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Hydroxylamine intermediate governs selectivity in nitrite hydrogenation on Pd-based catalysts for sustainable water treatment

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Catalytic hydrogenation of nitrate (NO_3^-) and nitrite (NO_2^-) is a promising route for drinking water purification and rebalancing the global nitrogen cycle. Recently, hydroxylamine (NH_2OH) was detected as a persistent reaction intermediate although ammonium (NH_4^+) and dinitrogen (N_2) were assumed to be the only significant reaction products for several decades. In this work, we systematically investigate NO_2^- hydrogenation over $\text{Pd}/\text{Al}_2\text{O}_3$ and $\text{SnPd}/\text{Al}_2\text{O}_3$ while explicitly quantifying NH_2OH under various conditions, including changes in H_2 partial pressure, the initial NO_2^- concentration, and reaction temperature, and through co-feeding of NH_2OH . We reveal that NH_4^+ selectivity depends strongly on the NO_2^- conversion level, reflecting shifts in surface coverages as the reaction progresses. Suppression of both NH_2OH and NH_4^+ formation is only achievable under H_2 -deficient conditions, though this comes at the expense of lower overall hydrogenation activity. Elevated temperatures enhance NH_2OH decomposition and thereby promote NH_4^+ formation, while leaving N_2 selectivity largely unaffected. Co-feeding experiments further show that externally introduced NH_2OH does not influence the NO_2^- hydrogenation rate. We critically reviewed prior mechanistic studies on NO_2^- hydrogenation and propose a refined Langmuir–Hinshelwood scheme that explicitly incorporates NH_2OH as a desorbed intermediate. This work highlights the importance of NH_2OH in the reaction network and underscores the need to include it in the assessment of the reaction selectivity.

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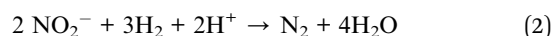
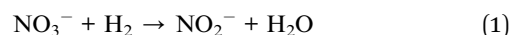
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1 Introduction

Nitrate (NO_3^-) and nitrite (NO_2^-) are water contaminants that pose a serious threat to both human health and aquatic ecosystems if not properly controlled. Although these species are natural components of the biogeochemical nitrogen cycle, the excessive use of nitrogen-based fertilizers has severely disrupted this balance in recent decades.^{1–4} As a consequence, nitrogen nutrient levels have risen in inland, coastal, and marine waters, driving eutrophication.⁵ Eutrophication negatively impacts entire ecosystems by reducing biodiversity of animals and plants. In addition, elevated nitrate and nitrite concentrations can directly affect human health. When present in drinking water, these species may cause methemoglobinemia—commonly known as “blue baby syndrome”⁶ and have, therefore, strict limits (50 and 5 mg L^{-1} , respectively).⁷

Catalytic nitrate and nitrite reduction has emerged as a promising technology to convert these species into harmless

dinitrogen (N_2).⁸ In contrast to alternative remediation methods such as reverse osmosis, ion exchange, or electrodialysis, catalytic reduction degrades the contaminants rather than concentrating them into waste brines.⁸ Nitrate is first reduced to nitrite, which is then further hydrogenated to N_2 . In this reaction network, the hydrogenation of nitrate to nitrite is the rate determining step (RDS) and requires a bimetallic catalyst (*e.g.* Sn–Pd, Cu–Pd, or In–Pd), while the subsequent nitrite hydrogenation can be catalyzed by Pd alone.^{9–12}



The main challenge for application remains the formation of ammonium (NH_4^+), which follows even stricter regulations (0.5 mg L^{-1}).¹³



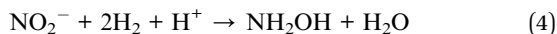
While the formation of NH_2OH in electro- and photocatalytic NO_3^- and NO_2^- reduction has been reported in the past,^{14–16} its presence in thermo-catalytic conversion was only reported very recently. The results showed that hydroxylamine (NH_2OH) is an

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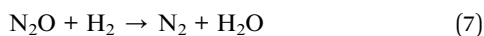
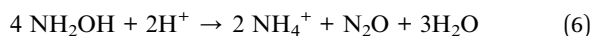
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omnipresent and long-lasting reaction intermediate under various reaction conditions on several different catalysts (eqn (4)).¹⁷ Until then, a pervasive assumption in the field was that N₂ and ammonium (NH₄⁺) were the only relevant reaction products of thermocatalytic NO₃⁻ and NO₂⁻ hydrogenation under relevant reaction conditions for drinking water purification.^{8–12,18–22}



