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On the subtle tuneability of cellulose hydrogels: implications for binding of biomolecules demonstrated for CBM 1†

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Cellulose-based hydrogel materials prepared by regeneration from cellulose solutions in ionic liquids, or ionic liquid containing solvent mixtures (organic electrolyte solutions), are becoming widely used in a range of applications from tissue scaffolds to membrane ionic diodes. In all such applications knowledge of the nature of the hydrogel with regards to porosity (pore size and tortuosity) and material structure and surface properties (crystallinity and hydrophobicity) is critical. Here we report significant changes in hydrogel properties, based on the choice of cellulose raw material (α - or bacterial cellulose – with differing degree of polymerization) and regeneration solvent (methanol or water). Focus is on bioaffinity applications, but the findings have wide ramifications, including in biomedical applications and cellulose saccharification. Specifically, we report that the choice of cellulose and regeneration solvent influences the surface area accessible to a family 1 carbohydrate-binding module (CBM), CBM affinity for the cellulose material, and rate of migration through the hydrogel. By regenerating bacterial cellulose in water, a maximum accessible surface area of 33 m² g⁻¹ was achieved. However, the highest CBM migration rate, 1.76 $\mu\text{m}^2 \text{min}^{-1}$, was attained by regenerating α -cellulose in methanol, which also resulted in the maximum affinity of the biomolecule for the material. Thus, it is clear that if regenerated cellulose hydrogels are to be used as support materials in bioaffinity (or other) applications, a balance between accessible surface area and affinity, or migration rate, must be achieved.

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Introduction

Cellulose is well established as a raw material supply for environmentally friendly and biocompatible products, including property-determining additives for foods, cosmetics, coatings, and synthetic fibres.¹ Recent applications include tissue scaffolds,² biomimetic 4D printing,³ and membrane ionic diodes.⁴ A naturally occurring biopolymer, it is biocompatible and is viewed as being almost inexhaustible, with an estimated 28.2 billion tonnes produced *via* biomass each year.^{1,5} The use of ionic liquids to

dissolve cellulose, followed by regeneration with an anti-solvent, has enabled the development of cellulose-based materials of variable forms, including hydrogels.^{6–8} More recently, Rinaldi demonstrated that the instantaneous dissolution of cellulose at room temperature is made possible by combining the ionic liquid with a dipolar aprotic co-solvent.⁹ It has been demonstrated that the choice of anti-solvent, used to regenerate cellulose from an ionic liquid solution can influence the material properties of the resultant hydrogel. For example, it has been reported that less crystalline materials result when alcohol anti-solvents are applied compared with water¹⁰ and that enhanced enzymatic hydrolysis is observed for cellulose regenerated in alcohol.¹¹

Carbohydrate-binding modules (CBMs) are protein domains found in cellulose-degrading enzymes that are responsible for guiding the appended catalytic domain of the enzyme to the cellulose surface.¹² They can be independently expressed *via* recombinant plasmid cloning,¹³ enabling their use in bioaffinity attachment without modification, or grafting, of the cellulose substrate. Bioaffinity attachment is of particular interest as it ensures controlled orientation of the active molecule, resulting in improved activity, and is generally reversible despite the attached agent being strongly bound.¹⁴ This enables the production of

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novel biocatalysts and biosorbents with enhanced performance;^{15–18} support matrices for affinity chromatography and biosensors;^{19–21} and biocompatible scaffolds for human tissue growth.^{22–24}

Tomme *et al.* previously reported that CBMs belonging to family 1, such as CBM1 of cellobiohydrolase I from *Trichoderma harzianum* (*ThCBM_{CBHI}*), used in this work, reversibly bind to cellulose.²⁵ This provides the opportunity to develop separation and purification applications, or regenerable biosensors, both of which require reversible binding of the active biomolecule.¹⁴ In order to assess whether cellulose hydrogels regenerated from ionic liquids are suitable supports for these applications, and to develop an understanding of their subsequent degradation rate, three parameters need to be investigated: (i) the accessible surface area of the hydrogel; (ii) the CBM partition constant; and (iii) the CBM diffusion rate.

It is desirable that the accessible surface area of the hydrogel is high, as this minimizes the mass of cellulose required for the application. It might also be expected to enable a higher rate of hydrolysis. In the same vein, a high CBM partition constant (a measurement that describes the affinity of the CBM for the material) is desirable in order to minimise excess CBM remaining in solution once the CBM has adsorbed onto the material. This is more important than the accessible surface area for bioaffinity applications given that cellulose is inexpensive compared to biomolecules, which require laborious expression, isolation and purification. Finally, a high CBM diffusion rate is desirable, as this will minimize the time required to load the hydrogel with the CBM and aid its subsequent removal. This is of importance at an industrial scale, as time is directly linked to cost.

It is known that family 1 CBMs preferentially bind to surfaces that are crystalline and hydrophobic.^{12,26,27} Therefore, we investigated hydrogels regenerated from an ionic liquid/co-solvent mixture (organic electrolyte solution) comprised of 30:70 1-ethyl-3-methyl imidazolium acetate:dimethyl sulfoxide ([EMIm][OAc]:DMSO) by weight using either methanol, or water, as the anti-solvent. Such materials are designated regenerated in methanol (rM), or regenerated in water (rW), respectively. The effect of the cellulose degree of polymerization (DP) on the resulting pore structure was evaluated using α -cellulose (AC), DP: 500–1300,²⁸ and bacterial cellulose (BC), DP: 2000–6000.²⁹ Herein, we demonstrate that the crystallinity, hydrophobicity and tortuosity of the regenerated hydrogel is dependent on both the type of cellulose and the anti-solvent used to regenerate the hydrogel, which, in turn affects the affinity of the CBM for the material and also modulates the rate of CBM migration within the hydrogel.

