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## Balancing atomic hydrogen supply and nitrate electroreduction for enhanced ammonia synthesis on Pt-Cu<sub>2</sub>O/Cu electrocatalysts

Xiaolong Zhu,<sup>a</sup> Rong Chen,<sup>a</sup> Jiahao Tao,<sup>b</sup> Siyi Liang,<sup>c</sup> Kai Zhang<sup>\*b</sup> and Wenzheng Yu<sup>ID \*b</sup>

Electrochemical nitrate reduction to ammonia represents a dual-purpose solution for environmental remediation and sustainable ammonia synthesis, yet faces intrinsic kinetic limitations from inefficient hydrogen adsorption, dominant hydrogen evolution pathways, and undesirable byproduct formation. Addressing these challenges, we engineered Pt-Cu<sub>2</sub>O/Cu-R and Pd-Cu<sub>2</sub>O/Cu-R electrocatalysts via cation exchange. Comprehensive structural characterization confirmed successful synthesis, with Pt-Cu<sub>2</sub>O/Cu-R exhibiting enhanced crystallinity and superior hydrogen adsorption capacity. In 0.1 M NaOH/0.1 M NO<sub>3</sub><sup>-</sup> electrolyte, Pt-Cu<sub>2</sub>O/Cu-R achieved exceptional performance metrics with 86.55% faradaic efficiency and 4.16 mg h<sup>-1</sup> cm<sup>-2</sup> ammonia yield at 75 mA cm<sup>-2</sup>, significantly surpassing Pd-Cu<sub>2</sub>O/Cu-R and unmodified Cu<sub>2</sub>O/Cu-R. *In situ* spectroscopic studies revealed the operative mechanism that persistent Cu<sup>+</sup> species activate nitrogenous intermediates while adjacent platinum sites dissociate water, generating reactive hydrogen for sequential hydrogenation. This activity enhancement originates from platinum's unique ability to optimize the kinetic equilibrium between hydrogen generation and nitrate reduction demands. Furthermore, the catalyst retained outstanding operational stability through 20 consecutive electrolysis cycles, demonstrating negligible performance decay. Our work establishes Pt-Cu<sub>2</sub>O/Cu-R as an efficient and robust platform for sustainable electrochemical ammonia synthesis.

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## Introduction

The imperative to decarbonize ammonia (NH<sub>3</sub>) synthesis, a cornerstone of global agriculture and emerging energy systems, is underscored by the energy- and carbon-intensive Haber–Bosch process, which consumes ~2% of worldwide energy expenditure while relying on fossil-derived H<sub>2</sub>. The electrochemical nitrate reduction reaction (NO<sub>3</sub>RR) presents a transformative alternative, enabling sustainable NH<sub>3</sub> production while remediating pervasive nitrate (NO<sub>3</sub><sup>-</sup>) pollution from industrial effluents and surface waters.<sup>1,2</sup> The ubiquitous presence of NO<sub>3</sub><sup>-</sup> in industrial wastewater and surface water bodies positions the electrochemical NO<sub>3</sub>RR as a dual-action strategy, enabling concurrent nitrate pollution remediation and nitrogen resource recovery. This environmental burden directly drives ecologically catastrophic eutrophication,

carcinogen-contaminated groundwater systems, and methemoglobinemia risks in vulnerable populations.<sup>3</sup> Conventional denitrification technologies, including biological treatment and thermal catalysis, are limited by kinetic constraints, secondary waste generation, and energy-intensive operating conditions. Consequently, efficient electrochemical conversion of waste NO<sub>3</sub><sup>-</sup> into value-added NH<sub>3</sub> emerges as an essential pathway to close the nitrogen loop, simultaneously mitigating ecological damage and establishing a circular economy for fertilizer production.<sup>4–6</sup>

Cathode materials critically determine the efficiency of the electrochemical NO<sub>3</sub>RR to NH<sub>3</sub>, a complex multi-electron/proton transfer process involving eight electrons and nine protons.<sup>9</sup> Extensive research has focused on transition metal catalysts, particularly Cu, Ni, Co, Fe and Sn, due to their tunable d-band electronic structures and variable nitrate adsorption energetics.<sup>7–11</sup> Copper-based electrocatalysts occupy a prominent position in this landscape, offering an optimal balance between cost efficiency and intrinsic ability to stabilize key reaction intermediates (\*NO<sub>3</sub> and \*NO<sub>2</sub>) through favorable orbital hybridization.<sup>12–14</sup> Nevertheless, monometallic Cu systems exhibit intrinsic limitations. Their weak hydrogen binding energy impedes \*H coverage during sequential deoxygenation steps, while unoptimized d-band centers lead to suboptimal N-containing intermediate adsorption, resulting in

<sup>a</sup>Key Lab of Environmental Engineering, Shaanxi Province, Xi'an University of Architecture and Technology, No. 13 Yanta Road, Xi'an 710055, PR China

<sup>b</sup>Key Laboratory of Environmental Aquatic Chemistry, State Key Laboratory of Regional Environment and Sustainability, Research Center for Eco-Environmental Sciences, Chinese Academy of Sciences, Beijing 100085, China. E-mail: [kaizhang@rcees.ac.cn](mailto:kaizhang@rcees.ac.cn); [wzyu@rcees.ac.cn](mailto:wzyu@rcees.ac.cn)

<sup>c</sup>MCC Capital Engineering and Research Incorporation Ltd, 7 Jian'an Street, Beijing Economical and Technological Development Area, Beijing 100176, China



the low faradaic efficiencies for  $\text{NH}_3$  production.<sup>15</sup> These challenges have driven the development of supported copper architectures, where nanostructuring on conductive substrates enhances active site density and modifies electronic properties.<sup>18</sup> Such configurations achieve high  $\text{NH}_3$  selectivity by facilitating nitrate-to-nitrite conversion kinetics and suppressing N–N coupling side reactions.<sup>16–19</sup> However, the rate-determining proton-coupled electron transfer steps remain kinetically sluggish at environmental temperatures due to high activation barriers.<sup>20</sup>

To address this, bifunctional designs incorporating Pd or Pt nanoparticles create catalytically synergistic interfaces.<sup>23</sup> The noble metal components serve as hydrogenation promoters.<sup>21–24</sup> Their near-zero HBE values enable spontaneous  $\text{H}_2$  dissociation and  $^*\text{H}$  spillover onto adjacent Cu sites, maintaining optimal surface  $^*\text{H}$  coverage ( $\theta_{\text{H}} > 0.25$  ML) while dynamically suppressing the hydrogen evolution reaction (HER) through competitive site blocking.<sup>25–28</sup> Besides, Pd/Cu or Pt/Cu interfaces generate interfacial charge redistribution, lowering the energy barrier for  $^*\text{NO}$  dissociation through enhanced back-donation into  $\text{NO} \pi^*$  orbitals.<sup>29,30</sup> This synergistic effect concurrently strengthens adsorption of critical intermediates ( $\text{NH}_2$  and  $\text{NH}$ ) via covalent bonding interactions, improving  $\text{NH}_3$  faradaic efficiencies.<sup>31–33</sup> We thus posit that Pd/Pt-Cu catalysts enable balancing of  $\text{NO}_3^-$  activation and  $^*\text{H}$  supply, enhancing  $\text{NO}_3^-$ -to- $\text{NH}_3$  conversion. Despite demonstrated activity, critical knowledge gaps persist regarding electrode architecture engineering and durability optimization.

To address inherent limitations in hydrogen management, novel Pt- $\text{Cu}_2\text{O}/\text{Cu-R}$  and Pd- $\text{Cu}_2\text{O}/\text{Cu-R}$  electrocatalysts on copper foam were synthesized, specifically engineered for efficient nitrate-to-ammonia conversion. The Pt- $\text{Cu}_2\text{O}/\text{Cu-R}$  variant demonstrated superior performance under identical conditions, achieving maximal  $\text{NH}_3$  yield at  $75 \text{ mA cm}^{-2}$  alongside a faradaic efficiency of 86.55%, substantially exceeding the 75.39% of Pd- $\text{Cu}_2\text{O}/\text{Cu-R}$ . This performance divergence was attributed to distinct metal–support interactions. Combined *in situ* characterization confirmed two critical phenomena: persistent stabilization of  $\text{Cu}^+$  species during nitrate reduction and optimized configuration of key  $^*\text{NO}$  intermediates to facilitate hydrogenation. Mechanistically,  $\text{Cu}^+$  sites activated nitrogen-containing intermediates while adjacent Pt sites dissociated  $\text{H}_2\text{O}$ , supplying reactive hydrogen for sequential hydrogenation steps. Spectroscopic studies definitively identified atomic hydrogen species participating directly in nitrate reduction. Crucially, Pt achieved a more optimal kinetic balance between  $^*\text{H}$  generation and its utilization within the nitrate reduction cascade than Pd, simultaneously minimizing competitive hydrogen evolution. This mechanistic synergy underpinned the exceptional activity and selectivity of Pt- $\text{Cu}_2\text{O}/\text{Cu-R}$ .

## Experimental section

### Preparation of $\text{Cu}_2\text{O}/\text{Cu}$ -based catalysts

Copper membranes (1 mm thickness) were sectioned into pieces measuring 2 cm × 1.5 cm. To remove surface impurities

and oxides and enhance hydrophilicity, the copper pieces underwent a sequential cleaning protocol involving ultrasonic treatment in acetone, 0.1 M aqueous hydrochloric acid, and anhydrous ethanol for 5 min per step. Subsequently, the cleaned membranes were subjected to electrochemical oxidation in a 2 M NaOH electrolyte at a constant current density of  $10 \text{ mA cm}^{-2}$ . This process yielded a dense layer of blue copper hydroxide ( $\text{Cu}(\text{OH})_2$ ) nanowires, serving as the precursor material. Two of the  $\text{Cu}(\text{OH})_2$  nanowire-coated samples were then functionalized *via* immersion in 5 mM solutions of  $\text{PdCl}_2$  and  $\text{PtCl}_2$ , respectively, for 12 h. The third sample remained unmodified as a control. All three samples were subsequently annealed under an oxygen atmosphere (heating rate:  $2 \text{ }^{\circ}\text{C min}^{-1}$ ) at  $200 \text{ }^{\circ}\text{C}$  for 2 h. After cooling to ambient temperature, the samples underwent electrochemical reduction in 1 M NaOH at a constant current of 30 mA for 12 h. This final step produced the target catalysts: Pt- $\text{Cu}_2\text{O}/\text{Cu-R}$ , Pd- $\text{Cu}_2\text{O}/\text{Cu-R}$ , and  $\text{Cu}_2\text{O}/\text{Cu-R}$ .

