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## Structural engineering of catalysts for ammonia electrosynthesis from nitrate: recent advances and challenges

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Ammonia (NH<sub>3</sub>) is an indispensable industrial chemical used in fertilizer production and energy carriers. However, its production through the Haber–Bosch process requires high temperature and high pressure, consuming significant energy and releasing large amounts of CO<sub>2</sub>, rendering it unsustainable. As a result, sustainable approaches for ammonia synthesis powered by renewable electricity have gained significant attention, such as the electrocatalytic N<sub>2</sub> reduction reaction (N<sub>2</sub>RR) and nitrate reduction reaction (NitRR). This review summarizes recent advancements in the design strategies of electrocatalysts for the NitRR, highlighting synthetic methods such as doping, alloying, single-atom engineering, nanoconfinement, size-regulation, and tandem catalysis. These strategies aim to tune the adsorption of reactants and intermediates or enhance proton–electron transfer. Future studies could explore new electrocatalysts for efficient NitRR based on the strategies summarized in this review to improve nitrate pollution removal efficiency and ammonia production rates. Furthermore, the challenging questions raised at the end of the paper, such as optimizing the reaction kinetics of the NitRR and improving catalyst selectivity and stability, can provide new directions and insights for future catalyst design.

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### Broader context

The production of ammonia (NH<sub>3</sub>) under mild conditions utilizing renewable energy sources without CO<sub>2</sub> emissions is a promising solution to the energy crisis and environmental concerns. NH<sub>3</sub> electrosynthesis powered by electricity has emerged as an alternative to the Haber–Bosch process, which is energy-consuming and environmentally unfriendly. However, the electrocatalytic nitrate reduction reaction (NitRR) involved in this process is complex and involves a nine-proton and eight-electron transfer process, lowering the overall kinetic rate, lifting the overpotentials, and resulting in unexpected byproducts. Additionally, the competing hydrogen evolution reaction (HER) leads to low faradaic efficiency. Therefore, designing catalysts with good activity and selectivity is crucial. To ensure high performance, research focuses on advancing catalyst design strategies. This review presents the recent advances in designing strategies to construct improved electrocatalysts for the NitRR, highlighting alloy, doping, single-atom engineering, nanoconfinement, size-regulation, and tandem catalysis. These strategies aim to tailor the adsorption of reactants and intermediates or strengthen proton–electron transfer. Although the strategies have shown potential to boost NitRR catalytic activity and efficiency, there are still challenges in the future development of this field, as illustrated at the end of the review.

## Introduction

Nitrogen is an essential element for life in living organisms. The nitrogen cycle plays a crucial role in maintaining the

balance of elements in the biosphere and has a direct impact on human life.<sup>1,2</sup> Unfortunately, anthropogenic activities are severely damaging the nitrogen cycle.<sup>3</sup> For instance, the excessive release of nitrate into the environment poses a significant threat to both the ecological environment and public health.<sup>4</sup> The accumulation of nitrate in rivers and lakes can cause water eutrophication, which is detrimental to aquatic life.<sup>5</sup> In addition, the presence of nitrate in drinking water causes damage to the human endocrine system and leads to severe diseases.<sup>6,7</sup> Moreover, nitrite, produced from nitrate, is a carcinogenic compound that can cause cancer.<sup>8</sup> Therefore, removing nitrate from water is of utmost importance.<sup>9,10</sup> Traditional biological, physical, and

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chemical methods have been used to remove nitrate from water, but they generate secondary pollution and require post-treatment, which limits their widespread use.<sup>11–14</sup> Compared with these technologies, the electrocatalytic nitrate reduction reaction (NitRR) is a promising alternative approach as it uses renewable electricity and operates under mild conditions without producing harmful residues.<sup>4,15–17</sup>

Electrocatalytic nitrate reduction is a promising approach for mitigating and upcycling nitrate pollution by producing ammonia (NH<sub>3</sub>), a valuable chemical commodity.<sup>18,19</sup> NH<sub>3</sub> is not only a crucial synthetic chemical for nitrogen-containing compound production but is also recognized as a carbon-free energy carrier for hydrogen storage.<sup>20,21</sup> Currently, large-scale ammonia production is achieved *via* the energy-intensive Haber–Bosch (H–B) method, which converts N<sub>2</sub> and H<sub>2</sub> to NH<sub>3</sub> under high pressure and temperature. However, the H–B process consumes 1–2% of the world's annual fossil energy and results in roughly 1% of the global annual CO<sub>2</sub> emissions.<sup>22</sup> The electrochemical synthesis of ammonia is a promising alternative that can reduce energy consumption and carbon runoff during industrial production. However, the low solubility of nitrogen in aqueous electrolytes, the difficulties in breaking the triple bond of N<sub>2</sub> (941 kJ mol<sup>-1</sup>), and the suppression of the hydrogen evolution reaction (HER) lead to poor efficiency and limit the further reliable application of the electrochemical nitrogen reduction reaction (NRR). Nitrogen oxides,<sup>23–25</sup> including NO<sub>3</sub><sup>-</sup>, NO<sub>2</sub><sup>-</sup>, NO, and N<sub>2</sub>O, are considered more potential ammonia synthesis pathways due to the lower dissociation energies of the N=O bond (204 kJ mol<sup>-1</sup>) and/or N–O bond (176 kJ mol<sup>-1</sup>). However, nitrogen oxide concentrations are generally lower than those that have been reported. For example, the concentrations of nitrate in industrial wastewater, textile wastewater, and polluted groundwater were only 41.6 mM, 7.4 mM, and 0.9–1.2 mM, respectively, whereas the other nitrogen oxide concentrations were lower. Consequently, potential solutions include concentrating diluted

nitrogen-containing reagents prior to reduction and designing highly selective catalysts suitable for treating low-concentration wastewater. In addition, with the consideration of disturbing species and complex components in real wastewater, the design of electrocatalysts with high anti-interference is more conducive to its practical application. As the major nitrogen pollutant in surface and groundwater, converting NO<sub>3</sub><sup>-</sup> into more valuable ammonia is an effective way to manage the disturbed nitrogen cycle, which has attracted much attention in past decades. However, the NitRR involves the transfer of nine protons coupled with eight electrons, which is a kinetically sluggish process.<sup>26</sup> Moreover, undesired by-products, such as NO<sub>2</sub><sup>-</sup>, N<sub>2</sub>H<sub>4</sub>, and N<sub>2</sub>, generated during the NitRR can affect the selectivity of ammonia production.<sup>27</sup> Additionally, the hydrogen evolution reaction (HER) competes with the NitRR at high overpotential, leading to low faradaic efficiency. To address these challenges, researchers have been focusing on designing efficient electrocatalysts with high selectivity for producing NH<sub>3</sub>.<sup>28</sup>

A large number of catalytic materials have been intensively studied as potential electrocatalysts for the NitRR, including noble metals,<sup>29</sup> transition metals,<sup>30–32</sup> and metal-free catalysts.<sup>33</sup> Recent advances in catalysts have emphasized the importance of catalysts' structure and composition at the nanoscale or even at the atomic level. In this review, we summarize the latest developments in the NitRR for NH<sub>3</sub> production and structural engineering strategies such as electronic structure optimization and mass transport regulation to improve the NitRR activity and selectivity. First, we discuss the possible reaction pathways for nitrate electroreduction to NH<sub>3</sub>. We then categorize a series of design strategies into six sections, alloying, doping, single-atom engineering, size regulation, nanoconfinement, and tandem catalysis as shown in Fig. 1 and Table 1. These strategies aim to either tune the adsorption of reactants and intermediates or enhance proton–electron transfer. Hence, it is necessary to understand in-depth the reaction pathways



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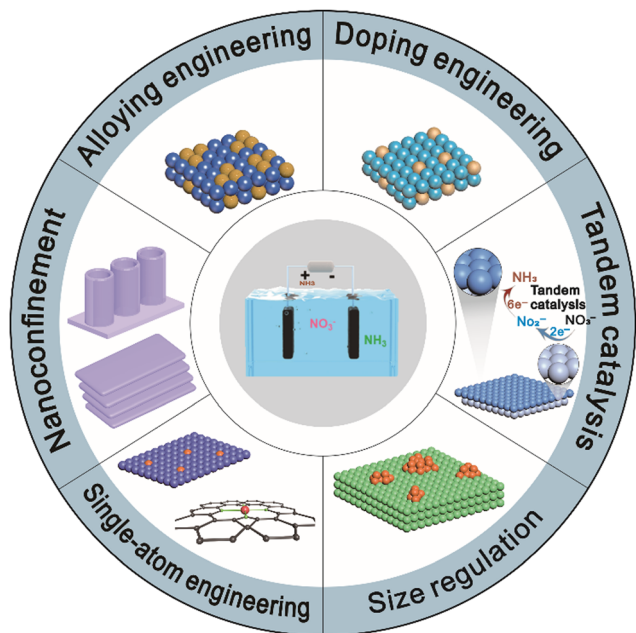


Fig. 1 The schematic illustration of electrocatalyst design strategies for promoting the NitRR performance.

through theoretical calculations and advanced characterization, which can guide the design of enhanced electrocatalysts for the NitRR. Finally, we offer an overview of the current challenges and prospects associated with the design strategies for NitRR catalysts.

## Reaction mechanisms

### Pathways and mechanisms

Understanding the electrocatalytic nitrate reduction reaction mechanism is essential for designing efficient electrocatalysts. This complex process involves the transport of multiple electrons and protons, with various nitrogen oxidation states ranging from  $-3$  to  $+5$ . Among them,  $N_2$  and  $NH_3$  are the most thermodynamically stable forms,<sup>6,34</sup> with  $N_2$  being harmless and environmentally friendly. From the perspective of “upcycling waste to value”,  $NH_3$  is the desirable product. These species are obtained from the following Reactions (1) and (2), respectively. Nitrate electroreduction is divided into two parts, including the indirect autocatalytic reduction pathway and the indirect electrocatalytic reduction pathway.<sup>35</sup> The pathway without nitrate participation is called indirect autocatalytic reduction.<sup>36</sup> Direct nitrate electroreduction involves the regulation of active adsorbed hydrogen atoms ( $H_{ad}$ ) and the electron reduction from the cathode. In the adsorbed-hydrogen-mediated pathway,  $H_2O$  is adsorbed on the electrode surface and then reduced to produce  $H_{ad}$ . Then,  $H_{ad}$  and nitrate are gradually converted into  $NH_4^+$  via intermediates such as  $NO_2^-_{ad}$ ,  $NO_{ad}$ ,  $N_{ad}$ ,  $NH_{ad}$ , and  $NH_{2ad}$ , among others.<sup>37</sup> It is worth noting that two  $N_{ad}$  species combine to form  $N_2$ . The migration barrier of  $N_{ad}$  (0.75 eV) is significantly higher than that of  $H_{ad}$  (0.10 eV). Therefore, the N–N bond is generated less kinetically than the N–H bond.<sup>38</sup>

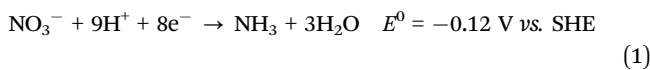


Table 1 The performance of different catalysts for the NitRR

|                       | Catalyst                                      | Electrolyte                            | Faradaic efficiency                      | Ammonia yield rate   | Ref. |
|-----------------------|---|--|--|--|------|
| Alloying              | CuNi alloys                                   | 1.0 M KOH + 0.1 M $KNO_3$              | $99.0 \pm 1\%$ at $-0.15$ V vs. RHE      | N.A.   | 31   |
|                       | CuNi Ns/CF                                    | 1.0 M KOH + 44.3 g $L^{-1}$ $NO_3^-$   | 97.03% at $-0.48$ V vs. RHE              | $94.57 \text{ mg h}^{-1} \text{ cm}^{-2}$ at $-0.48$ V vs. RHE               | 85   |
|                       | PdCu/Cu <sub>2</sub> O hybrids                | 0.5 M $Na_2SO_4$ + 100 ppm $NO_3^-$ -N | 94.32% at $-0.8$ V vs. RHE               | $0.19 \text{ mmol h}^{-1} \text{ cm}^{-2}$ at $-0.8$ V vs. RHE               | 86   |
|                       |   |  |  |  |      |
| Doping                | N–C-1000                                      | 0.1 M KOH + 0.1 M $KNO_3$              | 95% at $-0.7$ V vs. RHE                  | $1.30 \text{ mg h}^{-1} \text{ cm}^{-2}$ at $-0.7$ V vs. RHE                 | 85   |
|                       | B–MoS <sub>2</sub> /CC                        | 0.5 M $Na_2SO_4$ + 0.1 M $NaNO_3$      | 92.3% at $-0.7$ V vs. RHE                | $10.8 \text{ mg h}^{-1} \text{ cm}^{-2}$ at $-0.7$ V vs. RHE                 | 95   |
|                       | Fe/Ni <sub>2</sub> P                          | 0.2 M $K_2SO_4$ + 0.05 M $NO_3^-$      | 94.3% at $-0.4$ V vs. RHE                | $4.17 \text{ mg h}^{-1} \text{ cm}^{-2}$ at $-0.4$ V vs. RHE                 | 96   |
| Single-atom catalysts | Fe–PPy SACs                                   | 0.1 M KOH + 0.1 M $KNO_3$              | $\sim 100.0\%$ at $-0.30$ V vs. RHE      | $2.75 \text{ mg h}^{-1} \text{ cm}^{-2}$ at $-0.7$ V vs. RHE                 | 78   |
|                       | Fe SAC  | 0.25 M $K_2SO_4$ + 0.50 M $KNO_3$      | 75% at $-0.66$ V vs. RHE                 | $20.0 \text{ mg h}^{-1} \text{ cm}^{-2}$ at $-0.85$ V vs. RHE                | 79   |
|                       | Cu– <i>cis</i> -N <sub>2</sub> O <sub>2</sub> | 0.5 M $Na_2SO_4$ + 1000 ppm $KNO_3$ -N | N.A.                                     | $27.84 \text{ mg h}^{-1} \text{ cm}^{-2}$ at $-1.6$ V vs. RHE                | 111  |
|                       | Gd <sub>5A</sub> -D-NiO <sub>400</sub>        | 1.0 M KOH + 1.0 M $KNO_3$              | 97% at $-0.1$ V vs. RHE                  | $0.628 \text{ mg mg}_{cat}^{-1} \text{ h}^{-1}$ at $-0.1$ V vs. RHE          | 77   |
|                       | Ru <sub>1</sub> -TiO <sub>x</sub> /Ti         | 1.0 M KOH + 0.5 M $NaNO_3$             | 87.6% at $-0.3$ V vs. RHE                | $2.2 \text{ mol g}^{-1} \text{ h}^{-1}$ at $-0.3$ V vs. RHE                  | 124  |
|                       | V <sub>Cu</sub> -Au <sub>1</sub> Cu SAAs      | 1.0 M KOH + 0.1 M $KNO_3$              | 98.7% at $-0.2$ V vs. RHE                | $0.55 \text{ mg h}^{-1} \text{ cm}^{-2}$ at $-0.2$ V vs. RHE                 | 125  |
| Size regulation       | Ru NCS/TiO <sub>2</sub> NTs                   | 0.05 M $Na_2SO_4$ + 100 ppm $KNO_3$ -N | $> 90\%$ from $-0.1$ to $-0.4$ V vs. RHE | $600 \mu\text{g h}^{-1} \text{ cm}^{-2}$ at $-0.4$ V vs. RHE                 | 132  |
|                       | Rh@Cu-0.6%                                    | 0.1 M $Na_2SO_4$ + 0.1 M $KNO_3$       | 93.0% at $-0.20$ V vs. RHE               | $1.27 \text{ mmol h}^{-1} \text{ cm}^{-2}$ at $-0.4$ V vs. RHE               | 133  |
| Nanoconfinement       | TiO <sub>2</sub> NTS/CuO <sub>x</sub>         | 0.5 M $Na_2SO_4$ + 100 ppm $KNO_3$ -N  | 92.23% at $-0.75$ V vs. RHE              | $1.24 \text{ mg NH}_3 \text{ cm}^{-2} \text{ h}^{-1}$ at $-0.75$ V vs. RHE   | 138  |
|                       | Cu SAG  | 1.0 M PBS + 20 mM $NO_3^-$             | 78% at $-0.8$ V vs. RHE                  | $440 \mu\text{g cm}^{-2} \text{ h}^{-1}$ at $-0.8$ V vs. RHE                 | 144  |
|                       | PdCu–H  | 0.1 M KOH + 0.1 M $KNO_3$              | 87.3% at $-0.3$ V vs. RHE                | $0.551 \text{ mmol h}^{-1} \text{ mg}^{-1}$ at $-0.3$ V vs. RHE              | 140  |
| Tandem catalysis      | CuCoSP  | 0.1 M KOH + 0.1 M $KNO_3$              | 93.3% at $-0.175$ V vs. RHE              | $19.89 \text{ mg NH}_3 \text{ cm}^{-2} \text{ h}^{-1}$ at $-0.175$ V vs. RHE | 142  |
|                       | Cu nanosheets                                 | 1.0 M KOH + 0.2 M $KNO_3$              | 95% at $-0.36$ V vs. RHE                 | $1.41 \text{ mmol h}^{-1} \text{ cm}^{-2}$ at $-0.59$ V vs. RHE              | 143  |
|                       | FeB <sub>2</sub>                              | 0.1 M KOH + 0.1 M $KNO_3$              | 96.8% at $-0.6$ V vs. RHE                | $25.5 \text{ mg h}^{-1} \text{ cm}^{-2}$ at $-0.6$ V vs. RHE                 | 158  |