Experimental

Materials

Glucose, yeast extract, peptone, anhydrous disodium phosphate, citric acid monohydrate, sodium hypochlorite, 1-ethyl-3-methyl-imidazolium acetate, dimethyl sulfoxide, methanol, methylene blue, trifluoroacetic acid, acetonitrile, kanamycin sulfate,

chloramphenicol, isopropyl- β -D-thiogalactopyranoside, Trizma[®] base, 2-mercaptoethanol, glycerol, imidazole and α -cellulose were purchased from Sigma Aldrich. Alexa Fluor 488 C5 Maleimide dye was purchased from Invitrogen.

Bacterial cellulose production

Cellulose-producing bacteria from an acetobacter containing culture§ were grown at 25 °C in Hestrin & Schramm medium (distilled water supplemented with 2 wt% glucose, 0.5 wt% yeast extract, 0.5 wt% peptone, 0.27 wt% anhydrous disodium phosphate, and 0.15 wt% citric acid monohydrate).³⁰ The resulting bacterial cellulose pellicle was treated with a solution of 10 wt% sodium hypochlorite for 1 h before being washed three times with copious amounts of distilled water and lyophilised using a mini lyotrap (LTE Scientific) freeze dryer.

CBM mutagenesis, expression and purification

The cellobiohydrolase I carbohydrate-binding module gene from *Trichoderma harzianum* (*ThCBM1_{CBHI}*) was cloned as described by Mello & Polikarpov.³¹ The CBM gene was cloned into a pSMT3 expression vector, which encodes a 6His-SUMO N-terminal tag.³² A CBM site direct-mutagenesis S19C was performed, introducing a free cysteine residue, to ensure efficient protein labelling with fluorescent probes. DNA single mutation was introduced using QuickChange II Site-Directed Mutagenesis Kit (Stratagene) as per the manufacturer's protocol. For this approach, PCR amplification of an entire plasmid was performed using primers with mutation 5'-TGCGCTTGCGGCTACACTTG-3' (forward) and 5'-TCTGGTAGGTCCGGTCCAGCC-3' (backward). The mutagenesis product was transformed into *E. coli* DH5 α , and plasmid mini-preparations were used in the single colonies that grew in presence of kanamycin. The coding regions in the mutant plasmid were verified by DNA sequencing and then chemically transformed into *E. coli* Rosetta (DE3) strain for protein expression.

Transformed *E. coli* cells were cultured in LB broth containing kanamycin (50 μ g mL⁻¹) and chloramphenicol (34 μ g mL⁻¹) at 37 °C. After the medium absorbance at 600 nm reached 0.8, protein expression was induced with 1 mM isopropyl- β -D-thiogalactopyranoside and cells incubated for 16 h at 18 °C. The cells were harvested by centrifugation and resuspended in buffer A (20 mM Tris pH 7.5, 300 mM NaCl, 5% glycerol, 1 mM phenylmethanesulfonylfluoride and 4.3 M 2-mercaptoethanol). The sample was sonicated to disrupt the cells and centrifuged at 14 000 rpm for 40 min. The soluble fraction of *ThCBM1_{CBHI}* + SUMO was submitted to Ni²⁺ affinity purification. Buffer A was used to wash the set proteins/resin and protein elution was achieved with an imidazole gradient through a gradual increase of buffer B (20 mM Tris pH 7.5, 150 mM NaCl, 300 mM

§ While BC is often ascribed to production by a particular strain, it can be more productive to use mixed cultures, such as those used in production of the drink 'kombucha', followed by appropriate purification, particularly where the material is then dissolved so removing any structural features. Reva *et al.*, have reported that the core of such communities are comprised of acetobacteria of two genera, *Komagataeibacter* (formerly *Gluconacetobacter*) and *Gluconobacter*.⁶⁰



imidazole, 5% glycerol, and 4.3 M 2-mercaptoethanol). All the eluted samples were analyzed by 15% (wt/wt) SDS-PAGE.

Cellulose hydrogel generation

Cellulose (4 wt%, α -, or bacterial) was dissolved in a solution of 30:70 wt% [EMIm][OAc]:DMSO at 25 °C overnight on a roller table in order to achieve complete dissolution. The solutions were then tape cast using an Elcometer 4340 Automatic Film Applicator with a distance of 500 μ m between the blade and glass surface. The resulting film was regenerated by immersion in the chosen anti-solvent for 20 min and washed twice with copious amounts of distilled water to remove excess solvent before being stored in a solution of 20 wt% MeOH in water in order to inhibit bacterial growth.

Powder X-ray diffraction (pXRD)

Pieces of the cellulose hydrogels were frozen using liquid nitrogen and ground to powders using a pestle and mortar. These were analyzed using a flat plate BRUKER D8-Advance (Cu K α , λ 1.5418 Å radiation) powder X-ray diffractometer over the 2θ range 4–60° with a step size of 0.016° and step time of 0.8 s. The curve-fitting software, Fityk, was used to deconvolute the raw pXRD data: Gaussian curves were fitted to the signals in the amorphous and crystalline regions.³³ The crystallinity index was calculated as the ratio between the sum of the crystalline peak areas and the total peak area.

NMR cryoporometry

The cellulose samples were soaked in water overnight, excess surface water removed, and the samples placed in individual NMR tubes and sealed using damp absorbent paper to maintain high humidity. The ¹H NMR signal was recorded on a 400 MHz Bruker Avance spectrometer equipped with a 5 mm BBO probe, running with the boil-off from liquid nitrogen as cooling gas, and a BVT3200 temperature control unit with precision of ± 0.1 K. Actual *versus* recorded temperatures had previously been calibrated using a methanol sample.³⁴ A simple spin echo pulse sequence was used, with an echo time of 2.2 ms, to ensure minimal suppression of signal from liquid water and complete suppression of signals from both cellulose and frozen water.^{35,36} Measurements were performed by decreasing the temperature to 218 K in order to completely freeze the sample, followed by increasing the temperature stepwise by 5 K up to 258 K, then in 1 K steps to 267 K, 0.2 K steps to 271 K, and finally to bulk melting temperature using a temperature step of 0.1 K. At each increment signals were recorded after establishment of thermal equilibrium, achieved by a waiting time of 20 min.

