}$ , (c)  $j_{\text{formate}}$  of  $\text{Bi}_5\text{O}_7\text{I}$  NTs in different concentrations of  $\text{HCO}_3^-$  at  $-1.0$  V vs. RHE, and (d) potential-dependent Raman spectra on  $\text{Bi}_5\text{O}_7\text{I}$  NTs in  $0.5$  M  $\text{CO}_2$ -saturated  $\text{KHCO}_3$ .



of Bi<sub>5</sub>O<sub>7</sub>I NTs. Such results make it outperform many recently reported electrocatalysts for CO<sub>2</sub> to formate conversion in MEA systems (Fig. 3e and Table S3, ESI†). Conclusively, the Bi<sub>5</sub>O<sub>7</sub>I NTs possess strengthened electrocatalytic activity, selectivity and durability for CO<sub>2</sub>-to-formate conversion in both the flow cell and MEA systems, thereby demonstrating the promising future for their practical applications in the field of CO<sub>2</sub>RR technology.

#### 2.4 Reaction kinetics and mechanistic studies for CO<sub>2</sub>RR to formate

To investigate the reaction kinetics for CO<sub>2</sub>RR to formate formation, Tafel plots were derived based on static state *j* and FE<sub>formate</sub> (Fig. 4a). Compared with Bi<sub>5</sub>O<sub>7</sub>I NBs (70.2 mV dec<sup>-1</sup>), its smaller Tafel slope of 63.4 mV dec<sup>-1</sup> indicates the faster reaction kinetics process and better stabilization for the \*CO<sub>2</sub><sup>-</sup> intermediate on Bi<sub>5</sub>O<sub>7</sub>I NTs, which ensures the improved CO<sub>2</sub>RR performance. It is generally recognized that the rate-determining step (RDS) of formate formation could be identified by matching the theoretical Tafel slopes and experimentally derived values.<sup>46–48</sup> The theoretical Tafel slope of 118 mV dec<sup>-1</sup> suggests the RDS of the initial electron transfer to the adsorbed CO<sub>2</sub>, *i.e.*, \* + CO<sub>2</sub> + e<sup>-</sup> → \*CO<sub>2</sub><sup>-</sup>, where (\*) corresponds to the active site for adsorption species, while the value of 59 mV dec<sup>-1</sup> corresponds to the RDS of proton (H<sup>+</sup>) transfer served by bicarbonate (HCO<sub>3</sub><sup>-</sup>), *i.e.*, \*CO<sub>2</sub><sup>-</sup> + HCO<sub>3</sub><sup>-</sup> → OCHO\* + CO<sub>3</sub><sup>2-</sup>. It is worth noting that the RDS for the CO<sub>2</sub>RR toward formate formation is identical for Bi<sub>5</sub>O<sub>7</sub>I NTs and NBs, where the Tafel slopes are close to the theoretical value of 59 mV dec<sup>-1</sup>. Therefore, the electroreduction of CO<sub>2</sub> to formate on Bi<sub>5</sub>O<sub>7</sub>I follows the steps below.<sup>11</sup>



It is also noted that the initial electron transfer step to form the intermediate \*CO<sub>2</sub><sup>-</sup>, *i.e.*, eqn (1), plays a fundamental role for the CO<sub>2</sub>RR toward formate. The better stabilization ability of \*CO<sub>2</sub><sup>-</sup> could facilitate the faster reaction process and improve the selectivity for CO<sub>2</sub> conversion. To evaluate the binding affinity of \*CO<sub>2</sub><sup>-</sup> on the catalyst surface, the oxidative LSV measurements were conducted in N<sub>2</sub>-saturated 0.1 M KOH electrolyte where the OH<sup>-</sup> is considered as the surrogate for \*CO<sub>2</sub><sup>-</sup>. As shown in Fig. 4b, the Bi<sub>5</sub>O<sub>7</sub>I NTs exhibit a higher peak intensity at more negative potential compared to Bi<sub>5</sub>O<sub>7</sub>I NBs, an indication of the better adsorption and stabilization capability for the \*CO<sub>2</sub><sup>-</sup> intermediate and thus, the enhanced CO<sub>2</sub>RR performance. The reaction step (2) is further supported by the constant electrolysis performed at -1.0 V *vs.* RHE with different concentrations of KHCO<sub>3</sub> electrolyte ranging from 0.1 to 0.5 M (Fig. S16, ESI†). The *j* increases with increasing [HCO<sub>3</sub><sup>-</sup>] so that the *j* of 32.1 mA cm<sup>-2</sup> in 0.5 M KHCO<sub>3</sub> is about four times higher than that of 8.2 mA cm<sup>-2</sup> in 0.1 M KHCO<sub>3</sub>.

The reaction order with respect to HCO<sub>3</sub><sup>-</sup> concentration was derived, as displayed in Fig. 4c. It is found that the log *j*<sub>formate</sub> shows nearly linear increase with log[HCO<sub>3</sub><sup>-</sup>] and the slope of 0.865 suggests the first-order relation to [HCO<sub>3</sub><sup>-</sup>], in agreement with the result of Tafel slope that HCO<sub>3</sub><sup>-</sup> serves as the proton donor as the RDS.

