


 Cite this: *EES Batteries*, 2025, **1**, 853

## Interphase design from ionic liquid cation mixtures and multi-mode surface analysis for safe and stable Na metal batteries†

 Lixu Huang, <sup>a</sup> Mahin Maleki,<sup>a</sup> Manuel Salado, <sup>a,b,e</sup> José M. Porro, <sup>b,e</sup> Viktor Petrenko, <sup>b,e</sup> Anton Le Brun,<sup>f</sup> Kilian Shani Fraysse, <sup>a</sup> Hua Li,<sup>c</sup> Xuedong Zhang,<sup>d</sup> Rob Atkin, <sup>c</sup> Jianyu Huang, <sup>d</sup> Fangfang Chen, <sup>a</sup> Faezeh Makhlooghiyazad, <sup>a</sup> Patrick C. Howlett<sup>a</sup> and Maria Forsyth \*<sup>a</sup>

Enhancing the cycling performance of sodium metal batteries requires deliberate electrolyte design to optimize interfacial structuring and sodium deposition. This study explores novel ionic liquid (IL) electrolyte mixtures containing 20 mol% phosphonium cations (tributylmethyl phosphonium)  $P_{1444}^{+}$  and (trimethyl isobutyl phosphonium)  $P_{1114}^{+}$ ) as co-solvent additives in a base (*N*-propyl-*N*-methylpyrrolidinium bis(fluorosulfonyl) imide)  $C_3mpyrFSI$  electrolyte. The effects of these mixtures on electrochemical performance, physicochemical properties, interfacial nano-structuring, and sodium deposition morphology are investigated using a multifaceted approach, including cell cycling, cyclic voltammetry (CV), differential scanning calorimetry (DSC), ionic conductivity measurements, and *in situ* techniques such as neutron reflectometry (NR), atomic force microscopy (AFM), and optical microscopy (OM). The addition of the larger  $P_{1444}^{+}$  cation, while decreasing ionic conductivity, surprisingly exhibits reduced polarisation overpotential and significantly extended lifespan and improved solid electrolyte interphase (SEI) formation kinetics. Our results, supported by NR, AFM, and *in situ* optical studies, reveal that incorporating  $P_{1444}^{+}$  as a co-solvent disrupts interfacial nano-structuring. Under applied negative potentials, this disruption increases the presence of  $Na^{+}$  cations at the interface and their coordinated  $FSI^{-}$  anions, leading to enhanced SEI formation kinetics as evidenced by CV results. This facilitates improved cycling stability and more uniform sodium deposition morphology. This work highlights the potential of mixed-cation ILs in achieving long-term performance and stability in sodium metal batteries. By shedding light on the poorly understood mechanisms underlying SEI-related performance improvements, it provides new strategies for optimizing interfacial structuring and electrolyte design.

Received 11th March 2025,

Accepted 13th May 2025

DOI: 10.1039/d5eb00052a

[rsc.li/EESBatteries](http://rsc.li/EESBatteries)

### Broader context

The pursuit of high-performance sodium metal batteries requires the development of advanced electrolyte formulations capable of addressing critical challenges related to interfacial stability, cycling efficiency, and sodium deposition morphology. While lithium-ion batteries currently dominate the market, the abundance and cost-effectiveness of sodium make it a promising alternative for large-scale energy storage applications. This study introduces a novel approach through the use of mixed-cation ionic liquid (IL) in highly concentrated NaFSI electrolytes to control the interfacial chemistry which in turn controls the solid electrolyte interphase (SEI) and electrode cycling. By integrating cutting-edge *in situ* characterization techniques such as neutron reflectometry (NR), optical microscopy (OM), and atomic force microscopy (AFM), this work reveals how these mixed-cation electrolytes modulate interfacial nano-structuring, enhance SEI formation kinetics, and promote more uniform sodium deposition. The findings demonstrate that the incorporation of larger phosphonium cations reduces polarization overvoltage and significantly improves cycling stability. These insights provide a deeper understanding of the SEI formation process and interfacial phenomena, offering practical strategies for the design of next-generation electrolytes with optimized performance. By addressing key challenges in sodium battery technology, this research contributes to the broader goal of sustainable and scalable energy storage solutions, ultimately supporting the transition to more affordable and environmentally friendly energy systems.

<sup>a</sup>Institute for Frontier Materials (IFM), Deakin University, Burwood, Victoria 3125, Australia. E-mail: maria.forsyth@deakin.edu.au

<sup>b</sup>BCMaterials, Basque Center for Materials, Applications and Nanostructures, UPV/EHU Science Park, 48940 Leioa, Spain

<sup>c</sup>School of Molecular Sciences, University of Western Australia, Crawley, Western Australia, Australia

<sup>d</sup>Clean Nano Energy Center, State Key Laboratory of Metastable Materials Science and Technology, Yanshan University, Qinhuangdao 066004, P. R. China

<sup>e</sup>IKERBASQUE, Basque Foundation for Science, 48009 Bilbao, Spain

<sup>f</sup>Australian Centre for Neutron Scattering, Australian Nuclear Science and Technology Organisation (ANSTO), Lucas Heights, NSW 2234, Australia

 † Electronic supplementary information (ESI) available. See DOI: <https://doi.org/10.1039/d5eb00052a>


## Introduction

In recent years, batteries have been actively developed as a critical technology to address the intensifying greenhouse effects and climate change. Increasing attention has been directed towards sodium batteries, recognized for their low cost and inherent stability.<sup>1</sup> Sodium (Na) metal anodes are widely regarded as highly promising candidates for next-generation, high-energy sodium-based batteries due to their exceptional theoretical specific capacity ( $1166 \text{ mA h g}^{-1}$ ) and low standard electrode potential.<sup>2</sup> In addition to the electrode, the selection of the electrolyte is crucial for the development of the sodium batteries.

Ionic liquids (ILs), composed of large organic cations and charge-delocalized anions, offer unique properties such as negligible vapor pressure, low flammability, and high thermal stability, making them a promising alternative to conventional electrolytes.<sup>3</sup> Additionally, the modular design of ILs enables the tuning of their physicochemical and electrochemical properties by altering cation–anion combinations or mixing different ILs.

Among ILs, systems based on imidazolium and pyrrolidinium cations are the most extensively studied.<sup>4</sup> Modifications to cation structures, such as the introduction of asymmetric alkyl chains, allow for adjustments in melting point, viscosity, and ionic conductivity. Non-aromatic pyrrolidinium cations, like  $\text{C}_3\text{mpyr}^+$ , exhibit higher reductive stability than imidazolium-based counterparts, making them particularly suitable for battery applications.<sup>5</sup> Phosphonium-based ILs, such as  $\text{P}_{1114}\text{FSI}$ , offer additional advantages over nitrogen-based ILs, including higher ionic conductivity and enhanced electrochemical stability.<sup>6</sup> Previous studies revealed that mixtures of phosphonium ILs with high NaFSI concentrations achieve superior performance in sodium batteries, with stable Na stripping/plating and SEI properties. Comparative studies also showed that phosphonium ILs provide better cycling stability and capacity than pyrrolidinium ILs, particularly when water is added to improve SEI characteristics.<sup>7</sup>

It is recognised that the SEI is a controlling factor in the electrochemical performance of Li and Na batteries. Moreover, the structuring of the electrolyte at the electrode interface (electrical double layer, EDL) has also been shown to be important in determining the electrochemical behaviour.<sup>8</sup> Several methods have been used to study electrolyte structuring at interfaces including atomic force microscopy (AFM),<sup>9,10</sup> Raman spectroscopy,<sup>11,12</sup> molecular dynamics (MD) simulations,<sup>9,13,14</sup> neutron reflectometry (NR)<sup>15</sup> and differential capacitance (DC).<sup>16</sup> In combination, these techniques provide a powerful approach to studying the interface and correlating to cell performance.

In addition to using chemical modification of the ionic species to control IL properties, mixtures of cations and/or anions can also be used as cost-effective methods to design new electrolyte systems. For example, early work by Lopes *et al.*<sup>17</sup> and Annat *et al.*<sup>18</sup> studied mixtures of ILs where the anion was kept constant while the cations varied in chemistry

and composition. These studies showed that such mixing is a viable method to control physicochemical properties such as conductivity and ion diffusion in IL mixtures. In the area of electrolytes for lithium batteries, mixtures of anions have been shown to have a major impact on both physical properties, including conductivity and Li diffusion, and electrochemistry.<sup>19–22</sup> In the case of Na batteries, it was demonstrated that combining different fluorosulfonamide anions (FSI, TFSI and FTFSI) with dicyanamide led to significant differences in sodium metal cycling. These differences were attributed to differences in ion speciation within these mixtures in addition to changes in the interfacial structuring which impacted SEI formation.

Additives, including FEC,<sup>23,24</sup> DME<sup>25</sup> *etc.*<sup>26,27</sup> (or co-solvents) have also been shown to influence physicochemical and electrochemical behaviour of IL electrolytes for both lithium and sodium batteries. However, little work has been reported on the use of different cations as co-solvents in ionic liquid-based electrolytes.