The melting point depression, ΔT , is related to the pore radius, r , *via* the bulk properties of the probe liquid, P , as described by the Gibbs–Thomson equation:

$$\Delta T \propto \frac{P}{(r-s)}$$

where P is 25 nm for water and s represents the thickness of a pre-molten liquid-like layer on the surface of the substrate, here

assumed constant over the temperature range and two monolayers thick, *i.e.* 0.6 nm.¹⁰

NMR relaxometry

Transverse relaxation times, T_2 , were measured *via* Carr–Purcell–Meiboom–Gill (CPMG) echo train acquisition using a Bruker Minispec MQ-20 spectrometer operating with a magnetic field of 0.5 T (¹H Larmor frequency of 20 MHz) at 40 °C. 10 000 Echoes were acquired with echo (relaxation delay) times (t_E) of 1 ms and total recycle delays of 15 s. In fluids in the fast diffusion regime, there is a close relation between the T_2 values and the surface-to-volume ratio of pores.^{35,37} In this particular case, the magnetic field is not highly heterogeneous; there are no paramagnetic, or magnetic, impurities on the pore surface; and relatively short echo times were used. Under these conditions the relation between T_2 and the surface to volume ratio is:

$$\frac{1}{T_2} = \left(\frac{1}{T_2}\right)_{\text{bulk}} + \rho_2 \left(\frac{S}{V}\right)$$

where ρ_2 is the relaxivity constant of the fluid in the pores of the material, and S and V are the pore surface area and volume respectively. As the relaxivity constant of the fluid used to fill the cellulose pores, *i.e.* water in PBS, is unknown, it is not possible to obtain the surface to volume ratio of the pores, but the trends of T_2 may be directly associated with variation in the sizes of regions filled with the solution. Larger T_2 values correspond to larger pores.³⁸

Besides the averaged T_2 values, the measurement of the decay of the CPMG echo train, CPMG decay $S_{\text{CPMG}}(t)$, T_2 distribution profiles, $g(T_2)$, associated with distribution of pore sizes and variations in the water mobility within the pores, can be obtained using a non-negative least square procedure also known as a numerical inverse Laplace transform (ILT) to fit the $S_{\text{CPMG}}(t)$ curves.^{39,40} In this case, an ILT method implemented in Matlab was used.

Scanning electron microscopy

Samples of the cellulose hydrogels were dried using a mini lyotrap (LTE Scientific) freeze dryer. The dense skin layer was peeled off with adhesive tape to reveal the core pore structure. Samples were sputter coated with gold for 5 min in an Edwards S150B sputter coater and specimens imaged with a JEOL SEM6480LV operating at 5 kV.

Molecular probe adsorption

Methylene blue (MB) depletion isotherms were constructed by incubating five 134.2 mm² pieces of the cellulose hydrogels with various concentrations (5–1000 μ M) of MB in 5 mL of distilled water with 0.01 wt% trifluoroacetic acid. MB controls without cellulose were included and all experiments were carried out in triplicate. Samples were incubated at 4 °C for 24 h, after which time the concentration of the bound MB was calculated from the difference in the original and final MB concentrations in the supernatant: 1 mL of the supernatant was removed and spectrophotometrically analysed in a 1260 Infinity Series (Agilent Technologies) HPLC (flow rate: 1 mL min⁻¹,



injection volume: 1 μL , absorbance wavelength: 660 nm, column: Poroshell 120 EC-C18 2.7 μm 4.6 \times 50 mm (Agilent Technologies), mobile phase: 50:50 water:acetonitrile with 0.01 wt% trifluoroacetic acid). A calibration curve of absorbance against MB concentrations was obtained by using MB solutions of known concentrations (Fig. S1, ESI[†]).

Carbohydrate-binding module (CBM) depletion isotherms were constructed by incubating a 78.5 mm² piece of the produced cellulose hydrogels with various concentrations (6.25–200 μM) of *ThCBM*_{CBHI} in 100 μL of 50 mM PBS pH 7.0. Controls without cellulose were included and all experiments were conducted in triplicate. Samples were incubated at 4 $^{\circ}\text{C}$ for 24 h with agitation (roller table); 2 μL of the supernatant were removed and the concentration of free protein calculated by the absorbance measured at 280 nm using a NanoDrop 2000 Spectrophotometer (Thermo Fisher Scientific). The concentration of the bound *ThCBM*_{CBHI} was calculated from the difference in initial and final *ThCBM*_{CBHI} concentration in the supernatant.

Partition constants were obtained from the depletion isotherms (plot of final concentration *versus* mass of molecular probe adsorbed per gram of cellulose) after fitting of the raw data to a Langmuir-type adsorption model:

$$Y = \frac{N}{N_m} = \frac{KC}{1 + KC}$$

where Y is the fraction of the surface covered by the adsorbed molecular probe, N is the number of moles of the molecular probe adsorbed per gram of cellulose at the equilibrium concentration ($\mu\text{mol g}^{-1}$), N_m is the number of moles of the molecular probe per gram of cellulose required to form a monolayer ($\mu\text{mol g}^{-1}$), K is the equilibrium association constant (μM^{-1}), and C is the molecular probe concentration at equilibrium (μM).

Rearrangement of the equation enabled calculation of N_m and K (Table S4, ESI[†]) for the molecular probes by plotting C/N *versus* C (Fig. S2 and S3, ESI[†]):

$$\frac{C}{N} = \frac{C}{N_m} + \frac{1}{KN_m}$$

enabling the specific surface area, and the partition constant (initial gradient of the fitted isotherm) to be calculated for each hydrogel:

$$S = N_m a N_{\text{Av}}$$

where S is the specific surface area accessible to the probe molecule, a is the occupied surface area of the probe molecule, and N_{Av} is Avogadro's number.