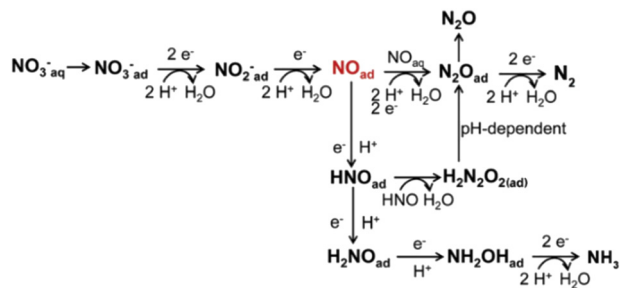


Fig. 2 Reaction pathway diagram for nitrate electroreduction.

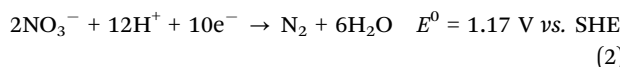
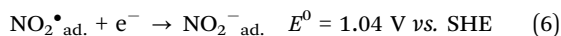
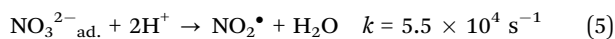
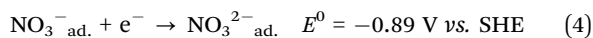
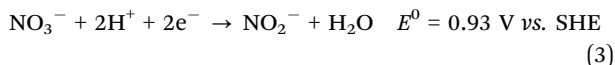
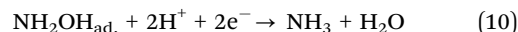
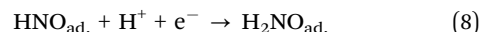


Fig. 2 displays the electron-mediated pathway of nitrate electroreduction. Initially, nitrate is transformed into nitrite.<sup>39–41</sup> The first step of the NitRR is the adsorption of nitrate on the active sites, which is considered to be the rate-determining step.<sup>42,43</sup> Adsorption energy plays a pivotal role in the initiation of the reaction and the adsorption efficiency is related to the nitrate concentration, cathode materials, and the mass transfer rate of reactants.<sup>44,45</sup> After the adsorption step, the electroreduction of  $\text{NO}_3^-$  to nitrite is depicted as Reaction (3), which comprises a proton-coupled double-electron transfer and another proton coupling process successively. This three-step reaction follows an electrochemical–chemical–electrochemical (ECE) mechanism and is known as one of the rate-determining steps during the overall reaction. The first electron transfer reaction ( $\text{NO}_3^-$  to  $\text{NO}_3^{2-}$ ) occurs at a significant negative potential with estimated Tafel slopes of  $120 \text{ mV dec}^{-1}$ .<sup>44</sup> Through the initial electrochemical reduction, a short-lived ( $\approx 20 \text{ }\mu\text{s}$ )  $\text{NO}_3^{2-}$  is generated according to Reaction (4).<sup>39,46</sup> Then, with further homogenous chemical reduction,  $\text{NO}_3^{2-}$  is hydrolyzed to a nitrogen dioxide radical (Reaction (5)).<sup>47,48</sup> Consequently, the second electron transfer reaction converts  $\text{NO}_2^\bullet$  to  $\text{NO}_2^-$  as shown in Reaction (6).<sup>49</sup>



Moreover, nitrite can be reduced to NO by direct electron transfer and a deoxidation process.<sup>42</sup> This step is a divergent center for generating dinitrogen or ammonia. The selectivity of the subsequent pathway is determined by nitric oxide.<sup>50</sup> There are multiple pathways to form  $\text{N}_2$ , while the  $\text{NO}_{\text{ad}}$  intermediate undergoes a continuous charge-transfer path to produce ammonia. One pathway involves the reaction of  $\text{NO}_{\text{ad}}$  with aqueous NO to generate the  $\text{N}_2\text{O}_{\text{ad}}$  intermediate.<sup>51–53</sup>  $\text{N}_2\text{O}_{\text{ad}}$  can be reduced to  $\text{N}_2$  instead of desorbing from the cathode surface.<sup>54,55</sup> The hydrogenation of  $\text{NO}_{\text{ad}}$  produces  $\text{HNO}_{\text{ad}}$  as

per Reaction (7). The produced  $\text{HNO}_{\text{ad}}$  obtains an electron and yields  $\text{H}_2\text{NO}_{\text{ad}}$  according to Reaction (8). Next, the reduction of  $\text{H}_2\text{NO}_{\text{ad}}$  occurs (Reaction (9)), releasing hydroxylamine ( $\text{NH}_2\text{OH}_{\text{ad}}$ ). Finally, the absorbed hydroxylamine is rapidly deoxidized to ammonia by Reaction (10).<sup>56</sup> Many simulations support the large energy barrier in the step of  $\text{NO}_{\text{ad}}$  to  $\text{HNO}_{\text{ad}}$ , making this step the rate-determining step. Another reaction for  $\text{HNO}_{\text{ad}}$  involves rapid dimerization to produce hyponitrous acid ( $\text{H}_2\text{N}_2\text{O}_2$ ).<sup>57,58</sup> However, the monoanionic form ( $\text{HN}_2\text{O}_2^-$ ) is unstable and easily decomposes to give  $\text{N}_2\text{O}$  in a pH-dependent process. Consequently,  $\text{N}_2\text{O}$  can be reduced to  $\text{N}_2$ .<sup>59</sup>



### Catalyst chemical composition

The selectivity of the electrocatalytic reduction-to-nitrate reaction highly depends on the chemical composition of catalysts. Several studies have summarized the activity trends and selectivity of the NitRR on various metals, providing guidelines for catalyst design.<sup>22,52–55</sup> Experimental results have demonstrated the NitRR performance on noble metals in sulfuric acid solutions. Rh has the highest NitRR activity, with the activity decreasing in the order of  $\text{Rh} > \text{Ru} > \text{Ir} > \text{Pt} \approx \text{Pd}$ .<sup>27,60</sup> The high coverage of hydrogen on the active sites of the catalyst could hinder the adsorption of  $\text{NO}_3^-$  and its reduced intermediates, resulting in a low FE for the NitRR. Therefore, noble metals are not desirable catalysts for this reaction. Pt has low activity for the NitRR because of the weak adsorption for  $\text{NO}_3^-$ .<sup>61–63</sup> Yet,  $\text{NH}_3$  FE on the Pd surface is low because of a serious competing HER and complicated intermediates, such as  $\text{NO}_x$ ,  $\text{N}_2\text{H}_4$ , and  $\text{NH}_2\text{OH}$  produced during the pathways from  $\text{NO}_3^-$  to  $\text{NH}_3$ .<sup>64</sup> However, Ru shows a significant increase in  $\text{NH}_3$  FE from 0 V vs. RHE.<sup>65</sup> To optimize the activity for the NitRR, the surface of noble metals can be modified with adatoms or alloys and the synergistic effect is beneficial for nitrate reduction in a tandem catalysis process, such as simultaneous acceleration of sequential  $\text{NO}_3^-$ -to- $\text{NO}_2^-$  and  $\text{NO}_2^-$  reduced to  $\text{N}_2$ ,  $\text{NH}_3$  or other products.<sup>55,66,67</sup>

The premise for achieving high conversion of nitrate to  $\text{NH}_3$  is the moderate H adsorption ability of active sites. Several transition metals are preferred, such as Cu-, Ti-, Co- and Ni-based materials. Among these, Cu dominates and presents the highest activity toward the nitrate reduction reaction, as it can manage the competing HER better than others, including Ag, Au, Ni, Zn, Al, Sn and Bi.<sup>59,68–70</sup> However, undesirable byproducts, such as nitrite, are usually generated during the NitRR when using Cu as the catalyst. The efficiency of Cu-based materials can be improved by modifying or alloying other metals. For instance, Li *et al.* reported a metasequoia-like nanocrystalline  $\text{Cu}_{49}\text{Fe}_1$  catalyst for the NitRR in a neutral



medium.  $\text{Cu}_{49}\text{Fe}_1$  achieved a faradaic efficiency of up to 94.5% and a good  $\text{NH}_3$  selectivity of 86.8% due to the enhanced adsorption of the intermediates *via* a Fe-shifted Cu d-band center.<sup>71</sup>

### Electronic structure

The electronic structure of the catalyst determines the adsorption strength of  $\text{NO}_3^-$  and other reaction intermediates, which considerably influence the NitRR catalytic activity. We could change the electronic structure of catalysts based on various design strategies. With the introduction of other metals,<sup>72–74</sup> elements,<sup>33,75,76</sup> or a single atom,<sup>77–79</sup> the electronic structure of the catalyst surface and the outermost orbital electronic properties can be regulated due to the different properties of dopants and host atoms. These changes include valence, electronegativity, charge density and polarization, which can strengthen orbital hybridization between the electrocatalyst and nitrate or intermediates, thereby improving its adsorption strength.<sup>80</sup> In single-atom catalysts, the surrounding matrix is an effective parameter for modulating the electronic states of the single metal atom due to strong interaction with the coordinated elements. Similarly, regulation of the size of the catalyst to clusters can tune the electronic states of active sites, leading to better activity.

### Catalyst geometry

In addition to chemical composition, geometry is another crucial factor in designing high-activity catalysts, as it closely correlates with reactant delivery and gas diffusion during the catalytic reaction. The electrocatalytic nitrate reduction reaction involves charge transfer and liquid–solid phase mass transport. The development of catalysts with two-dimensional (2D) or three-dimensional (3D) structures is expected to provide liquid channels and gas channels. Pak *et al.*<sup>81</sup> reported that the Ti plate with  $\text{TiO}_2$  nanotube arrays showed improved nitrate reduction efficiency. The nanotube array geometric structure helps the diffusion of nitrate and intermediates. The arrays of vertically aligned metal nanowires leads to high electrocatalytic activity due to their geometry. Napolskii *et al.*<sup>82</sup> prepared highly ordered rhodium nanowire arrays with an average diameter of 55 nm and a length of 1.5–11  $\mu\text{m}$  *via* a template method and used them for the nitrate reduction reaction. The much-increased current density was achieved due to the enhanced mass transport in the shortest Rh nanowires catalyst. To evaluate the effect of layer morphology on transport, Cattarin *et al.*<sup>83</sup> reported that a spongy Cu–Ni alloy layer with bimodal porosity was deposited from vigorous hydrogen evolution using a large current. The Cu–Ni alloy featured in macroscopic pores tens of micrometers in diameter. The porous Cu–Ni alloy electrode showed a higher current due to the enhanced transport.

## Design strategies for electrocatalysts

The dependency of NitRR on the composition and geometry of the electrode has been reported, and therefore the catalyst

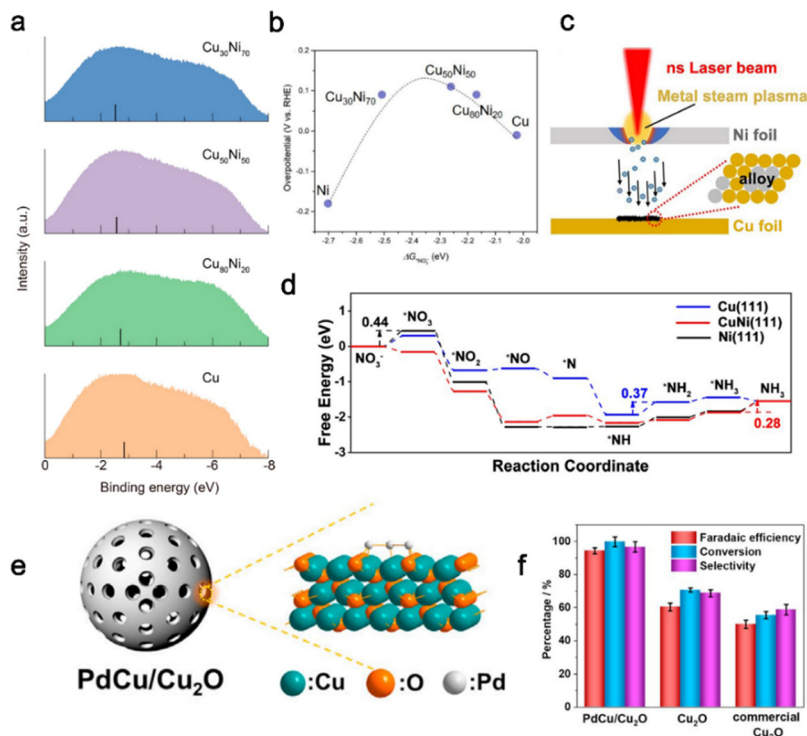
design strategies must take these critical factors into account for achieving excellent selectivity and efficiency. In this section, we aim to provide a summary of recent advances in the investigation of nitrate reduction electrocatalysts, with a focus on design strategies that consider cross-scale interactions over the surface and interface. Our goal is to categorize the design strategies for promoting the intrinsic activity of catalysts based on changes in the local electronic environment of the active centers. In the sections below, we discuss different strategies and provide insights into the structure–activity relationship of electrocatalysts.