### Characterization

Phase purity and crystallinity were determined by X-ray diffraction (XRD) (Bruker D8 Advance; Cu  $\text{K}\alpha$ ,  $\lambda = 1.5418 \text{ \AA}$ ). Raman spectroscopy (Renishaw inVia Qontor; 532 nm excitation) was used to identify vibrational modes and defect states. Morphology and elemental distribution were mapped *via* field-emission scanning electron microscopy (FE-SEM) (JEOL JSM-7800) coupled with energy-dispersive X-ray spectroscopy (EDS). Surface chemistry and oxidation states were analyzed by X-ray photoelectron spectroscopy (XPS) (Thermo Scientific Escalab 250Xi). The atomic-scale structure and lattice parameters were resolved by high-resolution transmission electron microscopy (HRTEM) (FEI Tecnai G2 F30). The concentrations of copper (Cu) and platinum (Pt) were then quantitatively determined using Inductively Coupled Plasma Mass Spectrometry (ICP-MS, Agilent 7900).

### Electrochemical measurements

Electrocatalytic nitrate reduction performance was assessed in a standard three-electrode configuration using a Gamry Interface 1010E workstation. The system employed the synthesized catalyst as the working electrode, a platinum foil counter electrode, and an Ag/AgCl (3 M KCl) reference electrode. All measurements utilized an alkaline electrolyte (0.1 M NaOH + 0.1 M  $\text{NaNO}_3$ ) to optimize nitrate reduction kinetics. Linear sweep voltammetry (LSV) and cyclic voltammetry (CV) were performed at  $5 \text{ mV s}^{-1}$  to evaluate electrode activity and reaction pathways. Potentials were converted to the reversible hydrogen electrode (RHE) scale using:  $E_{\text{RHE}} = E_{\text{Ag/AgCl}} + 0.059 \times \text{pH} + 0.200 \text{ V}$ . Electrochemical impedance spectroscopy (EIS) probed interfacial kinetics from 0.01 Hz to 100 kHz with an AC amplitude of 5 mV. During the stability test, 20 cycles of two-hour electrolysis were conducted at  $75 \text{ mA cm}^{-2}$ . The electrolyte was collected after each two-hour electrolysis for product analysis, and fresh electrolyte was used for the next cycle. The  $\text{NH}_3$  faradaic efficiency was calculated according to the following equation:  $\text{FE}_{\text{NH}_3} = N_{\text{NH}_3} V C_{\text{NH}_3} F / Q$ ; in this equation,  $Q$



is the total Coulomb count applied,  $N$  is the electron transfer number (8 for 1 mol  $\text{NH}_3$ ),  $V$  is the cathode chamber's catholyte volume,  $C_{\text{NH}_3}$  is the  $\text{NH}_3$  concentration, and  $F$  is the Faraday constant (96 485 C mol $^{-1}$ ).

### Electron paramagnetic resonance (EPR) measurements

Electron paramagnetic resonance (EPR) spectroscopy (Bruker EMXplus) was employed to detect hydrogen radicals ( $^1\text{H}$ ) using 5,5-dimethyl-1-pyrroline N-oxide (DMPO) as a spin trap. Following electrocatalytic nitrate reduction ( $\text{NO}_3\text{RR}$ ) at  $-0.2$  V vs. RHE for 5 min in 0.1 M NaOH electrolyte with/without 0.1 M  $\text{NO}_3^-$ , 0.5 mL of catholyte from the cathodic chamber was rapidly mixed with 0.2 mL of 0.2 M DMPO. The mixture was transferred *via* capillary tube, and spectra were acquired at room temperature.

### In situ Raman measurements

*In situ* Raman spectroscopy (LabRAM Odyssey, 633 nm excitation) coupled with a CHI760E electrochemical workstation was used to probe reaction intermediates under operational conditions. Catalysts were deposited on glassy carbon working electrodes (3 mm diameter), with Pt wire and Ag/AgCl as counter and reference electrodes, respectively. Measurements commenced at open-circuit potential (OCP) in 0.1 M KOH + 0.1 M  $\text{NaNO}_3$  electrolyte to establish baseline vibrational features. Potentiostatic *in situ* spectra were then acquired from  $+0.2$  V to  $-0.2$  V vs. RHE in 0.1 V increments. At each potential, the system equilibrated for 60 s prior to spectral acquisition to stabilize surface species.

### In situ FTIR spectrometry measurements

*In situ* electrochemical Fourier transform infrared (FTIR) spectroscopy measurements were performed using a Nicolet iN10MX FTIR spectrophotometer (Thermo Fisher Scientific) interfaced with an electrochemical workstation. A custom spectroelectrochemical cell (Tianjin Aida Hengsheng Technology Development Co., Ltd) featured a catalyst-modified Au working electrode at its base. The infrared beam path was configured for reflection from the catalyst surface, passing through a  $\text{CaF}_2$  window and an  $\sim 10$   $\mu\text{m}$  thin-layer electrolyte (0.1 M NaOH + 0.1 M  $\text{NaNO}_3$ ). Potential-dependent FTIR spectra were collected in a time-resolved mode at  $4$  cm $^{-1}$  resolution, averaging 64 scans per spectrum. All experiments were conducted under potentiostatic control, with the applied potential stepped systematically to probe potential-dependent interfacial processes.

### Determination of aqueous-phase N content

A calibration curve relating ammonia concentration to absorbance was established using standard solutions prepared from ammonium chloride ( $\text{NH}_4\text{Cl}$ , dried at 105 °C for 2 h). Ammonia nitrogen ( $\text{NH}_3\text{-N}$ ) quantification employed an optimized salicylic acid method. Following appropriate dilution of the post-reaction electrolyte, 2 mL aliquots were sequentially mixed with: (1) 2 mL chromogenic reagent (1 M NaOH containing 5%

(w/v) salicylic acid and 5% (w/v) sodium citrate); (2) 1 mL of 0.05 M sodium hypochlorite ( $\text{NaClO}$ ) solution; and (3) 200  $\mu\text{L}$  of 1.0% (w/v) sodium nitroferricyanide solution. The reaction mixture was vortex-mixed and incubated in darkness for 2 h to facilitate indophenol blue formation. Absorbance of the resulting chromogen was measured at 655 nm using a Shimadzu UV-2600 spectrophotometer, with each sample analyzed in triplicate.

Nitrite concentrations ( $\text{NO}_2^-$ -N) were quantified by interpolation from a standard calibration curve relating concentration to absorbance. The curve was established using sodium nitrite standard solutions following identical pretreatment protocols. The Griess reagent was prepared by dissolving 2 g sulfanilamide, 0.1 g *N*-(1-naphthyl) ethylenediamine dihydrochloride, and 5 mL phosphoric acid (85% v/v) in 25 mL deionized water. For analysis, the 0.1 mL chromogenic agent was added to the 5 mL diluted sample, followed by vortex mixing and incubation for 20 min at  $25 \pm 1$  °C. Absorbance of the resulting azo dye was measured at 540 nm using a Shimadzu UV-2600 spectrophotometer.

Sodium nitrate ( $\text{NaNO}_3$ ) was dried at 105 °C for 2 h to minimize hydration effects. Standard solutions spanning a concentration gradient were prepared to establish a calibration curve relating nitrate concentration ( $\text{NO}_3^-$ -N) to UV absorbance. For analysis, 5 mL sample aliquots were diluted with deionized water, acidified with 0.1 mL of 6 M HCl (37% w/w), and thoroughly mixed. After 20 min equilibration at 25 °C, absorbance was measured at 220 nm and 275 nm using a Shimadzu UV-2600 spectrophotometer. Nitrite-corrected absorbance ( $A$ ) was calculated as:  $A = A_{220\text{nm}} - 2A_{275\text{nm}}$ , where the factor of 2 corrects for background organic interference.

## Results and discussion

### Synthesis and characterization

These Pt-Cu<sub>2</sub>O/Cu-R, Pd-Cu<sub>2</sub>O/Cu-R, and Cu<sub>2</sub>O/Cu-R materials were synthesized *via* sequential anodization, cation exchange ( $\text{Cu}^{2+}$  with  $\text{Pd}^{2+}/\text{Pt}^{2+}$ ), calcination, and electroreduction (Fig. 1). XRD analysis confirmed the structural evolution. The as-calcined samples exhibited characteristic CuO (JCPDS #45-0937) and Cu<sub>2</sub>O (JCPDS No. 05-0667) diffraction peaks (Fig. S1).<sup>34</sup> After electroreduction, the primary CuO diffraction intensity diminished significantly, accompanied by a concurrent enhancement of Cu<sub>2</sub>O (JCPDS #05-0667) and metallic Cu peaks (Fig. 2a). Notably, the Cu<sub>2</sub>O (111) diffraction peak intensity at 36.4° was highest for Pt-Cu<sub>2</sub>O/Cu-R compared to Pd-

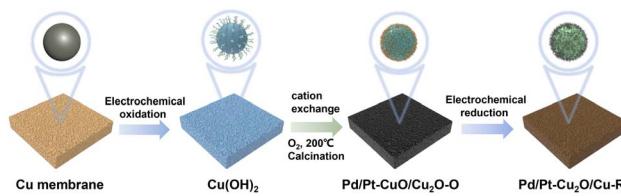


Fig. 1 Schematic illustration of the fabrication process of the Pd/Pt-Cu<sub>2</sub>O/Cu-R membrane.