Confocal microscopy bleaching

The cysteine residue inserted into *ThCBM*_{1CBHI} by mutation was specifically labelled with Alexa Fluor 488 C5 Maleimide (Invitrogen) dye, following the manufacturer's instructions. Briefly, 100 μM of *ThCBM*_{1CBHI} + SUMO in 50 mM phosphate buffer, pH 7.0, was incubated with excess dye (1:10 mole ratio of protein:dye) overnight at 10 $^{\circ}\text{C}$. Size exclusion chromatography was used to remove excess dye from the labelled protein: the

sample was passed through a GE Superdex 75 10/300 GL column, connected to a GE Healthcare ÄKTAprime system, pre-equilibrated with 50 mM phosphate buffer, pH 7.0, and 150 mM NaCl. Fractions collected as the labelled protein eluted were combined and the concentration of labelled protein, and the degree of labelling, were estimated by absorbance measurements at 280 nm and 494 nm (dye absorbance maximum) using a NanoDrop 2000 Spectrophotometer (Thermo Fisher Scientific).

Cellulose hydrogel samples, 134.2 mm², were incubated with fluorescein-modified *ThCBM*_{CBHI} at a concentration of 10 nM for 19 h at 16 $^{\circ}\text{C}$. The samples were then washed twice with PBS before being analysed using a Zeiss LSM 780 confocal microscope. Images were taken using a 405 nm diode laser at 17% power output, an excitation wavelength of 488 nm and absorption wavelength of 525 nm. An area of the sample was selectively bleached by multiple passes of the laser operating at 100% power until the fluorescence intensity of the area had halved (Fig. S5, ESI[†]). Images of the sample were then taken every minute for 1 h to measure recovery.

Theoretical fluorescence recovery curves based on the equation developed by Axelrod *et al.*⁴¹ were applied to the raw data in order to calculate the maximum fluorescence intensity recovery and the recovery half-life, *i.e.* the time required for the intensity of the bleached area to recover its intensity to half that of the final intensity value:

$$Z_t = \frac{I_t}{I_{\text{max}}} = 1 - \frac{k}{2\left(1 + \frac{t}{\tau_D}\right)}$$

where Z_t is the fraction of maximum recoverable intensity recovered at time t , I_t is the fluorescence intensity at time t , I_{max} is the maximum recoverable fluorescence intensity, k is a constant, and τ_D is the characteristic diffusion time. The diffusion coefficient, D , is related to τ_D and the half-width of the bleached profile, ω :

$$D = \frac{\omega^2}{4\tau_D}$$

Results and discussion

The dissolution and regeneration of cellulose results in highly porous hydrogels that contain very little cellulosic material (Table 1); densities were *ca.* 20 kg m⁻³ compared to the absolute density of pure cellulose of 1592 kg m⁻³.⁴² Analysis of pXRD patterns revealed that both cellulose and anti-solvent type affect the overall crystallinity of the regenerated hydrogel (Fig. 1). Both untreated BC and AC are type I cellulose, indicated by pXRD peaks around $2\theta = 14.8, 16.8, 22.0$ and 22.5° , whilst all the regenerated samples are type II, indicated by peaks around $2\theta = 12.1, 13.0, 19.8$ and 20.6° .^{43–45} Dissolution and regeneration of cellulose resulted in hydrogels with reduced crystallinity compared to the starting materials – the crystallinity indices for untreated BC and AC were 0.88 and 0.45 respectively (Table 1). Regeneration in water resulted in a



Table 1 Effects of choice of cellulose starting material and anti-solvent on regenerated cellulose hydrogel density, porosity, crystallinity, modal nanopore diameter, median micropore diameter, and nano : micro pore ratio

Sample	Density [kg m ⁻³]	Porosity [%]	Crystallinity index	Modal nanopore diameter ^a [nm]	Median micropore diameter ^b [nm]	Nano : micro pore ratio ^c
ACrM	17 ± 1	99	0.18	50	226	10 : 1
ACrW	22 ± 2	99	0.27	36	224	12 : 1
BCrM	18 ± 1	99	0.19	54	190	5 : 1
BCrW	17 ± 1	99	0.32	44	206	6 : 1

^a Determined from NMR cryoporometry. ^b Determined from SEM micrographs. ^c Determined from NMR relaxometry studies.



Fig. 1 pXRD patterns of samples with crystalline and amorphous peaks fitted: (a) unprocessed α -cellulose (AC); (b) unprocessed bacterial cellulose (BC); (c) α -cellulose regenerated in water (ACrW); (d) bacterial cellulose regenerated in water (BCrW); (e) α -cellulose regenerated in methanol (ACrM); and (f) bacterial cellulose regenerated in methanol (BCrM). Dissolution and regeneration of cellulose results in type II crystalline material with more amorphous material formed after regeneration using methanol compared to water.

higher degree of crystallinity than regeneration in methanol for both cellulose types with an average increase of 59%.

To probe the pore structure of the hydrogels without drying, two NMR techniques were employed: relaxometry and cryoporometry. In the former the dependence of proton transverse relaxation time (T_2) and surface to volume ratio of pores was exploited. To complement this, and overcome difficulties in defining pore diameters,³⁸ cryoporometry was used to probe specific pore size (<100 nm).^{46,47}

The ILT of the CPMG decays obtained for the hydrogels revealed a T_2 distribution profile with three distinct peaks. The peak at the highest T_2 value is ascribed to the bulk water in the PBS, which is justified by the comparison with the T_2 distribution profile obtained for the pure solution (Fig. 2C, inset).