### Alloying engineering

Alloy catalysts with metal elements can provide different and active centers,<sup>84</sup> while the multiple compositions of alloy catalysts can tune the d-band center and surface potential,<sup>87–89</sup> influencing the adsorption of reactants and intermediates. In the NitRR field, the alloying catalyst is also a promising design strategy.<sup>72,73,85,90–93</sup> Wang *et al.*<sup>74</sup> synthesized a series of CuNi alloys by adjusting the concentration ratio of Cu and Ni. When Cu : Ni = 50 : 50, the  $\text{Cu}_{50}\text{Ni}_{50}$  exhibited the highest NitRR catalytic activity. The d-band center of CuNi alloys shifts 0.14, 0.28, and 0.32 eV towards the Fermi level with the increase of Ni composition ratio, enhancing the adsorption energy of intermediates (Fig. 3a). From Fig. 3b, the volcanic-type relationship between  $\text{NO}_3^-$  adsorption energy and experimental overpotential on all CuNi alloys indicates the introduction of Ni atoms leads to a higher adsorption energy of  $\text{NO}_3^-$ . However, with increasing Ni concentration, the Cu site decreases, and the adsorption energy of  $^*\text{NH}_2$  intermediates exceeds the optimal value, resulting in a decline in the NitRR performance. Notably, the ratio of two metals in copper–nickel alloy has an important effect on the catalytic performance. To explore the relationship between the proportion of copper–nickel metal and catalytic performance, a series of copper–nickel alloys with different proportions have been reported with carbon substrate. For instance, Dong *et al.*<sup>94</sup> fabricated a series of CuNi alloy nanoparticles embedded in a nitrogen-doped carbon matrix (CuNi/NC) with different Cu–Ni ratios; Liu *et al.*<sup>93</sup> reported a series of Cu–Ni catalysts with component-controllable  $\text{Cu}_x\text{Ni}_y$  nanoparticles encapsulated in N-doped carbon film ( $\text{Cu}_x\text{Ni}_y/\text{NC}$ ).

Except for traditional chemical synthesis, the laser irradiation method is also a fast and facile strategy, which is conducive to the formation of alloys due to the characteristics of rapid heating and cooling during the preparation. Yu *et al.*<sup>85</sup> synthesized CuNi alloy nanoparticles (CuNi NPs/CF) using a laser irradiation method. As shown in Fig. 3c, when the Ni foil located in the upper layer was irradiated by the laser beam, the Ni atoms on its surface absorbed the laser energy and instantly evaporated to produce Ni plasma gas. After the laser treatment, a black CuNi alloy was formed in the corresponding region of the Cu foil surface in the lower layer. CuNi NPs/CF showed excellent NitRR activity with a maximum FE of 97.03% and a highest yield rate of 94.57  $\text{mg h}^{-1} \text{cm}^{-2}$ . By comparing the free energies of  $\text{NO}_3^-$  reduction on CuNi(111), Ni(111), and Cu(111) (Fig. 3d), the energy barrier of the hydrogenation reduction step





**Fig. 3** Alloy engineering. (a) UPS spectra of various CuNi alloys and pure Cu catalysts. (b) The volcano-type relationship between overpotentials of electrocatalytic nitrate reduction and adsorption energies of  $^*NO_3^-$  on all CuNi alloys.<sup>74</sup> Copyright 2020, American Chemistry Society. (c) Mechanism illustration of the laser irradiation process. (d) Free energies for electrocatalytic reduction of nitrate into  $NH_3$  on different catalyst surfaces, respectively.<sup>85</sup> Copyright 2023, The Royal Society of Chemistry. (e) Schematic illustration of mesoporous hollow sphere PdCu/Cu<sub>2</sub>O hybrid structures. (f) Faradaic efficiency and selectivity of ammonia, and the conversion rate of nitrate over different samples.<sup>86</sup> Copyright 2021, Cell Press.

of the intermediate  $^*NH$  was significantly reduced after introducing Ni atoms, which could be attributed to the surrounding Ni sites providing sufficient  $H^*$  to Cu sites. Besides, the Gibbs free energy change ( $\Delta G$ ) of the potential-determining step (PDS) on CuNi(111) was 0.28 eV, while the  $\Delta G$  of PDS on Ni(111) and Cu(111) was 0.44 eV and 0.37 eV, respectively (Fig. 3d), implying a more favorable reaction path on CuNi(111).

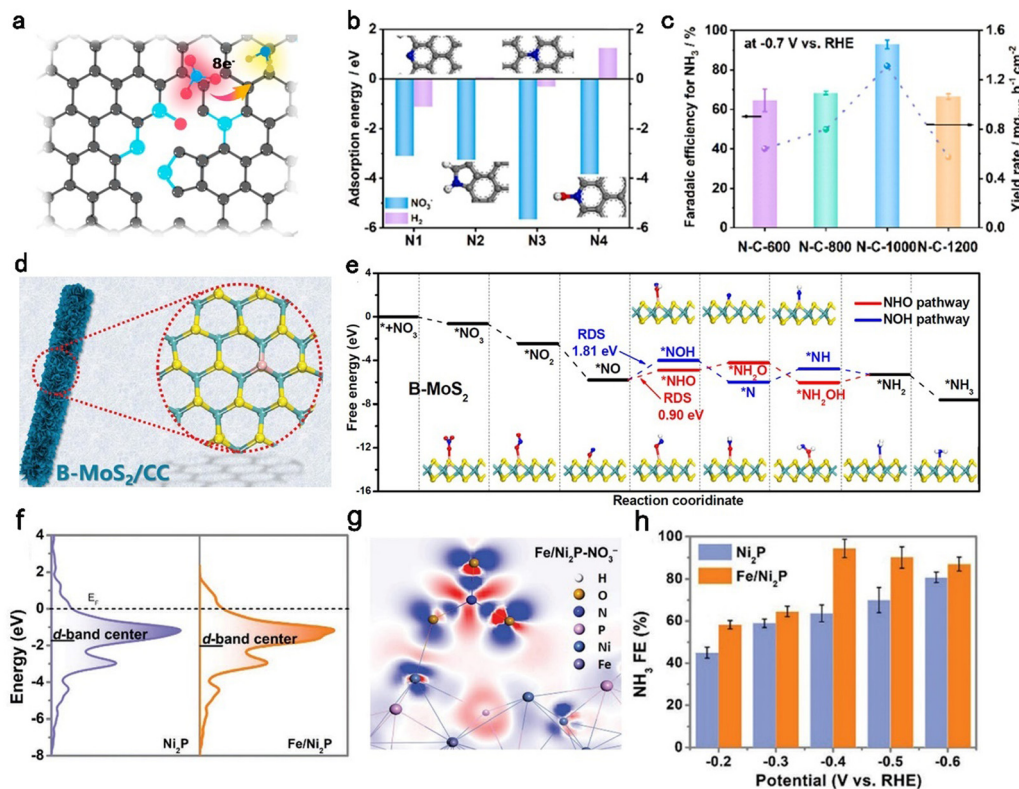
Alloying has presented a unique strategy to tailor the electronic structure of catalysts. Noble metals such as Pd, Pt, Rh and Ag show high activity for nitrate reduction, and many noble metal alloys for the NitRR have been reported, such as PdAg alloys, PtRh alloys, PtIr alloys and PdN alloys. However, due to the high cost and resource scarcity of precious metals, the choice of non-metallic elements is considered more promising. Alloying precious metals with non-metals is an effective option.<sup>97</sup> Yin *et al.*<sup>86</sup> reported a PdCu/Cu<sub>2</sub>O hybrid with a mesoporous hollow sphere structure obtained by depositing Pd species on Cu<sub>2</sub>O (Fig. 3e). Benefitting from the highly dispersed PdCu alloy on the ultrathin Cu<sub>2</sub>O shell, the PdCu/Cu<sub>2</sub>O hybrid exhibits excellent NitRR activity. As shown in Fig. 3f, the maximum values of Faraday efficiency, selectivity, and conversion rate of PdCu/Cu<sub>2</sub>O hybrid reach 94.32%, 96.7%, and 99.82% respectively, which are superior to those of Cu<sub>2</sub>O and commercial Cu<sub>2</sub>O. Further theoretical evidence demonstrates that the existence of PdCu alloy is more conducive to the formation of intermediate  $^*N$  to regulate the reaction

path of ammonia synthesis. Given the advantages of alloys, fabricating commercial catalysts at an industrial scale should be explored extensively. Their composition should be controlled and studied.<sup>98</sup>

### Doping engineering

Doping is considered to be an important approach to optimize the electronic structure of catalysts, thus improving catalytic performance.<sup>99–105</sup> The different electronegativity among elements induces electron transfer and shifts the Fermi energy level of the catalysts, which is crucial for intrinsic activity. Besides, the crystal structure of the catalyst is destroyed once the intrinsic atoms are substituted by heteroatoms. Hence, defects arise along with the change in the crystal structure and give more sites for the reaction intermediates. Additionally, doping is a significant method to increase the number of active sites. Carbon materials with many advantages are employed as catalysts.<sup>25,76,106</sup> Initial studies have reported that carbon-based catalysts doped with heteroatoms can modulate their physicochemical properties and enhance catalytic activity.<sup>75,107–110</sup> Li *et al.*<sup>33</sup> developed a group of carbon-based aerogel catalysts doping different N species for highly efficient nitrate-to-ammonia reduction. Fig. 4a depicts the constructions of four N moieties which are defined as pyridinic-N (N1), pyrrolic-N (N2), graphitic-N (N3), and pyridinic-N-oxide (N4). The adsorption energy of  $NO_3^-$  on each N-C site was determined as  $-3.10$  eV,





**Fig. 4** Doping strategy. (a) Schematic of the structure of the N-C-1000 catalyst. (b) The adsorption energy of  $\text{NO}_3^-$  and hydrogen on pyridinic-N, pyrrolic-N, graphitic-N, and pyridinic-N-oxide moieties, respectively. (c) Faradaic efficiency and yield rate of  $\text{NH}_3$  for N-C-1000.<sup>33</sup> Copyright 2023, Elsevier. (d) Schematic of B-MoS<sub>2</sub>/CC. (e) Free energy diagram of the nitrate reduction to ammonia on B-MoS<sub>2</sub>.<sup>95</sup> Copyright 2022, Elsevier. (f) The d-DOS of the Ni atom on the Fe/Ni<sub>2</sub>P and pristine Ni<sub>2</sub>P. (g) The charge density difference of Fe/Ni<sub>2</sub>P after absorbing  $\text{NO}_3^-$ . (h) FE of Ni<sub>2</sub>P and Fe/Ni<sub>2</sub>P.<sup>96</sup> Copyright 2022, Wiley.

−3.25 eV, −5.66 eV, and −3.84 eV, respectively (Fig. 4b). The highest adsorption energy of  $\text{NO}_3^-$  on N3 suggests this site was favorable for the nitrate reduction reaction. The electrochemical experiments further discovered that N-C-1000 with a maximum of N3 absolute content (1.55 at%) exhibited the highest FE of 95% and YR of 1.3 mg h<sup>−1</sup> cm<sup>−2</sup> at −0.7 V vs. RHE.

This work emphasized the effect of the doping element species on catalytic behaviors in the NitRR.

Compared to the N element, the B element possesses a smaller atomic radius and moderately suitable electronegativity, providing it with a certain capacity to suppress the HER. Luo *et al.*<sup>95</sup> reported a B-doped MoS<sub>2</sub> nanosheet array on carbon cloth (B-MoS<sub>2</sub>/CC, Fig. 4d). The B-MoS<sub>2</sub>/CC reached a maximum FE of 92.3% and YR of 10.8 mg h<sup>−1</sup> cm<sup>−2</sup> at −0.7 V vs. RHE, while the MoS<sub>2</sub>/CC without doping B element only delivered a poor FE of 56.2% and YR of 5.1 mg h<sup>−1</sup> cm<sup>−2</sup>, suggesting that the B-doping effectively improved the catalytic activity of the NitRR. DFT calculations further provided a theoretical understanding of the developed NitRR performance originating from B-doping. The NOH pathway (\*NO→\*NOH) and NHO pathway (\*NO→\*NH) were determined both on B-MoS<sub>2</sub>/CC (Fig. 4e) and MoS<sub>2</sub>/CC. Compared to the two pathways on MoS<sub>2</sub>/CC, the NOH pathway on B-MoS<sub>2</sub>/CC with the lowest rate-determining step energy barrier (0.90 eV) is more favorable for the conversion of  $\text{NO}_3^-$  to  $\text{NH}_3$ .

Except for popular non-metal elements, metal dopants have attracted attention owing to their high activity. Zhang *et al.*<sup>96</sup> synthesized an iron-doped nickel phosphides catalyst (Fe/Ni<sub>2</sub>P) for efficient NitRRs. As depicted in Fig. 4f, Fe doping regulated the electronic structure of Ni atoms with an obvious downshift of the d-band center from −1.73 eV (Ni<sub>2</sub>P) to 0.36 eV (Fe/Ni<sub>2</sub>P). Besides, the charge density differences of Fe/Ni<sub>2</sub>P and Ni<sub>2</sub>P after adsorption of  $\text{NO}_3^-$  illustrated different energy distributions around the active center Ni sites, implying the electronic structure of Ni<sub>2</sub>P was regulated (Fig. 4g). As a result, Fe/Ni<sub>2</sub>P reached a maximum FE of 94.3% with a corresponding YR of 4.17 mg h<sup>−1</sup> cm<sup>−2</sup> for  $\text{NH}_3$  at −0.4 V vs. RHE, which was far higher than that of Ni<sub>2</sub>P (Fig. 4h). Although all types of dopant atoms have their advantages, it is difficult to design and coordinate their respective advantages rationally. More studies should be conducted to achieve quantitative control of heteroatom doping.