The reaction mechanism for the CO<sub>2</sub>RR to formate formation was further validated by the *in situ* electrochemical Raman spectroscopy measurement (Fig. S17, ESI†). Fig. 4d shows the Raman spectra on Bi<sub>5</sub>O<sub>7</sub>I NTs at different applied potentials in 0.5 M CO<sub>2</sub>-saturated KHCO<sub>3</sub> electrolyte, in which two obvious peaks are observed at the applied negative potentials. As stated before, the initial electron transfer to form \*CO<sub>2</sub><sup>-</sup> is the first reaction step during the CO<sub>2</sub>RR. The Raman peaks at 450 to 550 cm<sup>-1</sup> (Fig. S17c, ESI†) start to appear when the applied potential reaches -0.6 V *vs.* RHE, which are assigned to the peak of carboxylate δ(CO<sub>2</sub><sup>-</sup>).<sup>49</sup> The increased peak intensity suggests the first stage of reaction (1) during the CO<sub>2</sub>RR. Moreover, the peak located at about 1065 cm<sup>-1</sup> is ascribed to the symmetric C–O stretching vibration ν<sub>1</sub>(CO<sub>3</sub><sup>2-</sup>),<sup>50</sup> and the surface weakly adsorbed monodentate carbonate η<sup>1</sup>-CO<sub>3</sub><sup>2-</sup> (Fig. S17d, ESI†). It is noted that the peak intensity gradually increases as the applied potential shifts to a more negative range, while no peak is observed when the applied potential is lower than -0.6 V *vs.* RHE. This demonstrates the occurrence of reaction step (2) during the CO<sub>2</sub>RR when the intermediate is formed and accompanied by the production of carbonate ions. Notably, the peaks of δ(CO<sub>2</sub><sup>-</sup>) and ν<sub>1</sub>(CO<sub>3</sub><sup>2-</sup>) disappear when the applied potential is stopped, further proving that the carbonate intermediate comes from the reaction process (Fig. S18, ESI†). All these results provide solid evidence to confirm the reaction mechanism on Bi<sub>5</sub>O<sub>7</sub>I NTs for the electroreduction of CO<sub>2</sub> to formate.

Density functional theory (DFT) calculations were performed to deepen our understanding on the origins of the enhanced catalytic activity and selectivity toward the CO<sub>2</sub>RR. Given the full reduction of Bi<sub>5</sub>O<sub>7</sub>I NTs to defective metallic Bi NTs during the CO<sub>2</sub>RR, the three models of perfect Bi and Bi with different defects were investigated (Bi-V<sub>1</sub> means Bi surface with a mono vacancy and V<sub>2</sub> means di-vacancy). As depicted in Fig. 5a, the charge density difference between Bi and the adsorbate \*OCHO on perfect Bi shows relatively low interaction compared to those on Bi-V<sub>1</sub> and Bi-V<sub>2</sub>. The apparent charge transfer between Bi and O atoms on defective Bi demonstrates the stronger interaction of the adsorbate on the Bi surface, which is beneficial for the formation of the \*OCHO intermediate. Given the structure difference of Bi, the electronic local functions were further studied (Fig. 5b). The local charge distribution of adjacent Bi atoms can be clearly observed with the existence of defects, which is attributed to the increased orbital overlap caused by the shortened bond length between two adjacent atoms (Fig. S19, ESI†), thus resulting in electron delocalization. The p orbital delocalization of the Bi atoms leads to orbital hybridization between the Bi atoms and the adsorbed \*OCHO. The more delocalized electrons near the Bi atom with vacancies can effectively promote the formation of the intermediate \*OCHO