The absence of a precise value for the relaxivity constant of water (PBS) inside cellulose pores frustrates association of T_2 distributions with specific pore diameters. However, based on previously published data⁴⁸ and on the averaged T_2 values reported for pure water filling pores of known dimensions in cellulose,^{49–52} the relaxivity of pure water inside cellulose pores can be estimated to be in the range 10^{-6} – 10^{-7} nm s⁻¹. Thus, using the relation between pore dimension T_2 and relaxivity constant previously reported,⁴⁸ the T_2 range from 10–100 ms was ascribed to pores with dimensions in the range 10–100 nm and the T_2 range from 100 ms to 1 s to pores with dimensions in the range 100 nm to a few μ m. Thus, in Fig. 2C, the peaks at the shorter T_2 values reflect nanopores, while the peaks with intermediate T_2 reflect micropores. The peak corresponding to





Fig. 2 (A) (i) SEM micrograph of a lyophilised cellulose hydrogel showing the porous structure below a dense skin layer – all hydrogels exhibited this bulk structure, (ii) and (iii) SEM micrographs of ACrM and BCrW samples showing differences in micropore size. (B) Nanometer pore size distribution of hydrogels based on NMR cryoporometry: (i) specific pore surface area density (ρ), and (ii) specific cumulative pore surface area. Both choice of cellulose and anti-solvent have an effect on the overall pore structure of the hydrogels in agreement with relaxometry studies. (C) NMR T_2 relaxation distribution curves for regenerated cellulose hydrogels providing relative surface areas for nano- and micropores. Both choice of cellulose and anti-solvent have an effect on the overall pore structure of the hydrogels. Bulk PBS measurement included in inset.

nanopores for AC reflected a smaller median pore diameter than that for BC, whilst hydrogels regenerated in methanol exhibited larger pores than those regenerated in water. NMR cryoporometry confirmed these observations, yielding a modal pore diameter of 36 nm for AC regenerated in water and 54 nm for BC regenerated in methanol (Fig. 2B and Table 1). It is of interest to note that Östlund *et al.* reported a pore radius distribution between 2–15 nm, based on NMR cryoporometry for cellulose samples regenerated from [EMIm][OAc] only,¹⁰ whilst the distribution in these hydrogels is between 10–70 nm, suggesting that the ratio of ionic liquid to co-solvent in the organic electrolyte solution used could influence the pore size of the resultant regenerated hydrogels, providing further opportunities to tune porosity.

NMR relaxometry studies revealed that micropores (above the range that can be probed with NMR cryoporometry) in AC exhibited a slightly larger median diameter than those in BC, as confirmed by analysis of SEM micrographs (Fig. 2A and Table 1). Significantly more nanopores were present in AC, as

reflected in the ratio between the integrated nano- and micropore peak areas in the relaxometry data: that of AC was double that of BC (Table 1). In both cases, hydrogels regenerated in water show a 20% increase in nano- to micropore ratio *versus* those regenerated in methanol. To validate these results, and to discern whether such differences were important at a molecular scale, passive MB adsorption (used to characterize cotton fibers)⁵³ was conducted. This enabled calculation of the cellulose surface area in the never-dried hydrogels, whilst providing a molecular probe small enough to access pores inaccessible to the larger CBM. (MB has an occupied surface area of 197.2 \AA^2 whilst $ThCBM_{CBHI}$ has a maximum occupied area of approximately 985 \AA^2 , assuming a globular structure.^{54,55})

MB adsorption isotherms (Fig. 3a) revealed that BCrM had a lower surface area than ACrW (Table 2), in accordance with the observation that ACrW has a higher population of nanopores with smaller diameters (Table 1). The choice of cellulose influences the surface area by a factor of 1.6 ($total_{AC}/total_{BC}$),





Fig. 3 (a) Methylene blue adsorption isotherms on regenerated cellulose scaffolds, (b) $ThCBM_{CBHI}$ adsorption isotherms on regenerated cellulose scaffolds. Error bars ± 1 standard error. Whilst a greater surface area is accessible to methylene blue in α -cellulose samples, a greater area is accessible to $ThCBM_{CBHI}$ in bacterial cellulose samples. Water regenerated samples have a greater accessible area in all cases.

Table 2 Specific surface area and partition constants per unit mass and per unit area for methylene blue (MB) and $ThCBM_{CBHI}$ adsorption on regenerated cellulose hydrogels

Sample	MB specific surface area [$m^2 g^{-1}$]	MB partition constant [$\times 10^{-3} L g^{-1}$]	MB partition constant [$\times 10^{-3} L m^{-2}$]	CBM specific surface area [$m^2 g^{-1}$]	CBM partition constant [$\times 10^{-3} L g^{-1}$]	CBM partition constant [$\times 10^{-3} L m^{-2}$]
ACrM	47	855	18.3	14	53	3.8
ACrW	56	874	15.5	16	43	2.7
BCrM	30	288	9.5	29	70	2.4
BCrW	35	236	6.8	33	76	2.3

whilst the choice of anti-solvent affects the surface area by a factor of 1.2 ($total_{rW}/total_{rM}$).

The surface area available for CBM attachment was also affected by the cellulose and anti-solvent type: rW hydrogels had a 1.2 increase in the $ThCBM_{CBHI}$ accessible surface area, due either to the higher proportion of nanopores with smaller diameters, or to the increase in crystallinity, compared to rM hydrogels. However, the use of AC resulted in a reduction of the surface area accessible to $ThCBM_{CBHI}$ by a factor of 0.4. It is hypothesised that a significant proportion of the pores in the AC samples accessible to MB are inaccessible to $ThCBM_{CBHI}$ (due to its larger size). Of the pore surface accessible to MB, 95% is accessible to $ThCBM_{CBHI}$ in hydrogels prepared from BC, whilst only 24% is accessible in hydrogels prepared from AC. This is supported by the nanopore:micropore ratios derived from the NMR relaxometry experiments (Table 1).