### Single-atom engineering

Except for the above polyatomic doping, single-atom doping is a desirable design strategy to develop single-atom catalysts (SACs). SACs demonstrate high atomic utilization, distinct activity, and selectivity,<sup>112–116</sup> which opens up a new avenue for designing efficient catalysts.<sup>117–123</sup> Electronic structures of SACs are highly dependent on the electronegativity and ionic

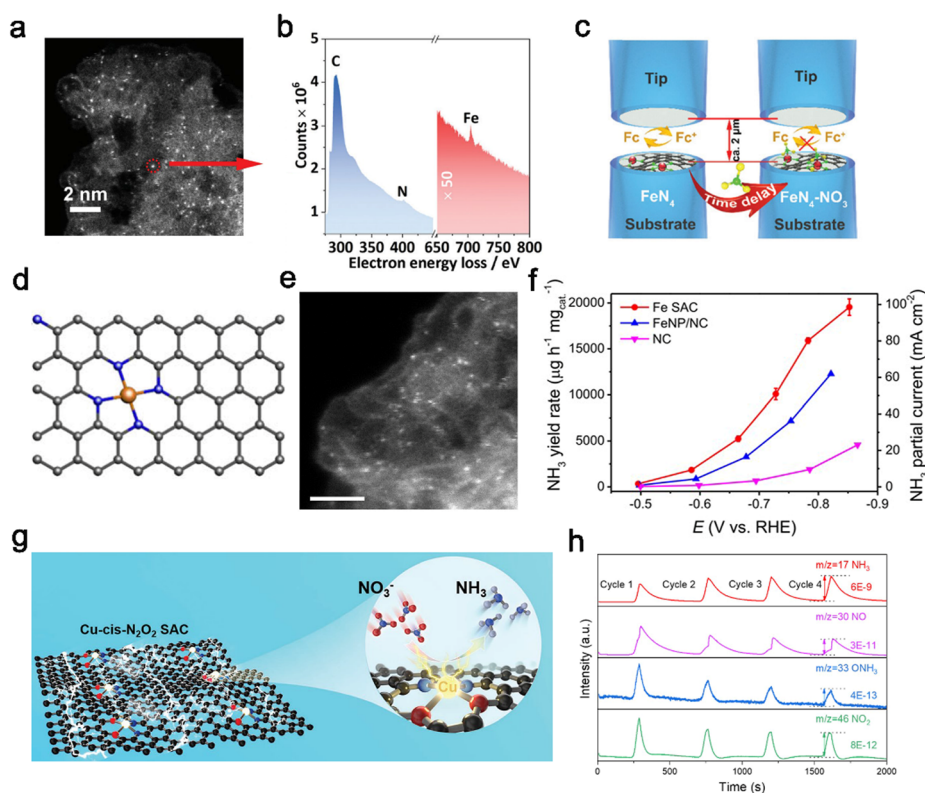


radius of metal centers, affecting the adsorption of reactive species. Additionally, the coordination environment, *e.g.*, coordination atoms and numbers, greatly contributes to tailoring the electronic structure of SACs.<sup>28</sup> Notably, carbon materials have the advantage of the support being sustainable and environmentally friendly,<sup>126</sup> which are considered as important factors for SACs.<sup>127</sup> Fe single-atom catalysts (Fe-PPy SACs) derived from ferric acetylacetonate-polypyrrole hydrogels were reported by Li *et al.*,<sup>78</sup> possessing densely populated Fe active sites and demonstrated high activity for electroreduction of nitrate to ammonia. The Fe(II)-N<sub>x</sub> sites as active centers in Fe-PPy SACs were embedded in carbon support, which were preferentially occupied by NO<sub>3</sub><sup>-</sup> before being reduced to Fe(0)-N<sub>x</sub>. Thus, the competitive hydrogen evolution reactions were inhibited for the lack of active sites to provide water molecules, while the Fe(0) sites in Fe nanoparticles (Fe NP) suffered from fierce competition. The single metal atoms were indicated by the HAADF-STEM image, which showed isolated bright spots with a diameter of *ca.* 0.1 nm. The electron energy loss spectrum (EELS) was collected at a local area of one atom marked in Fig. 5a. Iron, carbon and nitrogen elements were mainly distributed in the selected region in Fig. 5b. Additionally, SI-SECM was employed to time-dependently analyze the site density of the single-site Fe moiety with a dynamic oxidation state toward nitrate reduction and water dissociation at

given potentials (Fig. 5c). Fe-PPy SACs reached a maximum FE of nearly 100% at -0.3 V vs. RHE with a corresponding YR of 2.75 mg NH<sub>3</sub> h<sup>-1</sup> cm<sup>-2</sup>. Besides, at least a twelve-fold turnover frequency difference was observed in Fe-PPy SACs and Fe NP, suggesting the higher producing-NH<sub>3</sub> rate on isolated Fe atoms compared with bulk Fe. Single atomic Fe-N-C catalysts have attracted wide interest for different reactions.<sup>128-130</sup> Particularly, Fe active sites are found in both Haber-Bosch catalysts and nitrogenase enzymes.<sup>131</sup> Inspired by the single-site of iron, Wu *et al.*<sup>79</sup> also designed a Fe single-atom catalyst (Fe SAC) with isolated Fe atoms uniformly embedded in the carbon matrix for reducing NO<sub>3</sub><sup>-</sup> towards NH<sub>3</sub>. The observed results of EXAFS and STEM (Fig. 5e) both demonstrated the Fe-N<sub>4</sub> construction in Fe SAC. In detail, a single Fe atom was coordinated by surrounding four N atoms (Fig. 5d), implying the Fe active sites were atomically dispersed in the N-doped carbon (NC) substrate.

Electrochemical tests showed that the Fe SAC delivered an impressive YR for NH<sub>3</sub> of *ca.* 20 000 μg h<sup>-1</sup> mg<sub>cat</sub><sup>-1</sup>, while Fe nanoparticles only exhibited poor catalytic behaviors (Fig. 5f).

Metallic Cu has relatively high activity for nitrate reduction, but it suffers from poor stability and nitrite accumulation.<sup>134,135</sup> Fortunately, Cu incorporated on carbon support has been studied as a Cu SAC, which presents a superior catalytic performance in comparison to bulk Cu. Cu has been incorporated into PTCDA



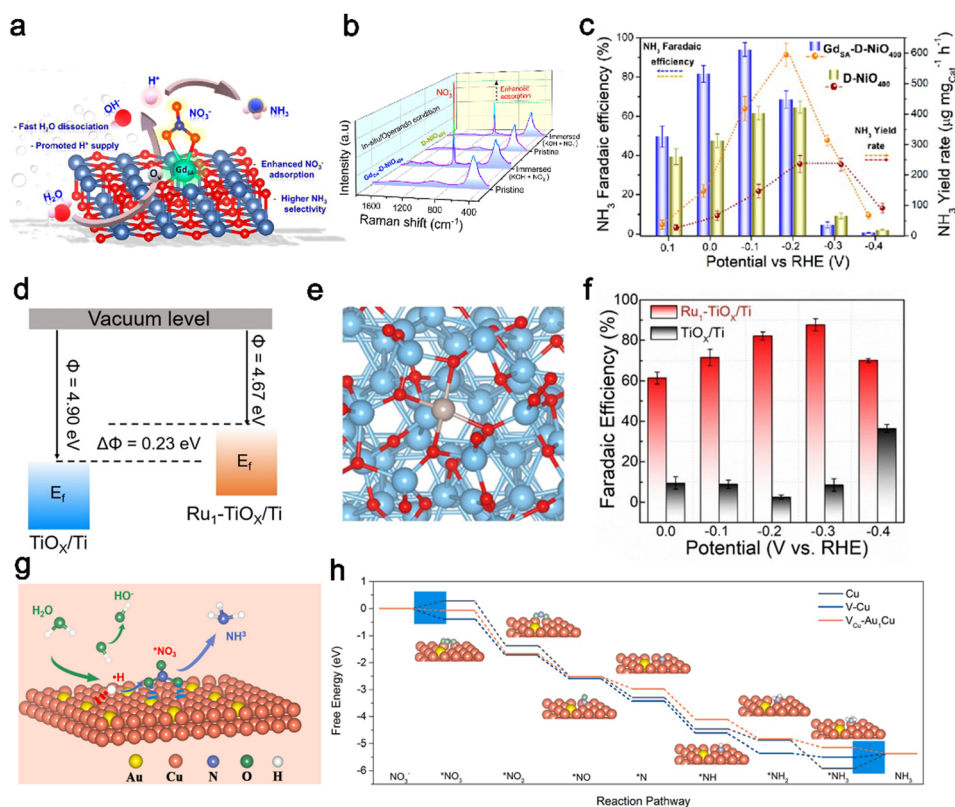
**Fig. 5** Single-atom engineering. (a) HAADF-STEM images of the Fe-PPy SACs. (b) The local EELS of the isolated Fe site. (c) Schematic of the SI-SECM setup for the titration of Fe sites.<sup>78</sup> Copyright 2021, The Royal Society of Chemistry. (d) Schematic illustration of the Fe SAC. (e) AC MAADF-STEM. (f) NH<sub>3</sub> yield rate and partial current density of Fe SAC, FeNP/NC, and NC.<sup>79</sup> Copyright 2021, Springer. (g) Schematic illustration of the Cu-*cis*-N<sub>2</sub>O<sub>2</sub> SAC. (h) DEMS measurements of nitrate reduction reaction over Cu-*cis*-N<sub>2</sub>O<sub>2</sub> SAC.<sup>111</sup> Copyright 2022, Wiley.



(3,4,9,10-perylene-tetracarboxylic dianhydride) for the  $\text{NO}_3^-$ -to- $\text{NH}_3$  reduction reaction with the properties of the proton/electron transfer regulation and HER suppression.<sup>136</sup> More importantly, Feng *et al.* found that Cu single-atom anchored on nitrogenated carbon nanosheets (Cu-N-C) enabled significant alleviation of nitrite production. Nitrite is often observed for metallic Cu catalysts.<sup>137</sup> Furthermore, Cheng *et al.*<sup>111</sup> regulated the locally coordinated atoms of the center Cu single atom from four N atoms to two N and two O atoms, forming a *cis*-configuration Cu single-atom catalyst (Cu-*cis*- $\text{N}_2\text{O}_2$ , Fig. 5g). Moreover, the control catalysts Cu-*trans*- $\text{N}_2\text{O}_2$  in the *trans*-configuration (two N atoms on opposite sides) were prepared to better investigate the coordination symmetry effect. *In situ* online differential electrochemical mass spectrometry (DEMS) was employed to investigate the proposed reaction pathways. The intermediate species  $\text{NH}_3$ ,  $\text{NO}$ ,  $\text{ONH}_3$  and  $\text{NO}_2$  as shown in 5 h, confirmed the reaction pathways. Furthermore, a comparison of the partial density of states of the Cu 3d orbitals in Cu-*trans*- $\text{N}_2\text{O}_2$  and Cu-*cis*- $\text{N}_2\text{O}_2$  indicated that Cu-*cis*- $\text{N}_2\text{O}_2$  was more polar due to the asymmetric structure. The high polarity sites of Cu-*cis*- $\text{N}_2\text{O}_2$  could accumulate more  $\text{NO}_3^-$  around the surface and lower the energy barrier for the limiting step of  $^*\text{NO}$ - $^*\text{ONH}$  by forming a  $\pi$ -complex. Therefore, Cu-*cis*- $\text{N}_2\text{O}_2$  exhibited outstanding NitRR activity with the highest YR of

27.84  $\text{mg h}^{-1} \text{cm}^{-2}$  and impressive durability of continuous operation for more than 2000 h.

Due to strong interactions between a single-atom and substrates, the composition of the substrate is another factor influencing the electronic structure of SAC catalysts. Stable metals and metallic oxides have been investigated as promising candidates to replace the carbon support for anchoring single atoms. The metal oxides possess poor crystallinity with abundant dangling bonds and defects, providing hosts for the dispersion of single atoms.<sup>141</sup> Lee *et al.*<sup>77</sup> reported a highly electron deficient (electrophile) f-block  $\text{Gd}_{\text{SA}}$  stabilized on the surface of an oxygen-defect-rich NiO (denoted as  $\text{Gd}_{\text{SA}}\text{-D-NiO}_{400}$ ) support for efficient  $\text{NO}_3^-$ -to- $\text{NH}_3$  reduction. The synergistic coupling between the highly electron-deficient  $\text{Gd}_{\text{SA}}$  and the defective NiO substrate can significantly enhance the  $\text{NH}_3$  selectivity and yield rate by facilitating stronger  $\text{NO}_3^-$  adsorption, effectively stabilizing the NitRR intermediates and improving the protonation kinetics by capturing  $\text{H}^+$  from water dissociation with a suppressed HER (Fig. 6a). As compared to D-NiO<sub>400</sub>, the  $\text{Gd}_{\text{SA}}\text{-D-NiO}_{400}$  with higher adsorption of  $\text{NO}_3^-$  was revealed by *in situ/operando* Raman measurement (Fig. 6b). The  $\text{Gd}_{\text{SA}}\text{-D-NiO}_{400}$  achieved a maximum  $\text{NH}_3$  FE of ca. 97% at  $-0.1 \text{ V vs. RHE}$  and yield rate of ca.  $628 \mu\text{g mg}_{\text{cat}}^{-1} \text{h}^{-1}$  for the



**Fig. 6** Single-atom engineering. (a) The proposed electrocatalytic nitrate reduction mechanism for the  $\text{Gd}_{\text{SA}}\text{-D-NiO}$  surface assisted *via* fast proton capture from  $\text{H}_2\text{O}$ . (b) *In situ* Raman spectra for  $\text{Gd}_{\text{SA}}\text{-D-NiO}_{400}$  and D-NiO<sub>400</sub> recorded under dry conditions and after immersion in electrolyte (KOH +  $\text{NO}_3^-$ ). (c) FE and mass-normalized YR of  $\text{Gd}_{\text{SA}}\text{-D-NiO}_{400}$  and D-NiO<sub>400</sub>.<sup>77</sup> Copyright 2022, American Chemical Society. (d) Schematic illustration of the work functions of  $\text{Ru}_1\text{-TiO}_x/\text{Ti}$  and  $\text{TiO}_x/\text{Ti}$ .  $E_f$  refers to the Fermi level. (e) Structural model of  $\text{Ru}_1\text{-TiO}_x/\text{Ti}$ . (f) FE of  $\text{NH}_3$  at various potentials.<sup>124</sup> Copyright 2022, Wiley. (g) Schematic illustration of the reaction mechanism for the NitRR on the  $\text{V}_{\text{Cu}}\text{-Au}_1\text{CuSAAs}$  surface. (h) Free energy diagrams for the NitRR to  $\text{NH}_3$  on Cu NSs(111), V-Cu NSs(111) and  $\text{V}_{\text{Cu}}\text{-Au}_1\text{CuSAAs}$ (111) surfaces.<sup>125</sup> Copyright 2023, Wiley.



alkaline NitRR, significantly outperforming the Gd nanoparticles (Gd-NPs), D-NiO, and defect-free Gd<sub>SA</sub>-P-NiO<sub>400</sub> (Fig. 6c).

Similarly, Yao *et al.*<sup>124</sup> proposed an inherent oxide anchoring strategy to synthesize a Ru single-atom monolithic electrode by fastening isolated Ru atoms on the amorphous layer of the Ti support (Ru<sub>1</sub>-TiO<sub>x</sub>/Ti). This method enhanced the metal-support interactions (MSI) effect between Ru single atoms and the Ti support, which played a key role in catalytic performance. Compared with TiO<sub>x</sub>/Ti (4.9 eV), the work function of Ru<sub>1</sub>-TiO<sub>x</sub>/Ti was reduced by 0.23 eV and accompanied by the upward shift of its Fermi level, indicating that metal Ru populated with more electrons into TiO<sub>x</sub>/Ti (Fig. 6d). The charge density difference of Ru<sub>1</sub>-TiO<sub>x</sub>/Ti in Fig. 6e further visualized the enhanced electronic MSI owing to a Bader charge transfer of 0.66 *e* from the Ru atom to the Ti support. Meanwhile, Ru<sub>1</sub>-TiO<sub>x</sub>/Ti exhibited impressive improvement in electrocatalytic behavior for the NitRR. As shown in Fig. 6f, Ru<sub>1</sub>-TiO<sub>x</sub>/Ti reached a maximum FE of 87.6% at -0.3 V with a superior YR of 22.2 mol g<sup>-1</sup> h<sup>-1</sup>, far higher than that of TiO<sub>x</sub>/Ti.