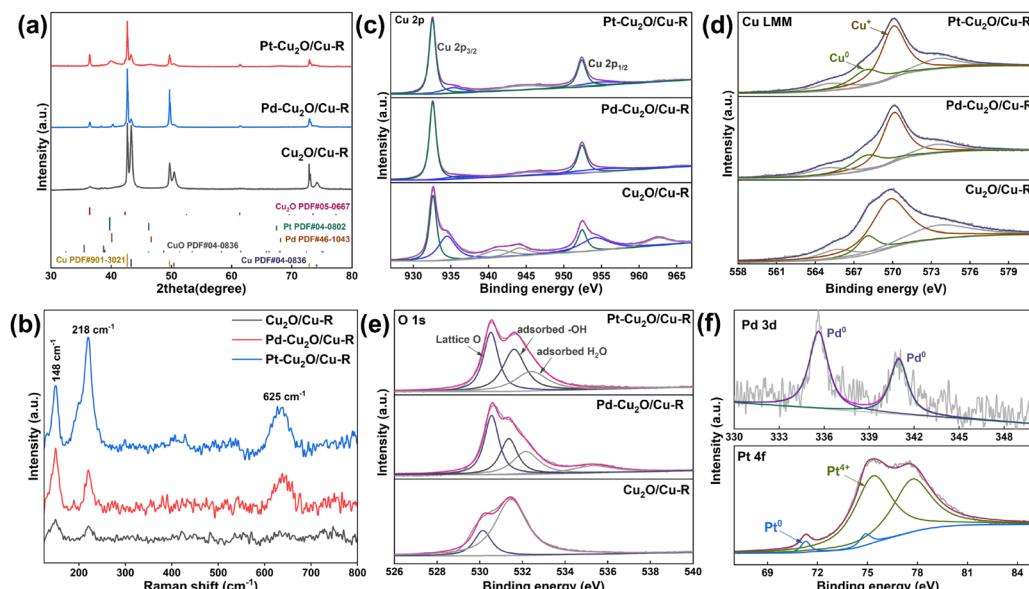


Fig. 2 (a) XRD patterns and (b) Raman spectra of Pt-Cu<sub>2</sub>O/Cu-R, Pd-Cu<sub>2</sub>O/Cu-R, and Cu<sub>2</sub>O/Cu-R; XPS spectra of Pt-Cu<sub>2</sub>O/Cu-R, Pd-Cu<sub>2</sub>O/Cu-R, and Cu<sub>2</sub>O/Cu-R: (c) Cu 2p; (d) AES spectra of Cu LMM; (e) O 1s and (f) Pd 3d and Pt 4f.

Cu<sub>2</sub>O/Cu-R and Cu<sub>2</sub>O/Cu-R. Furthermore, distinct diffraction peaks corresponding to the Pt (111) and Pd (111) planes were evident in Pt-Cu<sub>2</sub>O/Cu-R and Pd-Cu<sub>2</sub>O/Cu-R samples, respectively (Fig. 2a).<sup>35</sup> Raman spectra of the Cu oxide-based electrodes are presented in Fig. S2 and 2b. CuO and Cu<sub>2</sub>O exhibited distinct Cu–O vibrational modes. Characteristic Raman peaks for CuO were observed at 294 cm<sup>-1</sup>, 347 cm<sup>-1</sup>, and 635 cm<sup>-1</sup>.<sup>12</sup> After electroreduction, the spectrum revealed features attributable to Cu<sub>2</sub>O: an IR-active peak at 148 cm<sup>-1</sup>, a second-order overtone at 218 cm<sup>-1</sup>, and a Cu–O stretching vibration at 625 cm<sup>-1</sup>. No characteristic Raman peaks were observed for Pd or Pt within the analyzed spectral range.<sup>36</sup>

X-ray photoelectron spectroscopy (XPS) analysis elucidated the valence states of the catalytic electrodes. Deconvolution of Cu 2p core levels (Fig. S3a) revealed peaks at 932.8 eV (2p<sub>3/2</sub>) and 952.6 eV (2p<sub>1/2</sub>) characteristic of Cu<sup>+</sup>/Cu<sup>0</sup>, alongside Cu<sup>2+</sup> signatures at 934.8 eV and 954.7 eV. The prominent Cu LMM peak observed in Fig. S3b corresponded to the main Cu<sup>2+</sup> species. Post-electroreduction spectra exhibited dominant Cu<sup>+</sup>/Cu<sup>0</sup> peaks at 932.6 eV and 952.4 eV, with a residual Cu<sup>2+</sup> feature attributable to surface oxidation (Fig. 2c).<sup>37</sup> Complementary X-ray-induced Auger electron spectroscopy (AES) resolved this ambiguity. The prominent Cu LMM peak at 570.1 eV confirmed Cu<sub>2</sub>O, while a weaker feature at 568.1 eV corresponded to Cu<sup>0</sup> (Fig. 2d).<sup>38</sup> Deconvoluted O 1s spectra (Fig. S4 and 2e) showed lattice oxygen (530.6 eV), adsorbed -OH (531.5 eV), and adsorbed H<sub>2</sub>O (532.4 eV). Noble metal states were unequivocally assigned. Pt-CuO/Cu<sub>2</sub>O-O exhibited Pt 4f peaks at 77.3 eV and 79.6 eV (Fig. S5). Deconvolution of Pt 4f spectra in Pt-Cu<sub>2</sub>O/Cu-R revealed two spin-orbit doublets, indicating that Pt<sup>4+</sup> at 75.4 eV and 77.8 eV dominated with minimal Pt<sup>0</sup> contribution, consistent with surface oxidation during air exposure (Fig. 2f).<sup>39</sup> Partial oxidation of Pt species suggested electronic metal–support interactions with Cu<sub>2</sub>O. As shown in Fig. S4, Pd-CuO/Cu<sub>2</sub>O-O

demonstrated Pd<sup>2+</sup> peaks at 337.1 eV and 342.9 eV. Pd-Cu<sub>2</sub>O/Cu-R showed Pd 3d<sub>5/2</sub> and 3d<sub>3/2</sub> peaks. Besides, Pd-Cu<sub>2</sub>O/Cu-R exhibited binding energies at 336.3 eV and 341.5 eV, confirming Pd<sup>0</sup> dominance (Fig. 2f).<sup>40</sup>

Scanning electron microscopy (SEM) imaging revealed Cu<sub>2</sub>O nanorods composed of micrometre-long nanowires (Fig. 3a). Sequential treatments generated a Pd-Cu<sub>2</sub>O/Cu-R composite, with Pd nanospheres decorating the Cu<sub>2</sub>O nanorod surfaces (Fig. 3b). Conversely, Pt deposition preserved the pristine Cu<sub>2</sub>O nanorod morphology (Fig. 3c). The SEM images of CuO/Cu<sub>2</sub>O-O, Pd-CuO/Cu<sub>2</sub>O-O, Pt-CuO/Cu<sub>2</sub>O-O are also clearly demonstrated in Fig. S6–S8. Energy-Dispersive X-ray (EDX) spectroscopy elemental mapping confirmed the homogeneous distribution of Cu and O within the Cu<sub>2</sub>O/Cu-R composite (Fig. 3d). After Pd deposition, EDX mapping revealed uniform distributions of Cu, O, and Pd throughout the Pd-Cu<sub>2</sub>O/Cu-R sample (Fig. 3e). A similarly homogeneous distribution of Cu, O, and Pt was observed for Pt-Cu<sub>2</sub>O/Cu-R (Fig. 3f). Inductively coupled plasma-optical emission spectrometry (ICP-OES) analysis determined Pd and Pt loadings of approximately 4.2 wt% and 5.8 wt% in Pd-Cu<sub>2</sub>O/Cu-R and Pt-Cu<sub>2</sub>O/Cu-R, respectively. Transmission electron microscopy (TEM) analysis identified lattice spacings of 0.246 nm and 0.213 nm, corresponding to the Cu<sub>2</sub>O (111) and (200) planes (Fig. 3g). Spacings of 0.213 nm for Cu<sub>2</sub>O (200) and 0.224 nm for Pd (111) were resolved at the Pd/Cu<sub>2</sub>O interface (Fig. 3i). Similarly, spacings of 0.213 nm for Cu<sub>2</sub>O (200) and 0.195 nm for Pt (200) were measured at the Pt/Cu<sub>2</sub>O interface in the Pt-Cu<sub>2</sub>O/Cu-R composite (Fig. 3i).