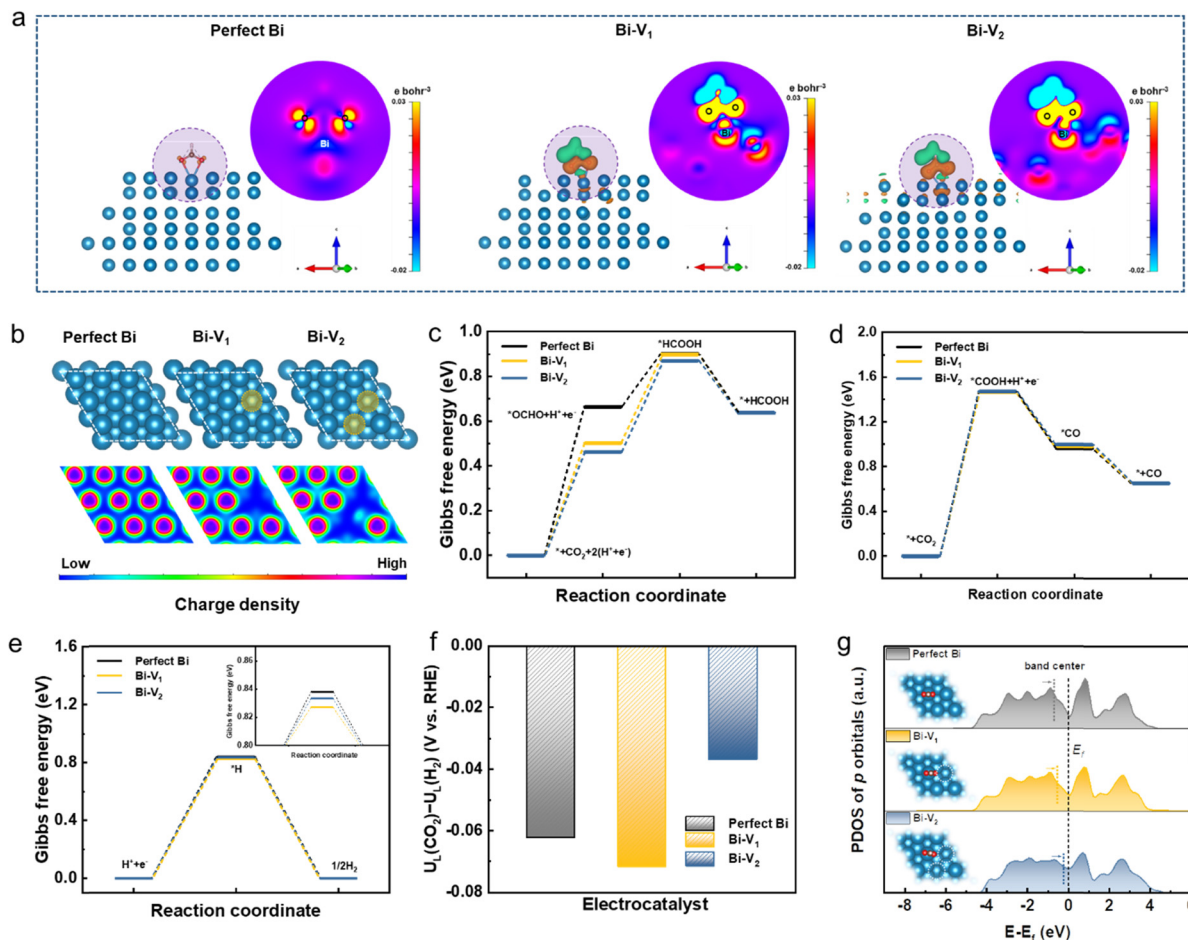


Fig. 5 DFT calculation results. (a) The electron density difference with  $^*\text{OCHO}$  adsorbates (2D view generated from the plane derived by Bi–O–O atoms), (b) electron local functions, Gibbs free energy of the  $\text{CO}_2\text{RR}$  to (c)  $\text{HCOOH}$  pathway and (d)  $\text{CO}$  pathway, (e) Gibbs free energy of HER, (f) difference in limiting potentials for the  $\text{CO}_2\text{RR}$  and HER, and (g) the Bi p-PDOS with  $^*\text{OCHO}$  adsorbates of perfect Bi, Bi- $\text{V}_1$  and Bi- $\text{V}_2$ .

by donating electrons to the reaction, enhancing the interaction between  $^*\text{OCHO}$  as evidenced by the electron density difference. In addition, the adsorbed intermediate  $^*\text{OCHO}$  shift to the electron delocalized region on Bi atoms, as shown in Fig. S20 (ESI $^\dagger$ ), further confirming the favorable formation of intermediates over the electron delocalized region.

Furthermore, the Gibbs free energies for  $\text{CO}_2$  to  $\text{HCOOH}$  formation were calculated over the optimized structures shown in Fig. 5c and Fig. S21 (ESI $^\dagger$ ). The formation energy of intermediate  $^*\text{OCHO}$  decreases from 0.66 to 0.46 eV when introducing a di-vacancy on the Bi, suggesting the lower energy barrier compared to the perfect Bi. The stronger charge interaction between Bi and O atoms and higher local charge distribution near Bi atoms synergistically contribute to better adsorption ability of  $^*\text{OCHO}$ , leading to the decreased energy barrier in the rate determining step. In addition, the Gibbs free energies for  $\text{CO}_2$  to  $\text{CO}$  formation were also calculated (Fig. 5d and Fig. S22, ESI $^\dagger$ ). It can be found that the rate determining step is the formation of intermediate  $^*\text{COOH}$  on perfect Bi and defective Bi where no obvious energy difference is observed. The high energy barrier of about 1.47 eV for  $^*\text{COOH}$  formation is significantly higher than that for  $^*\text{OCHO}$  formation, leading

to the unfavorable  $\text{CO}$  formation. Given the competing reaction of the HER during the  $\text{CO}_2\text{RR}$ , the DFT calculation was further conducted on the HER, as shown in Fig. 5e and Fig. S23 (ESI $^\dagger$ ). When introducing defects on the Bi structure, the Gibbs free energies of the formed  $^*\text{H}$  display less difference compared to that of perfect Bi. The energy barrier of over 0.8 eV on  $^*\text{H}$  formation is higher than the rate determining step of  $^*\text{OCHO}$  formation, indicating the suppression of the HER during the  $\text{CO}_2\text{RR}$ . Furthermore, the limiting potential difference ( $\Delta U_L$ ) between the  $\text{CO}_2\text{RR}$  and HER was also determined to reveal the selectivity toward the  $\text{CO}_2\text{RR}$ . As depicted in Fig. 5f, Bi- $\text{V}_2$  has a more positive potential value ( $-0.036$  V) than perfect Bi ( $-0.062$  V) and Bi- $\text{V}_1$  ( $-0.072$  V), demonstrating the higher selectivity for  $\text{CO}_2$  to formate conversion. The projected density of states (PDOS) for Bi p orbitals with adsorbed  $^*\text{OHCO}$  were plotted where the band center shifts upwards to the Fermi level with increased vacancies, indicating the stronger interaction between  $^*\text{OCHO}$  and Bi that facilitates the  $\text{HCOOH}$  formation that also accounts for the high selectivity for  $\text{CO}_2$ -to-formate conversion (Fig. 5g). Thus, the vacancies present on Bi can effectively modulate the electronic structure and lower the energy barrier, leading to the superior catalytic performance for the  $\text{CO}_2\text{RR}$ .