Additionally, Zhang *et al.*<sup>125</sup> synthesized a highly active Au single-atom catalyst for the NitRR by dispersing Au atoms on a Cu(111) surface with further construction of Cu vacancies (V<sub>Cu</sub>-Au<sub>1</sub>Cu SAAs). The Cu vacancies and Au atoms coordinate to regulate the local electronic structure so that V<sub>Cu</sub>-Au<sub>1</sub>Cu SAAs has a stronger ability to capture and crack H<sub>2</sub>O molecules into \*H. As shown in Fig. 6g, the obtained \*H can be devoted to the hydrogenation processes of NO<sub>3</sub><sup>-</sup> and intermediates to ammonia. The free energy on V<sub>Cu</sub>-Au<sub>1</sub>Cu SAAs surfaces is decreased gradually without any uphill step (Fig. 6h), demonstrating that the formation of NH<sub>3</sub> from NO<sub>3</sub><sup>-</sup> on the V<sub>Cu</sub>-Au<sub>1</sub>Cu SAAs(111) was thermodynamically favorable. However, there were energy barriers on the reaction pathways of pure Cu nanosheets (Cu NSs) and Cu NSs with vacancies (V-Cu NSs), resulting in poor NitRR activity and selectivity. Moreover, V<sub>Cu</sub>-Au<sub>1</sub>Cu SAAs(111) exhibited a maximum FE of 98.7% and the highest NH<sub>3</sub> selectivity of 94.5%, much higher than that of Cu NSs (72.9%, 64.6%) and V-Cu NSs (81.1%, 81.4%). Overall, the rapid development of single-atom catalysis in the NitRR field suggests that it is reasonable to obtain robust SACs with high stability, selectivity and activity for industrial important reactions. The development of SACs as tunable catalysts is interesting and promising.

### Size regulation

The catalytic behaviour of ammonia electrosynthesis is dependent upon the electronic structure of the catalyst, determining the adsorption of reactants and other reaction intermediates.<sup>145</sup> Previous literature showed that the N<sub>2</sub> conversion into NH<sub>3</sub> catalyzed by metal nanoparticles (NPs) and nanoclusters (NCs) was relevant to the size of the catalyst.<sup>145-148</sup> With the size of active sites decreasing, more unsaturated coordination sites are exposed and a more efficient atom-utilization rate is achieved. Metal clusters with sizes below about 2 nm show a discrete electronic structure and molecule-like properties. These features are crucial for the performance of catalysts. From the perspective of nitrate electroreduction, electrocatalysts should be designed for

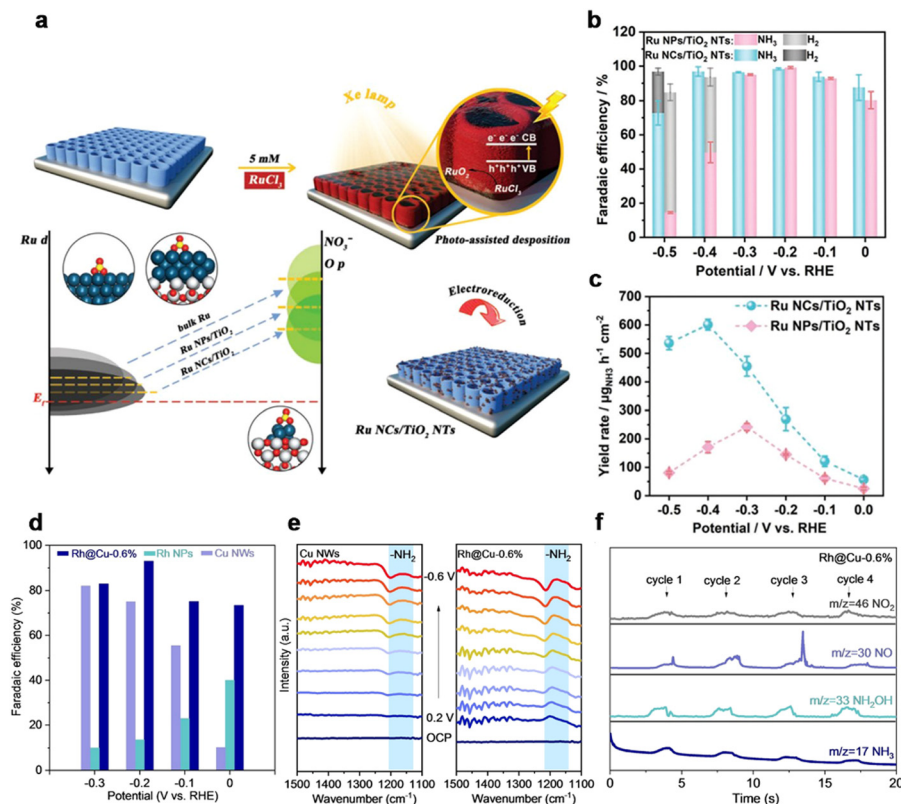
the simultaneous enhancement of the M-N bond and activation of nitrate. The regulation in the size of the catalyst would cause a dramatic tuning in the electronic environment of active centers, which could affect the intrinsic activity of the catalyst for the NitRR. Recently, Li *et al.*<sup>132</sup> reported that Ru-based catalysts with sizes ranging from nanoparticles to nanoclusters demonstrated different performances. The photo-deposition of size-defined Ru nanoclusters (NCs, average size: *ca.* 1.66 nm) on TiO<sub>2</sub> nanotubes (NTs) showed enhanced activity for NO<sub>3</sub><sup>-</sup>-to-NH<sub>3</sub> conversion with a maximum yield of *ca.* 600 μg h<sup>-1</sup> cm<sup>-2</sup> and a Faradaic efficiency (FE) of >90% across a broad range of potential in comparison with electrodeposited Ru nanoparticles (NPs, average size: *ca.* 23.78 nm) on TiO<sub>2</sub> NTs (Fig. 7b and c). In particular, the theoretical calculations revealed that the Ru nanoclusters catalyst with the strong metal/substrate interaction and unsaturated coordination state enabled stronger NO<sub>3</sub><sup>-</sup> affinity, the lower energy barrier of \*NHO intermediate, and the suppressed HER compared with Ru nanoparticles, facilitating the NO<sub>3</sub><sup>-</sup>-to-NH<sub>3</sub> conversion.

Additionally, Lou *et al.* prepared Rh clusters and Rh single-atoms dispersed onto Cu nanowires (NWs) for the NitRR. Rh@Ru-0.6% delivered the highest performance with an FE of 93% at -0.2 V *vs.* RHE and the highest ammonia yield rate of 1.27 mmol h<sup>-1</sup> cm<sup>-2</sup> compared with other catalysts with both lower and higher Rh loadings (Fig. 7d).<sup>133</sup> Higher loading of Rh led to nanoparticles and lower loading resulted in too little Rh doping. *In situ* infrared spectroscopy (IR) results (Fig. 7e) showed an obvious -NH<sub>2</sub> peak when Rh@Cu-0.6% catalyzed the NitRR. On-line differential electrochemical mass spectrometry (DEMS) was used to detect the intermediates during the NitRR (Fig. 7h). DEMS, *in situ* Raman and theoretical calculations proved that the high activity was attributed to the synergistic catalytic cooperation between Rh and Cu sites. Rh single atoms and Rh clusters provided H to \*NO intermediates absorbed on Cu, thus promoting the hydrogenation step and ammonia formation. Ammonia synthesis is sensitive to the electronic states. Regulation of the catalyst's size would cause a dramatic change in electronic structure, which would promote the activity. However, the small size of catalysts might degrade into larger-sized aggregates during the catalytic process, leading to a decline in activity. So, it is crucial to explore a suitable support to immobilize the clusters and keep them stable.

### Nanoconfinement

The fabrication of various nanostructures brings significant opportunities for electrocatalyst designs. One should take notice of the fact that the nanoconfinement effect of an electrocatalyst stems from a unique spatial environment, which would confine the reactant and thus promote interaction between the reactant molecule and the catalyst surface.<sup>149-153</sup> This section induces the nanoconfinement effects in electrocatalysts for confining intermediates during the NitRR and the recent progress in this field. Li *et al.*<sup>138</sup> reported the incorporation of CuO<sub>x</sub> active species into a TiO<sub>2</sub>-nanotube reactor for the NitRR (Fig. 8a). With the help of the experiment and finite element simulations, the nanotubular electrode exhibited remarkably diminished NO<sub>2</sub><sup>-</sup> in contrast to





**Fig. 7** Size regulation. (a) Schematic of Ru nanoclusters loaded on TiO<sub>2</sub> NTs via irradiation. (b) FE of NH<sub>3</sub> and H<sub>2</sub> for Ru NCs/TiO<sub>2</sub> NTs and Ru NPs/TiO<sub>2</sub> NTs at varying potentials. (c) The YR of NH<sub>3</sub> for Ru NCs/TiO<sub>2</sub> NTs and Ru NPs/TiO<sub>2</sub> NTs.<sup>132</sup> Copyright 2023, Wiley. (d) FE of NH<sub>3</sub> over Cu NWs, Rh@Cu-0.6% and carbon cloth loaded with Rh NPs. (e) Electrochemical *in situ* infrared spectroscopy (IR) of Rh@Cu-0.6% and Cu NWs with different potentials at 0.1 M Na<sub>2</sub>SO<sub>4</sub> electrolyte (pH 11.5) with 0.1 M KNO<sub>3</sub>. (f) Differential electrochemical mass spectrometry (DEMS) measurements of the NITRR over Rh@Cu-0.6%.<sup>133</sup> Copyright 2022, Wiley.

planar geometry, confirming the confinement effect toward intermediates (Fig. 8c). Thus, the nanoreactor performed a FE of 92.23% and yield rate of 1241.81  $\mu\text{g h}^{-1} \text{cm}^{-2}$  for ammonia production (Fig. 8b). Furthermore, theoretical calculations were used to give insight into the NitRR mechanism, where TiO<sub>2</sub>/Cu<sub>2</sub>O/Cu active species with a lower energy barrier of \*NHO formation facilitated more favorable NO<sub>3</sub><sup>-</sup>-to-NH<sub>3</sub> conversion efficiency as well as inhibited the HER. Given the confinement effect in strengthening reaction kinetics, Li *et al.*<sup>139</sup> prepared a Cu single-atom gel (Cu SAG) electrocatalyst with spatial confinement. The aberration-corrected high-angle annular dark-field scanning transmission electron microscopy (HAADF-STEM) analysis with the bright spots marked in red circles confirmed the carbon-supported isolated single Cu atoms (Fig. 8d). Cu SAAs revealed a higher NitRR performance in comparison with Cu foil and PPy-C (Fig. 8e). In addition, finite element simulations were performed to demonstrate how the nanoconfinement effect promoted the transformation of the intermediate NO<sub>2</sub><sup>-</sup> within 3D channels of the SAA catalyst during the NitRR.

Moreover, the PdCu hollow (PdCu-H) catalyst was prepared *via in situ* reduction and nucleation of PdCu nanocrystals along a self-assembled micelle of a well-designed surfactant,<sup>140</sup> which aimed to confine the intermediates and promote selective NH<sub>3</sub> electrosynthesis from nitrate (Fig. 8g). The PdCu-H catalyst

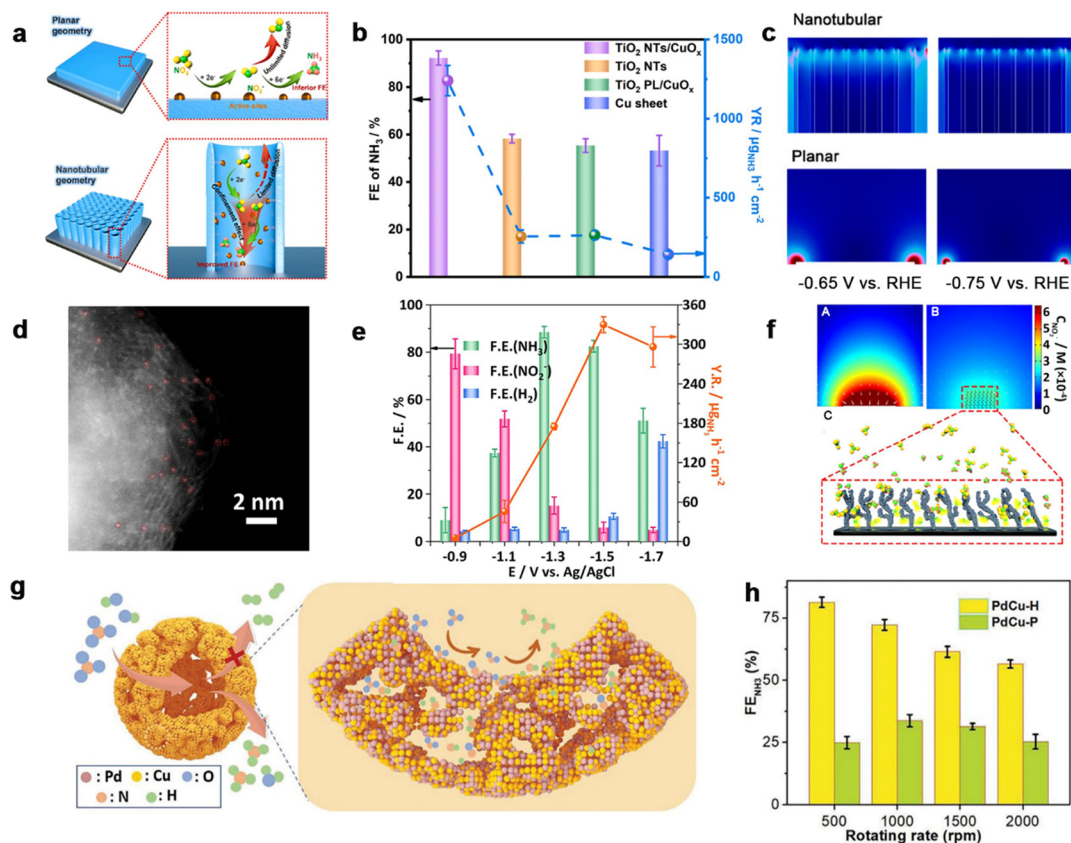
disclosed a high NH<sub>3</sub> FE of 87.3% and a remarkable NH<sub>3</sub> yield rate of 0.551 mmol h<sup>-1</sup> mg<sup>-1</sup> at -0.3 V vs. RHE (Fig. 8h). Mechanism studies were investigated to provide details of the PdCu-H promoted selectivity of NitRR of PdCu-H for NitRR, suggesting that the confinement of a hollow structure not only activated NO<sub>3</sub><sup>-</sup> but also facilitated the deeper electroreduction to NH<sub>3</sub>.

With the development of nanomaterials, nanoconfinement is becoming more important in electrochemistry. The above studies have investigated how the nanoconfinement tunes the NitRR reaction. There should be more studies on the influence of nanoconfinement on the kinetics and selectivities of electrochemical reactions.