### Electrocatalytic properties of the NO<sub>3</sub>RR

We systematically assessed nitrate reduction reaction performance in pretreated catalytic electrodes using a standard three-electrode H-cell configuration. Electrochemical evaluation in



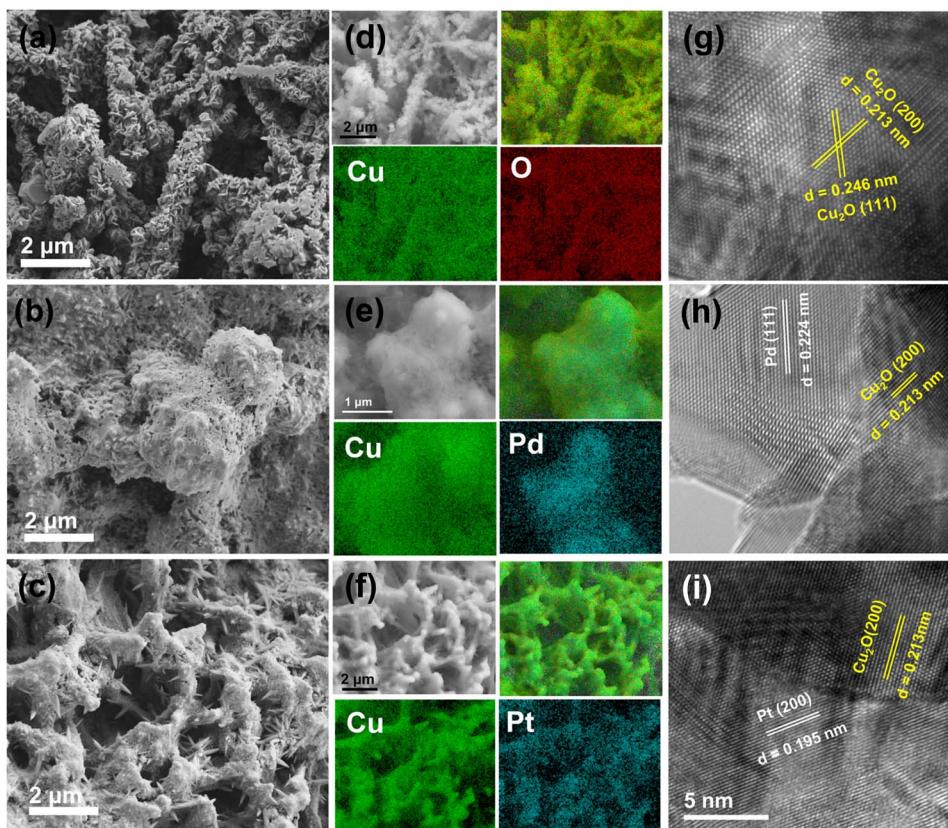


Fig. 3 SEM images of (a)  $\text{Cu}_2\text{O}/\text{Cu-R}$ ; (b)  $\text{Pd}-\text{Cu}_2\text{O}/\text{Cu-R}$  and (c)  $\text{Pt}-\text{Cu}_2\text{O}/\text{Cu-R}$ ; the corresponding EDX mapping of (d)  $\text{Cu}_2\text{O}/\text{Cu-R}$ ; (e)  $\text{Pd}-\text{Cu}_2\text{O}/\text{Cu-R}$  and (f)  $\text{Pt}-\text{Cu}_2\text{O}/\text{Cu-R}$ ; TEM images of (g)  $\text{Cu}_2\text{O}/\text{Cu-R}$ ; (h)  $\text{Pd}-\text{Cu}_2\text{O}/\text{Cu-R}$  and (i)  $\text{Pt}-\text{Cu}_2\text{O}/\text{Cu-R}$ .

0.1 M  $\text{NaOH}/0.1 \text{ M } \text{NO}_3^-$  electrolyte revealed significant mass transport limitations from continuous nitrate depletion at the electrode interface, constraining electrocatalytic activity. To ensure efficient reactant supply, all experiments maintained constant 800 rpm agitation. Initial performance screening *via* chronoamperometry applied cathodic current densities from  $-25$  to  $-125 \text{ mA cm}^{-2}$  in identical electrolyte. Quantitative analysis of reduction products employed UV-visible absorption spectroscopy (Fig. S9–11), with comprehensive performance metrics, including  $\text{NH}_3\text{-N}$  faradaic efficiency and yield rates, presented in Fig. 4a–c.

Electrocatalytic testing over a 2-hour period, with current-time profiles detailed in Fig. S12–14, revealed significant performance variations for the  $\text{Cu}_2\text{O}$  electrode during nitrate reduction. Notably, at  $25 \text{ mA cm}^{-2}$ , both the  $\text{NH}_3\text{-N}$  yield rate and faradaic efficiency (FE) reached their minimum values of  $0.31 \text{ mg h}^{-1} \text{ cm}^{-2}$  and  $19.22\%$ , respectively (Fig. 4a). The low FE strongly suggested insufficient generation of critical atomic hydrogen intermediates at this low current density. Performance improved at higher current densities, with the  $\text{NH}_3\text{-N}$  yield rate peaking at  $2.92 \text{ mg h}^{-1} \text{ cm}^{-2}$  at  $100 \text{ mA cm}^{-2}$  and  $\text{NH}_3\text{-N}$  FE maximizing at  $51.58\%$  at  $75 \text{ mA cm}^{-2}$ . However, further increases in current density diminished both metrics, indicating that the hydrogen evolution reaction (HER) became increasingly dominant as a competing side reaction. Modification with precious metals markedly enhanced performance. Pd

loading elevated the  $\text{NH}_3\text{-N}$  yield rate from  $0.39 \text{ mg h}^{-1} \text{ cm}^{-2}$  at  $-25 \text{ mA cm}^{-2}$  to  $5.02 \text{ mg h}^{-1} \text{ cm}^{-2}$  at  $-125 \text{ mA cm}^{-2}$ , while  $\text{NH}_3\text{-N}$  FE rose from  $23.92\%$  at  $-25 \text{ mA cm}^{-2}$  to a maximum of  $75.39\%$  at  $-75 \text{ mA cm}^{-2}$  (Fig. 4b). Similarly, Pt loading boosted the yield rate from  $0.82 \text{ mg h}^{-1} \text{ cm}^{-2}$  at  $-25 \text{ mA cm}^{-2}$  to  $5.14 \text{ mg h}^{-1} \text{ cm}^{-2}$  at  $-125 \text{ mA cm}^{-2}$  and increased FE from  $50.32\%$  at  $-25 \text{ mA cm}^{-2}$  to a peak of  $86.55\%$  at  $-75 \text{ mA cm}^{-2}$  (Fig. 4c). Critically, for both  $\text{Pd}-\text{Cu}_2\text{O}/\text{Cu-R}$  and  $\text{Pt}-\text{Cu}_2\text{O}/\text{Cu-R}$ , the  $\text{NH}_3\text{-N}$  FE declined when the current density exceeded  $75 \text{ mA cm}^{-2}$ , a phenomenon again attributable to the heightened HER activity overwhelming the nitrate reduction pathway at excessive overpotentials. Under identical conditions, both precious-metal-modified electrodes consistently outperformed the bare  $\text{Cu}_2\text{O}$ , demonstrating that Pd and Pt loading synergistically enhanced electrocatalytic activity and selectivity for nitrate-to-ammonia conversion, with  $\text{Pt}-\text{Cu}_2\text{O}/\text{Cu-R}$  exhibiting the highest overall performance.

In light of potential side reactions during the  $\text{NO}_3\text{RR}$ , the product selectivity efficiency (SE) of each catalytic electrode was systematically assessed. As shown in Fig. S15, the  $\text{Cu}_2\text{O}$  electrode exhibited predominant  $\text{N}_2$  selectivity at current densities below  $75 \text{ mA cm}^{-2}$ , above which  $\text{NO}_2^-$  became the major product. With Pd modification, the electrode favoured  $\text{NO}_2^-$  formation, while Pt loading markedly enhanced  $\text{NH}_3$  selectivity (Fig. S16 and S17). To enable a fair comparison of the intrinsic activity contributed by the noble metals, the  $\text{NH}_3$  yield rate was