The IL electrolyte, super concentrated  $\text{C}_3\text{mpyrFSI}$  with 50 mol% NaFSI, has been well-studied and shown to support Na metal and Na/NFP battery cycling at current densities up to  $1 \text{ mA cm}^{-2}$  for  $1 \text{ mA h cm}^{-2}$ . However, this was a significantly lower performance than the equivalent  $\text{P}_{1114}\text{FSI}$  super concentrated electrolyte (42 mol% NaFSI due to lower solubility).<sup>7</sup> The reason for this difference was not clear in our previous work, however, there was a hint that the SEI layer composition was modified in the presence of the  $\text{P}_{1114}^+$  cation.<sup>6</sup> Prior work also indicated that the near-electrode structuring of the IL electrolyte also affected the SEI and subsequent electrochemical cycling.<sup>28,29</sup> Begić *et al.* demonstrated that the chemical structure of the IL cation in DCA-based ILs also affected the electrolyte structuring and the subsequent Zn electrochemistry.<sup>30</sup> It, therefore, seems logical that mixing of cations could modify the near-electrode ion structuring and the subsequent electrochemistry.

This paper will demonstrate the potential for adding IL co-solvent to control bulk physical properties, interfacial structuring and electrochemical behaviour for sodium battery electrochemistry. To investigate the potential for making a significant improvement to Na battery cycling, we consider the influence of several IL cations (see Fig. S1†) to the base  $\text{C}_3\text{mpyrFSI}$  electrolyte at a fixed concentration of 20 mol% in ILs (based our previous work with  $\text{P}_{1114}^+$  cation, which showed a slight enhancement).<sup>6,31</sup> We compare the previously studied small phosphonium with a larger IL cation,  $\text{P}_{1444}^+$  as well as the influence of adding an ether oxygen to the pyrrolidinium, which has been suggested to improve Li cycling.<sup>32,33</sup> A further reason for using 20 mol% co-solvent/additive is that for this larger phosphonium cation, the NaFSI solubility significantly decreases due to the increase in hydrophobicity. We will discuss a multifaceted study of these novel IL systems including NR, AFM and *in situ* optical cell to compare the influence of adding different IL additives/co-solvent to the base  $\text{C}_3\text{mpyrFSI}$  electrolyte keeping the NaFSI content constant at 42 mol%. A significant enhancement in cell cycling stability



was observed with the addition of a larger tributyl, methyl phosphonium  $P_{1444}^+$  cation to the base IL which correlated with changes in deposition morphology and interfacial structuring near the electrode surface.

## Results and discussion

Fig. 1 presents the cycling profiles of all electrolyte mixtures where  $P_{11114}^+$ ,  $P_{1444}^+$  and  $C_{201}mpyr^+$  IL cations are incorporated into the base  $C_3mpyrFSI$  IL electrolyte. The four samples were evaluated in sodium symmetric cells under constant current conditions of  $1 \text{ mA cm}^{-2}/1 \text{ mA h cm}^{-2}$  over extended cycles at  $50^\circ\text{C}$  to compare their electrochemical performance. The electrochemical performance of the mixtures demonstrated significant variations in polarisation overpotential and cycling lifespan. Pure  $C_3mpyrFSI$  exhibited short-circuiting after 96 cycles, while the addition of  $C_{201}mpyrFSI$  led to higher overpotentials and rapid shorting. Incorporating  $P_{11114}FSI$  improved the electrochemical performance by doubling the cycling lifespan. Surprisingly, the inclusion of the larger cation,  $P_{1444}^+$  led to a remarkable enhancement, extending cycling stability, by more than fivefold achieving at least 552 cycles without any evidence of shorting.

The initial cycling profiles further highlighted these trends: the  $C_3mpyrFSI/P_{1444}FSI$  mixture exhibited the lowest overpotential, followed by pure  $C_3mpyrFSI$  and the  $C_3mpyrFSI/P_{11114}FSI$  mixture, which showed similar overpotentials, while the  $C_3mpyrFSI/C_{201}mpyrFSI$  mixture showed the highest overpotential. These differences remained consistent beyond 10 cycles. The cycling profiles were characterized by pronounced voltage spikes in  $C_3mpyrFSI/C_{201}mpyrFSI$  mixture at the beginning and end of each cycle, leading to a curved profile. The observed “peaking” behaviour during initial cell polarization can be attributed to spatially varying surface kinetics at the electrode/electrolyte interphase, where mass-transport limitations are minimal.<sup>34,35</sup> Notably, this “peaking” behaviour was

less pronounced in the  $C_3mpyrFSI/P_{1444}FSI$  curve. In contrast, the  $C_3mpyrFSI/C_{201}mpyrFSI$  sample exhibited two distinct plateaus during Na stripping, indicating a two-step dissolution process. As reported in previous studies,<sup>36</sup> such behaviour occurs when Na initially dissolves from surface dendrites, which present lower interfacial impedance. After these dendrites are depleted, stripping proceeds from the bulk, where the higher interfacial resistance leads to a second plateau at elevated potential. This transition in dissolution pathway gives rise to the characteristic “double step” feature observed in the polarization curve.

To further investigate the influence of IL co-solvent on electrochemical behaviour, cyclic voltammetry measurements were performed in a two electrode Cu/Na cell. The CV results, shown in Fig. 2, indicate that the onset potentials for sodium deposition in  $C_3mpyrFSI/P_{1444}FSI$ ,  $C_3mpyrFSI/P_{11114}FSI$ , and  $C_3mpyrFSI$  electrolytes are  $-0.16 \text{ V}$ ,  $-0.21 \text{ V}$ , and  $-0.25 \text{ V}$ , respectively. These results suggest that sodium deposition occurs at a less negative potential in the  $C_3mpyrFSI/P_{1444}FSI$  electrolyte, reflecting enhanced electrochemical performance. Additionally, focussing on the peaks prior to Na deposition (Fig. 2b), the CV curves reveal that the cathodic peaks of the  $C_3mpyrFSI/P_{1444}FSI$  mixture both appear at different potentials



Fig. 1 Cycling profile for Na/Na coin cells of the mixtures.



Fig. 2 (a) Cyclic voltammetry curves for the mixtures with 42 mol% NaFSI system at 1<sup>st</sup> cycle. (b) The enlarged reduction process.



compared to the other two samples and are larger. As discussed by Begić *et al.*<sup>37</sup> for Zn electrochemistry, the onset potential likely reflects a different electrode/electrolyte interface and/or may be attributed to differences in SEI composition. Previous experimental and computational studies suggest that in ionic liquid systems, the anion-originated reactions are responsible for the formation of the SEI layer which itself controls metal (Li/Na) deposition.<sup>14</sup> To further elucidate the electrochemical reactions occurring in the SEI formation region of the electrochemical window, three-electrode CVs were conducted on a gold electrode, as depicted in Fig. 3.

As shown in Fig. 3a and b, the electrolyte containing P<sub>1444</sub>FSI (b) demonstrates greater stability and reversibility over multiple cycles compared to the electrolyte with the P<sub>1114</sub>FSI cosolvent (a), which exhibits reduced activity after the first cycle. During the first cycle, the reduction current density in the P<sub>1114</sub>FSI-containing electrolyte reaches approximately  $-8 \text{ mA cm}^{-2}$ , which is higher than the current density observed in the P<sub>1444</sub>FSI-containing electrolyte ( $\sim -6 \text{ mA cm}^{-2}$ ). However, in subsequent cycles (cycles 2–6), the reduction and oxidation current densities exhibit a greater increase and more stable behaviour in the P<sub>1444</sub>FSI-containing electrolyte, likely due to the formation of a more stable interphase.

A closer examination of the anion-derived reaction region during the first and second cycles in both systems (Fig. 3c) reveals multiple irreversible reactions occurring in the first cycle. These reactions can be attributed to electrolyte degradation and interphase formation.

Previous work has identified these reduction peaks as being associated with the electrolyte decomposition, in particular, the anion (FSI or TFSI).<sup>38</sup> However, identifying the origin of these peaks is challenging due to the complexity of the anion coordination environment in the mixed cation system, which is affected by multiple factors, such as salt concentration, the IL cation chemistry and the electrode voltage. The different cation–anion interaction and anion coordination structures can influence the HOMO–LUMO energy levels.<sup>14,39</sup>

Interestingly, the peaks observed in the first cycle differ between the two systems in terms of current densities and

potential ranges. The P<sub>1444</sub>FSI-containing electrolyte exhibits overall higher current densities in this system, suggesting more favourable kinetics for this electrochemical process which we attribute to the SEI formation step. Considering the lower overpotential and improved cycling in the Na/Na symmetric cell data shown in Fig. 1, we suggest that a less resistive and more homogeneous SEI is able to form in this mixed cation system.

To determine whether the bulk physicochemical properties also have a positive effect on the low overpotential and long lifespan of the C<sub>3</sub>mpyrFSI/P<sub>1444</sub>FSI mixture, we compared the glass transition temperature,  $T_g$ , and ionic conductivity for the base C<sub>3</sub>mpyrFSI/42 mol% NaFSI with the mixtures containing either P<sub>1114</sub><sup>+</sup> or P<sub>1444</sub><sup>+</sup> cations (Fig. 4).

After mixing with 42 mol% NaFSI, only the glass transition temperatures ( $T_g$ ) were detected, as shown in Fig. S5† and Fig. 4a. The  $T_g$  of C<sub>3</sub>mpyrFSI was the highest, but the differences among the three samples were less than 2 °C, suggesting a relatively minor impact from the mixtures. Incorporating P<sub>1114</sub>FSI into the C<sub>3</sub>mpyrFSI/42 mol% NaFSI system resulted in a slight increase in ionic conductivity, as shown in Fig. 4b.

Addition of P<sub>1444</sub><sup>+</sup> reduced the ionic conductivity as would be expected due to its larger molecular structure. The ionic conductivity of the C<sub>3</sub>mpyrFSI/P<sub>1444</sub>FSI mixture was the lowest of the three systems, reflecting higher resistance within the bulk electrolyte. Moreover, to have a deeper understanding of the electrolyte resistance in the coin cell setup compared to the flooded electrolyte cell can also be considered, EIS measurements of the cells before cycling and after the first cycle shown in Fig. S2 and Table S1† presents EIS fitting results after first cycle.