### Tandem catalysis

Electroreduction of nitrate to ammonia in microorganisms is a tandem process: combining nitrate reductase enzymes reducing NO<sub>3</sub><sup>-</sup> to NO<sub>2</sub><sup>-</sup> and nitrite reductase converting NO<sub>2</sub><sup>-</sup>-to-NH<sub>3</sub>.<sup>154-156</sup> The enzyme tandem system allows efficient NH<sub>3</sub> generation based on coordination binding with NO<sub>3</sub><sup>-</sup> and NO<sub>2</sub><sup>-</sup>,<sup>157</sup> meanwhile the concept of tandem reaction is implemented in electrocatalyst design for the NitRR. Schuhmann *et al.* coupled the potential-dependent intermediated phase of transition metals as cooperative catalytic sites for cascade NO<sub>3</sub><sup>-</sup>





**Fig. 8** Confinement effect. (a) Schematic illustration of  $\text{NO}_3^-$ -to- $\text{NH}_3$  reduction over an electrode with nanotubular geometries. (b) Comparison of FE of  $\text{NH}_3$  over  $\text{TiO}_2$  NTs/ $\text{CuO}_x$ ,  $\text{TiO}_2$  NTs,  $\text{TiO}_2$  PL/ $\text{CuO}_x$  and Cu sheet at  $-0.75$  V vs. RHE. (c) Simulated  $\text{NO}_2^-$  concentration distribution on nanotubular and planar electrodes.<sup>138</sup> Copyright 2022, Elsevier. (d) Aberration-corrected HAADF-STEM image of Cu SAAs. (e) Faradaic efficiency of products and  $\text{NH}_3$  yield rate of Cu SAAs, Cu foil, and PPy-C at  $-0.9$  V (vs. RHE). (f) A flat electrode (A) and a porous electrode (B) at the same potential, where  $\text{NO}_3^-/\text{NO}_2^-$  and  $\text{NO}_2^-/\text{NH}_4^+$  transformation simultaneously occur. Schematic diffusion process of  $\text{NO}_2^-$  in interconnecting networks (C).<sup>139</sup> Copyright 2023. (f) Schematic illustrations for NitRR over PdCu-P with high selectivity. (g) The relationships between FE of  $\text{NH}_3$  and rotating rates over PdCu-H, PdCu-P, and Pd-P.<sup>140</sup> Copyright 2023, Wiley.

to  $\text{NH}_3$  conversion, demonstrating the tandem catalyst design strategy (Fig. 9a).<sup>142</sup> In this work, Cu/Co-base binary metal sulfides were electrochemically transformed into Cu/CuO<sub>x</sub>-Co/CoO hybrids. The rate constants  $k_1$  and  $k_2$  of each catalyst for  $\text{NO}_3^-$ -to- $\text{NO}_2^-$  and  $\text{NO}_2^-$ -to- $\text{NH}_3$  reactions were evaluated to validate that Cu and Co active phases synergistically catalyze the tandem NitRR (Fig. 9b).

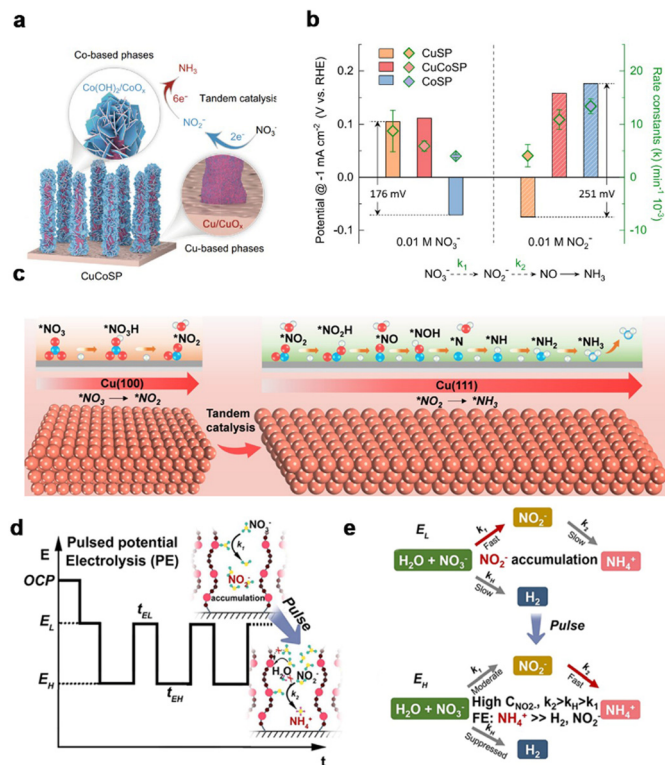
Recently, a tandem catalyst has been developed for enhancing  $\text{NH}_3$  selectivity. Inspired by Cu facets with different adsorption of reactants and intermediates, Wang *et al.*<sup>143</sup> developed Cu nanosheets *in situ* derived from CuO nanosheets to catalyze the NitRR for  $\text{NH}_3$  production. The catalyst delivered an improved  $\text{NH}_3$  yield rate of  $1.41 \text{ mmol h}^{-1} \text{ cm}^{-2}$  and FE of ca. 88% at  $365 \text{ mA cm}^{-2}$ . Electrochemical studies and DFT calculations featured the tandem interaction of the Cu(100) and Cu(111) facets. The Cu(100) facets were responsible for the absorption of  $\text{NO}_3^-$  and conversion of  $\text{NO}_3^-$ -to- $\text{NO}_2^-$ , while the Cu(111) facets contribute to the hydrogenation of  $\text{NO}_2^-$ , thereby promoting the tandem catalysis from  $\text{NO}_3^-$  to  $\text{NH}_3$  (Fig. 9c). As further proof of the advantages of tandem catalysts, Li *et al.* constructed a Cu single-atom gel electrocatalyst for

highly efficient nitrate-to-ammonia conversion enabled by tandem catalysis of unfavorable intermediates.<sup>144</sup> A pulse electro-synthesis strategy was proposed (Fig. 9d) to accumulate the localized nitrite. A locally concentrated  $\text{NO}_2^-$  enabled tandem accumulation-conversion process promoted nitrate-to-ammonia electro reduction (Fig. 9e). In summary, the development of materials for tandem electrocatalysis has attracted attention. Tandem catalysts with multifunctional active sites can promote the selectivity and efficiency of production, by eliminating the unnecessary separation steps and reducing the cost and energy consumption. Additionally, toxic or unstable intermediates can be decreased during tandem catalysis.

## Summary and outlook

The imbalance in the global nitrogen cycle has attracted wide attention, as it causes considerable environmental and human health problems. The removal of nitrates from wastewater has been achieved using different processes including physical, chemical, and biological technologies. Among them,





**Fig. 9** Tandem catalysis. (a) Schematic illustration of the structure of the Cu/Co-based binary “tandem catalyst”. (b) The LSV-derived potentials and the calculated reaction constants for NO<sub>3</sub><sup>-</sup> and NO<sub>2</sub><sup>-</sup> reduction on CuSP, CoSP and CuCoSP catalysts.<sup>142</sup> Copyright 2022, Springer. (c) Tandem interaction of Cu(100) and Cu(111) facets.<sup>143</sup> Copyright 2023, Wiley. (d) Profile of the applied potential for PE. (e) Reaction pathways of the NO<sub>3</sub>RR through the tandem NO<sub>2</sub><sup>-</sup> accumulation–conversion process with PE.<sup>144</sup> Copyright 2023, American Chemical Society.

electrocatalytic nitrate reduction has attracted much attention because of various advantageous features, such as mild operation conditions, high efficiency, and no sludge generation. Besides, this process does not depend on fossil fuels but uses renewable electricity without carbon dioxide emission. Additionally, NH<sub>3</sub> is a key commodity product, which can be used in fertilizers, promising energy carriers, and chemical precursors. From the perspective of addressing environmental pollution and converting waste into value-added products, electroreduction of nitrate to NH<sub>3</sub> opens up the field for an alternative, sustainable route for ammonia synthesis. The storage of large amounts of ammonium nitrate poses a serious explosion risk. Hence, the electrocatalytic NO<sub>3</sub><sup>-</sup>-to-NH<sub>3</sub> conversion can facilitate the production of ammonia on demand, lowering the risk of storage of ammonium nitrate. However, the nitrate reduction reaction is a complicated process including multiple proton and electron transfer. It is hoped to construct catalysts with stability and specific geometric structures, facilitating activation of nitrate and enhancing the mass transfer of protons and electrons. Currently, it is necessary to explore design strategies for electrocatalysts for the practical application of electrocatalytic nitrate reduction technology. The composition, geometric structure, and size of the catalyst are all key factors

that affect the activity of the catalyst. In this review, we have summarized catalyst design strategies for improving the activity and efficiency of the nitrate reduction reaction. First, we discussed the electrocatalytic nitrate reduction reaction mechanism. Then, recent catalyst design strategies for the NitRR were summarized including alloying, doping, single-atom engineering, size regulation, nanoconfinement effect, and tandem catalysis, which are highlighted in the development of efficient tandem catalysts as shown in Table 1. In particular, doping and alloying engineering change the surface electronic structure of active sites, while single-atom engineering and size regulation not only increase the exposure sites but also regulate the electronic structure. Besides, confinement controls the mass transport and tandem catalysis involves cooperative sites that facilitate the proton–electron transfer. Although such strategies enable boosting catalytic efficiency and activity, challenges remain in the future development of this field.

(1) Insight into the mechanism of the nitrate reduction reaction on catalysts provides meaningful guidance for choosing appropriate design strategies. More attention should be paid to tailoring the adsorption strength of NO<sub>3</sub><sup>-</sup> and H<sub>ad</sub>. Strong adsorption of NO<sub>3</sub><sup>-</sup> on the catalyst would be favorable for the NitRR. When the proton affinity of catalyst active sites is high, the competing HER dominates the majority of active sites. The favorable adsorption of H<sub>ad</sub> not only supplies protons for deoxygenation and protonation steps but also prohibits the formation of H<sub>2</sub>. Thus, the coverage of H<sub>ad</sub> should be adjusted by regulating the electronic structure of catalysts. Theoretical calculation is one of the most important methods to describe the electronic structures of catalysts. Therefore, one would focus on the rational theoretical simulation, which could optimize the adsorption of active intermediates and thus suppress the competing side reactions.

(2) During the NitRR process, *in situ* and *operando* characterization methods are significant for monitoring the change of catalyst structure and intermediate generation at a molecular level. For example, attenuated total reflectance surface-enhanced infrared absorption spectroscopy,<sup>159</sup> surface-enhanced Raman spectroscopy,<sup>160</sup> and differential electrochemical mass spectrometry<sup>26</sup> would contribute to providing the adsorption states and conformation of intermediates on the catalyst surface. Additionally, scanning electrochemical microscopy and scanning electrochemical cell microscopy have been recognized as powerful tools for studying the local information at the catalyst surface during various reactions, including products, intermediates, active sites, kinetic rates, *etc.*<sup>161–165</sup> Investigating real-time working state information of the catalyst is crucial for understanding the effects of structure–activity relationships for the nitrate reduction reaction and giving directions for the future electrocatalyst design strategies, thereby promoting the efficiency of this reaction.

(3) With regard to designing an electrocatalyst, stability is another important parameter. It is evaluated by consecutive recycling tests at the optimal potential, and a slight fluctuation in the yield rate and faradaic efficiency of the product ammonia represents the good stability of the catalyst. Good stability of



catalysts is a prerequisite for industrial applications, while the reported catalysts hardly meet the durability standard. After long-time operation, catalysts may encounter related problems *e.g.*, geometric structure collapse, active sites losing activity, corrosion, and others. Along with high efficiency and selectivity, enhancing stability should be considered as part of catalyst designing. We should choose the cathode material with high stability and excellent chemical and physical properties. Besides, we aim to achieve a controllable morphological structure to give good stability and high activity through tuning the edge structure, doping and some other methods.<sup>166–168</sup>

(4) Hydrogen from the competing HER at a large-scale nitrate electroreduction should not be ignored. From the perspective of safety, a mass of hydrogen is prominent. When the concentration of nitrate is low, the HER becomes serious. More research on the selectivity of catalysts for hindering H<sub>2</sub> generation is required. The change in the electronic structure of catalysts could regulate the adsorption of hydrogen to favor ammonia production with suppressed hydrogen evolution.

(5) Moreover, upcycling of nitrate wastes into value-added ammonia is very interesting. It is necessary to extract and collect high-purity ammonia products. Designing catalysts with industrial-relevant current density is one of the key factors for the green and large-scale production of ammonia. Meanwhile, researchers should try to design superior reaction and production conditions, feasible solutions with low energy consumption and low carbon for ammonia collection due to the original intention of environmental protection.

(6) Nowadays, 90% of synthetic ammonia is produced using the Haber–Bosch process, which consumes about 500 kJ to produce 1 mol of NH<sub>3</sub>, equivalent to nearly 4 kW h per kilogram of ammonia produced. The application of reported electrocatalysts to the actual ammonia synthesis industry requires assessing their power consumption in terms of their cell voltage, partial current density, and productivity. For example, the strained ruthenium nanocluster catalyst requires about 22 kW h per kilogram of ammonia produced. However, the price of electricity will constitute a large part of the overall expenses, thus, the cost required for the electrochemical synthesis of marketable NH<sub>4</sub>NO<sub>3</sub> can be directly assessed according to the local electricity price. As a result, the production cost of electrocatalytic ammonia synthesis (approximately \$776 per metric ton ammonium nitrate) is very close to that of the current Haber–Bosch process (\$560 per metric ton). On the other hand, the electricity supply can be replaced by renewable energy in the future, which promotes the reduction of production costs. Overall, the electrochemical synthesis of ammonia has potential economic benefits and is a promising candidate to replace the Haber–Bosch process.

By taking a forward outlook, further advancing the field of electroreduction of nitrate to ammonia may be decisive for an environment compatible energy economy. A well-designed electrocatalyst can boost the activity and selectivity of the NitRR.<sup>139,169</sup> We hope this review helps researchers to develop new catalyst strategies to realize green ammonia electrosynthesis from nitrate under mild conditions. In addition, outstanding

electrocatalysts are encouraged to promote the nitrate electroreduction technology from the laboratory to industry, thereby managing nitrate-rich wastewater.

## Conflicts of interest

There are no conflicts to declare.

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## References

- J. N. Galloway, A. R. Townsend, J. W. Erisman, M. Bekunda, Z. Cai, J. R. Freney, L. A. Martinelli, S. P. Seitzinger and M. A. Sutton, *Science*, 2008, **320**, 889–892.
- D. E. Canfield, A. N. Glazer and P. G. Falkowski, *Science*, 2010, **330**, 192–196.
- J. G. Chen, R. M. Crooks, L. C. Seefeldt, K. L. Bren, R. M. Bullock, M. Y. Darensbourg, P. L. Holland, B. Hoffman, M. J. Janik, A. K. Jones, M. G. Kanatzidis, P. King, K. M. Lancaster, S. V. Lymar, P. Pfromm, W. F. Schneider and R. R. Schrock, *Science*, 2018, **360**, eaar6611.
- M. Duca and M. T. M. Koper, *Energy Environ. Sci.*, 2012, **5**, 9726–9742.
- R. J. Diaz and R. Rosenberg, *Science*, 2008, **321**, 926–929.
- S. Garcia-Segura, M. Lanzarini-Lopes, K. Hristovski and P. Westerhoff, *Appl. Catal., B*, 2018, **236**, 546–568.
- P. J. Weyer, J. R. Kantamneni, X. Lu, M. H. Ward and J. R. Cerhan, *Epidemiology*, 2008, **12**, 327–338.
- J. O. Lundberg, E. Weitzberg, J. A. Cole and N. Benjamin, *Nat. Rev. Microbiol.*, 2004, **2**, 593–602.
- N. Gruber and J. N. Galloway, *Nature*, 2008, **451**, 293–296.
- C. Yu, X. Huang, H. Chen, H. C. J. Godfray, J. S. Wright, J. W. Hall, P. Gong, S. Ni, S. Qiao, G. Huang, Y. Xiao, J. Zhang, Z. Feng, X. Ju, P. Ciais, N. C. Stenseth, D. O. Hessen, Z. Sun, L. Yu, W. Cai, H. Fu, X. Huang, C. Zhang, H. Liu and J. Taylor, *Nature*, 2019, **567**, 516–520.
- R. Epsztein, O. Nir, O. Lahav and M. Green, *Chem. Eng. J.*, 2015, **279**, 372–378.
- A. D. Fonseca, J. G. Crespo, J. S. Almeida and M. A. Reis, *Energy Environ. Sci.*, 2000, **34**, 1557–1562.
- F. Rezvani, M.-H. Sarrafzadeh, S. Ebrahimi and H.-M. Oh, *Environ. Sci. Pollut. Res.*, 2019, **26**, 1124–1141.
- S. Xu, K. Lan, J. Li, T. He and C. Hu, *Sep. Purif. Technol.*, 2018, **204**, 281–289.