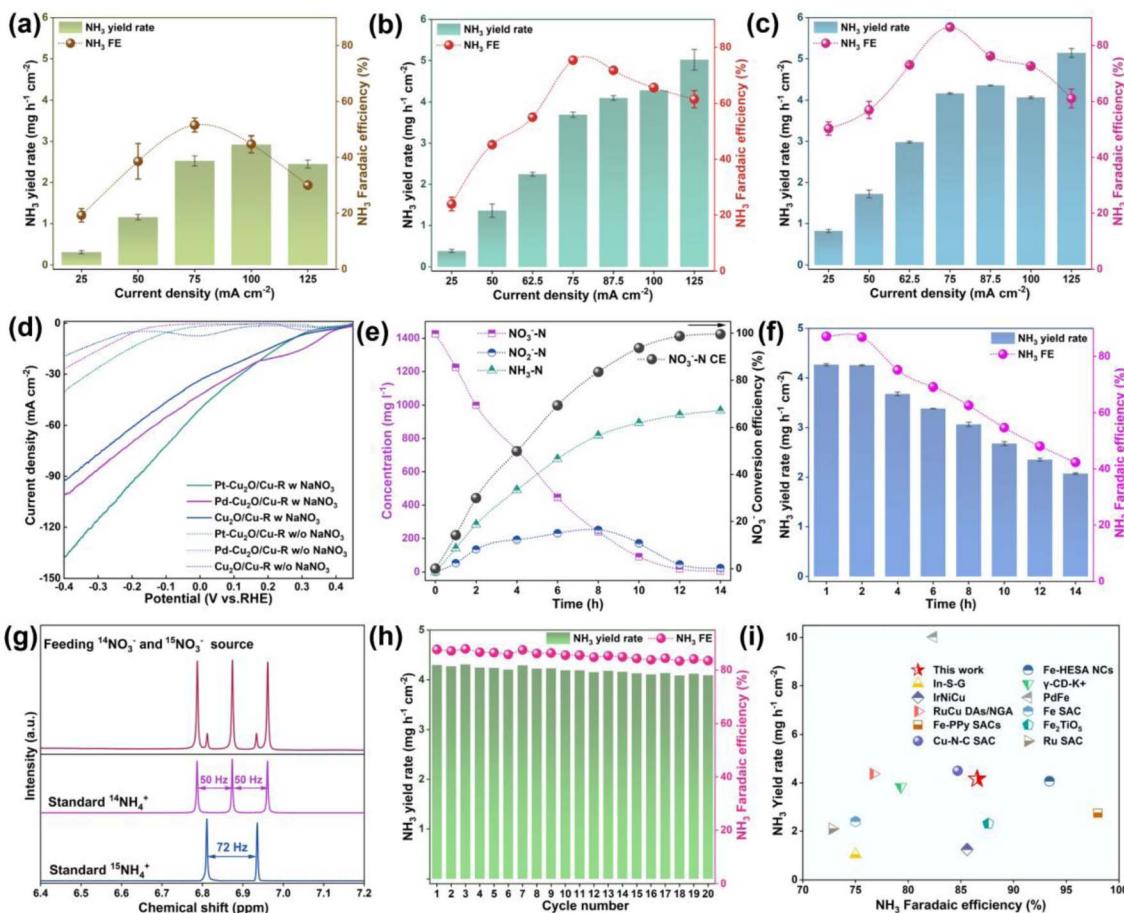


Fig. 4 Potentiostatic  $\text{NO}_3$ RR:  $\text{NH}_3$ -N yield rate and FE of (a)  $\text{Cu}_2\text{O}/\text{Cu}-\text{R}$ ; (b)  $\text{Pd}-\text{Cu}_2\text{O}/\text{Cu}-\text{R}$  and (c)  $\text{Pt}-\text{Cu}_2\text{O}/\text{Cu}-\text{R}$ ; (d) LSV curves of  $\text{Cu}_2\text{O}/\text{Cu}-\text{R}$ ,  $\text{Pd}-\text{Cu}_2\text{O}/\text{Cu}-\text{R}$  and  $\text{Pt}-\text{Cu}_2\text{O}/\text{Cu}-\text{R}$  without and with  $\text{NO}_3^-$  in 0.1 M  $\text{NaOH}$ ; Time-dependent variation of (e)  $\text{NO}_3^-$ -N,  $\text{NO}_2^-$ -N, and  $\text{NH}_3$ -N concentration and  $\text{NO}_3$ -N CE; (f)  $\text{NH}_3$ -N yield rate and FE during the  $\text{NO}_3$ RR; (g)  $^1\text{H}$  NMR spectra of  $\text{Pt}-\text{Cu}_2\text{O}/\text{Cu}-\text{R}$  after the  $\text{NO}_3$ RR using  $^{14}\text{NO}_3^-$  and  $^{15}\text{NO}_3^-$ ; (h) stability test of the  $\text{NO}_3$ RR for  $\text{Pt}-\text{Cu}_2\text{O}/\text{Cu}-\text{R}$ ; (i) specific  $\text{NH}_3$ -N yield rate of previously reported systems with different FEs for the  $\text{NO}_3$ RR.

normalized by the mass of Pd or Pt, as quantified by ICP-OES. The resulting mass activity revealed that  $\text{Pt}-\text{Cu}_2\text{O}/\text{Cu}-\text{R}$  consistently outperformed  $\text{Pd}-\text{Cu}_2\text{O}/\text{Cu}-\text{R}$  across the tested current densities (Fig. S18).

Linear sweep voltammetry (LSV) tests performed on  $\text{Cu}_2\text{O}/\text{Cu}-\text{R}$ ,  $\text{Pd}-\text{Cu}_2\text{O}/\text{Cu}-\text{R}$ , and  $\text{Pt}-\text{Cu}_2\text{O}/\text{Cu}-\text{R}$  electrodes revealed significantly enhanced current densities for the  $\text{Pd}-\text{Cu}_2\text{O}/\text{Cu}-\text{R}$  and  $\text{Pt}-\text{Cu}_2\text{O}/\text{Cu}-\text{R}$  electrodes relative to  $\text{Cu}_2\text{O}$  in nitrate-free electrolyte, as depicted in Fig. 4d. Crucially, the presence of nitrate ions substantially increased the current density of all catalytic electrodes at identical applied potentials, directly indicating effective electrocatalytic nitrate reduction. The  $\text{Pt}-\text{Cu}_2\text{O}/\text{Cu}-\text{R}$  electrode exhibited the most pronounced current density enhancement under these conditions, unequivocally demonstrating its superior intrinsic catalytic activity. Subsequent nitrate batch conversion test was conducted on the optimal  $\text{Pt}-\text{Cu}_2\text{O}/\text{Cu}-\text{R}$  electrode in 0.1 M  $\text{NaOH}$  containing 0.1 M  $\text{NO}_3^-$  ( $1400 \text{ mg L}^{-1}$ ) at  $75 \text{ mA cm}^{-2}$  for 14 hours. Continuous nitrate degradation was observed, achieving near-complete removal by the 14-hour endpoint, while the intermediate nitrite was fully converted to the terminal products  $\text{NH}_3$ -N

and  $\text{N}_2$ , the latter partially escaping as gaseous  $\text{N}_2$  (Fig. 4e). Notably, both the  $\text{NH}_3$ -N yield rate and faradaic efficiency peaked at 2 hours before progressively declining over the remaining reaction time (Fig. 4f). This performance decay likely stemmed from the progressively depleted nitrate concentration diminishing the electrode's surface enrichment capacity, coupled with accumulating atomic hydrogen favouring the competing hydrogen evolution reaction. In addition, the  $\text{Pd}-\text{Cu}_2\text{O}/\text{Cu}-\text{R}$  electrode was also tested under the same conditions for 14 h (Fig. S19). Finally,  $^{14}\text{NO}_3^-/^{15}\text{NO}_3^-$  isotope labelling experiments analyzed by nuclear magnetic resonance unambiguously confirmed the nitrate source of the produced ammonia. Characteristic doublet peaks for  $^{15}\text{NH}_4^+$  emerged when using  $^{15}\text{NO}_3^-$  feedstock, while triplet peaks corresponding to  $^{14}\text{NH}_4^+$  originated from  $^{14}\text{NO}_3^-$ , definitively verifying electrocatalytic nitrate reduction as the exclusive origin of ammonia, excluding contamination artifacts<sup>41</sup> (Fig. 4g).

To evaluate the long-term operational stability of the Pt electrode, prolonged immersion was conducted within a solution containing 0.1 M  $\text{NaOH}$  and 0.1 M  $\text{NO}_3^-$  electrolytes, followed by 20 consecutive electrochemical cycle tests. As



evidenced in Fig. 4h, the Pt-Cu<sub>2</sub>O/Cu-R electrode consistently achieved a stable NH<sub>3</sub>-N faradaic efficiency of approximately 85.58% alongside an average NH<sub>3</sub>-N yield rate of 4.19 mg h<sup>-1</sup> cm<sup>-2</sup> throughout these cycling experiments. To unequivocally verify the structural and chemical integrity of the Pt-Cu<sub>2</sub>O/Cu-R electrode after extended operation, we employed a suite of post-test characterization techniques. *Ex situ* XPS analysis revealed that the chemical states remained largely unchanged: the Cu 2p spectrum was still dominated by Cu<sup>+</sup>/Cu<sup>0</sup> signatures, with only a minor increase in Cu<sup>2+</sup> satellites attributable to superficial air exposure, while the Pt 4f region maintained its mixed Pt<sup>4+</sup>/Pt<sup>0</sup> character, indicating no significant agglomeration or leaching (Fig. S20). The negligible Pt and Cu dissolution was further corroborated by ICP-MS. Moreover, SEM imaging confirmed the preservation of the nanorod morphology without visible collapse or detachment (Fig. S21). This retained structural integrity directly accounted for the consistent electrochemical performance observed during cycling. This sustained high performance demonstrated robust preservation of active site integrity and confirmed the electrode's practical applicability under extended operational conditions. Furthermore, benchmarking against other catalytic systems confirms the superior performance of the Pt-Cu<sub>2</sub>O/Cu-R electrode, positioning it among the most active catalysts reported to date (Fig. 4i and Table S1). While direct comparisons are constrained by differing experimental conditions across studies, the paramount advantage of our system lies in its well-balanced combination of high faradaic efficiency, remarkable NH<sub>3</sub> yield, and excellent operational durability, complemented by minimal metal leaching and a clearly elucidated synergistic mechanism. This holistic performance, supported by mechanistic insight and stability, establishes Pt-Cu<sub>2</sub>O/Cu-R not only as a high-performing catalyst but also as a thoroughly understood and reliable material system, representing a meaningful step forward in nitrate reduction electrocatalysis.

### Mechanisms of enhanced NO<sub>3</sub>RR on Pt-Cu<sub>2</sub>O/Cu-R

*In situ* electrochemical impedance spectroscopy (EIS) elucidated the interfacial charge transfer dynamics and provided indirect evidence for the enhanced reaction kinetics facilitated by the precious metals (Fig. S22). Analysis of Bode phase plots (Fig. 5a-c) across applied potentials revealed a systematic decrease in phase angle peak magnitude concurrent with a shift towards higher frequencies upon cathodic polarization.<sup>42</sup> This behaviour is characteristic of a diminishing faradaic resistance and an acceleration of the rate-determining step(s) of the surface reaction. The critical insight comes from comparing the EIS response in different electrolytes. This modulation of the phase angle (decrease and frequency shift) progressed more rapidly and was more pronounced in nitrate-containing electrolytes compared to nitrate-free conditions. This demonstrates that the presence of nitrate actively lowers the activation barrier for the charge transfer process, consistent with the initiation of the NO<sub>3</sub>RR.

Furthermore, the Pd-Cu<sub>2</sub>O/Cu-R and Pt-Cu<sub>2</sub>O/Cu-R electrodes exhibited a more substantial displacement of the phase

angle peak towards higher frequencies relative to the unmodified Cu<sub>2</sub>O/Cu-R electrode under identical conditions. In the context of the NO<sub>3</sub>RR, which involves multiple proton-coupled electron transfers, the rate of the overall process is often limited by the supply of reactive hydrogen intermediates (H). A significant reduction in charge transfer resistance, as indicated by the EIS data, strongly suggested that the incorporated noble metal sites are facilitating a key step that provides these species. We posited that this step was the dissociation of water (H<sub>2</sub>O + e<sup>-</sup> → H + OH<sup>-</sup>), which is the primary proton source in alkaline media. The more efficient this dissociation, the faster the subsequent formation of H and the hydrogenation of N-intermediates can occur, leading to the observed lower impedance. The Pt-Cu<sub>2</sub>O/Cu-R electrode displayed the most pronounced effect, exhibiting significantly reduced phase angles compared to Pd-Cu<sub>2</sub>O/Cu-R. This difference directly correlates with platinum's superior capability, as an oxidized species (Pt<sup>4+</sup>), to activate water molecules and stabilize the resulting \*H intermediates, a conclusion subsequently supported by our CV and EPR results, which showed greater H generation and consumption on Pt. Therefore, the EIS trends provide strong, correlative evidence that the precious metals, particularly Pt, enhance the kinetics of the NO<sub>3</sub>RR by optimizing the interfacial environment for water dissociation and hydrogen intermediate stabilization.