## 2.5 Structural merits of Bi<sub>5</sub>O<sub>7</sub>I nanotubes towards the enhanced CO<sub>2</sub>RR performance

To uncover the merits of the defective nanotubular structure, the electrochemical double-layer capacitance ( $C_{dl}$ ) was measured (Fig. S24, ESI<sup>†</sup>) to determine the electrochemically active surface area (ECSA). As shown in Fig. S25a (ESI<sup>†</sup>), the ultrathin Bi<sub>5</sub>O<sub>7</sub>I NTs possess a higher  $C_{dl}$  (6.81 mF cm<sup>-2</sup>) than Bi<sub>5</sub>O<sub>7</sub>I NBs (3.26 mF cm<sup>-2</sup>), suggesting that the defective nanotubular structure offers a substantial number of active sites and thereby improves the electrocatalytic activity for the CO<sub>2</sub>RR. Moreover, the previous study<sup>51–53</sup> also manifests the benefits of the ultrathin nanostructure for CO<sub>2</sub>RR performance. The thinner thickness of the electrocatalyst provides higher surface area and more active sites. Compared to the nanobelt structure, the ultrathin nanotube structure of Bi<sub>5</sub>O<sub>7</sub>I endows it with larger surface area and more exposed electrocatalytic active sites for the CO<sub>2</sub>RR to proceed, which improves both the electrocatalytic activity and selectivity for the conversion of CO<sub>2</sub> to formate. To exclude the effect of morphology on the CO<sub>2</sub>RR performance, the  $j_{formate}$  was further normalized by the ECSA. As shown in Fig. S25b (ESI<sup>†</sup>), the Bi<sub>5</sub>O<sub>7</sub>I NTs still deliver a higher  $j_{formate}$  compared to Bi<sub>5</sub>O<sub>7</sub>I NBs, suggesting the higher intrinsic electrocatalytic activity of the Bi<sub>5</sub>O<sub>7</sub>I NTs for the CO<sub>2</sub>RR to formate conversion. In addition, the electrochemical impedance spectroscopy (EIS) measurement was conducted to evaluate the charge transfer process between the electrocatalyst and electrolyte. Apparently, the Bi<sub>5</sub>O<sub>7</sub>I NTs show comparably smaller interfacial charge transfer resistance compared to NBs (Fig. S26, ESI<sup>†</sup>), indicating a better charge transfer ability to facilitate the occurrence of the CO<sub>2</sub>RR. As stated before, the defective nanotubular structure is conducive to gas adsorption, and volumetric CO<sub>2</sub> adsorption isotherms prove the superb CO<sub>2</sub> capture ability of Bi<sub>5</sub>O<sub>7</sub>I NTs that is three times

higher than that of Bi<sub>5</sub>O<sub>7</sub>I NBs (Fig. 6a). The enhanced CO<sub>2</sub> adsorption capability originates from the abundant nanopores on the ultrathin nanotube wall. This ensures the good mass transfer in aqueous media and benefits the reaction processes on the active sites and consequently, promotes the electrocatalytic performance for formate formation. Aside from the observed nanopores, the result of electron paramagnetic resonance (EPR) measurement displays an obvious signal peak at  $g = 2.001$ , which is ascribed to the oxygen vacancies in Bi<sub>5</sub>O<sub>7</sub>I NTs (Fig. 6b). Previous results have demonstrated that the spare electrons at the defect sites of oxygen vacancies could serve as the electron donor to ease the activation of electron-deficient CO<sub>2</sub> molecules, which is beneficial for the CO<sub>2</sub> activation to form the \*CO<sub>2</sub><sup>-</sup>.<sup>38,39,54</sup> This also accounts for the improved electrocatalytic activity over Bi<sub>5</sub>O<sub>7</sub>I NTs for CO<sub>2</sub>-to-formate conversion.

Since the CO<sub>2</sub>RR is a proton-coupled electron transfer (PCET) process and the complicated multi-electron transfer steps occur on the catalyst surface, it is important to take the charge transfer ability into consideration to achieve higher activity and selectivity. Work function (WF) is regarded as an effective indicator to describe the electron transfer ability over the catalyst surface. A lower WF corresponds to a higher tunneling probability of electrons, *i.e.*, the electrons are easier to transfer from the catalyst to the reactant and participate in the subsequent reactions of the CO<sub>2</sub>RR.<sup>55,56</sup> It can be inferred that the unique channel structure of the nanotubes with abundant nanopores and oxygen vacancies can serve as the charge transport pathway to ensure the faster electron transfer on the catalyst. To this end, the WFs of Bi<sub>5</sub>O<sub>7</sub>I NTs and NBs were measured by ultraviolet photoelectron spectroscopy (UPS) as shown in Fig. 6c. Apparently, the defective Bi<sub>5</sub>O<sub>7</sub>I NTs possess a lower WF of about 4.75 eV compared to NBs (*i.e.*,