The C<sub>3</sub>mpyrFSI/P<sub>1444</sub>FSI mixture shows the lowest overall resistance among the samples, which corresponds to its minimal overpotential observed in the cycling profile. Although the ionic conductivity of the C<sub>3</sub>mpyrFSI/P<sub>1444</sub>FSI mixture was the lowest, reflecting higher resistance within the bulk electrolyte, its fitted bulk resistance in Table S1† was lower. This finding suggests that the addition of P<sub>1444</sub>FSI reduces resistance associated with ion transport through the separator and across the sodium metal electrode interface.

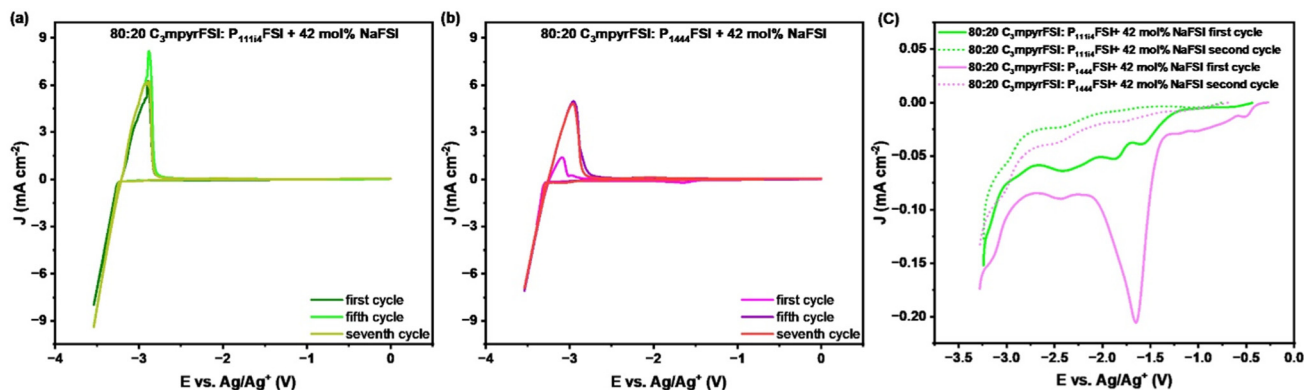


Fig. 3 Three-electrode cyclic voltammetry curves for mixed ILs. (a) C<sub>3</sub>mpyrFSI/P<sub>1114</sub>FSI mixture, (b) C<sub>3</sub>mpyrFSI/P<sub>1444</sub>FSI mixture, (c) enlarged view of the first and second cycles prior to the onset of Na deposition.





Fig. 4 (a) Glass transition temperature (b) temperature-dependent ionic conductivity.

As shown in Fig. S2,<sup>†</sup> the wettability of  $C_3\text{mpyrFSI}/P_{1444}\text{FSI}$  with the Solupor separator was significantly better than that of  $C_3\text{mpyrFSI}/P_{1114}\text{FSI}$  and  $C_3\text{mpyrFSI}$ . When 60  $\mu\text{L}$  of electrolyte was dropped onto the separator, the  $C_3\text{mpyrFSI}/P_{1444}\text{FSI}$  mixture penetrated the separator within 5 minutes, spreading into a flat droplet. In contrast,  $C_3\text{mpyrFSI}/P_{1114}\text{FSI}$  and  $C_3\text{mpyrFSI}$  formed rounded droplets and did not readily penetrate the separator. This improved wettability of the  $C_3\text{mpyrFSI}/P_{1444}\text{FSI}$  mixture effectively enhanced electrolyte permeation into the Solupor separator, correlating with the observed reduction in resistance for ion transport through the separator.<sup>40</sup>

Thus far we have observed that the addition of the large  $P_{1444}^+$  IL cation has a significant positive influence on the Na metal electrochemistry despite its lower overall ionic conductivity. The CV data shows dramatic differences between the two phosphonium mixtures with a large irreversible cathodic reaction at approximately  $-1.65 \text{ V vs. Ag/AgCl}$  present in the  $P_{1444}^+$  system not evident for the  $P_{1114}^+$ . This cathodic peak originates from the chemical species at the electrode interface and leads to the formation of a favourable SEI. In the following section we probe the interfacial structuring in various mixtures on model electrodes (Au) and correlate this with the observed electrochemical behaviour.

## Interphase ion layering

*In situ* NR experiments were conducted under different voltage applications (0 V and  $-0.7 \text{ V}$ ) to investigate the interface between the solid electrode and the described electrolytes. The measured neutron reflectivity signal,  $R$ , versus scattering wave vector ( $q$ ) curves for various electrolyte-electrode interfaces under different voltage applications are presented in Fig. 5, along with the corresponding fitted results and Table 1 presents the scattering length density (SLD) value (estimated for each component in studied materials (see Table S2<sup>†</sup>)) for each system at open circuit potential (OCP) and  $-0.7 \text{ V}$ . Notably, the SLD of the  $C_3\text{mpyrFSI}/P_{1444}\text{FSI}$  mixture is negative at both potentials whereas for base  $C_3\text{mpyrFSI}$  system and the  $C_3\text{mpyrFSI}/P_{1114}\text{FSI}$  mixture the values are positive with the latter being significantly lower than that of the base sample. The thickness values extracted from the raw data and presented in Table 1, indicate that, at OCP the values are similar within the uncertainty range, however, upon applying a negative potential the  $C_3\text{mpyrFSI}/P_{1444}\text{FSI}$  mixture doesn't appear



Fig. 5 Neutron reflectometry curves for electrolyte/electrode interfaces for (a) 0 V; (b)  $-0.7 \text{ V}$  vs. OCP. Solid lines are fitting curves with four-slab model with varied parameters only for EDL. Insets are SLD profiles.



**Table 1** Parameters of EDL layer derived from the fitting of the experimental NR data

Potential (vs. OCP)	Samples (with 42 mol% NaFSI)	SLD ( $10^{-6} \text{ \AA}^{-2}$ )	Thickness ( $\text{\AA}$ )
0 V	80 : 20 $\text{C}_3\text{mpyrFSI} : \text{P}_{1444}\text{FSI}$	$-0.12 \pm 0.09$	$30 \pm 2$
	80 : 20 $\text{C}_3\text{mpyrFSI} : \text{P}_{1114}\text{FSI}$	$0.18 \pm 0.07$	$32 \pm 2$
	$\text{C}_3\text{mpyrFSI}$	$0.23 \pm 0.06$	$33 \pm 2$
-0.7 V	80 : 20 $\text{C}_3\text{mpyrFSI} : \text{P}_{1444}\text{FSI}$	$-0.24 \pm 0.09$	$29 \pm 2$
	80 : 20 $\text{C}_3\text{mpyrFSI} : \text{P}_{1114}\text{FSI}$	$0.15 \pm 0.05$	$36 \pm 2$
	$\text{C}_3\text{mpyrFSI}$	$0.24 \pm 0.05$	$36 \pm 2$

to change significantly whereas the thickness of the other two systems increases. These differences in behaviour have important implications for the chemistry at the interface observed when scanning to negative potentials in the CV data described earlier.

For the  $\text{C}_3\text{mpyrFSI}/\text{P}_{1444}\text{FSI}$  mixture, the SLD decreases under an applied negative potential. Considering that the SLD of the cations is negative and that of the anions is positive (as shown in Table S1<sup>†</sup>), this indicates that more cations are attracted to the electrode. However, the thickness remains nearly unchanged, which could be attributed to a larger number of  $\text{Na}^+$  ions being attracted compared to  $\text{P}_{1444}^+$ , as  $\text{Na}^+$  is significantly smaller than the other cations. For the  $\text{C}_3\text{mpyrFSI}/\text{P}_{1114}\text{FSI}$  mixture, there is almost no change (3% decrease) in SLD between OCP and -0.7 V, while EDL thickness increases. In contrast, for pure  $\text{C}_3\text{mpyrFSI}$ , a 10% increase in both SLD and EDL thickness is observed under a negative potential, likely due to the attraction of cations to the

electrode. At the same potential, the SLD and EDL thickness of the  $\text{C}_3\text{mpyrFSI}/\text{P}_{1444}\text{FSI}$  mixture are much smaller than those of the other samples. This observation suggests that more  $\text{Na}^+$  ions and fewer  $\text{P}_{1444}^+$  and  $\text{C}_3\text{mpyr}^+$  ions are attracted to the electrode, which may contribute to the reduced charge transfer resistance. Furthermore, the increase in  $\text{Na}^+$  most likely also increases the fraction of coordinated  $\text{FSI}^-$  anions (in  $\text{Na}_x\text{FSI}_y$  clusters) at the interface. These coordinated  $\text{FSI}^-$  species have been shown to more readily undergo reduction to form a favorable SEI.<sup>14</sup>

AFM measurements were performed to examine the interfacial nanostructure adjacent to an Au(111) electrode at OCP and OCP -0.7 V, focusing on the effect of adding different phosphonium-based cations to the base electrolyte of  $\text{C}_3\text{mpyrFSI} + 42 \text{ mol\% NaFSI}$  (Fig. 6). Previous studies by Rakov *et al.*<sup>41</sup> and Fraysse *et al.*<sup>16</sup> have investigated the interfacial structure of the  $\text{C}_3\text{mpyrFSI}$  system at various salt concentrations and the  $\text{P}_{1114}\text{FSI} + 42 \text{ mol\% NaFSI}$  electrolyte. Their findings reveal that increasing the salt concentration or using a phosphonium-based cation results in a less structured or unstructured EDL. Additionally, they report that the  $\text{P}_{1114}\text{FSI} + 42 \text{ mol\% NaFSI}$  electrolyte shows a thinner innermost layer at OCP +0.5 V compared to the  $\text{C}_3\text{mpyrFSI}$  system which exhibits an innermost layer with a thickness of 0.55 nm, comparable to the diameter of the  $\text{FSI}^-$  anion (0.53 nm), suggesting the presence of small  $\text{P}_{1114}^+$  cations along with the  $\text{FSI}^-$  anion in the innermost layer in  $\text{P}_{1114}\text{FSI} + 42 \text{ mol\% NaFSI}$  system.<sup>16</sup>

In our study, as shown in Fig. 6, the EDL overall does not show significant ordering in either system. At OCP, the



**Fig. 6** Interfacial layering structure of mixed ILs through AFM force–distance two-dimensional histogram with probability colour bar on the right-hand. (a and b) at OCP; (c and d) at OCP-0.7V for  $\text{C}_3\text{mpyrFSI}/\text{P}_{1114}\text{FSI}$  mixture and  $\text{C}_3\text{mpyrFSI}/\text{P}_{1444}\text{FSI}$  mixture.