It is apparent that both the cellulose type (differing by DP only) and anti-solvent identity influenced the partition constants of MB (Table 2). MB partition constants measured for AC derived hydrogels are higher than for BC derived hydrogels and this may reflect differences in processing of the raw materials used.¶ CBM partition constants expressed in units of $L m^{-2}$ (which more accurately reflects the surfaces available for adsorption of the probe molecules) gave distinctly larger values for rM samples versus rW samples when MB was used as the probe molecule. It has been reported that the partition constant for monosaccharide adsorption increased with the hydrophobicity

index of the monosaccharide.⁵⁶ Considering this to reflect in the reverse, *i.e.* adsorption onto polysaccharide surfaces, this might suggest greater hydrophobicity of surfaces in rM samples versus rW samples. This reflects previously published data pertaining to crystallinity: Östlund *et al.* argued that faster rates of demixing in water ‘trap’ the methylhydroxyl groups in the *gauche-trans* formation that is found in cellulose II.¹⁰ This results in a higher crystallinity for samples regenerated in water than those regenerated in methanol, where the methylhydroxyl groups adopt the more energetically favourable *gauche-gauche* confirmation, demonstrated computationally by Liu *et al.*⁵⁷ If samples regenerated in methanol are more hydrophobic – due either to the conformation of the methylhydroxyl groups, or to the specific crystalline faces exposed – this would account for the observed difference. No such differences are noted in binding of $ThCBM_{CBHI}$, with partition constants ranging between 3.8 and 2.3 $mL m^{-2}$, reflecting the inaccessibility of the smaller pores to the large biomolecule (Table 2).

It is also of note that the partition constants expressed per unit mass, reported here for a family 1 CBM, are two orders of magnitude lower than those reported previously: a partition constant of $1.0 \times 10^5 M^{-1}$ was reported for *T. reesei* CBM_{CBHI} on native BC,²⁵ and $4.9 L g^{-1}$ on microcrystalline cellulose;⁵⁸ compared to $1.5 \times 10^3 M^{-1}$ and $7.6 \times 10^{-2} L g^{-1}$ on BCrW in this work. This reflects the lower degree of crystallinity in these regenerated samples, although, as previously discussed in the literature, these values do not take into account the accessible surface area.⁵⁹

To test the hypothesis that some pores are inaccessible to CBMs, the rates of diffusion of fluorescently tagged $ThCBM_{CBHI}$ in hydrogels were determined from rates of recovery of fluorescent intensity after bleaching, using confocal microscopy. Recovery of the fluorescence intensity after bleaching is observed (Fig. 4),

¶ AC materials may be subjected to an acid wash during purification potentially leading to introduction of a very small number of acid groups on the surfaces that would bind a positively charged probe, such as MB, strongly.



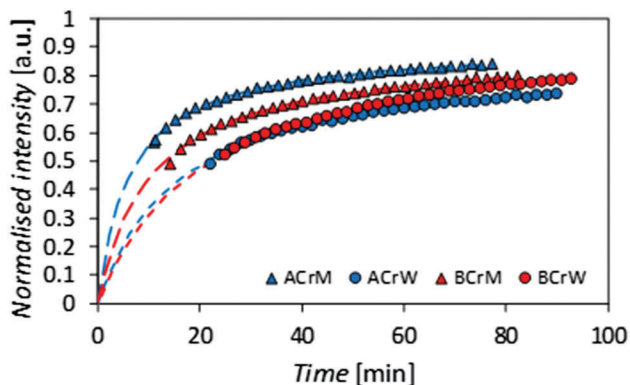


Fig. 4 Recovery of fluorescence intensity for regenerated cellulose hydrogels after bleaching. A more rapid recovery is observed in the methanol regenerated samples and those generated from α -cellulose.

Table 3 Maximum recoverable fluorescence intensity, I_{\max} , curve constant, k , characteristic diffusion time, τ_D , recovery half-life, $t_{1/2}$, and $ThCBM_{CBHI}$ diffusion coefficient, D , for hydrogels based on bleaching studies

Sample	I_{\max}	k [min^{-1}]	τ_D [min]	$t_{1/2}$ [min]	D [$\mu\text{m}^2 \text{min}^{-1}$]
ACrM	0.91	2.00	6.3	7.8	1.76
ACrW	0.86	2.01	15.3	21.6	0.73
BCrM	0.90	2.00	10.4	13.2	1.07
BCrW	0.96	2.01	20.3	22.5	0.55

confirming that $ThCBM_{CBHI}$ is reversibly bound to the cellulose, in agreement with previous reports.²⁵ The differences in the recovery half-lives and subsequent diffusion coefficients of the samples can be attributed to three different effects: (i) the pore structure of the hydrogels – a structure with fewer pores accessible to the CBM is more tortuous, resulting in a lower CBM diffusion rate and thus a longer recovery period; (ii) the affinity of the CBM to the cellulose, a higher partition constant resulting in a higher diffusion rate; and (iii) the hydrophobicity of the sample – it has been reported, based on computational simulations, that CBM could diffuse from hydrophilic to hydrophobic surfaces, but that the reverse transition was not observed in 43 ms of simulation,²⁷ suggesting that a slower diffusion rate would be observed along surfaces with more hydrophilic character.

Given that the diffusion coefficient increases by a factor of 1.5 for AC compared to BC (Table 3), it is apparent that the affinity of the CBM for the cellulose surfaces is more important than the hydrogel tortuosity (assumed to be proportional to the difference in accessible surface area for $ThCBM_{CBHI}$ compared to MB). With regards to the anti-solvent type, rM hydrogels increase the diffusion coefficient by a factor of 2.2 over rW hydrogels. In this instance, the tortuosity and presumed hydrophobicity of the hydrogel are more important than the CBM affinity.

Conclusions

Cellulose hydrogels regenerated from solutions containing ionic liquids have been used in a plethora of applications,

but, in many cases, the materials have primarily been characterised using techniques requiring drying. Here, careful “wet” characterisation of never-dried cellulose hydrogels has revealed that subtle changes in choice of raw material and regeneration solvents can result in significant differences in the hydrogel products. This has wide ramifications for many cellulose hydrogel and material applications.