- 15 N. Singh and B. R. Goldsmith, *ACS Catal.*, 2020, **10**, 3365–3371.
- 16 B. P. Chaplin, *Acc. Chem. Res.*, 2019, **52**, 596–604.
- 17 Y. Liu, K. Liu, P. Wang, Z. Jin and P. Li, *Carbon Neutrality*, 2023, **2**, 14.
- 18 J. M. McEnaney, S. J. Blair, A. C. Nielander, J. A. Schwalbe, D. M. Koshy, M. Cargnello and T. F. Jaramillo, *ACS Sustainable Chem. Eng.*, 2020, **8**, 2672–2681.
- 19 J. Liang, Q. Liu, A. A. Alshehri and X. Sun, *Nano Res. Energy*, 2022, **1**, e9120010.
- 20 K. E. Lamb, M. D. Dolan and D. F. Kennedy, *Int. J. Hydrogen Energy*, 2019, **44**, 3580–3593.
- 21 J. Cha, T. Lee, Y.-J. Lee, H. Jeong, Y. S. Jo, Y. Kim, S. W. Nam, J. Han, K. B. Lee, C. W. Yoon and H. Sohn, *Appl. Catal., B*, 2021, **283**, 119627.
- 22 C. Smith, A. K. Hill and L. Torrente-Murciano, *Energy Environ. Sci.*, 2020, **13**, 331–344.
- 23 G. Meng, T. Wei, W. Liu, W. Li, S. Zhang, W. Liu, Q. Liu, H. Bao, J. Luo and X. Liu, *Chem. Commun.*, 2022, **58**, 8097–8100.
- 24 T. Wei, H. Bao, X. Wang, S. Zhang, Q. Liu, J. Luo and X. Liu, *ChemCatChem*, 2023, **15**, e202201411.
- 25 D. Qi, F. Lv, T. Wei, M. Jin, G. Meng, S. Zhang, Q. Liu, W. Liu, D. Ma, M. S. Hamdy, J. Luo and X. Liu, *Nano Res. Energy*, 2022, **1**, e9120022.
- 26 X. Zou, C. Chen, C. Wang, Q. Zhang, Z. Yu, H. Wu, C. Zhuo and T. C. Zhang, *Sci. Total Environ.*, 2021, **800**, 149645.
- 27 J. Yang, P. Sebastian, M. Duca, T. Hoogenboom and M. T. M. Koper, *Chem. Commun.*, 2014, **50**, 2148–2151.
- 28 P. Wang, Z. Jin, P. Li and G. Yu, *Chem Catal.*, 2022, **2**, 1277–1287.
- 29 J.-Y. Zhu, Q. Xue, Y.-Y. Xue, Y. Ding, F.-M. Li, P. Jin, P. Chen and Y. Chen, *ACS Appl. Mater. Interfaces*, 2020, **12**, 14064–14070.
- 30 X. Fu, X. Zhao, X. Hu, K. He, Y. Yu, T. Li, Q. Tu, X. Qian, Q. Yue, M. R. Wasielewski and Y. Kang, *Appl. Mater. Today*, 2020, **19**, 100620.
- 31 Y. Wang, W. Zhou, R. Jia, Y. Yu and B. Zhang, *Angew. Chem., Int. Ed.*, 2020, **59**, 5350–5354.
- 32 J. Ding, X. Hou, Y. Qiu, S. Zhang, Q. Liu, J. Luo and X. Liu, *Inorg. Chem. Commun.*, 2023, **151**, 110621.
- 33 R. Li, T. Gao, P. Wang, W. Qiu, K. Liu, Y. Liu, Z. Jin and P. Li, *Appl. Catal., B*, 2023, **331**, 122677.
- 34 Y. Yao, S. Zhu, H. Wang, H. Li and M. Shao, *Angew. Chem., Int. Ed.*, 2020, **59**, 10479–10483.
- 35 Y. Wang, C. Wang, M. Li, Y. Yu and B. Zhang, *Chem. Soc. Rev.*, 2021, **50**, 6720–6733.
- 36 R. Lange, E. Maisonhaute, R. Robin and V. Vivier, *Electrochem. Commun.*, 2013, **29**, 25–28.
- 37 D. Xu, Y. Li, L. Yin, Y. Ji, J. Niu and Y. Yu, *Front. Environ. Sci. Eng.*, 2018, **12**, 9.
- 38 J. Gao, B. Jiang, C. Ni, Y. Qi and X. Bi, *Chem. Eng. J.*, 2020, **382**, 123034.
- 39 A. R. Cook, N. Dimitrijevic, B. W. Dreyfus, D. Meisel, L. A. Curtiss and D. M. Camaioni, *J. Phys. Chem. A*, 2001, **105**, 3658–3666.
- 40 Y. Li, Y. K. Go, H. Ooka, D. He, F. Jin, S. H. Kim and R. Nakamura, *Angew. Chem., Int. Ed.*, 2020, **59**, 9744–9750.
- 41 R. Jia, Y. Wang, C. Wang, Y. Ling, Y. Yu and B. Zhang, *ACS Catal.*, 2020, **10**, 3533–3540.
- 42 Z. Chen, J. Chen, G. Barcaro, T. M. Budnyak, A. Rokicińska, R. Dronskowski, S. Budnyk, P. Kuśtrowski, S. Monti and A. Slabon, *Catal. Sci. Technol.*, 2022, **12**, 3582–3593.
- 43 X. Lu, H. Song, J. Cai and S. Lu, *Electrochem. Commun.*, 2021, **129**, 107094.
- 44 G. E. Dima, A. C. A. de Vooy and M. T. M. Koper, *J. Electroanal. Chem.*, 2003, **554–555**, 15–23.
- 45 C. Zhou, J. Bai, Y. Zhang, J. Li, Z. Li, P. Jiang, F. Fang, M. Zhou, X. Mei and B. Zhou, *J. Hazard. Mater.*, 2021, **401**, 123232.
- 46 H. O. N. Tugaoen, S. Garcia-Segura, K. Hristovski and P. Westerhoff, *Sci. Total Environ.*, 2017, **599–600**, 1524–1551.
- 47 M. Fedurco, P. Kedzierzawski and J. Augustynski, *J. Electrochem. Soc.*, 1999, **146**, 2569.
- 48 R. Tenne, K. Patel, K. Hashimoto and A. Fujishima, *J. Electroanal. Chem.*, 1993, **347**, 409–415.
- 49 M. C. P. M. da Cunha, M. Weber and F. C. Nart, *J. Electroanal. Chem.*, 1996, **414**, 163–170.
- 50 H. Xu, Y. Ma, J. Chen, W.-X. Zhang and J. Yang, *Chem. Soc. Rev.*, 2022, **51**, 2710–2758.
- 51 A. C. A. de Vooy, M. T. M. Koper, R. A. van Santen and J. A. R. van Veen, *Electrochim. Acta*, 2001, **46**, 923–930.
- 52 A. S. Dutton, J. M. Fukuto and K. N. Houk, *Inorg. Chem.*, 2005, **44**, 4024–4028.
- 53 T. Yoshioka, K. Iwase, S. Nakanishi, K. Hashimoto and K. Kamiya, *J. Phys. Chem. C*, 2016, **120**, 15729–15734.
- 54 J. Zheng, T. Lu, T. M. Cotton and G. Chumanov, *J. Phys. Chem. B*, 1999, **103**, 6567–6572.
- 55 J. Yang, M. Duca, K. J. P. Schouten and M. T. M. Koper, *J. Electroanal. Chem.*, 2011, **662**, 87–92.
- 56 Y. Zeng, C. Priest, G. Wang and G. Wu, *Small Methods*, 2020, **4**, 2000672.
- 57 F. T. Bonner and M. N. Hughes, *Comments Inorg. Chem.*, 1988, **7**, 215–234.
- 58 J. F. E. Gootzen, P. G. J. M. Peeters, J. M. B. Dukers, L. Lefferts, W. Visscher and J. A. R. van Veen, *J. Electroanal. Chem.*, 1997, **434**, 171–183.
- 59 I. Katsounaros and G. Kyriacou, *Electrochim. Acta*, 2008, **53**, 5477–5484.
- 60 P. M. Tucker, M. J. Waite and B. E. Hayden, *J. Appl. Electrochem.*, 2004, **34**, 781–796.
- 61 G. E. Dima, G. L. Beltramo and M. T. M. Koper, *Electrochim. Acta*, 2005, **50**, 4318–4326.
- 62 T. Chen, H. Li, H. Ma and M. T. M. Koper, *Langmuir*, 2015, **31**, 3277–3281.
- 63 M. A. Hasnat, N. Ahamad, S. M. Nizam Uddin and N. Mohamed, *Appl. Surf. Sci.*, 2012, **258**, 3309–3314.
- 64 J. Lim, C.-Y. Liu, J. Park, Y.-H. Liu, T. P. Senftle, S. W. Lee and M. C. Hatzell, *ACS Catal.*, 2021, **11**, 7568–7577.
- 65 J. Li, G. Zhan, J. Yang, F. Quan, C. Mao, Y. Liu, B. Wang, F. Lei, L. Li, A. W. M. Chan, L. Xu, Y. Shi, Y. Du, W. Hao,



- P. K. Wong, J. Wang, S.-X. Dou, L. Zhang and J. C. Yu, *J. Am. Chem. Soc.*, 2020, **142**, 7036–7046.
- 66 M. R. Ehrenburg, A. I. Danilov, I. G. Botryakova, E. B. Molodkina and A. V. Rudnev, *J. Electroanal. Chem.*, 2017, **802**, 109–117.
- 67 K.-W. Kim, S.-M. Kim, Y.-H. Kim, E.-H. Lee and K.-Y. Jee, *J. Am. Chem. Soc.*, 2007, **154**, E145.
- 68 H. Liu, J. Park, Y. Chen, Y. Qiu, Y. Cheng, K. Srivastava, S. Gu, B. H. Shanks, L. T. Roling and W. Li, *ACS Catal.*, 2021, **11**, 8431–8442.
- 69 M. Dortsiou and G. Kyriacou, *J. Electroanal. Chem.*, 2009, **630**, 69–74.
- 70 S. Cattarin, *J. Appl. Electrochem.*, 1992, **22**, 1077–1081.
- 71 C. Wang, Z. Liu, T. Hu, J. Li, L. Dong, F. Du, C. Li and C. Guo, *ChemSusChem*, 2021, **14**, 1825–1829.
- 72 V. R. Stamenkovic, B. Fowler, B. S. Mun, G. Wang, P. N. Ross, C. A. Lucas and N. M. Marković, *Science*, 2007, **315**, 493–497.
- 73 D. Kim, J. Resasco, Y. Yu, A. M. Asiri and P. Yang, *Nat. Commun.*, 2014, **5**, 4948.
- 74 Y. Wang, A. Xu, Z. Wang, L. Huang, J. Li, F. Li, J. Wicks, M. Luo, D.-H. Nam, C.-S. Tan, Y. Ding, J. Wu, Y. Lum, C.-T. Dinh, D. Sinton, G. Zheng and E. H. Sargent, *J. Am. Chem. Soc.*, 2020, **142**, 5702–5708.
- 75 Z. Dong, H. Yang, Z. Liu, P. Chen, Y. Chen, X. Wang and H. Chen, *Fuel*, 2021, **303**, 121237.
- 76 S. A. Shah, Z. Ji, X. Shen, X. Yue, G. Zhu, K. Xu, A. Yuan, N. Ullah, J. Zhu, P. Song and X. Li, *ACS Appl. Energy Mater.*, 2019, **2**, 4075–4083.
- 77 A. Kumar, J. Lee, M. G. Kim, B. Debnath, X. Liu, Y. Hwang, Y. Wang, X. Shao, A. R. Jadhav, Y. Liu, H. Tüysüz and H. Lee, *ACS Nano*, 2022, **16**, 15297–15309.
- 78 P. Li, Z. Jin, Z. Fang and G. Yu, *Energy Environ. Sci.*, 2021, **14**, 3522–3531.
- 79 Z.-Y. Wu, M. Karamad, X. Yong, Q. Huang, D. A. Cullen, P. Zhu, C. Xia, Q. Xiao, M. Shakouri, F.-Y. Chen, J. Y. Kim, Y. Xia, K. Heck, Y. Hu, M. S. Wong, Q. Li, I. Gates, S. Siahrostami and H. Wang, *Nat. Commun.*, 2021, **12**, 2870.
- 80 S. Wei, W. Liu, C. Yang, P. Bai, X. Kong, W. Sun and L. Xu, *Mater. Chem. Front.*, 2023, **7**, 4723–4743.
- 81 D. E. Kim and D. Pak, *Chemosphere*, 2019, **228**, 611–618.
- 82 A. P. Leontiev, O. A. Brylev and K. S. Napolskii, *Electrochim. Acta*, 2015, **155**, 466–473.
- 83 L. Mattarozzi, S. Cattarin, N. Comisso, R. Gerbasi, P. Guerriero, M. Musiani, L. Vázquez-Gómez and E. Verlato, *ECS Electrochem. Lett.*, 2013, **2**, D58.
- 84 M. Luo and S. Guo, *Nat. Rev. Mater.*, 2017, **2**, 17059.
- 85 W. Yu, J. Yu, M. Huang, Y. Wang, Y. Wang, J. Li, H. Liu and W. Zhou, *Energy Environ. Sci.*, 2023, **16**, 2991–3001.
- 86 H. Yin, Z. Chen, S. Xiong, J. Chen, C. Wang, R. Wang, Y. Kuwahara, J. Luo, H. Yamashita, Y. Peng and J. Li, *Chem Catal.*, 2021, **1**, 1088–1103.
- 87 H. Miura and T. Shishido, *Chem. Lett.*, 2021, **50**, 346–352.
- 88 A. Lima, C. Coutanceau, J. M. LÉger and C. Lamy, *J. Appl. Electrochem.*, 2001, **31**, 379–386.
- 89 G. Yang, Q. Zhang, H. Yu and F. Peng, *Particuology*, 2021, **58**, 169–186.
- 90 J. K. Nørskov, J. Rossmeisl, A. Logadottir, L. Lindqvist, J. R. Kitchin, T. Bligaard and H. Jónsson, *J. Phys. Chem. B*, 2004, **108**, 17886–17892.
- 91 H. Huang, H. Jia, Z. Liu, P. Gao, J. Zhao, Z. Luo, J. Yang and J. Zeng, *Angew. Chem., Int. Ed.*, 2017, **56**, 3594–3598.
- 92 S. Roy, P. Pachfule and Q. Xu, *Eur. J. Inorg. Chem.*, 2016, 4353–4357.
- 93 L. Fang, S. Wang, C. Song, X. Yang, Y. Li and H. Liu, *J. Hazard. Mater.*, 2022, **421**, 126628.
- 94 Y. Liu, B. Deng, K. Li, H. Wang, Y. Sun and F. Dong, *J. Colloid Interface Sci.*, 2022, **614**, 405–414.
- 95 Y. Luo, K. Chen, P. Shen, X. Li, X. Li, Y. Li and K. Chu, *J. Colloid Interface Sci.*, 2023, **629**, 950–957.
- 96 R. Zhang, Y. Guo, S. Zhang, D. Chen, Y. Zhao, Z. Huang, L. Ma, P. Li, Q. Yang, G. Liang and C. Zhi, *Adv. Energy Mater.*, 2022, **12**, 2103872.
- 97 N. Comisso, S. Cattarin, S. Fiameni, R. Gerbasi, L. Mattarozzi, M. Musiani, L. Vázquez-Gómez and E. Verlato, *Electrochem. Commun.*, 2012, **25**, 91–93.
- 98 P. Zhou, P. Niu, J. Liu, N. Zhang, H. Bai, M. Chen, J. Feng, D. Liu, L. Wang, S. Chen, C. T. Kwok, Y. Tang, R. Li, S. Wang and H. Pan, *Adv. Funct. Mater.*, 2022, **32**, 2202068.
- 99 J. Duan, S. Chen, M. Jaroniec and S. Z. Qiao, *ACS Catal.*, 2015, **5**, 5207–5234.
- 100 R. Kumar, S. Sahoo, E. Joanni, R. K. Singh, K. Maegawa, W. K. Tan, G. Kawamura, K. K. Kar and A. Matsuda, *Mater. Today*, 2020, **39**, 47–65.
- 101 P. Xu, D. Wu, L. Wan, P. Hu and R. Liu, *J. Colloid Interface Sci.*, 2014, **421**, 160–164.
- 102 W. Chen, C. Ge, J. T. Li, J. L. Beckham, Z. Yuan, K. M. Wyss, P. A. Advincula, L. Eddy, C. Kittrell, J. Chen, D. X. Luong, R. A. Carter and J. M. Tour, *ACS Nano*, 2022, **16**, 6646–6656.
- 103 Q. Zhang, D. Zhang, Y. Zhou, J. Qian, X. Wen, P. Jiang, L. Ma, C. Lu, F. Feng and X. Li, *ChemistrySelect*, 2022, **7**, e202102581.
- 104 P. Zhang, Z. Wang, P. Wang, X. Hui, D. Zhao, Z. Zhang and L. Yin, *ACS Appl. Energy Mater.*, 2022, **5**, 3359–3368.
- 105 Y. Liu, Y. Ying, L. Fei, Y. Liu, Q. Hu, G. Zhang, S. Y. Pang, W. Lu, C. L. Mak, X. Luo, L. Zhou, M. Wei and H. Huang, *J. Am. Chem. Soc.*, 2019, **141**, 8136–8145.
- 106 Z. Jin, P. Li and D. Xiao, *ChemSusChem*, 2017, **10**, 483–488.
- 107 X. Wan, F. Shen, J. Hu, M. Huang, L. Zhao, Y. Zeng, D. Tian, G. Yang and Y. Zhang, *Int. J. Biol. Macromol.*, 2021, **180**, 51–60.
- 108 G. Nazir, A. Rehman and S.-J. Park, *J. CO2 Util.*, 2020, **42**, 101326.
- 109 M. Demir, A. A. Farghaly, M. J. Decuir, M. M. Collinson and R. B. Gupta, *Mater. Chem. Phys.*, 2018, **216**, 508–516.
- 110 J. P. Paraknowitsch and A. Thomas, *Energy Environ. Sci.*, 2013, **6**, 2839–2855.
- 111 X.-F. Cheng, J.-H. He, H.-Q. Ji, H.-Y. Zhang, Q. Cao, W.-J. Sun, C.-L. Yan and J.-M. Lu, *Adv. Mater.*, 2022, **34**, 2205767.
- 112 C. Zhu, S. Fu, Q. Shi, D. Du and Y. Lin, *Angew. Chem., Int. Ed.*, 2017, **56**, 13944–13960.