$C_3\text{mpyrFSI}/P_{1444}\text{FSI}$  mixture with 42mol% NaFSI maintains a similar interfacial layering structure to  $C_3\text{mpyrFSI} + 50\text{mol}\%$  NaFSI at OCP as reported by Rakov *et al.*,<sup>41</sup> exhibiting three distinct layers with similar thicknesses. However, the push-through force of the innermost layer decreases significantly. In contrast, the  $C_3\text{mpyrFSI}/P_{1114}\text{FSI}$  mixture with 42mol% NaFSI demonstrates a considerably reduced interfacial nanostructure, featuring only a single, weaker layer. This layer, with a thickness of  $\sim 0.7$  nm, is thicker than those observed in both pure  $C_3\text{mpyrFSI}$  and the  $C_3\text{mpyrFSI}/P_{1444}\text{FSI}$  mixture ( $\sim 0.5$  nm), aligning with the neutron reflectometry (NR) data presented in Table 1. The enhanced interfacial structure observed in the  $C_3\text{mpyrFSI}/P_{1444}\text{FSI}$  mixture compared to the  $C_3\text{mpyrFSI}/P_{1114}\text{FSI}$  mixture suggests minimal participation of the larger  $P_{1444}$  cation in the innermost layer, thereby preserving the interfacial structure integrity.

Applying a negative potential (OCP  $-0.7$  V) induces distinct changes in the interfacial structuring, particularly evident in both the apparent separation distance and rupture forces of the innermost ionic layers, Fig. 6c and d. Although both systems show an increase in the innermost layer thickness, they demonstrate opposing trends in the forces required to rupture these layers – decreasing for  $C_3\text{mpyrFSI}/P_{1444}\text{FSI}$  but increasing for  $C_3\text{mpyrFSI}/P_{1114}\text{FSI}$ . These contrasting behaviours suggest different interfacial nanostructures. The observed changes for the  $C_3\text{mpyrFSI}/P_{1444}\text{FSI}$  system align well with our NR measurements, which reveal a decrease in SLD values under negative polarization. This decrease in SLD can be attributed to enhanced  $\text{Na}^+$  participation at the interface, leading to disruption of the original IL nanostructure. The larger  $P_{1444}^+$  cation appears to facilitate this process by allowing more efficient  $\text{Na}^+$  access to the electrode surface, as evidenced by both AFM and NR data. However, for the  $C_3\text{mpyrFSI}/P_{1114}\text{FSI}$  system at the negative potential of OCP  $-0.7$  V, the smaller  $P_{1114}^+$  cation, compared to  $P_{1444}^+$ , enables more efficient packing with  $\text{FSI}^-$  anions and better coordi-

nation with  $\text{Na}^+$  ions at the interface. The compact size of  $P_{1114}^+$  allows it to effectively compete with  $\text{Na}^+$  ions for interfacial positions while maintaining structural integrity, resulting in a more ordered interfacial layer that requires greater force to disrupt. In contrast, the larger  $P_{1444}^+$  cation disrupts this ordered structure, leading to decreased rupture forces and facilitating  $\text{Na}^+$  access to the electrode surface.

Apart from force–distance curves, surface imaging of the gold electrode upon applying a negative potential of OCP  $-2.3$  V was captured, as shown in Fig. 7a–c for the  $C_3\text{mpyrFSI}/P_{1444}\text{FSI}$  mixture, the  $C_3\text{mpyrFSI}/P_{1114}\text{FSI}$  mixture, and for  $P_{1114}\text{FSI} + 42\text{ mol}\%$  NaFSI, respectively. As mentioned earlier, previous studies indicate that neat  $P_{1114}\text{FSI} + 42\text{ mol}\%$  NaFSI demonstrates significantly better performance than neat  $C_3\text{mpyrFSI} + 50\text{ mol}\%$  NaFSI.<sup>42</sup>

In the mixed systems, as shown in Fig. 7a and b, the  $C_3\text{mpyrFSI}/P_{1444}\text{FSI}$  electrolyte forms a morphology more similar to  $P_{1114}\text{FSI} + 42\text{ mol}\%$  NaFSI, Fig. 7c, at the same potential (OCP  $-2.3$  V), compared to the  $C_3\text{mpyrFSI}/P_{1114}\text{FSI}$  electrolyte.

The similarities between the interface surface morphologies of these phosphonium systems suggests that these globular morphologies may be correlated with better cycling performance, through their contribution to the SEI formation process and/or in enabling better  $\text{Na}^+$  ion flux to the electrode surface.

### Surface morphology

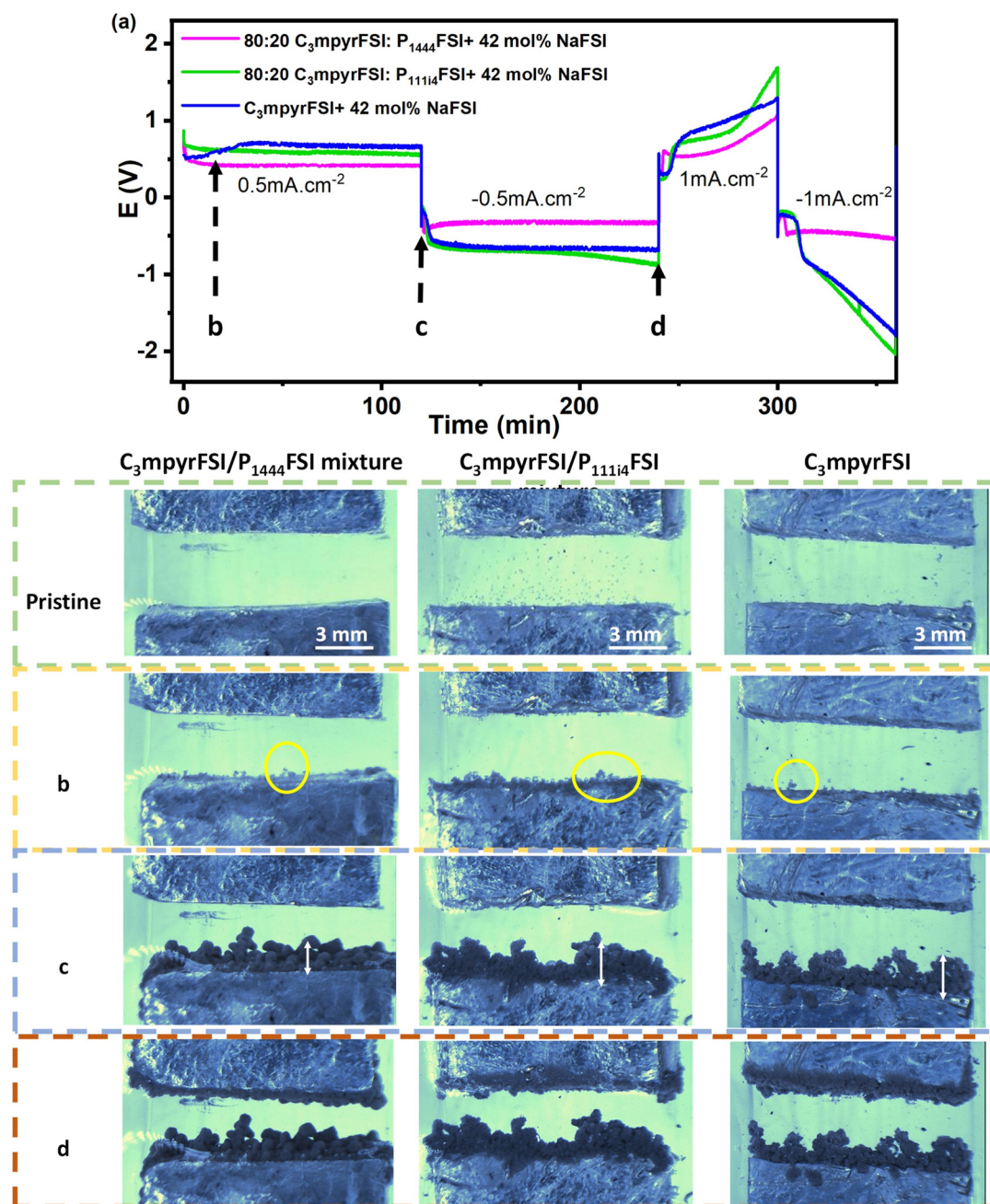
Changes in the electrode surface were recorded in the attached videos, and the corresponding cycling profiles of the open cell were analysed, as shown in Fig. 8. These observations provide insight into the impact of different electrolyte compositions on the morphology and behaviour of the sodium electrode during cycling.