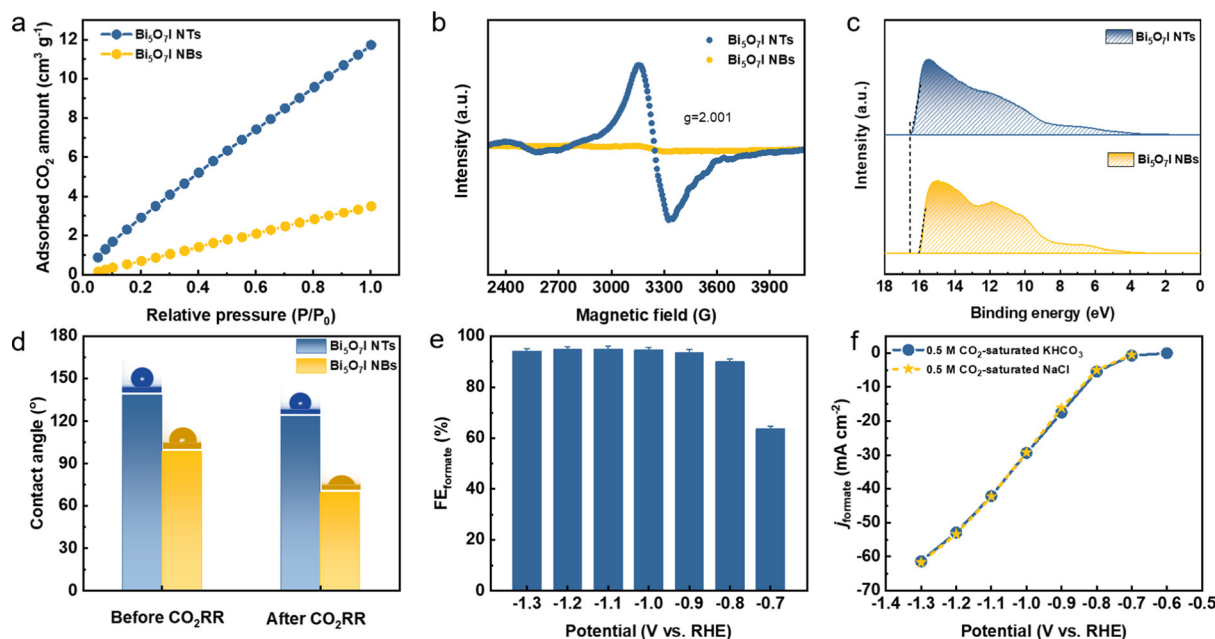


Fig. 6 (a) CO<sub>2</sub> adsorption isotherms, (b) EPR spectra, (c) UPS spectra and (d) contact angle measurements before and after the CO<sub>2</sub>RR on Bi<sub>5</sub>O<sub>7</sub>I NTs and NBs, (e) FE<sub>formate</sub> and (f)  $j_{formate}$  of Bi<sub>5</sub>O<sub>7</sub>I NTs in CO<sub>2</sub>-saturated 0.5 M NaCl.





5.25 eV), demonstrating the enhanced electron transfer ability (Fig. S27, ESI†). The fast electron transfer on the catalyst surface facilitates the quick pre-equilibrium of  $\text{CO}_2$  to  $^*\text{CO}_2^-$ , thereby ensuring the formate formation from the highly selective  $\text{CO}_2\text{RR}$ .

It is widely accepted that the  $\text{CO}_2\text{RR}$  is a gas involved reaction and takes place at the triple-phase boundaries. The wettability of the catalyst plays an indispensable role in the reaction process and can consequently tune the product selectivity. Previous studies have suggested that the hydrophobic interface is favorable for formate formation owing to the limited supply of protons to participate in the competitive HER.<sup>57–59</sup> In light of the substantial amount of nanopores on the defective  $\text{Bi}_5\text{O}_7\text{-I}$  NTs, the hydrophobicity is expected across the catalyst surface. Thus, the influence of wettability on  $\text{CO}_2\text{RR}$  performance was further studied (Fig. S28, ESI†). As shown in Fig. 6d, the defective  $\text{Bi}_5\text{O}_7\text{-I}$  NTs present a hydrophobic surface with the contact angle of  $138.4^\circ$ , while a lower hydrophobicity is observed on NBs. After  $\text{CO}_2\text{RR}$  measurement, the defective nanotubular structure still maintains the hydrophobicity with a slight decrement of the contact angle to  $123.5^\circ$ . Nevertheless, the surface of  $\text{Bi}_5\text{O}_7\text{-I}$  NBs turns out to be hydrophilic with an obvious change of contact angle (Fig. S28d, ESI†). The hydrophobic  $\text{Bi}_5\text{O}_7\text{-I}$  NTs can effectively limit the proton supply to suppress the HER, which is consistent with the product distribution result. Concurrently, the enhanced  $\text{CO}_2$  adsorption capability can promote sufficient proton donors of  $\text{HCO}_3^-$  to enhance the proton-depleted formate formation, thus improving the selectivity of the  $\text{CO}_2\text{RR}$ . Moreover, the parasitic HER during the  $\text{CO}_2\text{RR}$  process usually deteriorates the reaction selectivity toward the target product. The research results suggest that the higher local pH near the electrode surface can change the concentrations of proton-donating species and effectively suppress the HER during the  $\text{CO}_2\text{RR}$ .<sup>36,60,61</sup> It is speculated that a higher local pH could be achieved on the catalyst surface considering the superior hydrophobicity of the  $\text{Bi}_5\text{O}_7\text{-I}$  NTs. To better observe the local pH effect, the phenolphthalein color transition experiment was performed on the prepared catalysts (Fig. S29, ESI†). It is found that the defective  $\text{Bi}_5\text{O}_7\text{-I}$  NTs show more significant color change to pink in comparison to the NBs, demonstrating the higher local pH around its surface. This higher pH can lead to a local conversion of  $\text{CO}_2$  to  $\text{HCO}_3^-$ , *i.e.*,  $\text{CO}_2 + \text{OH}^- \rightarrow \text{HCO}_3^-$ , which facilitates the reaction process by providing more proton-donating species and simultaneously suppressing the HER. Based on the above-mentioned, the defective nanotubular structure of  $\text{Bi}_5\text{O}_7\text{-I}$  demonstrates the advantages of creating massive uncoordinated active sites, ensuring the  $\text{CO}_2$  adsorption capability and improving the charge transfer capability. Concurrently, the hydrophobic surface with a higher local pH effectively inhibits the HER, thus achieving the selective formation of formate.