Specifically, the choice of cellulose starting material (with different DP) and anti-solvent used in generating cellulose hydrogels from solutions containing ionic liquids influence the crystallinity and pore structure of the resulting hydrogel. In turn, these affect the tortuosity and hydrophobicity of the porous material and, thus, the affinity of molecules adsorbing onto and migrating through, the hydrogel. Small molecules, such as the widely used probe methylene blue, do not yield information that can be extrapolated to larger probes, such as proteins, including CBMs. It is also clear that compromises may need to be made between the maximum accessible surface area for the CBM, here $33 \text{ m}^2 \text{ g}^{-1}$ for bacterial cellulose regenerated in water, and maximum CBM partition constant per unit area and CBM diffusion coefficient, here 3.8 mL m^{-2} and $1.76 \mu\text{m}^2 \text{ min}^{-1}$ for α -cellulose regenerated in methanol. Thus, cellulose hydrogels optimized for various CBM-based bioaffinity applications may be prepared by manipulating the cellulose DP and anti-solvent. For example, the use of methanol to regenerate the hydrogel will lead to a higher enzymatic hydrolysis rate due to the increased CBM migration rate. In addition, bacterial cellulose has been widely posited as a biocompatible material and many potential applications of such hydrogels will rely on hydrogel structure.

Conflict of interest

There are no conflicts of interest to declare.

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Notes and references

- 1 D. Klemm, B. Heublein, H.-P. Fink and A. Bohn, *Angew. Chem., Int. Ed.*, 2005, **44**, 3358–3393.
- 2 J. C. Courtenay, M. A. Johns, F. Galembeck, C. Deneke, E. M. Lanzoni, C. A. Costa, J. L. Scott and R. I. Sharma, *Cellulose*, 2017, **24**, 253–267.