The flooded optical cell was cycled at two conditions:  $0.5\text{ mA cm}^{-2}/1\text{ mA h cm}^{-2}$  for the first cycle and  $1\text{ mA cm}^{-2}/1\text{ mA h cm}^{-2}$  for the second. Initially, the  $C_3\text{mpyrFSI}/P_{1444}\text{FSI}$



**Fig. 7** Surface morphology of the formed solid interphase using ILs through AFM surface imaging at OCP  $-2.3$  V for (a)  $C_3\text{mpyrFSI}/P_{1444}\text{FSI}$  mixture, (b)  $C_3\text{mpyrFSI}/P_{1114}\text{FSI}$  mixture and (c)  $P_{1114}\text{FSI} + 42\text{ mol}\%$  NaFSI.





**Fig. 8** *In situ* optical micrographs obtained for flooded optical cell cycled at  $0.5 \text{ mA cm}^{-2}$ . (a) Cycling profile and morphology are shown at pristine; (b) after 10 min (Na deposition); (c) after first half-cycle; (d) after first cycle.

mixture exhibited the lowest polarisation overpotential, while the  $\text{C}_3\text{mpyrFSI}/\text{P}_{1114}\text{FSI}$  mixture and the base  $\text{C}_3\text{mpyrFSI}$  system showed similar overpotentials. This trend in overpotential remained consistent throughout cycling, aligning with the cycling profile in Fig. 1 using the sodium symmetric coin cell setup. Additionally, the “peaking” behaviour was less significant for the  $\text{C}_3\text{mpyrFSI}/\text{P}_{1444}\text{FSI}$  mixture in the flooded optical cell. When  $-1 \text{ mA cm}^{-2}$  current density was applied, the polarisation of the  $\text{C}_3\text{mpyrFSI}/\text{P}_{1114}\text{FSI}$  mixture and the base  $\text{C}_3\text{mpyrFSI}$  system cells increased rapidly. In contrast, the

$\text{C}_3\text{mpyrFSI}/\text{P}_{1444}\text{FSI}$  mixture maintained stable and low overpotentials, demonstrating enhanced stability and performance under higher current densities.

The addition of  $\text{C}_3\text{mpyrFSI}/\text{P}_{1114}\text{FSI}$  and  $\text{C}_3\text{mpyrFSI}$  resulted in the formation of numerous bubbles on the pristine electrode surface. These bubbles are either reaction of residual water in the electrolyte, or entrapped gases from the electrolyte drops which escape with time. Upon applying a deposition potential, these microbubbles coalesce and eventually disappear. In contrast, the addition of  $\text{C}_3\text{mpyrFSI}/\text{P}_{1444}\text{FSI}$  intro-



duced fewer bubbles, as evident in the videos. This difference could be attributed to less water absorption due to more hydrophobic character of  $P_{1444}$  IL cation and/or better immediate spreading of the electrolyte on the metal surface, resulting from improved contact between  $C_3\text{mpyrFSI}/P_{1444}\text{FSI}$  and the sodium electrode; improved contact is thought to promote more homogeneous sodium deposition.<sup>43</sup> Supporting this observation, Fig. 8c, d, and the SEM images in Fig. S3† illustrate the uniform deposition and less aggregated pattern achieved with  $C_3\text{mpyrFSI}/P_{1444}\text{FSI}$  which is consistent with the AFM images (Fig. 7) showing more evenly distributed inter-phase morphology using this electrolyte.

Fig. 8b demonstrates that after applying a current density of  $0.5 \text{ mA cm}^{-2}$  for 10 minutes, the sodium metal particles formed in the presence of  $C_3\text{mpyrFSI}/P_{1444}\text{FSI}$  are smaller compared to those formed with other electrolytes. Over time, as shown in Fig. 8c and d, these deposits grow progressively smoother, leading to a thinner and less porous sodium deposition layer.<sup>35,44,45</sup> This improved morphology is consistent with the electrochemical behaviour in Fig. 1 and the CV data in Fig. 2 and 3 described above, even though in this case a flooded optical cell was used, without any pressure controlling the surface morphology. We can surmise that the smoother, more uniform particle deposition obtained when using  $C_3\text{mpyrFSI}/P_{1444}\text{FSI}$  relates to surface modification in the presence of the  $P_{1444}^+$  cation and the preferential availability of  $\text{Na}^+$  ions as suggested by the NR and AFM results.

## Discussion and conclusions

In recent years, studies employing ionic liquid (IL) electrolytes have demonstrated that despite having similar bulk compositions and properties, ILs can exhibit significantly different cycling performances in batteries. These disparities are often attributed to differences in the SEI they form. However, the underlying mechanisms governing these differences at the nanoscale level on electrode surfaces remain poorly understood.

It has also been observed that super-concentrated electrolytes can disrupt the electrode interface by increasing the aggregation of  $\text{Na}_x\text{FSI}_y$  clusters at the interface. Since increasing the salt concentration requires ILs with high salt solubility, this study explores novel mixtures of ILs with a fixed salt concentration. By incorporating different cations as co-solvents in an IL, we demonstrate that this approach disrupts the interfacial structuring of the electrolytes at the electrode interface without significantly altering bulk physicochemical properties, such as ionic conductivity. Notably, incorporating the larger phosphonium cation,  $P_{1444}^+$ , results in significant improvements in cycling performance, as confirmed by our coin cell and optical cell cycling results.

Cyclic voltammetry (CV) measurements reveal that the addition of the  $P_{1444}^+$  cation to the base electrolyte,  $C_3\text{mpyrFSI}$  with 42 mol% NaFSI, promotes more favourable kinetics for irreversible reactions involved in SEI formation. NR and AFM

studies further confirm that the introduction of different cations induces a disruption in the innermost interfacial nanostructuring of the electrolyte, akin to the effects observed with increased salt concentration in the literature.<sup>14</sup> These findings suggest that the improved performance of the  $P_{1444}\text{FSI}/C_3\text{mpyrFSI}$  mixture arises from increased number of  $\text{Na}^+$  cation at the interface and their coordinated  $\text{FSI}^-$ , effectively excluding IL cations from this region.

Surface imaging of the SEI formed on a model gold electrode using AFM, as well as Na deposition morphology studies in the flooded Na|Na optical cells, reveal that the addition of  $P_{1444}^+$  cations leads to a more homogeneous and less aggregated SEI and Na deposition morphology.

Overall, this study employs a multifaceted, multiscale approach to highlight the potential of using ILs as co-solvents to modify the interfacial nanostructuring of electrolytes. This strategy improves SEI formation and cycling performance without the need to increase salt concentration, providing a promising pathway for advancing next-generation energy storage technologies by improving the performance and properties like density and reducing the cost.

## Methods

### Sample preparation

$P_{11114}\text{FSI}$  and  $C_3\text{mpyrFSI}$  were supplied by the Boron Molecular company with 99.9% purity.  $P_{1444}\text{FSI}$  was purchased from IoLiTec with 99% purity, sodium bis(fluorosulfonyl)imide (NaFSI, 99.9%) and *N*-methyl-*N*-methoxymethylpyrrolidinium bis(fluorosulfonyl)imide ( $C_{201}\text{mpyrFSI}$ ) were purchased from Solvionic. The structures of the cations and anion are presented in Fig. S1.† To minimize water contamination, the three ILs were dried under vacuum at  $50 \text{ }^\circ\text{C}$  for 48 hours, reducing water content to less than 50 ppm, as confirmed by Karl Fischer titration (831 Karl Fischer Coulometer with Hydranal® Coulomat AG as the titrant).  $C_3\text{mpyrFSI}$  was mixed with  $P_{11114}\text{FSI}$ ,  $P_{1444}\text{FSI}$ , or  $C_{201}\text{mpyrFSI}$  in an 80 : 20 molar ratio, with a fixed NaFSI concentration of 42 mol%. Pure  $C_3\text{mpyrFSI}$  was also mixed with 42 mol% NaFSI for comparison purposes. All sample preparations were carried out inside an argon-filled glove box. The prepared electrolytes were then stored in sealed vials under argon inside the glove box.

### Electrochemical experiments

Na/Na symmetric coin cells (components CR2032) were purchased from Hohsen Corporation, Japan. The electrodes were two 8 mm diameter sodium metal electrodes (Sigma-Aldrich, purity 99.9%). A 16 mm diameter polyethylene separator (gratis, Lydall, 7P03A, 50 mm thickness, 85% 0.3 mm porosity) soaked with the electrolyte solution was used. A 0.5 mm spacer and 1.4 mm spring were used to ensure contact. After assembly, the cells were rested for 24 hours at  $50 \text{ }^\circ\text{C}$  before cycling at  $1 \text{ mA cm}^{-2}/1 \text{ mA h cm}^{-2}$  for long cycles at  $50 \text{ }^\circ\text{C}$ . Electrochemical impedance spectroscopy (EIS) was employed to monitor changes on the sodium electrode surface, with



measurements performed using a VMP3 multichannel potentiostat (Bio-Logic) over a frequency range of 50 mHz–1 MHz and a 10 mV voltage amplitude. Data analysis was conducted using EC-Lab software (Z Fit version 10.44).