The critical role of reactive atomic hydrogen intermediates in nitrate deoxygenation and hydrogenation is well-established. To directly monitor these H\* species, we performed *in situ* CV with varied starting potentials. As shown in Fig. 5d, voltammograms for pristine Cu<sub>2</sub>O and Pd/Pt-Cu<sub>2</sub>O/Cu-R in nitrate-free electrolyte exhibited two distinct oxidation peaks during the positive scan, attributable to hydrogen gas oxidation and adsorbed hydrogen species oxidation, respectively<sup>43</sup> (Fig. 5d and S17). Notably, the significantly higher peak intensities observed on the Pt-Cu<sub>2</sub>O/Cu-R electrode directly implicate Pt sites as primary centres for efficient H\* activation (Fig. S23). Crucially, the introduction of nitrate into the electrolyte caused the complete disappearance of these H-associated oxidation peaks, providing direct electrochemical evidence for H consumption during nitrate reduction. This participation of atomic hydrogen was further corroborated by electron paramagnetic resonance spectroscopy probing DMPO-H adduct formation. Fig. 5e reveals the characteristic nine-line EPR signature of DMPO-H for the Cu oxide-based catalyst in 0.1 M NaOH, with signal intensity progressively strengthening over reaction time.<sup>44</sup> Mirroring the CV observations, the addition of nitrate to the NaOH solution resulted in clear attenuation and ultimate disappearance of these nine-line peaks, as shown in Fig. 5f, unequivocally confirming the involvement of atomic hydrogen intermediates in driving nitrate reduction.

To probe the superior nitrate reduction reaction (NO<sub>3</sub>RR) catalytic activity of Pt-Cu<sub>2</sub>O/Cu-R, we conducted *in situ* Raman spectroscopy under operational conditions. Comparative spectra for Cu<sub>2</sub>O/Cu-R were also acquired across a potential range in 0.1 M NaOH containing 0.1 M NO<sub>3</sub><sup>-</sup>. Initial characterization at open circuit potential (OCP) revealed the definitive presence of Cu<sub>2</sub>O within both Pt-Cu<sub>2</sub>O/Cu-R and Cu<sub>2</sub>O/Cu-R,



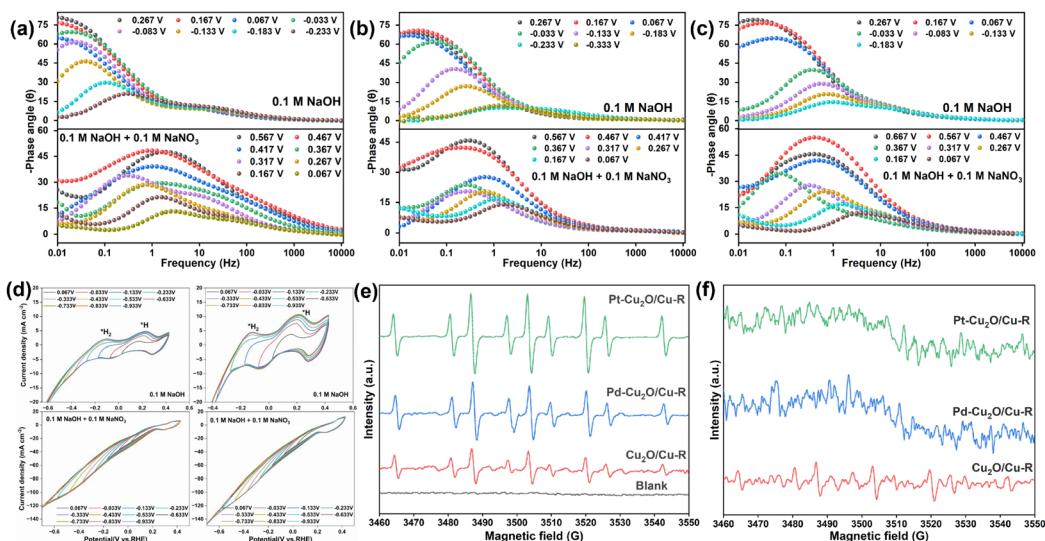


Fig. 5 Bode phase plots of (a)  $\text{Cu}_2\text{O}/\text{Cu-R}$ ; (b)  $\text{Pd}-\text{Cu}_2\text{O}/\text{Cu-R}$  and (c)  $\text{Pt}-\text{Cu}_2\text{O}/\text{Cu-R}$  in different electrolytes under various electrochemical conditions; (d) CV curves of (left)  $\text{Cu}_2\text{O}/\text{Cu-R}$  and (right)  $\text{Pd}-\text{Cu}_2\text{O}/\text{Cu-R}$  in  $0.1 \text{ M NaOH}$ , with or without addition of  $0.1 \text{ M } \text{NO}_3^-$ ; (e) EPR spectra of  $\text{Cu}_2\text{O}/\text{Cu-R}$ ,  $\text{Pd}-\text{Cu}_2\text{O}/\text{Cu-R}$  and  $\text{Pt}-\text{Cu}_2\text{O}/\text{Cu-R}$  in  $0.1 \text{ M NaOH}$ ; (f) EPR spectra with added  $\text{NO}_3^-$ .

signified by characteristic vibrational peaks at 148, 218, and  $625 \text{ cm}^{-1}$ .<sup>45</sup> A critical observation emerged as the applied potential was swept negatively. These  $\text{Cu}_2\text{O}$  signatures progressively diminished in intensity within the  $\text{Cu}_2\text{O}/\text{Cu-R}$  sample, ultimately vanishing completely at 0 V *versus* RHE. This behaviour directly indicated the electrochemical reduction of

$\text{Cu}^+$  species to metallic copper ( $\text{Cu}^0$ ) during the  $\text{NO}_3\text{RR}$  (Fig. 6a). Strikingly, the  $\text{Pt}-\text{Cu}_2\text{O}/\text{Cu-R}$  catalyst exhibited markedly different behavior; although attenuated, the characteristic  $\text{Cu}_2\text{O}$  Raman signals, particularly those at 148, 218, and  $625 \text{ cm}^{-1}$ , persisted discernibly throughout the entire applied potential window. This sustained presence provided compelling

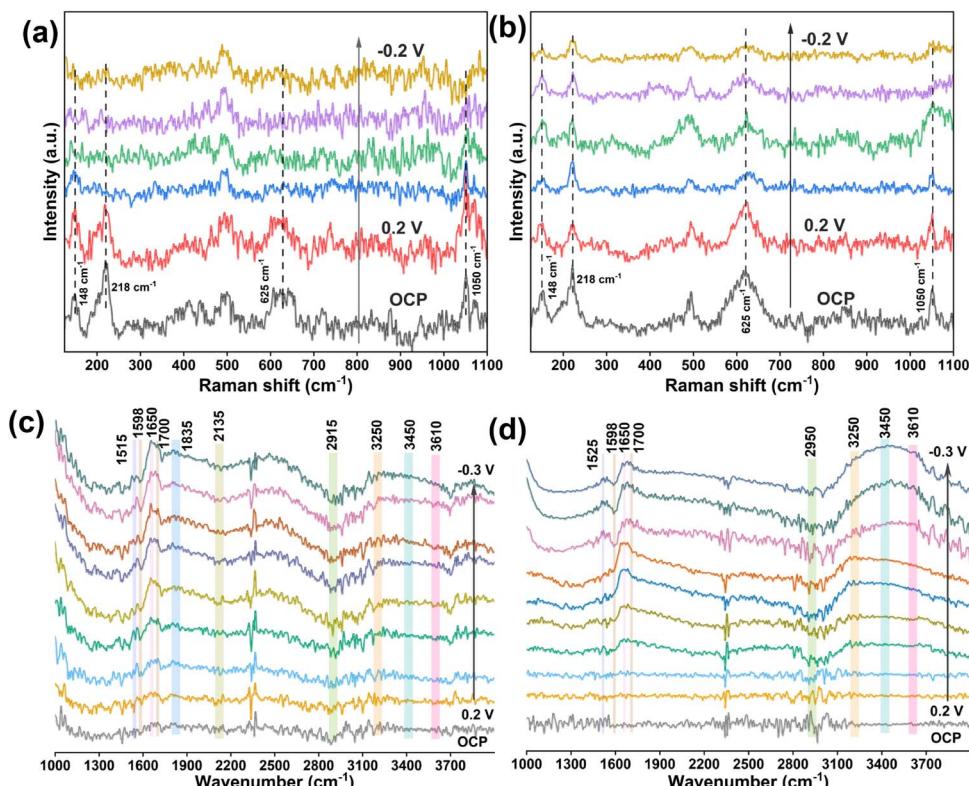
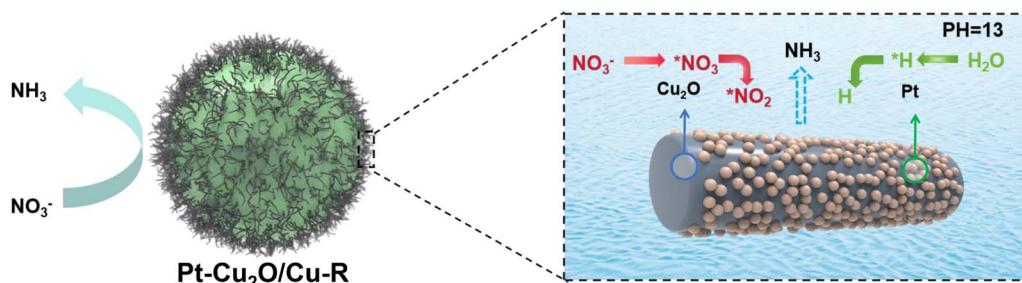


Fig. 6 *In situ* Raman spectra of (a)  $\text{Cu}_2\text{O}/\text{Cu-R}$  and (b)  $\text{Pt}-\text{Cu}_2\text{O}/\text{Cu-R}$  for the  $\text{NO}_3\text{RR}$  at different potentials; *in situ* FTIR spectra of (c)  $\text{Cu}_2\text{O}/\text{Cu-R}$  and (d)  $\text{Pt}-\text{Cu}_2\text{O}/\text{Cu-R}$  for the  $\text{NO}_3\text{RR}$  at different potentials.