- 3 A. Sydney Gladman, E. A. Matsumoto, R. G. Nuzzo, L. Mahadevan and J. A. Lewis, *Nat. Mater.*, 2016, **15**, 413–418.
- 4 B. D. B. Aaronson, D. He, E. Madrid, M. A. Johns, J. L. Scott, L. Fan, J. Doughty, M. A. S. Kadowaki, I. Polikarpov, N. B. McKeown and F. Marken, *ChemistrySelect*, 2017, **2**, 871–875.
- 5 C. B. Field, M. J. Behrenfeld, J. T. Randerson and P. Falkowski, *Science*, 1998, **281**, 237–240.
- 6 R. P. Swatloski, S. K. Spear, J. D. Holbrey and R. D. Rogers, *J. Am. Chem. Soc.*, 2002, **124**, 4974–4975.
- 7 J.-I. Kadokawa, M.-A. Murakami and Y. Kaneko, *Carbohydr. Res.*, 2008, **343**, 769–772.
- 8 O. Aaltonen and O. Jauhiainen, *Carbohydr. Polym.*, 2009, **75**, 125–129.
- 9 R. Rinaldi, *Chem. Commun.*, 2011, **47**, 511–513.
- 10 Å. Östlund, A. Idström, C. Olsson, P. Larsson and L. Nordstierna, *Cellulose*, 2013, **20**, 1657–1667.
- 11 X. Geng and W. A. Henderson, *RSC Adv.*, 2014, **4**, 31226–31229.
- 12 A. B. Boraston, D. N. Bolam, H. J. Gilbert and G. J. Davies, *Biochem. J.*, 2004, **382**, 769–781.
- 13 M. A. Goldstein, M. Takagi, S. Hashida, O. Shoseyov, R. H. Doi and I. H. Segel, *J. Bacteriol.*, 1993, **175**, 5762–5768.
- 14 J. Credou and T. Berthelot, *J. Mater. Chem. B*, 2014, **2**, 4767–4788.
- 15 Z. Xu, W. Bae, A. Mulchandani, R. K. Mehra and W. Chen, *Biomacromolecules*, 2002, **3**, 462–465.
- 16 A. Fishman, I. Levy, U. Cogan and O. Shoseyov, *J. Mol. Catal. B: Enzym.*, 2002, **18**, 121–131.
- 17 S. Hwang, J. Ahn, S. Lee, T. Lee, S. Haam, K. Lee, I.-S. Ahn and J.-K. Jung, *Biotechnol. Lett.*, 2004, **26**, 603–605.
- 18 H. Park, J. Ahn, J. Lee, H. Lee, C. Kim, J.-K. Jung, H. Lee and E. G. Lee, *Int. J. Mol. Sci.*, 2012, **13**, 358–368.
- 19 W. Lewis, E. Keshavarz-Moore, J. Windust, D. Bushell and N. Parry, *Biotechnol. Bioeng.*, 2006, **94**, 625–632.
- 20 Y. Cao, Q. Zhang, C. Wang, Y. Zhu and G. Bai, *J. Chromatogr. A*, 2007, **1149**, 228–235.
- 21 A. Karpol, L. Kantorovich, A. Demishtein, Y. Barak, E. Morag, R. Lamed and E. A. Bayer, *J. Mol. Recognit.*, 2009, **22**, 91–98.
- 22 A. Wierzbza, U. Reichl, R. F. B. Turner, R. A. J. Warren and D. G. Kilburn, *Biotechnol. Bioeng.*, 1995, **46**, 185–193.
- 23 F. K. Andrade, S. M. G. Moreira, L. Domingues and F. M. P. Gama, *J. Biomed. Mater. Res., Part A*, 2010, **92**, 9–17.
- 24 R. Pértile, S. Moreira, F. Andrade, L. Domingues and M. Gama, *Biotechnol. Prog.*, 2012, **28**, 526–532.
- 25 P. Tomme, A. Boraston, B. McLean, J. Kormos, A. L. Creagh, K. Sturch, N. R. Gilkes, C. A. Haynes, R. A. J. Warren and D. G. Kilburn, *J. Chromatogr. B: Biomed. Sci. Appl.*, 1998, **715**, 283–296.
- 26 J. Lehtiö, J. Sugiyama, M. Gustavsson, L. Fransson, M. Linder and T. T. Teeri, *Proc. Natl. Acad. Sci. U. S. A.*, 2003, **100**, 484–489.
- 27 M. R. Nimlos, G. T. Beckham, J. F. Matthews, L. Bu, M. E. Himmel and M. F. Crowley, *J. Biol. Chem.*, 2012, **287**, 20603–20612.
- 28 K. B. Pal, H. Chatterjee and P. B. Sarkar, *Nature*, 1952, **169**, 845–846.
- 29 É. Pecoraro, D. Manzani, Y. Messaddeq and S. J. L. Ribeiro, in *Monomers, Polymers and Composites from Renewable Resources*, ed. M. N. Belgacem and A. Gandini, Elsevier, Amsterdam, 2007, ch. 17, pp. 369–383, DOI: 10.1016/B978-0-08-045316-3.00017-X.
- 30 M. Schramm and S. Hestrin, *Microbiology*, 1954, **11**, 123–129.
- 31 B. L. Mello and I. Polikarpov, *AMB Express*, 2014, **4**, 1–6.
- 32 E. Mossessoiva and C. D. Lima, *Mol. Cell*, 2000, **5**, 865–876.
- 33 M. Wojdyr, *J. Appl. Crystallogr.*, 2010, **43**, 1126–1128.
- 34 S. Berger and S. Braun, *200 and More NMR Experiments*, Wiley-VCH, Weinheim, Germany, 2004.
- 35 H. Y. Carr and E. M. Purcell, *Phys. Rev.*, 1954, **94**, 630–638.
- 36 S. Meiboom and D. Gill, *Rev. Sci. Instrum.*, 1958, **29**, 688–691.
- 37 K. R. Brownstein and C. E. Tarr, *Phys. Rev. A: At., Mol., Opt. Phys.*, 1979, **19**, 2446–2453.
- 38 J. Mitchell, S. C. Stark and J. H. Strange, *J. Phys. D: Appl. Phys.*, 2005, **38**, 1950–1958.
- 39 S. W. Provencher, *Comput. Phys. Commun.*, 1982, **27**, 229–242.
- 40 G. C. Borgia, R. J. S. Brown and P. Fantazzini, *J. Magn. Reson.*, 1998, **132**, 65–77.
- 41 D. Axelrod, D. E. Koppel, J. Schlessinger, E. Elson and W. W. Webb, *Biophys. J.*, 1976, **16**, 1055–1069.
- 42 L. Y. Mwaikambo and M. P. Ansell, *J. Mater. Sci. Lett.*, 2001, **20**, 2095–2096.
- 43 M. Ago, T. Endo and T. Hirotsu, *Cellulose*, 2004, **11**, 163–167.
- 44 S. Park, J. O. Baker, M. E. Himmel, P. A. Parilla and D. K. Johnson, *Biotechnol. Biofuels*, 2010, **3**, 10.
- 45 N. Terinte, R. Ibbett and K. C. Schuster, *Lenzinger Ber.*, 2011, **89**, 118–131.
- 46 O. V. Petrov and I. Furó, *Prog. Nucl. Magn. Reson. Spectrosc.*, 2009, **54**, 97–122.
- 47 E. Shiko, K. J. Edler, J. P. Lowe and S. P. Rigby, *J. Colloid Interface Sci.*, 2012, **385**, 183–192.
- 48 C. Zhang, P. Li, Y. Zhang, F. Lu, W. Li, H. Kang, J.-F. Xiang, Y. Huang and R. Liu, *Polymer*, 2016, **98**, 237–243.
- 49 D. Capitani, N. Proietti, F. Ziarelli and A. L. Segre, *Macromolecules*, 2002, **35**, 5536–5543.
- 50 N. Proietti, D. Capitani, E. Pedemonte, B. Blümich and A. L. Segre, *J. Magn. Reson.*, 2004, **170**, 113–120.
- 51 C. Felby, L. G. Thygesen, J. B. Kristensen, H. Jørgensen and T. Elder, *Cellulose*, 2008, **15**, 703–710.
- 52 J. E. Tsuchida, C. A. Rezende, R. de Oliveira-Silva, M. A. Lima, M. N. d'Eurydice, I. Polikarpov and T. J. Bonagamba, *Biotechnol. Biofuels*, 2014, **7**, 127.
- 53 C. Kaewprasit, E. Hequet, N. Abidi and J. Paul, *J. Cotton Sci.*, 1998, **2**, 164–173.
- 54 D. Graham, *J. Phys. Chem.*, 1955, **59**, 896–900.
- 55 H. P. Erickson, *Biol. Proced. Online*, 2009, **11**, 32–51.
- 56 K. Miyajima, K. Machida, T. Taga, H. Komatsu and M. Nakagaki, *J. Chem. Soc., Faraday Trans. 1*, 1988, **84**, 2537–2544.
- 57 H. Liu, G. Cheng, M. Kent, V. Stavila, B. A. Simmons, K. L. Sale and S. Singh, *J. Phys. Chem. B*, 2012, **116**, 8131–8138.
- 58 M. Linder and T. T. Teeri, *Proc. Natl. Acad. Sci. U. S. A.*, 1996, **93**, 12251–12255.
- 59 R. Pinto, S. Moreira, M. Mota and M. Gama, *Langmuir*, 2004, **20**, 1409–1413.
- 60 O. N. Reva, I. E. Zaets, L. P. Ovcharenko, O. E. Kukharenko, S. P. Shpylova, O. V. Podolich, J.-P. de Vera and N. O. Kozyrovska, *AMB Express*, 2015, **5**, 35, DOI: 10.1186/s13568-015-0124-5.