Cu|Na coin cells were prepared for conducting cyclic voltammetry (CV) experiments. The working electrode was copper (12.7 mm diameter), and the counter and pseudo-reference electrode was sodium metal (8 mm diameter). The copper electrode was punched and washed with 1M HCl solution for 2 minutes followed by washing with deionized (DI) water for 2 minutes and finally with acetone for 2 minutes. The electrodes were then vacuum-dried for 24 hours at 100 °C and transferred into the glovebox. The rest of the assembly followed the same procedure as the Na/Na symmetric cells. All the measurements were carried out at 50 °C and at 20 mV s<sup>-1</sup> scan rate. The onset potential was determined by intersection of the tangent to the exponentially increasing current part of the current curve with the linear extrapolation of the baseline current.

To eliminate any contributions from chemically formed SEI in Cu|Na coin cells during CV measurements, and also to have a reference for more accurate comparison of potentials, an alternative set of CV measurements was performed using a three-electrode cell configuration on gold surface. This setup consisted of a platinum (Pt) coil-shaped electrode as the counter electrode (CE), refillable silver triflate (AgOTf) reference electrodes (RE) filled with the respective ionic liquid (IL) electrolytes containing ~5 mM AgOTf, and gold (Au) electrodes (3 mm diameter) as the working electrode (WE). Prior to the measurements, the electrodes underwent mechanical polishing using a micro-disc cloth covered with alumina (Al<sub>2</sub>O<sub>3</sub>) slurry (0.3 μm), followed by rinsing with deionized water and ethanol. Subsequently, the electrodes were sonicated in ethanol for 5 minutes, dried with argon (Ar) flow, and placed in an oven at 60 °C for 20 minutes. Additionally, the Pt electrodes were annealed using a butane flame. All measurements were conducted under a dry argon atmosphere inside a glovebox (H<sub>2</sub>O ~ 0 ppm, O<sub>2</sub> < 1 ppm) at 50 °C, with a scan rate of 20 mV s<sup>-1</sup>.

### Physicochemical properties

**Differential scanning calorimetry.** DSC measurements were conducted to investigate the thermal behaviour of the electrolytes, such as melting temperature, glass transition temperature ( $T_g$ ), transition entropies and enthalpies. The instrument used for DSC was a NETZSCH DSC 214 Polyma. Three heating and cooling cycles were performed at a scan rate of 10 °C min<sup>-1</sup> from -120 to 30 °C. The first scan was affected by the thermal history of the sample, therefore the reproducible data from the second and third scans are reported. The onset temperature was taken as the  $T_g$ . Cyclohexane from Sigma Aldrich was used as an analytical standard for temperature correction.

**Ionic conductivity.** A BioLogic MTZ-35 impedance analyzer was used to determine ionic conductivity through EIS measurements. In this study, a custom-built dip-cell was used

for conductivity measurements of the electrolyte solutions. This cell contained two platinum wires sheathed in glass sealed with a rubber O-ring and fitted into the cavity of a brass block that was connected to a Eurotherm 2204 temperature controller. Temperature ramping was set at 0.5 °C min<sup>-1</sup> until the desired temperature was obtained (±0.3 °C for 20 min). Electrolyte resistivity was determined from the touch down point of the Nyquist plot (x-axis). A standard solution, 0.01 M KCl, was used to calculate the cell constant at 30 °C. Frequency range was 10 MHz to 1 Hz with a voltage amplitude 0.1 V over the temperature range of -20 to 120 °C. Output data were graphically expressed as Bode or Nyquist plots; Nyquist plots, which present the imaginary part of impedance vs. real impedance were used in this study.<sup>46</sup> Electrolyte resistivity was determined from the touch down point of the Nyquist plot (x-axis).

### Surface morphology

**Scanning electron microscopy (SEM).** In order to investigate the sodium electrode surfaces the coin cells were disassembled using a coin cell disassembly tool (Hohsen, Japan). The electrode with the stainless steel spacer was washed with dimethyl carbonate (DMC, Sigma Aldrich 99%) to remove the residual electrolyte and maintained under vacuum for 15 min inside the antechamber connected to the glovebox. To avoid reaction between the sample and atmosphere an air sensitive container was used to transfer the sample from the glovebox to the SEM. The container was connected to the load lock chamber of the SEM which is designed for loading air sensitive samples. A JEOL JSM-IT300 SEM was used for imaging purposes under 5 kV accelerating voltage. The SEM was coupled with an EDX detector (Oxford X-Max 50 mm<sup>2</sup>) which enabled quantitative analysis of the elements present in the sample.

**In situ optical microscopy.** In the battery setup, sodium metal was pressed onto both ends of the surface of a polypropylene disk, leaving a 10 mm length and 3 mm width gap for the electrolytes. The two sodium electrodes were connected to an electrochemical workstation (LAND CT 3001A) for galvanostatic charge/discharge measurements, with voltage and current recorded simultaneously. Optical microscope images were recorded to monitor the process. The experiment was conducted in an argon environment within a glovebox to ensure an inert environment (Fig. 9).

### Interphase ion layering

**Neutron reflectometry.** In specular reflectometry experiments, the reflectivity (ratio between reflected and incident beam intensities) is measured as a function of  $q_z = 4\pi/\lambda \sin\theta$ , the component of the momentum transfer vector along the normal to the interface plane where  $\lambda$  is neutron wavelength and  $\theta$  is incident angle of neutron beam to the planar surface. The specular reflectivity of neutrons was measured at the neutron reflectometer Spatz<sup>47</sup> which operates in time-of-flight regime (using a 2.5 to 19 Å range of wavelengths) at the 20 MW OPAL reactor (ANSTO, Australia) viewing the cold-neutron





Fig. 9 *In situ* electrochemical/video optical microscopy setup.

source. The sample was placed on a custom electrochemical cell<sup>48</sup> with potentials applied through a BioLogic VSP-300 potentiostat (BioLogic, Grenoble, France). A neutron beam passes through a single-crystal silicon substrate (thickness of 7 mm) with low resistivity ( $<1 \Omega \cdot \text{cm}$ ) to reflect from the interface between a liquid sample and an electrode film (thickness below 300 Å) deposited on the substrate prior to the experiment. The electrode was a double layer of metals e-beam evaporation of  $8 \pm 0.8 \text{ nm}$  Cr and  $20 \pm 2 \text{ nm}$  Au on a single-crystal silicon block with dimensions of diameter 50.8 mm (2-inch) and roughness  $<5 \text{ Å}$  for the working surface (plane orientation  $\langle 111 \rangle$ ). A silicon single crystal with inlet and outlet tubes was used as a backing wafer to contain the bulk liquid and the electrode and backing wafer were separated using a PTFE gasket. The electrochemical cell was filled by the different IL mixture samples inside an argon filled glove box under moisture and oxygen-controlled conditions ( $\text{H}_2\text{O}$  level:  $<1 \text{ ppm}$  and  $\text{O}_2$  level:  $<10 \text{ ppm}$ ). To achieve the largest possible dynamic range of  $q_z$ , two neutron incident angles ( $0.85^\circ$  and  $3.5^\circ$  using a 20 mm footprint) for the same sample were used and the data from the two angles was combined to generate the final data to cover the entire range of  $q_z$  ( $0.008\text{--}0.24 \text{ Å}^{-1}$ ). Reflectivity curves were measured with a  $\Delta Q/Q$  resolution  $\sim 5\%$ . The NR data were fitted by a number of structural models with variation of SLD, thickness and roughness for each layer/layers at the interface using the RefnX package<sup>49</sup> to minimize the difference between the experimental and theoretical curves. A sketch of the NR experiment and interface structure are presented in Fig. 10.

Taking into account materials composition, gravimetric density and volume of the different ion molecules, neutron scattering length density (SLD) was estimated for each component in studied materials (see Table S2<sup>†</sup>).

The initial structure of the Si substrates with electrode layers was determined by fitting the NR measurements at the air/solid interface. The thicknesses of the Au and Cr layers showed good agreement with the manufacturer's specifications. Additionally, a thin  $\text{SiO}_2$  layer between the Si block and the Cr layer was identified and incorporated into the model. These structural parameters for the Si block, Au, Cr, and  $\text{SiO}_2$  layers were subsequently fixed during the fitting of the solid/liquid interface data. A new additional layer was introduced at

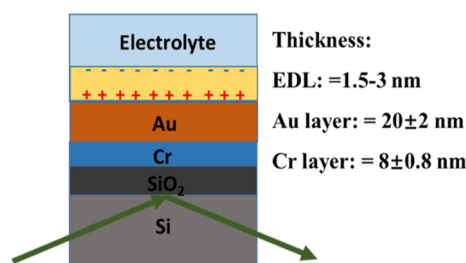


Fig. 10 Sketch of the NR experiment with approximate sizes of the layers.

the IL/solid interface and SLD, thickness and roughness of this layer were varied during the fitting process.

**Atomic force microscopy measurements and imaging.** Atomic force microscopy (AFM) measurements were conducted using a Bruker nanoscope IV Multimode system under ambient conditions. The ionic liquids (ILs) for these studies were stored in a degassed desiccator after being transferred from a glovebox under vacuum sealing and remained there throughout the testing period. Upon opening the IL vials, the liquids were promptly drawn into a syringe and transferred to an AFM liquid cell, which was then sealed for the duration of the measurements.

The working electrode consisted of Au(111) surfaces, comprising a 300 nm thick atomically smooth gold film on mica, obtained from Georg Albert PVD – Beschichtungen. Two 0.25 mm platinum wires (Alfa, 99.99%) were used as the reference and counter electrodes. AFM probes of type HQ:NSC36/Cr-Au BS, featuring gold-coated soft tapping mode cantilevers with a spring constant of approximately  $0.8 \text{ N m}^{-1}$ , were employed for the measurements.