**Fig. 7** Schematic representation of the  $\text{NO}_3$ RR active sites on the surface of the Pt– $\text{Cu}_2\text{O}/\text{Cu-R}$  electrode at pH 13. This schematic integrates the key experimental findings of this work: the stabilization of  $\text{Cu}^+$  sites, the critical role of atomic  $^*\text{H}$  supplied from Pt-facilitated water dissociation, and the detection of key nitrogenous intermediates.

spectroscopic evidence that the incorporation of  $\text{Pt}^{4+}$  ions significantly enhances the structural stability of the  $\text{Cu}_2\text{O}$  phase, specifically stabilizing the  $\text{Cu}^+–\text{O}$  bonding framework against cathodic reduction under reaction conditions. Concurrently, the Raman signature of nitrate ions, identified by its characteristic peak centered near  $1050\text{ cm}^{-1}$ , was monitored, offering insight into the interfacial reaction environment (Fig. 6b).<sup>46</sup>

The striking contrast in the stability of  $\text{Cu}^+$  species between Pt– $\text{Cu}_2\text{O}/\text{Cu-R}$  and the unmodified catalyst, as revealed by *in situ* Raman, pointed to a strong metal–support interaction (SMSI) that electronically stabilized the  $\text{Cu}_2\text{O}$  matrix. We proposed that this stabilization originated from electron transfer at the Pt– $\text{Cu}_2\text{O}$  interface. Our XPS analysis (Fig. 2f) showed that Pt species are predominantly present in an oxidized state ( $\text{Pt}^{4+}$ ), suggesting partial charge transfer from the  $\text{Cu}_2\text{O}$  support to Pt. This electronic redistribution contributes to  $\text{Cu}^+$  stabilization in two key ways: (i) it rendered the Cu centres in  $\text{Cu}_2\text{O}$  slightly electron-deficient, which raises the energy barrier for their reduction to  $\text{Cu}^0$  by hindering further electron uptake from the cathode; (ii) it strengthened the Pt–O–Cu linkage at the interface, thereby enhancing the structural integrity of the  $\text{Cu}_2\text{O}$  phase and improving its resistance to cathodic decomposition.

Complementary *in situ* FTIR spectroscopy tracked evolving interfacial species during the  $\text{NO}_3$ RR across potentials from open circuit to  $-0.3\text{ V}$ , as detailed in Fig. 6c and d. Spectra for the  $\text{Cu}_2\text{O}/\text{Cu-R}$  electrode revealed the sequential emergence and intensification of key intermediate signatures: a peak near  $1515\text{ cm}^{-1}$  assigned to  $\text{H–N–H}$  bending,  $^*\text{N–O}$  stretching near  $1600\text{ cm}^{-1}$ , adsorbed  $^*\text{NO}_3$  species at  $1700\text{ cm}^{-1}$ ,  $^*\text{NO}$  species near  $1835\text{ cm}^{-1}$ , and  $^*\text{N–H}$  stretching vibration near  $2950\text{ cm}^{-1}$  indicative of  $^*\text{NH}_3$  formation.<sup>47–50</sup> This progression confirms the electrocatalytic deoxygenation and hydrogenation pathway generating ammonia. Concurrently, a downward feature at  $2136\text{ cm}^{-1}$  signifying  $\text{N}=\text{N}$  stretching provided evidence for dinitrogen formation as a minor pathway.<sup>51</sup> Further spectral regions exhibited upward bands: the  $\text{H–O–H}$  bending mode near  $1650\text{ cm}^{-1}$  and a broad  $\text{O–H}$  stretching envelope between  $3000$  and  $3700\text{ cm}^{-1}$  encompassing contributions from ice-like water near  $3250\text{ cm}^{-1}$ , liquid-like water near  $3450\text{ cm}^{-1}$ , and free water near  $3610\text{ cm}^{-1}$ .<sup>52</sup> Crucially, comparative analysis demonstrated a pronounced enhancement in the liquid-like

and free water bands for the Pt– $\text{Cu}_2\text{O}/\text{Cu-R}$  electrode relative to pristine  $\text{Cu}_2\text{O}/\text{Cu-R}$ , particularly at low applied potentials. This distinct spectral evolution directly indicated significantly more effective water dissociation occurring at the Pt– $\text{Cu}_2\text{O}$  interface, where the electrophilic  $\text{Pt}^{4+}$  species facilitate the initial interaction with water molecules, thereby enhancing the local proton supply critical for the hydrogenation steps of nitrate reduction. This finding provides direct spectroscopic support for the enhanced interfacial kinetics inferred from the EIS analysis (Fig. 5c), confirming that Pt sites efficiently facilitate the proton-supplying step critical for the hydrogenation steps of nitrate reduction.

Based on the collective *in situ* spectroscopic and electrochemical evidence, we propose the synergistic reaction mechanism for the significantly enhanced nitrate-to-ammonia reduction activity. Platinum sites efficiently dissociate water molecules, providing a critical source of reactive hydrogen intermediates. Concurrently, *in situ* generated  $\text{Cu}_2\text{O}$  was identified as the primary active plane for nitrate reduction catalysis, as illustrated in Fig. 7. While the exact adsorption geometries of the intermediates are simplified representations, the identified species and the overall bifunctional pathway are directly corroborated by our experimental data. The sequential hydrogenation process from  $^*\text{NO}_3$  to  $\text{NH}_3$ , involving the detected intermediates ( $\text{NO}_2$ ,  $^*\text{NO}$ , and  $^*\text{NH}_2$ ), aligns with widely accepted mechanisms for nitrate electroreduction on copper-based catalysts.<sup>4,40</sup> Crucially, this bifunctional architecture optimally balances competing reaction kinetics: it promotes the nitrate reduction pathway leading to ammonia synthesis while simultaneously moderating the consumption of atomic hydrogen intermediates through parasitic hydrogen evolution. This strategic kinetic regulation directly underpins the catalyst's exceptional activity, enabling high-efficiency ammonia production at substantially reduced overpotentials.

## Conclusion

This study systematically evaluates the electrocatalytic nitrate reduction performance of Pt– $\text{Cu}_2\text{O}/\text{Cu-R}$  and Pd– $\text{Cu}_2\text{O}/\text{Cu-R}$  electrodes. The Pt– $\text{Cu}_2\text{O}/\text{Cu-R}$  electrode demonstrates superior activity, achieving a maximum ammonia-N faradaic efficiency of 86.55% and a yield rate of  $4.16\text{ mg h}^{-1}\text{ cm}^{-2}$ , significantly



exceeding the performance of both Pd-Cu<sub>2</sub>O/Cu-R and unmodified Cu<sub>2</sub>O/Cu-R. *In situ* Raman spectroscopy confirmed the critical persistence of stable Cu<sup>+</sup> species throughout nitrate reduction. These Cu<sup>+</sup> sites actively activate nitrogen-containing intermediates, while neighbouring platinum sites facilitate water dissociation to supply essential hydrogen species for intermediate hydrogenation. Complementary *in situ* FTIR spectroscopy revealed that the Pt-Cu<sub>2</sub>O/Cu-R architecture promotes efficient accumulation and conversion of nitrite intermediates while optimizing the configuration of key \*NO intermediates to favour subsequent hydrogenation steps. Cyclic voltammetry and electron spin resonance spectroscopy definitively identified the reactive H species central to this mechanism. These findings establish a vital strategy for stabilizing active Cu<sup>+</sup> catalytic centres *via* the creation of electron-deficient Cu sites through charge transfer to oxidized Pt species, and elucidate fundamental mechanistic insight into synergistic nitrate reduction pathways, paving the way for the design of advanced catalysts based on electronic-structure modulation.

## Author contributions

Wenzheng Yu and Kai Zhang designed the experiments; Xiaolong Zhu and Kai Zhang completed the main experiments and wrote the draft; Jiahao Tao and Siyi Liang were involved in some experiments; Rong Chen and Wenzheng Yu made the final revision to the manuscript.

## Conflicts of interest

There are no conflicts to declare.

## Data availability

The data supporting this article have been included as part of the supplementary information (SI). Supplementary information: additional supporting figures, tables, and experimental procedures are provided in the SI. See DOI: <https://doi.org/10.1039/d5ta06839h>.