## 2.6 $\text{CO}_2\text{RR}$ performance in a simulated seawater-based system

It has been shown that most  $\text{CO}_2\text{RR}$  performance is measured in bicarbonate electrolyte, typically potassium or sodium bicarbonate. To some extent, using low-carbon electrolyte is a promising

approach to reducing the carbon source for the  $\text{CO}_2\text{RR}$ . Natural seawater is considered as an alternative to substitute the bicarbonate-based electrolyte owing to its abundance and negligible cost.<sup>62,63</sup> The chlorine evolution reaction at the anode can simultaneously produce higher-value products rather than oxygen gas when directly using seawater as the electrolyte for the  $\text{CO}_2\text{RR}$ . The  $\text{CO}_2\text{RR}$  performance of defective  $\text{Bi}_5\text{O}_7\text{-I}$  NTs was further evaluated in a 0.5 M NaCl solution that mimics seawater (Fig. S30, ESI†). Remarkably, the high  $\text{FE}_{\text{formate}}$  is achieved over a wide potential range with a maximum value of 95% that is comparable to the result by using  $\text{KHCO}_3$  electrolyte (Fig. 6e). Furthermore, the derived  $j_{\text{formate}}$  shows a similar value compared to the measurement in bicarbonate solution, implying the good intrinsic electrocatalytic activity of the  $\text{Bi}_5\text{O}_7\text{-I}$  NTs toward formate formation (Fig. 6f) in a 0.5 M NaCl solution. Therefore, the highly active and selective  $\text{Bi}_5\text{O}_7\text{-I}$  NTs also demonstrate promising prospects for  $\text{CO}_2\text{RR}$  applications in future seawater-based electrolysis systems.

## 3. Conclusions

Ultrathin  $\text{Bi}_5\text{O}_7\text{-I}$  NTs with abundant nanopores and oxygen vacancies are successfully synthesized and exhibit excellent electrocatalytic performance for the  $\text{CO}_2\text{RR}$  toward formate with good selectivity and stability, which is further improved in the flow cell and MEA systems by overcoming the limitation of  $\text{CO}_2$  mass transport in aqueous media. The high selectivity and current density of formate over a wide potential window, as well as the good stability, make this electrocatalyst a possible candidate for  $\text{CO}_2\text{RR}$  applications at an industrial scale. The experimental results prove that the nanopores and oxygen vacancies can serve as massive uncoordinated active sites and facilitate the adsorption of  $\text{CO}_2$ , which promotes the charge transfer and stabilizes the reaction intermediates toward the  $\text{CO}_2\text{RR}$ . Theoretical calculations unveil that the existence of defects can effectively modulate the electronic structure, thus benefiting the formation of intermediate  $^*\text{OHCO}$  toward  $\text{HCOOH}$ . Furthermore, the hydrophobic catalyst surface with higher local pH effectively suppresses the HER and results in the very efficient performance of the  $\text{CO}_2\text{RR}$ . These findings highlight the importance of structure and defect engineering as an attractive strategy for designing advanced electrocatalysts for achieving carbon-neutral sustainability.

## Conflicts of interest

The authors declare no conflicts of interest.