Hydroxylamine is highly toxic and harmful for water bodies²³ and therefore represents a major challenge for the application of NO₃⁻ and NO₂⁻ as water purification technology. Upon extension of the reaction time, NH₂OH can be hydrogenated to NH₄⁺ (eqn (5)) or disproportionate into NH₄⁺ and nitrous oxide (N₂O, eqn (6)). The latter is quickly further hydrogenated into N₂ (eqn (7)).²⁴



Thus, NH₂OH is at least 50% decomposed into undesired NH₄⁺. In previous research it was shown that NH₂OH decomposition proceeds exclusively *via* the hydrogenation pathway in the absence of NO₃⁻ and NO₂⁻ and in the presence of H₂ over a Pd/Al₂O₃ catalyst. In contrast, in the presence of residual NO₃⁻, NO₂⁻ or their remaining surface species adsorbed on the catalyst, the hydrogenation and the disproportionation pathway contribute to the NH₂OH decomposition.¹⁷

In this study, NH₂OH is used as a reaction marker to unravel the interplay between the reaction rate of NO₂⁻ hydrogenation and the selectivity to NH₂OH, NH₄⁺ and N₂. To do this we investigated detailed reaction kinetics for the NO₂⁻ hydrogenation on Pd/Al₂O₃ and SnPd/Al₂O₃ catalysts at different H₂ partial pressures, initial NO₂⁻ concentrations, and temperatures while monitoring the NH₂OH and NH₄⁺ concentrations to deliver a complete picture of the selectivity patterns and reaction order dependencies. The results drastically change the prevailing view that ammonia and nitrogen are the only two reaction products while showcasing the complex interdependence between hydrogen, nitrite, and hydroxylamine ratios in the observed kinetics and product distribution.

2 Materials and methods

2.1 Materials

Pd/Al₂O₃ and Tin(II) chloride (SnCl₂) were purchased from Fisher Scientific and potassium nitrate (KNO₃), potassium nitrite (KNO₂), benzaldehyde (≥99.5%), benzaldehyde oxime (≥96.5%) and hydroxylamine (50 wt% in H₂O) were purchased from Sigma Aldrich.

2.2 Catalyst preparation

Pd/Al₂O₃ was dried before use and sieved to a support particle size <25 μm. SnPd/Al₂O₃ was prepared from the same Pd/Al₂O₃

(<25 μm) *via* controlled surface deposition.^{25,26} Therefore, Pd/Al₂O₃ was suspended in water and exposed to a continuous gas flow of 80 : 10 : 10 mL min⁻¹ H₂ : He : CO₂ to reduce the catalyst for 30 min at RT. SnCl₂ was dissolved in degassed Milli-Q water and a volume containing Sn in amounts corresponding to 40% of the monolayer capacity of Pd based on CO-chemisorption was added to the catalyst suspension. The suspension is stirred for another 30 min and subsequently filtered to recover the catalyst powder. The filter cake was dried in a vacuum at 70 °C followed by calcination (500 °C in 50 mL min⁻¹ air, 5 °C min⁻¹, 5 h) and reduction (500 °C in 30 mL min⁻¹ H₂ and N₂ each, 5 °C min⁻¹, 5 h) in a tube oven. The catalyst is stored in air at ambient temperature.

2.3 Catalyst characterization

The metal loadings were determined with X-ray fluorescence (XRF). For the measurements a Bruker S8 Tiger Series 1 4 kW X-ray spectrometer was used. The samples were measured as powder, in a sample cup with a Mylar film, in a helium environment. The concentrations of each element were calculated from the K α or L α lines of all elements, using the internal database. The metal dispersion and metal particle sizes were determined by CO-chemisorption. Therefore, the samples were reduced in H₂ for 1 h and purged with He for 20 min followed by CO-pulsing (all at RT, Micromeritics Chemisorb 2750). A Pd : CO 1 : 1 ratio and the geometry factor for a hemisphere (6) are assumed. The Brunauer–Emmet–Teller (BET) surface area was determined *via* N₂ physisorption at –196 °C after outgassing for 24 h at 300 °C (Micromeritics Tristar 3000). The characterization results are summarized in Table 1.