Before the measurements, the gold surfaces and AFM probes were cleaned by sequential rinsing with deionized water and ethanol, followed by drying under nitrogen ( $\text{N}_2$ ) flow. Both were subsequently treated in a UV- $\text{O}_3$  plasma cleaner for 20 minutes.

Measurements were performed at open circuit potential and under applied negative potentials to the working electrode. These potentials were precisely controlled using a Pine WaveNano potentiostat, operated *via* AfterMath software in a three-electrode configuration.

To reduce variability and ensure consistency in the AFM measurements, the same type of soft cantilever was used throughout, and the approach speed was kept low and constant across all samples. These settings were chosen based on literature and optimized to detect subtle ionic layering near the electrode surface. For neutron reflectometry, measurements were performed using the same cell setup and electrode structure, and data from two incident angles were combined to extend the  $q$ -range. All fittings were carried out using a consistent model across samples. While surface-sensitive techniques like AFM and NR can be affected by sample preparation or measurement conditions, the procedures used here were care-



fully controlled to ensure comparability and reliability of the results.

## Author contributions

The manuscript was written through the contributions of all authors. All authors have approved the final version of the manuscript. L. H. – experimental design, methodology, investigation, data analysis, writing original draft. M. M. – conducted AFM experiments (under the guidance of K. S. F., R. A. and H. L.), contributed to experimental design, methodology, investigation, data analysis, and writing the original draft for CV (three-electrode setup) and AFM. M. S., J. M. P. and V. P. – experimental design, methodology, investigation, data analysis, writing original draft for NR. J. H. and X. Z. – methodology guidance for *in situ* OM. F. C. and F. M. – supervising, scientific discussion and understanding concept. P. H. – conceptualization, supervising, scientific discussion and understanding concept. M. F. – conceptualization, supervising, scientific discussion and understanding concept.

## Data availability

Neutron reflectometry: <https://doi.org/10.5281/zenodo.14713708>.

Videos for *in situ* optical microscopy: <https://doi.org/10.26187/deakin.28282061>.

The remaining data supporting this article are included as part of the ESI.†

## Conflicts of interest

The authors declare no conflict of interest.

## Acknowledgements

The authors acknowledge the Australian Research Council (ARC) for funding under Discovery Project DP210101172, Future Energy Storage Technologies (StorEnergy) IC180100049, and Deakin University Battery Research and Innovation Hub facilities. M. S. acknowledges the funding from the European Union H2020 Program under the Marie Curie global fellowship (ROCHE, 101026163). J. M. P. acknowledges the Ramón y Cajal grant RYC2023-044841-I funded by MICIU/AEI/10.13039/501100011033 and by the FSE+. Neutron beamtime was awarded by ANSTO under proposal 17200. Spatz operations are supported by the National Collaborative Research Infrastructure Strategy (NCRIS), an Australian Government initiative. J. H. and X. Z. 's work was supported by the National Natural Science Foundation (NSFC) of China (U20A20336, and 21935009), and the Hebei Natural Science Foundation (B2024203054). The authors extend their thanks to Luke O'Dell, Agilio Padua, and Michel Armand for their supervision, scientific discussions, and conceptual insights.

## References

- 1 K. Matsumoto, J. Hwang, S. Kaushik, C.-Y. Chen and R. Hagiwara, Advances in sodium secondary batteries utilizing ionic liquid electrolytes, *Energy Environ. Sci.*, 2019, **12**(11), 3247–3287.
- 2 B. Sun, P. Xiong, U. Maitra, D. Langsdorf, K. Yan, C. Wang, J. Janek, D. Schroder and G. Wang, Design Strategies to Enable the Efficient Use of Sodium Metal Anodes in High-Energy Batteries, *Adv. Mater.*, 2020, **32**(18), e1903891.
- 3 K. Dong, X. Liu, H. Dong, X. Zhang and S. Zhang, Multiscale Studies on Ionic Liquids, *Chem. Rev.*, 2017, **117**(10), 6636–6695.
- 4 K. Karupphasamy, J. Theerthagiri, D. Vikraman, C.-J. Yim, S. Hussain, R. Sharma, T. Maiyalagan, J. Qin and H.-S. Kim, Ionic Liquid-Based Electrolytes for Energy Storage Devices: A Brief Review on Their Limits and Applications, *Polymers*, 2020, **12**(4), 918.
- 5 Z. Xue, L. Qin, J. Jiang, T. Mu and G. Gao, Thermal, electrochemical and radiolytic stabilities of ionic liquids, *Phys. Chem. Chem. Phys.*, 2018, **20**(13), 8382–8402.
- 6 S. A. Ferdousi, L. A. O'Dell, J. Sun, Y. Hora, M. Forsyth and P. C. Howlett, High-Performance Cycling of Na Metal Anodes in Phosphonium and Pyrrolidinium Fluoro(sulfonyl)imide Based Ionic Liquid Electrolytes, *ACS Appl. Mater. Interfaces*, 2022, **14**(13), 15784–15798.
- 7 M. Hilder, P. C. Howlett, D. Saurel, E. Gonzalo, A. Basile, M. Armand, T. Rojo, M. Kar, D. R. MacFarlane and M. Forsyth, The effect of cation chemistry on physicochemical behaviour of superconcentrated NaFSI based ionic liquid electrolytes and the implications for Na battery performance, *Electrochim. Acta*, 2018, **268**, 94–100.
- 8 C. M. Schott, P. M. Schneider, K.-T. Song, H. Yu, R. Götz, F. Haimerl, E. Gubanova, J. Zhou, T. O. Schmidt, Q. Zhang, V. Alexandrov and A. S. Bandarenka, How to Assess and Predict Electrical Double Layer Properties. Implications for Electrocatalysis, *Chem. Rev.*, 2024, **124**(22), 12391–12462.
- 9 X. Mao, P. Brown, C. Cervinka, G. Hazell, H. Li, Y. Ren, D. Chen, R. Atkin, J. Eastoe, I. Grillo, A. A. H. Padua, M. F. Costa Gomes and T. A. Hatton, Self-assembled nanostructures in ionic liquids facilitate charge storage at electrified interfaces, *Nat. Mater.*, 2019, **18**(12), 1350–1357.
- 10 J. M. Black, M. Zhu, P. Zhang, R. R. Unocic, D. Guo, M. B. Okatan, S. Dai, P. T. Cummings, S. V. Kalinin, G. Feng and N. Balke, Fundamental aspects of electric double layer force-distance measurements at liquid-solid interfaces using atomic force microscopy, *Sci. Rep.*, 2016, **6**, 32389.
- 11 G. Yang, I. N. Ivanov, R. E. Ruther, R. L. Sacci, V. Subjakova, D. T. Hallinan and J. Nanda, Electrolyte Solvation Structure at Solid-Liquid Interface Probed by Nanogap Surface-Enhanced Raman Spectroscopy, *ACS Nano*, 2018, **12**(10), 10159–10170.
- 12 Y. Gu, E.-M. You, J.-D. Lin, J.-H. Wang, S.-H. Luo, R.-Y. Zhou, C.-J. Zhang, J.-L. Yao, H.-Y. Li, G. Li, W.-W. Wang, Y. Qiao, J.-W. Yan, D.-Y. Wu, G.-K. Liu,