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## References

- P. H. van Langevelde, I. Katsounaros and M. T. Koper, *Joule*, 2021, **5**, 290–294.
- S. Garcia-Segura, M. Lanzarini-Lopes, K. Hristovski and P. Westerhoff, *App. Catal. B: Environ.*, 2018, **236**, 546–568.
- M. H. Ward, R. R. Jones, J. D. Brender, T. M. De Kok, P. J. Weyer, B. T. Nolan, C. M. Villanueva and S. G. Van Breda, *Int. J. Environ. Res. Public Health*, 2018, **15**, 1557.
- G. Zhang, B. Li, Y. Shi, Q. Zhou, W.-J. Fu, G. Zhou, J. Ma, S. Yin, W. Yuan, S. Miao, Q. Ji, J. Qu and H. Liu, *Nat. Sustain.*, 2024, **7**, 1251–1263.
- M. Duca and M. T. Koper, *Energy Environ. Sci.*, 2012, **5**, 9726–9742.
- S. Zhang, J. Wu, M. Zheng, X. Jin, Z. Shen, Z. Li, Y. Wang, Q. Wang, X. Wang and H. Wei, *Nat. Commun.*, 2023, **14**, 3634.
- N. Barrabés and J. Sá, *App. Catal. B: Environ.*, 2011, **104**, 1–5.
- Z. Ni, C. Luo, B. Cheng, P. Kuang, Y. Li and J. Yu, *App. Catal. B: Environ.*, 2023, **321**, 122072.
- Y. Hua, N. Song, Z. Wu, Y. Lan, H. Luo, Q. Song and J. Yang, *Adv. Funct. Mater.*, 2024, **34**, 2314461.
- Z.-Y. Wu, M. Karamad, X. Yong, Q. Huang, D. A. Cullen, P. Zhu, C. Xia, Q. Xiao, M. Shakouri and F.-Y. Chen, *Nat. Commun.*, 2021, **12**, 2870.
- Y.-J. Shih, Z.-L. Wu and Y.-C. He, *J. Hazard. Mater.*, 2024, **477**, 135276.
- P. Wang, S. Meng, B. Zhang, M. He, P. Li, C. Yang, G. Li and Z. Li, *J. Am. Chem. Soc.*, 2023, **145**, 26133–26143.
- K. Huang, K. Tang, M. Wang, Y. Wang, T. Jiang and M. Wu, *Adv. Funct. Mater.*, 2024, **34**, 2315324.
- B. Zhang, Z. Dai, Y. Chen, M. Cheng, H. Zhang, P. Feng, B. Ke, Y. Zhang and G. Zhang, *Nat. Commun.*, 2024, **15**, 2816.
- Y. Liu, C. Kong, L. Liu, X. Jiang, C. Liu, F. Liu, J. Sun and Y. Wang, *Chem. Eng. J.*, 2024, 150217.
- X. Zhu, K. Dong, D. T. Tran, S. Sidra, D. C. Nguyen, D. H. Kim, N. H. Kim and J. H. Lee, *Small*, 2025, **21**, 2405452.
- M. D. Marcinkowski, M. T. Darby, J. Liu, J. M. Wimble, F. R. Lucci, S. Lee, A. Michaelides, M. Flytzani-Stephanopoulos, M. Stamatakis and E. C. H. Sykes, *Nat. Chem.*, 2018, **10**, 325–332.
- Z. Xiong, Z. Lei, C.-C. Kuang, X. Chen, B. Gong, Y. Zhao, J. Zhang, C. Zheng and J. C. Wu, *App. Catal. B: Environ.*, 2017, **202**, 695–703.
- J. Su, K. Shi, B. Liu, Z. Xi, J. Yu, X. Xu, P. Jing, R. Gao and J. Zhang, *Adv. Funct. Mater.*, 2024, **34**, 2401194.
- H. Liu, X. Lang, C. Zhu, J. Timoshenko, M. Rüscher, L. Bai, N. Guijarro, H. Yin, Y. Peng and J. Li, *Angew. Chem., Int. Ed.*, 2022, **61**, e202202556.
- R. Liu, H. Zhao, X. Zhao, Z. He, Y. Lai, W. Shan, D. Bekana, G. Li and J. Liu, *Environ. Sci. Technol.*, 2018, **52**, 9992–10002.
- A. Tayal, O. Seo, J. Kim, H. Kobayashi, T. Yamamoto, S. Matsumura, H. Kitagawa and O. Sakata, *ACS Appl. Mater. Interfaces*, 2021, **13**, 23502–23512.
- C. A. Boasiako, Z. Zhou, X. Huo and T. Ye, *J. Hazard. Mater.*, 2023, **446**, 130661.
- O. Soares, J. Órfão, J. Ruiz-Martínez, J. Silvestre-Albero, A. Sepúlveda-Escribano and M. Pereira, *Chem. Eng. J.*, 2010, **165**, 78–88.
- H. Zhu, J. J. Wang, Z. Xu, Y. Tan and J. Wang, *Small*, 2024, **20**, 2404919.
- H. Guo, M. Li, Y. Yang, R. Luo, W. Liu, F. Zhang, C. Tang, G. Yang and Y. Zhou, *Small*, 2023, **19**, 2207743.



27 G. A. Cerrón-Calle, A. S. Fajardo, C. M. Sánchez-Sánchez and S. García-Segura, *App. Catal. B: Environ.*, 2022, **302**, 120844.

28 T. Chen, H. Li, H. Ma and M. T. Koper, *Langmuir*, 2015, **31**, 3277–3281.

29 K. Zhang, B. Li, F. Guo, N. Graham, W. He and W. Yu, *Angew. Chem., Int. Ed.*, 2024, **136**, e202411796.

30 Y. Wang, W. Zhou, R. Jia, Y. Yu and B. Zhang, *Angew. Chem., Int. Ed.*, 2020, **59**, 5350–5354.

31 H. Choi, M. Jun, W. Kang, T. Kim, S. Choi, C. Choi, H. Wang, H. Baik, Y. Jung and K. Jin, *Chem Catal.*, 2024, **4**, 101029.

32 M. Hasnat, S. B. Aoun, S. N. Uddin, M. M. Alam, P. Koay, S. Amertharaj, M. Rashed, M. M. Rahman and N. Mohamed, *Appl. Catal., A*, 2014, **478**, 259–266.

33 A. Aristizábal, S. Contreras, N. Barrabés, J. Llorca, D. Tichit and F. Medina, *App. Catal. B: Environ.*, 2011, **110**, 58–70.

34 L. Xiao, W. Dai, S. Mou, X. Wang, Q. Cheng and F. Dong, *Energy Environ. Sci.*, 2023, **16**, 2696–2704.

35 T. Ma, H. Cao, S. Li, S. Cao, Z. Zhao, Z. Wu, R. Yan, C. Yang, Y. Wang and P. A. van Aken, *Adv. Mater.*, 2022, **34**, 2206368.

36 P. P. Yang, X. L. Zhang, F. Y. Gao, Y. R. Zheng, Z. Z. Niu, X. Yu, R. Liu, Z. Z. Wu, S. Qin, L. P. Chi, Y. Duan, T. Ma, X. S. Zheng, J. F. Zhu, H. J. Wang, M. R. Gao and S. H. Yu, *J. Am. Chem. Soc.*, 2020, **142**, 6400–6408.

37 Y. Cheng, Q. Li, M. I. B. Salaman, C. Wei, Q. Wang, X. Ma, B. Liu and A. B. Wong, *J. Am. Chem. Soc.*, 2025, **147**, 12438–12448.

38 C. Liu, M. Wang, J. Ye, L. Liu, L. Li, Y. Li and X. Huang, *Nano Lett.*, 2023, **23**, 1474–1480.

39 M. Jiang, J. Xu, Q. Zhou, Y. Chen, P. Munroe, L. Li, Z.-H. Xie, Y. Wu and S. Peng, *Angew. Chem., Int. Ed.*, 2025, e202510259.

40 F. Dou, F. Guo, B. Li, K. Zhang, N. Graham and W. Yu, *J. Hazard. Mater.*, 2024, **472**, 134522.

41 K. Zhang, B. Li, F. Guo, N. Graham, W. He and W. Yu, *Angew. Chem., Int. Ed.*, 2024, **63**, e202411796.

42 H. Xu, G. Xu, B. Huang, J. Yan, M. Wang, L. Chen and J. Shi, *Angew. Chem., Int. Ed.*, 2023, **62**, e202218603.

43 W. Zheng, L. Zhu, Z. Yan, Z. Lin, Z. Lei, Y. Zhang, H. Xu, Z. Dang, C. Wei and C. Feng, *Environ. Sci. Technol.*, 2021, **55**, 13231–13243.

44 K. Fan, W. Xie, J. Li, Y. Sun, P. Xu, Y. Tang, Z. Li and M. Shao, *Nat. Commun.*, 2022, **13**, 7958.

45 Y. Deng, A. D. Handoko, Y. Du, S. Xi and B. S. Yeo, *ACS Catal.*, 2016, **6**, 2473–2481.

46 W. He, J. Zhang, S. Dieckhofer, S. Varhade, A. C. Brix, A. Lielpetere, S. Seisel, J. R. C. Junqueira and W. Schuhmann, *Nat. Commun.*, 2022, **13**, 1129.

47 K. Chen, Y. Zhang, J. Xiang, X. Zhao, X. Li and K. Chu, *ACS Energy Lett.*, 2023, **8**, 1281–1288.

48 Z.-H. Xue, H.-C. Shen, P. Chen, G.-X. Pan, W.-W. Zhang, W.-M. Zhang, S.-N. Zhang, X.-H. Li and C. T. Yavuz, *ACS Energy Lett.*, 2023, **8**, 3843–3851.

49 Z. Gong, W. Zhong, Z. He, Q. Liu, H. Chen, D. Zhou, N. Zhang, X. Kang and Y. Chen, *App. Catal. B: Environ.*, 2022, **305**, 121021.

50 N. C. Kani, J. A. Gauthier, A. Prajapati, J. Edgington, I. Bordawekar, W. Shields, M. Shields, L. C. Seitz, A. R. Singh and M. R. Singh, *Energy Environ. Sci.*, 2021, **14**, 6349–6359.

51 H. Hirakawa, M. Hashimoto, Y. Shiraishi and T. Hirai, *J. Am. Chem. Soc.*, 2017, **139**, 10929–10936.

52 K. Sun, X. Wu, Z. Zhuang, L. Liu, J. Fang, L. Zeng, J. Ma, S. Liu, J. Li, R. Dai, X. Tan, K. Yu, D. Liu, W. C. Cheong, A. Huang, Y. Liu, Y. Pan, H. Xiao and C. Chen, *Nat. Commun.*, 2022, **13**, 6260.