- 113 L. Wang, J. Wang, X. Gao, C. Chen, Y. Da, S. Wang, J. Yang, Z. Wang, J. Song, T. Yao, W. Zhou, H. Zhou and Y. Wu, *J. Am. Chem. Soc.*, 2022, **144**, 15999–16005.
- 114 A. Wang, J. Li and T. Zhang, *Nat. Rev. Chem.*, 2018, **2**, 65–81.
- 115 W. Zhang, X. Qin, T. Wei, Q. Liu, J. Luo and X. Liu, *J. Colloid Interface Sci.*, 2023, **638**, 650–657.
- 116 T. Gao, L. Qiu, M. Xie, Z. Jin, P. Li and G. Yu, *Mater. Horiz.*, 2023, **10**, 4270–4277.
- 117 H. Niu, Z. Zhang, X. Wang, X. Wan, C. Shao and Y. Guo, *Adv. Funct. Mater.*, 2021, **31**, 2008533.
- 118 Y. Pan, R. Lin, Y. Chen, S. Liu, W. Zhu, X. Cao, W. Chen, K. Wu, W.-C. Cheong, Y. Wang, L. Zheng, J. Luo, Y. Lin, Y. Liu, C. Liu, J. Li, Q. Lu, X. Chen, D. Wang, Q. Peng, C. Chen and Y. Li, *J. Am. Chem. Soc.*, 2018, **140**, 4218–4221.
- 119 H. T. Chung, D. A. Cullen, D. Higgins, B. T. Sneed, E. F. Holby, K. L. More and P. Zelenay, *Science*, 2017, **357**, 479–484.
- 120 L. Wang, W. Zhang, S. Wang, Z. Gao, Z. Luo, X. Wang, R. Zeng, A. Li, H. Li, M. Wang, X. Zheng, J. Zhu, W. Zhang, C. Ma, R. Si and J. Zeng, *Nat. Commun.*, 2016, **7**, 14036.
- 121 H. He, H. H. Wang, J. Liu, X. Liu, W. Li and Y. Wang, *Molecules*, 2021, **26**, 6501.
- 122 Y. Liu, W. Qiu, P. Wang, R. Li, K. Liu, K. M. Omer, Z. Jin and P. Li, *Appl. Catal., B*, 2024, **340**, 123228.
- 123 M. Xie, S. Tang, Z. Li, M. Wang, Z. Jin, P. Li, X. Zhan, H. Zhou and G. Yu, *J. Am. Chem. Soc.*, 2023, **145**, 13957–13967.
- 124 Y. Yao, L. Zhao, J. Dai, J. Wang, C. Fang, G. Zhan, Q. Zheng, W. Hou and L. Zhang, *Angew. Chem., Int. Ed.*, 2022, **61**, e202208215.
- 125 Y. Zhang, X. Chen, W. Wang, L. Yin and J. C. Crittenden, *Appl. Catal., B*, 2022, **310**, 121346.
- 126 Z. Chen, S. Mitchell, F. Krumeich, R. Hauert, S. Yakunin, M. V. Kovalenko and J. Pérez-Ramírez, *ACS Sustainable Chem. Eng.*, 2019, **7**, 5223–5230.
- 127 S. Mitchell, E. Vorobyeva and J. Pérez-Ramírez, *Angew. Chem., Int. Ed.*, 2018, **57**, 15316–15329.
- 128 M. Liu, J. Lee, T.-C. Yang, F. Zheng, J. Zhao, C.-M. Yang and L. Y. S. Lee, *Small Methods*, 2021, **5**, 2001165.
- 129 Y. Liu, Z. Zhao, W. Wei, X. Jin, G. Wang, K. Li and Y. Lin, *ACS Appl. Nano Mater.*, 2021, **4**, 13001–13009.
- 130 W.-J. Niu, Y.-Y. Yan, R.-J. Li, W.-W. Zhao, J.-L. Chen, M.-J. Liu, B. Gu, W.-W. Liu and Y.-L. Chueh, *Chem. Eng. J.*, 2023, **456**, 140858.
- 131 Y. Wan, J. Xu and R. Lv, *Mater. Today*, 2019, **27**, 69–90.
- 132 W. Qiu, M. Xie, P. Wang, T. Gao, R. Li, D. Xiao, Z. Jin and P. Li, *Small*, 2023, **19**, 2300437.
- 133 H. Liu, X. Lang, C. Zhu, J. Timoshenko, M. Rüscher, L. Bai, N. Guijarro, H. Yin, Y. Peng, J. Li, Z. Liu, W. Wang, B. R. Cuenya and J. Luo, *Angew. Chem., Int. Ed.*, 2022, **61**, e202202556.
- 134 C. Roy, J. Deschamps, M. H. Martin, E. Bertin, D. Reyter, S. Garbarino, L. Roué and D. Guay, *Appl. Catal., B*, 2016, **187**, 399–407.
- 135 D. Çirimi, R. Aydın and F. Köleli, *J. Electroanal. Chem.*, 2015, **736**, 101–106.
- 136 G.-F. Chen, Y. Yuan, H. Jiang, S.-Y. Ren, L.-X. Ding, L. Ma, T. Wu, J. Lu and H. Wang, *Nat. Energy*, 2020, **5**, 605–613.
- 137 T. Zhu, Q. Chen, P. Liao, W. Duan, S. Liang, Z. Yan and C. Feng, *Small*, 2020, **16**, 2004526.
- 138 W. Qiu, X. Chen, Y. Liu, D. Xiao, P. Wang, R. Li, K. Liu, Z. Jin and P. Li, *Appl. Catal., B*, 2022, **315**, 121548.
- 139 P. Li, L. Liao, Z. Fang, G. Su, Z. Jin and G. Yu, *Proc. Natl. Acad. Sci. U. S. A.*, 2023, **120**, e2305489120.
- 140 X. Min and B. Liu, *Small*, 2023, 2300794.
- 141 N. Daelman, M. Capdevila-Cortada and N. López, *Nat. Mater.*, 2019, **18**, 1215–1221.
- 142 W. He, J. Zhang, S. Dieckhöfer, S. Varhade, A. C. Brix, A. Lielpetere, S. Seisel, J. R. C. Junqueira and W. Schuhmann, *Nat. Commun.*, 2022, **13**, 1129.
- 143 Y. Fu, S. Wang, Y. Wang, P. Wei, J. Shao, T. Liu, G. Wang and X. Bao, *Angew. Chem., Int. Ed.*, 2023, **62**, e202303327.
- 144 P. Li, R. Li, Y. Liu, M. Xie, Z. Jin and G. Yu, *J. Am. Chem. Soc.*, 2023, **145**, 6471–6479.
- 145 L. Li, Y.-F. Jiang, T. Zhang, H. Cai, Y. Zhou, B. Lin, X. Lin, Y. Zheng, L. Zheng, X. Wang, C.-Q. Xu, C.-T. Au, L. Jiang and J. Li, *Chem*, 2022, **8**, 749–768.
- 146 M. Zybert, A. Tarka, W. Patkowski, H. Ronduda, B. Mierzwa, L. Kępiński and W. Raróg-Pilecka, *Catalysts*, 2022, **12**, 1285.
- 147 W. Raróg-Pilecka, E. Miśkiewicz, D. Szmigiel and Z. Kowalczyk, *J. Catal.*, 2005, **231**, 11–19.
- 148 R. Li, T. Gao, W. Qiu, M. Xie, Z. Jin and P. Li, *Nano Res.*, 2023, DOI: [10.1007/s12274-023-6094-z](https://doi.org/10.1007/s12274-023-6094-z).
- 149 M. Seo and T. D. Chung, *Curr. Opin. Electrochem.*, 2019, **13**, 47–54.
- 150 J. Wordsworth, T. M. Benedetti, S. V. Somerville, W. Schuhmann, R. D. Tilley and J. J. Gooding, *Angew. Chem., Int. Ed.*, 2022, **61**, e202200755.
- 151 J. H. Bae, J.-H. Han and T. D. Chung, *Phys. Chem. Chem. Phys.*, 2012, **14**, 448–463.
- 152 H. Li, J. Xiao, Q. Fu and X. Bao, *Proc. Natl. Acad. Sci. U. S. A.*, 2017, **114**, 5930–5934.
- 153 Y. Zhou, S. Chen, S. Xi, Z. Wang, P. Deng, F. Yang, Y. Han, Y. Pang and B. Y. Xia, *Cell Rep. Phys. Sci.*, 2020, **1**, 100182.
- 154 M. Duca, J. R. Weeks, J. G. Fedor, J. H. Weiner and K. A. Vincent, *ChemElectroChem*, 2015, **2**, 1086–1089.
- 155 R. D. Milton and S. D. Minter, *ChemPlusChem*, 2017, **82**, 513–521.
- 156 C. L. Ford, Y. J. Park, E. M. Matson, Z. Gordon and A. R. Fout, *Science*, 2016, **354**, 741–743.
- 157 C. Coelho and M. J. Romão, *Protein Sci.*, 2015, **24**, 1901–1911.
- 158 G. Zhang, X. Li, K. Chen, Y. Guo, D. Ma and K. Chu, *Angew. Chem., Int. Ed.*, 2023, **62**, e202300054.
- 159 Y. Yao, S. Zhu, H. Wang, H. Li and M. Shao, *J. Am. Chem. Soc.*, 2018, **140**, 1496–1501.
- 160 M. J. Weaver, *J. Raman Spectrosc.*, 2002, **33**, 309–317.
- 161 Z. Jin, *Anal. Chem.*, 2023, **95**, 6477–6489.
- 162 Z. Jin and A. J. Bard, *Angew. Chem., Int. Ed.*, 2021, **60**, 794–799.
- 163 Z. Jin, P. Li, Z. Fang and G. Yu, *Acc. Chem. Res.*, 2022, **55**, 759–769.



- 164 Z. Jin, P. Li, Y. Meng, Z. Fang, D. Xiao and G. Yu, *Nat. Catal.*, 2021, **4**, 615–622.
- 165 H. Li, Y. Guo and Z. Jin, *Carbon Neutrality*, 2023, **2**, 22.
- 166 T. Kajana, A. Pirashanthan, D. Velauthapillai, A. Yuvapragasam, S. Yohi, P. Ravirajan and M. Senthilnanthanan, *RSC Adv.*, 2022, **12**, 18041–18062.
- 167 Z. Zhang, S. Tang, X. Lin, C. Liu, S. Hu and Q. Huang, *Appl. Surf. Sci.*, 2022, **584**, 152546.
- 168 R. He, X. Huang and L. Feng, *Energy Fuels*, 2022, **36**, 6675–6694.
- 169 Y. Zhang, S. Li, W. Zheng and X. Wang, *Nano Res. Energy*, 2023, **2**, e9120068.