2.4 Catalytic testing

In a typical experiment, Pd/Al₂O₃ or SnPd/Al₂O₃ was suspended in 297 mL of deionized water in a 1 L baffled glass reactor equipped with a four-blade magnetic stirrer. The catalyst was reduced *in situ* under continuous gas flow (80 : 10 : 10 mL min⁻¹ H₂ : CO₂ : He) for 1 h at 600 rpm. After the activation period, 3 mL of a KNO₂ stock solution was injected to reach the desired initial concentration and to initiate the reaction. Liquid samples were withdrawn periodically, passed through a 0.2 μm syringe filters to remove catalyst particles to terminate the reaction in the sample, and subsequently analyzed. NO₃⁻, NO₂⁻ and NH₄⁺ concentrations were analyzed *via* ion chromatography (IC, a Dionex ICS-3000 with electronic suppression, Thermo Fisher AS19 and CS12 columns with 20 mmol L⁻¹ potassium hydroxide (KOH) and 20 mmol L⁻¹ methane sulfonic acid (MSA) as eluents and an Automate 2000 autosampler). For NH₂OH determination, 0.5 μL benzaldehyde was added right after sampling to derivatize NH₂OH to benzaldehyde oxime.¹⁷ Benzaldehyde oxime was quantified *via* HPLC (Shimadzu HPLC10AVP with an autosampler, a C18 hypersil gold column, a MeOH : H₂O (30 : 70 V% eluent, and a UV-vis detector at 248 nm). IC and HPLC analysis were conducted from the same sample vial and RT refers to 22 °C. In some experiments the analysis of the gas phase was attempted but ambient N₂ could not sufficiently be suppressed to ensure satisfactory sensitivity.



Table 1 Catalyst material properties based on N₂ physisorption, XRF and CO-chemisorption

Catalyst	BET surface area	Pd loading	Sn loading	Average Pd particle size
Pd/Al ₂ O ₃	110 m ² g ⁻¹	8.1 wt%	—	10.3 nm
SnPd/Al ₂ O ₃	—	8.4 wt%	0.7 wt%	—

In these approaches NO, NO₂ or N₂O could be detected. The selectivity was calculated as $S_{\text{NH}_4^+} = \frac{[\text{NH}_4^+]_t}{([\text{NO}_2^-]_0 - [\text{NO}_2^-]_t)}$ or $S_{\text{NH}_2\text{OH}} = \frac{[\text{NH}_2\text{OH}]_t}{([\text{NO}_2^-]_0 - [\text{NO}_2^-]_t)}$ and the remaining fraction to 1 considered as N₂.

3 Results and discussion

3.1 NO₂⁻ hydrogenation on Pd/Al₂O₃ at RT

The NO₂⁻ hydrogenation was conducted in a concentration window of 0.26–6.5 mmol L⁻¹ at 0.8 bar H₂ and at H₂ partial pressures between 0.05 and 0.8 bar for 0.8 mmol L⁻¹ NO₂⁻ in the absence of internal (SI, Fig. 1) and external mass transport limitations.^{27,28} Initial rate constants were obtained from concentration–time profiles (SI, Fig. 2) and plotted in log–log form (Fig. 1) to determine the reaction orders. At RT, a reaction order close to zero with respect to NO₂⁻ and ~0.2 with respect to H₂ was observed, confirming previous results from our group.^{27,28}

Thus, the NO₂⁻ hydrogenation activity at room temperature is independent of the NO₂⁻ concentration, while slightly accelerated by increasing H₂ partial pressure. The low sensitivity towards both NO₂⁻ and H₂ concentrations suggests that the catalyst surface is predominantly covered by intermediates prior to the rate-determining step, leaving few sites available for additional NO₂⁻ or H₂ adsorption. This interpretation is consistent with previous Attenuated Total Reflection Infrared Spectroscopy (ATR-IR) studies as discussed later.^{29–31}