- L. Zhang, J.-F. Li, R. Xu, Z.-Q. Tian, Y. Cui and B.-W. Mao, Resolving nanostructure and chemistry of solid-electrolyte interphase on lithium anodes by depth-sensitive plasmon-enhanced Raman spectroscopy, *Nat. Commun.*, 2023, **14**(1), 3536.
- 13 N. Kumar and J. M. Seminario, Lithium-Ion Model Behavior in an Ethylene Carbonate Electrolyte Using Molecular Dynamics, *J. Phys. Chem. C*, 2016, **120**(30), 16322–16332.
- 14 D. A. Rakov, F. Chen, S. A. Ferdousi, H. Li, T. Pathirana, A. N. Simonov, P. C. Howlett, R. Atkin and M. Forsyth, Engineering high-energy-density sodium battery anodes for improved cycling with superconcentrated ionic-liquid electrolytes, *Nat. Mater.*, 2020, **19**(10), 1096–1101.
- 15 H. Wang, D. Ning, L. Wang, H. Li, Q. Li, M. Ge, J. Zou, S. Chen, H. Shao and Y. Lai, In Operando Neutron Scattering Multiple-Scale Studies of Lithium-Ion Batteries, *Small*, 2022, **18**(19), 2107491.
- 16 K. S. Fraysse, L. Huang, H. Li, R. Atkin, A. Padua, M. Armand, P. C. Howlett and M. Forsyth, On the Parasitic Surface Adsorption of Pyrrolidinium and Phosphonium-based Ionic Liquids Preventing Accurate Differential Capacitance Measurements, *J. Electrochem. Soc.*, 2024, **171**(10), 106506.
- 17 J. N. Canongia Lopes, T. C. Cordeiro, J. M. S. S. Esperança, H. J. R. Guedes, S. Huq, L. P. N. Rebelo and K. R. Seddon, Deviations from Ideality in Mixtures of Two Ionic Liquids Containing a Common Ion, *J. Phys. Chem. B*, 2005, **109**(8), 3519–3525.
- 18 G. Annat, M. Forsyth and D. R. MacFarlane, Ionic liquid mixtures-variations in physical properties and their origins in molecular structure, *J. Phys. Chem. B*, 2012, **116**(28), 8251–8258.
- 19 H. Wu, K. Han, W. Hu, W. Feng, M. Armand, Z. Zhou and H. Zhang, Ionic liquids with sulfinyl-functionalized imide anion and their lithium electrolytes: (I) Physical and electrochemical properties, *J. Power Sources Adv.*, 2024, **28**, 100154.
- 20 V. Chaudoy, J. Jacquemin, F. Tran-Van, M. Deschamps and F. Ghamouss, Effect of mixed anions on the transport properties and performance of an ionic liquid-based electrolyte for lithium-ion batteries, *Pure Appl. Chem.*, 2019, **91**(8), 1361–1381.
- 21 V. Lesch, S. Jeremias, A. Moretti, S. Passerini, A. Heuer and O. Borodin, A combined theoretical and experimental study of the influence of different anion ratios on lithium ion dynamics in ionic liquids, *J. Phys. Chem. B*, 2014, **118**(26), 7367–7375.
- 22 M. Martinez-Ibañez, N. Boaretto, L. Meabe, X. Wang, H. Zhu, A. Santiago, O. Zugazua, M. Forsyth, M. Armand and H. Zhang, Revealing the Anion Chemistry Effect on Transport Properties of Ternary Gel Polymer Electrolytes, *Chem. Mater.*, 2022, **34**(16), 7493–7502.
- 23 N. N. Intan and J. Pfaendtner, Effect of Fluoroethylene Carbonate Additives on the Initial Formation of the Solid Electrolyte Interphase on an Oxygen-Functionalized Graphitic Anode in Lithium-Ion Batteries, *ACS Appl. Mater. Interfaces*, 2021, **13**(7), 8169–8180.
- 24 T. Gao, J. Bian, F. Huang, S. Ling, Z. Li, H. Yuan, H. Lin, L. Kong, B. Deng, Y. Zhao and Z. Lu, Enhanced cycling, safety and high-temperature performance of hybrid Li ion/Li metal batteries via fluoroethylene carbonate additive, *Mater. Chem. Phys.*, 2024, **314**, 128868.
- 25 U. Pal, D. Rakov, B. Lu, B. Sayahpour, F. Chen, B. Roy, D. R. MacFarlane, M. Armand, P. C. Howlett, Y. S. Meng and M. Forsyth, Interphase control for high performance lithium metal batteries using ether aided ionic liquid electrolyte, *Energy Environ. Sci.*, 2022, **15**(5), 1907–1919.
- 26 H. Ye, Y.-X. Yin, S.-F. Zhang, Y. Shi, L. Liu, X.-X. Zeng, R. Wen, Y.-G. Guo and L.-J. Wan, Synergism of Al-containing solid electrolyte interphase layer and Al-based colloidal particles for stable lithium anode, *Nano Energy*, 2017, **36**, 411–417.
- 27 S. Park, S. Y. Jeong, T. K. Lee, M. W. Park, H. Y. Lim, J. Sung, J. Cho, S. K. Kwak, S. Y. Hong and N. S. Choi, Replacing conventional battery electrolyte additives with dioxolone derivatives for high-energy-density lithium-ion batteries, *Nat. Commun.*, 2021, **12**(1), 838.
- 28 D. A. Rakov, J. Sun, P. V. Cherepanov, K. Arano, P. C. Howlett, A. N. Simonov, F. Chen and M. Forsyth, The impact of electrode conductivity on electrolyte interfacial structuring and its implications on the Na<sup>0/+</sup> electrochemical performance, *Energy Environ. Sci.*, 2023, **16**(9), 3919–3931.
- 29 T. Pathirana, D. A. Rakov, F. Chen, M. Forsyth, R. Kerr and P. C. Howlett, Improving Cycle Life through Fast Formation Using a Superconcentrated Phosphonium Based Ionic Liquid Electrolyte for Anode-Free and Lithium Metal Batteries, *ACS Appl. Energy Mater.*, 2021, **4**(7), 6399–6407.
- 30 S. Begić, F. Chen, E. Jónsson and M. Forsyth, Water as a catalyst for ion transport across the electrical double layer in ionic liquids, *Phys. Rev. Mater.*, 2020, **4**(4), 045801.
- 31 L. Huang, F. Makhlooghiyazad, L. A. O'Dell, P. C. Howlett and M. Forsyth, Investigating the role of mixed-cation ionic liquid electrolytes in sodium battery efficiency and stability, *Mater. Adv.*, 2024, **5**(17), 6899–6909.
- 32 A. Warrington, L. A. O'Dell, O. E. Hutt, M. Forsyth and J. M. Pringle, Structure and interactions of novel ether-functionalised morpholinium and piperidinium ionic liquids with lithium salts, *Energy Adv.*, 2023, **2**(4), 530–546.
- 33 A. Warrington, M. Hasanpoor, A. Balkis, P. C. Howlett, O. E. Hutt, M. Forsyth and J. M. Pringle, Investigation of properties and performance of three novel highly concentrated ether-functionalised ionic liquid electrolytes for lithium metal batteries, *Energy Storage Mater.*, 2023, **63**, 102984.
- 34 K.-H. Chen, K. N. Wood, E. Kazyak, W. S. LePage, A. L. Davis, A. J. Sanchez and N. P. Dasgupta, Dead lithium: mass transport effects on voltage, capacity, and failure of lithium metal anodes, *J. Mater. Chem. A*, 2017, **5**(23), 11671–11681.



- 35 K. N. Wood, E. Kazyak, A. F. Chadwick, K. H. Chen, J. G. Zhang, K. Thornton and N. P. Dasgupta, Dendrites and Pits: Untangling the Complex Behavior of Lithium Metal Anodes through Operando Video Microscopy, *ACS Cent. Sci.*, 2016, **2**(11), 790–801.
- 36 A. Aleshin, S. Bravo, K. Redquest and K. N. Wood, Rapid Oxidation and Reduction of Lithium for Improved Cycling Performance and Increased Homogeneity, *ACS Appl. Mater. Interfaces*, 2021, **13**(2), 2654–2661.
- 37 S. Begić, H. Li, R. Atkin, A. F. Hollenkamp and P. C. Howlett, A comparative AFM study of the interfacial nanostructure in imidazolium or pyrrolidinium ionic liquid electrolytes for zinc electrochemical systems, *Phys. Chem. Chem. Phys.*, 2016, **18**(42), 29337–29347.
- 38 P. C. Howlett, E. I. Izgorodina, M. Forsyth and D. R. MacFarlane, Electrochemistry at Negative Potentials in Bis(trifluoromethanesulfonyl)amide Ionic Liquids, *Z. für Phys. Chem.*, 2006, **220**(10), 1483–1498.
- 39 D. A. Rakov, J. Sun, S. A. Ferdousi, P. C. Howlett, A. N. Simonov, F. Chen and M. Forsyth, Polar Organic Cations at Electrified Metal with Superconcentrated Ionic Liquid Electrolyte and Implications for Sodium Metal Batteries, *ACS Mater. Lett.*, 2022, **4**(10), 1984–1990.
- 40 A. Davoodabadi, C. Jin, D. L. Wood III, T. J. Singler and J. Li, On electrolyte wetting through lithium-ion battery separators, *Extreme Mech. Lett.*, 2020, **40**, 100960.
- 41 D. A. Rakov, F. Chen, S. A. Ferdousi, H. Li, T. Pathirana, A. N. Simonov, P. C. Howlett, R. Atkin and M. Forsyth, Engineering high-energy-density sodium battery anodes for improved cycling with superconcentrated ionic-liquid electrolytes, *Nat. Mater.*, 2020, **19**(10), 1096–1101.
- 42 S. A. Ferdousi, L. A. O'Dell, J. Sun, Y. Hora, M. Forsyth and P. C. Howlett, High-performance cycling of Na metal anodes in phosphonium and pyrrolidinium fluoro (sulfonyl) imide based ionic liquid electrolytes, *ACS Appl. Mater. Interfaces*, 2022, **14**(13), 15784–15798.
- 43 J. Kim, G. R. Lee, R. B. K. Chung, P. J. Kim and J. Choi, Homogeneous Li deposition guided by ultra-thin lithiophilic layer for highly stable anode-free batteries, *Energy Storage Mater.*, 2023, **61**, 102899.
- 44 Q. Wang, C. Zhao, S. Wang, J. Wang, M. Liu, S. Ganapathy, X. Bai, B. Li and M. Wagemaker, Clarifying the Relationship between the Lithium Deposition Coverage and Microstructure in Lithium Metal Batteries, *J. Am. Chem. Soc.*, 2022, **144**(48), 21961–21971.
- 45 Y. Ji, H. Sun, Z. Li, L. Ma, W. Zhang, Y. Liu, L. Pan, W. Mai and J. Li, Salt engineering toward stable cation migration of Na metal anodes, *J. Mater. Chem. A*, 2022, **10**(48), 25539–25545.
- 46 E. M. Barsoukov and J. R. MacDonald, *Impedance Spectroscopy Theory Experiment And Applications*, 2004.
- 47 A. P. Le Brun, T. Y. Huang, S. Pullen, A. R. J. Nelson, J. Spedding and S. A. Holt, Spatz: the time-of-flight neutron reflectometer with vertical sample geometry at the OPAL research reactor, *J. Appl. Crystallogr.*, 2023, **56**(Pt 1), 18–25.
- 48 Y. Lauw, T. Rodopoulos, M. Gross, A. Nelson, R. Gardner and M. D. Horne, Electrochemical cell for neutron reflectometry studies of the structure of ionic liquids at electrified interface, *Rev. Sci. Instrum.*, 2010, **81**(7), 074101.
- 49 A. R. J. Nelson and S. W. Prescott, retnx: neutron and X-ray reflectometry analysis in Python, *J. Appl. Crystallogr.*, 2019, **52**(Pt 1), 193–200.