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## References

- G. Wang, J. Chen, Y. Ding, P. Cai, L. Yi, Y. Li, C. Tu, Y. Hou, Z. Wen and L. Dai, *Chem. Soc. Rev.*, 2021, **50**, 4993–5061.
- C. Xu, J. Hong, P. Sui, M. Zhu, Y. Zhang and J.-L. Luo, *Cell Rep. Phys. Sci.*, 2020, **1**, 100101.
- P. De Luna, C. Hahn, D. Higgins, S. A. Jaffer, T. F. Jaramillo and E. H. Sargent, *Science*, 2019, **364**, eaav3506.
- R. Francke, B. Schille and M. Roemelt, *Chem. Rev.*, 2018, **118**, 4631–4701.
- C. Costentin, M. Robert and J. M. Saveant, *Chem. Soc. Rev.*, 2013, **42**, 2423–2436.
- J. Qiao, Y. Liu, F. Hong and J. Zhang, *Chem. Soc. Rev.*, 2014, **43**, 631–675.
- S. Liu, H. Tao, L. Zeng, Q. Liu, Z. Xu, Q. Liu and J. L. Luo, *J. Am. Chem. Soc.*, 2017, **139**, 2160–2163.
- P.-F. Sui, S. Liu, C. Xu, J. Xiao, N. Duan, R. Feng and J.-L. Luo, *Chem. Eng. J.*, 2022, **427**, 131654.
- T. Burdyny and W. A. Smith, *Energy Environ. Sci.*, 2019, **12**, 1442–1453.
- Y. Y. Birdja, E. Pérez-Gallent, M. C. Figueiredo, A. J. Göttle, F. Calle-Vallejo and M. T. M. Koper, *Nat. Energy*, 2019, **4**, 732–745.
- N. Han, P. Ding, L. He, Y. Li and Y. Li, *Adv. Energy Mater.*, 2019, 1902338.
- M. F. Phillips, G.-J. M. Gruter, M. T. M. Koper and K. J. P. Schouten, *ACS Sustainable Chem. Eng.*, 2020, **8**, 15430–15444.
- T. Gunji, H. Ochiai, T. Ohira, Y. Liu, Y. Nakajima and F. Matsumoto, *Chem. Mater.*, 2020, **32**, 6855–6863.
- N. Han, M. Sun, Y. Zhou, J. Xu, C. Cheng, R. Zhou, L. Zhang, J. Luo, B. Huang and Y. Li, *Adv. Mater.*, 2021, **33**, 2005821.
- Z. Chen, T. Fan, Y.-Q. Zhang, J. Xiao, M. Gao, N. Duan, J. Zhang, J. Li, Q. Liu, X. Yi and J.-L. Luo, *Appl. Catal., B*, 2020, **261**, 118243.
- S. Liu, J. Xiao, X. F. Lu, J. Wang, X. Wang and X. W. D. Lou, *Angew. Chem., Int. Ed.*, 2019, **58**, 8499–8503.
- Y. Huang, X. Mao, G. Yuan, D. Zhang, B. Pan, J. Deng, Y. Shi, N. Han, C. Li, L. Zhang, L. Wang, L. He, Y. Li and Y. Li, *Angew. Chem., Int. Ed.*, 2021, **60**, 15844–15848.
- W. Guo, X. Tan, J. Bi, L. Xu, D. Yang, C. Chen, Q. Zhu, J. Ma, A. Tayal, J. Ma, Y. Huang, X. Sun, S. Liu and B. Han, *J. Am. Chem. Soc.*, 2021, **143**, 6877–6885.
- M. J. W. Blom, V. Smulders, W. P. M. van Swaaij, S. R. A. Kersten and G. Mul, *Appl. Catal., B*, 2020, **268**, 118420.
- C. H. Lee and M. W. Kanan, *ACS Catal.*, 2014, **5**, 465–469.
- P. Deng, H. Wang, R. Qi, J. Zhu, S. Chen, F. Yang, L. Zhou, K. Qi, H. Liu and B. Y. Xia, *ACS Catal.*, 2019, **10**, 743–750.
- C. W. Lee, J. S. Hong, K. D. Yang, K. Jin, J. H. Lee, H.-Y. Ahn, H. Seo, N.-E. Sung and K. T. Nam, *ACS Catal.*, 2018, **8**, 931–937.
- S. Liu, X. F. Lu, J. Xiao, X. Wang and X. W. D. Lou, *Angew. Chem., Int. Ed.*, 2019, **58**, 13828–13833.
- P. F. Sui, C. Xu, M. N. Zhu, S. Liu, Q. Liu and J. L. Luo, *Small*, 2021, e2105682.
- Y. Qiu, J. Du, W. Dong, C. Dai and C. Tao, *J. CO<sub>2</sub> Util.*, 2017, **20**, 328–335.
- J. H. Koh, D. H. Won, T. Eom, N.-K. Kim, K. D. Jung, H. Kim, Y. J. Hwang and B. K. Min, *ACS Catal.*, 2017, **7**, 5071–5077.
- F. P. Garcia de Arquer, O. S. Bushuyev, P. De Luna, C. T. Dinh, A. Seifitokaldani, M. I. Saidaminov, C. S. Tan, L. N. Quan, A. Proppe, M. G. Kibria, S. O. Kelley, D. Sinton and E. H. Sargent, *Adv. Mater.*, 2018, **30**, e1802858.
- Y. Wang, Y. Li, J. Liu, C. Dong, C. Xiao, L. Cheng, H. Jiang, H. Jiang and C. Li, *Angew. Chem., Int. Ed.*, 2021, **60**, 7681–7685.
- J. Yang, X. Wang, Y. Qu, X. Wang, H. Huo, Q. Fan, J. Wang, L. M. Yang and Y. Wu, *Adv. Energy Mater.*, 2020, **10**, 2001709.
- W. Ma, J. Bu, Z. Liu, C. Yan, Y. Yao, N. Chang, H. Zhang, T. Wang and J. Zhang, *Adv. Funct. Mater.*, 2020, 2006704.
- Y. Cheng, P. Hou, X. Wang and P. Kang, *Acc. Chem. Res.*, 2022, **55**, 231–240.
- R. I. Masel, Z. Liu, H. Yang, J. J. Kaczur, D. Carrillo, S. Ren, D. Salvatore and C. P. Berlinguette, *Nat. Nanotechnol.*, 2021, **16**, 118–128.
- Y. Guan, M. Liu, X. Rao, Y. Liu and J. Zhang, *J. Mater. Chem. A*, 2021, **9**, 13770–13803.
- A. Guan, C. Yang, Y. Quan, H. Shen, N. Cao, T. Li, Y. Ji and G. Zheng, *Chem. – Asian J.*, 2019, **14**, 3969–3980.
- S. P. Paula, M. Stefano, E. L. S. Ifan and E. E. María, *ChemCatChem*, 2019, **11**, 1–21.
- B. Zhang, J. Zhang, M. Hua, Q. Wan, Z. Su, X. Tan, L. Liu, F. Zhang, G. Chen, D. Tan, X. Cheng, B. Han, L. Zheng and G. Mo, *J. Am. Chem. Soc.*, 2020, **142**, 13606–13613.
- W. Yang, Y. Zhao, S. Chen, W. Ren, X. Chen, C. Jia, Z. Su, Y. Wang and C. Zhao, *Inorg. Chem.*, 2020, **59**, 12437–12444.
- Q. Wang, Y. Lei, D. Wang and Y. Li, *Energy Environ. Sci.*, 2019, **12**, 1730–1750.
- Y. Wang, P. Han, X. Lv, L. Zhang and G. Zheng, *Joule*, 2018, **2**, 2551–2582.
- W. Zhang, S. Yang, M. Jiang, Y. Hu, C. Hu, X. Zhang and Z. Jin, *Nano Lett.*, 2021, **21**, 2650–2657.
- Y. Xing, X. Kong, X. Guo, Y. Liu, Q. Li, Y. Zhang, Y. Sheng, X. Yang, Z. Geng and J. Zeng, *Adv. Sci.*, 2020, 1902989.
- P. Deng, F. Yang, Z. Wang, S. Chen, Y. Zhou, S. Zaman and B. Y. Xia, *Angew. Chem., Int. Ed.*, 2020, **59**, 10807–10813.
- F. Li, G. H. Gu, C. Choi, P. Kolla, S. Hong, T.-S. Wu, Y.-L. Soo, J. Masa, S. Mukerjee, Y. Jung, J. Qiu and Z. Sun, *Appl. Catal., B*, 2020, **277**, 119241.
- P. Lamagni, M. Miola, J. Catalano, M. S. Hvid, M. A. H. Mamakhel, M. Christensen, M. R. Madsen, H. S. Jeppesen, X. M. Hu, K. Daasbjerg, T. Skrydstrup and N. Lock, *Adv. Funct. Mater.*, 2020, 1910408.
- H. Rabiee, L. Ge, X. Zhang, S. Hu, M. Li and Z. Yuan, *Energy Environ. Sci.*, 2021, **14**, 1959–2008.
- C. W. Lee, N. H. Cho, S. W. Im, M. S. Jee, Y. J. Hwang, B. K. Min and K. T. Nam, *J. Mater. Chem. A*, 2018, **6**, 14043–14057.