To evaluate the selectivity of the reaction, NH₄⁺ and NH₂OH concentrations were measured delivering a typical reaction profile as shown in Fig. 2A. Initially both NH₄⁺ and NH₂OH concentrations increase with decreasing NO₂⁻ concentration. While the NH₄⁺ concentration consistently increases, the

NH₂OH concentration passes through a maximum and subsequently decreases illustrating its intermediary nature. The remaining part of the converted NO₂⁻ is assumed to be N₂. The NH₄⁺ selectivity ranges from <1% to 10%, depending on the H₂ partial pressure and the NO₂⁻ conversion level. The NH₄⁺ concentration increases at a faster rate when NO₂⁻ is near full conversion, reflecting shifts in surface coverages during the reaction. When plotted as a function of NO₂⁻ conversion, the NH₄⁺ selectivity follows a U-shaped dependence (Fig. 2B). Before NO₂⁻ injection (*i.e.*, at the start of the reaction), the catalyst is activated in H₂-saturated water, giving high surface H-coverage and a high H : N ratio, which promotes NH₄⁺ formation. As the reaction proceeds, H-coverage decreases while N-coverage increases, favoring N–N coupling and thereby enhancing N₂ selectivity. At high NO₂⁻ conversion, N-species are depleted, the H : N ratio shifts back toward higher H-coverage, and NH₄⁺ selectivity increases again. Thus, the time required to achieve a pseudo steady state is an intrinsic disadvantage of batch experiments due to their transient nature. The competitive adsorption of NO₂⁻ and H₂ was demonstrated by Postma *et al.*³² and Huang *et al.*²⁸ but is often not considered in batch experiments. This highlights the importance of monitoring NH₄⁺ selectivity over the entire conversion range, since relying on initial selectivity is likely biased by the initial high H-coverage. While NH₄⁺ formation generally decreases with decreasing H₂ partial pressure, substantial NH₄⁺ suppression occurs only under strongly H₂-deficient conditions (0.05 bar, Fig. 2B), which also reduces the NO₂⁻ hydrogenation rate. This dependence reflects the higher H₂ demand for NH₄⁺ formation relative to NO₂⁻ hydrogenation (3 vs. 1.5 H₂ per NO₂⁻, see eqn (2) and (3)).

Despite the intermediary character of NH₂OH, monitoring NH₂OH is crucial as its maximum concentration at RT is typically observed around full NO₂⁻ conversion (Fig. 1C), thus representing a point where the reaction could otherwise be

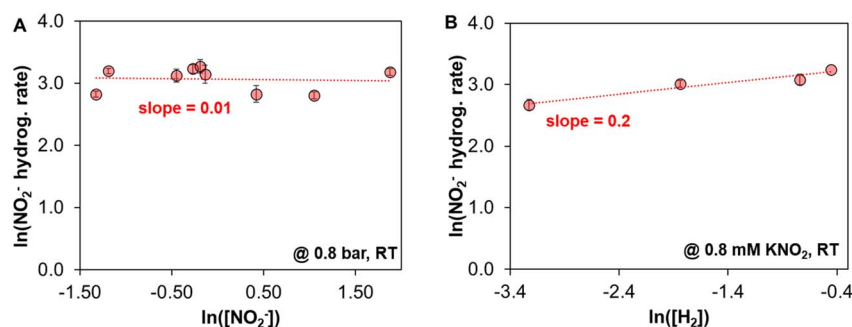


Fig. 1 Effect of NO₂⁻ (A) and H₂ concentration (B) on the NO₂⁻ hydrogenation rate on Pd/Al₂O₃. Reaction conditions: 300 mL H₂O, 0.3–6.5 mmol L⁻¹ KNO₂, 10 mg Pd/Al₂O₃, 10 mL min⁻¹ CO₂, 5–80 mL min⁻¹ H₂ and He to balance to 100 mL min⁻¹ total flow, RT, 600 rpm.