- 47 A. Wuttig, Y. Yoon, J. Ryu and Y. Surendranath, *J. Am. Chem. Soc.*, 2017, **139**, 17109–17113.
- 48 S. Zhang, P. Kang and T. J. Meyer, *J. Am. Chem. Soc.*, 2014, **136**, 1734–1737.
- 49 C. He, S. Chen, R. Long, L. Song and Y. Xiong, *Sci. China: Chem.*, 2020, **63**, 1721–1726.
- 50 I. V. Chernyshova, P. Somasundaran and S. Ponnuram, *Proc. Natl. Acad. Sci. U. S. A.*, 2018, **115**, E9261–E9270.
- 51 N. Han, Y. Wang, H. Yang, J. Deng, J. Wu, Y. Li and Y. Li, *Nat. Commun.*, 2018, **9**, 1320.
- 52 F. Yang, A. O. Elnabawy, R. Schimmenti, P. Song, J. Wang, Z. Peng, S. Yao, R. Deng, S. Song, Y. Lin, M. Mavrikakis and W. Xu, *Nat. Commun.*, 2020, **11**, 1088.
- 53 P. Su, W. Xu, Y. Qiu, T. Zhang, X. Li and H. Zhang, *ChemSusChem*, 2018, **11**, 848–853.
- 54 Z. Wu, Y. Zhao, W. Jin, B. Jia, J. Wang and T. Ma, *Adv. Funct. Mater.*, 2020, 2009070.
- 55 Z.-Z. Wu, F.-Y. Gao and M.-R. Gao, *Energy Environ. Sci.*, 2021, **14**, 1121–1139.
- 56 P. F. Sui, M. R. Gao, S. Liu, C. Xu, M. N. Zhu and J. L. Luo, *Adv. Funct. Mater.*, 2022, 2203794.
- 57 P. Yue, Q. Fu, J. Li, L. Zhang, L. Xing, Z. Kang, Q. Liao and X. Zhu, *Chem. Eng. J.*, 2021, **405**, 126975.
- 58 Z. Xing, L. Hu, D. S. Ripatti, X. Hu and X. Feng, *Nat. Commun.*, 2021, **12**, 136.
- 59 Z. Cai, Y. Zhang, Y. Zhao, Y. Wu, W. Xu, X. Wen, Y. Zhong, Y. Zhang, W. Liu, H. Wang, Y. Kuang and X. Sun, *Nano Res.*, 2018, **12**, 345–349.
- 60 M. Alfath and C. W. Lee, *Catalysts*, 2020, **10**, 859.
- 61 Y. Yoon, A. S. Hall and Y. Surendranath, *Angew. Chem., Int. Ed.*, 2016, **55**, 15282–15286.
- 62 A. Chen and B.-L. Lin, *Joule*, 2018, **2**, 594–606.
- 63 X. Tan, C. Yu, X. Song, C. Zhao, S. Cui, H. Xu, J. Chang, W. Guo, Z. Wang, Y. Xie and J. Qiu, *Adv. Energy Mater.*, 2021, 2100075.