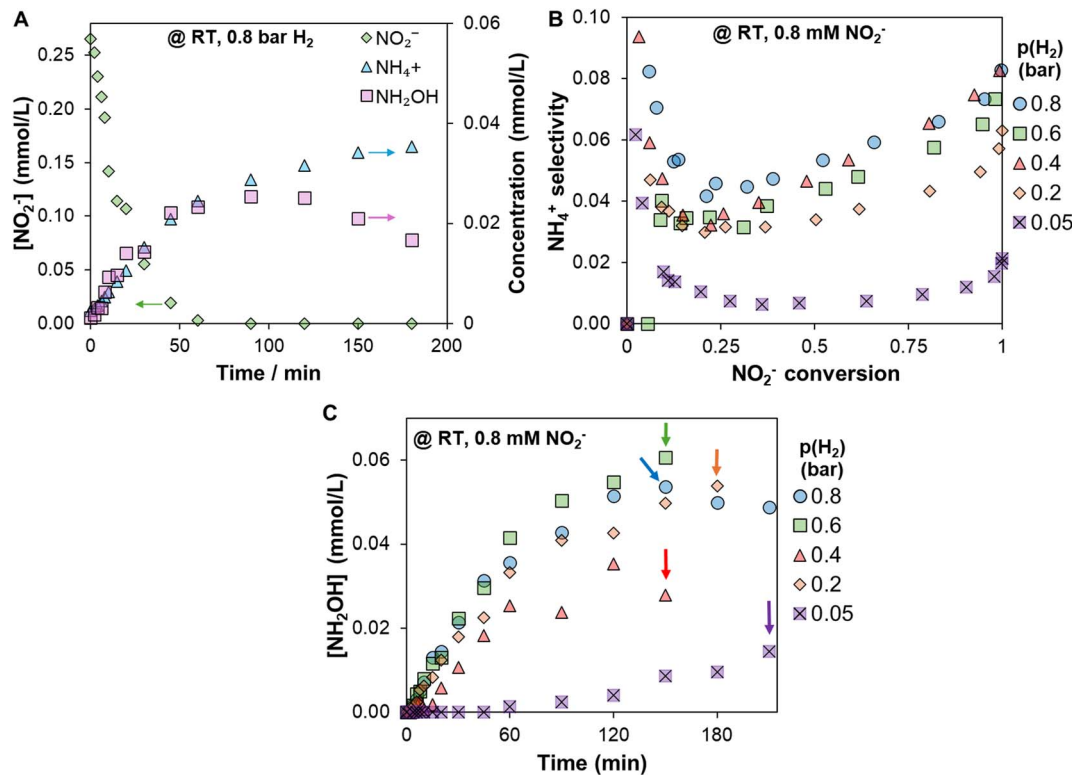


Fig. 2 Typical concentration profile of NO_2^- hydrogenation (A), NH_4^+ selectivity as a function of NO_2^- conversion (B) and NH_2OH concentration as a function of time in which arrows indicate full NO_2^- conversion (C). Reaction conditions: 300 mL H_2O , 10 mg $\text{Pd}/\text{Al}_2\text{O}_3$, 0.8 mmol L^{-1} KNO_2 , 10 mL min^{-1} CO_2 , 5–80 mL min^{-1} H_2 and He to balance to 100 mL min^{-1} total flow, RT, 600 rpm.

mistakenly considered complete. While the NH_2OH selectivity ranges from 3–8% at H_2 partial pressures ranging from 0.2 to 0.8 bar (SI, Fig. 3), the NH_2OH production is minimized when using very low H_2 partial pressure (0.05 bar, Fig. 2C). This drastic change in selectivity, however, comes at the expense of reduced NO_2^- hydrogenation. This behavior is consistent with the higher H_2 demand for NH_2OH formation compared to N_2 formation (2 vs. 1.5 H_2 per NO_2^- , see eqn (2) and (4)).

Varying the initial NO_2^- concentration had little influence on NH_4^+ and NH_2OH formation (Fig. 3A and B, respectively) which is consistent with an apparent reaction order of zero in

NO_2^- , implying that the surface coverages are only mildly influenced by variation of the NO_2^- concentration. At the highest initial NO_2^- concentration, the formation of NH_4^+ and NH_2OH appears to be slightly reduced. This can be rationalized by increased N-coverage on the catalyst surface resulting in a higher N–N coupling probability which is in line with findings of Xu *et al.*²⁷

3.2 NO_2^- hydrogenation on $\text{Pd}/\text{Al}_2\text{O}_3$ at 40 °C

The same set of experiments was performed at 40 °C to investigate the effect of reaction temperature. The H_2 reaction order

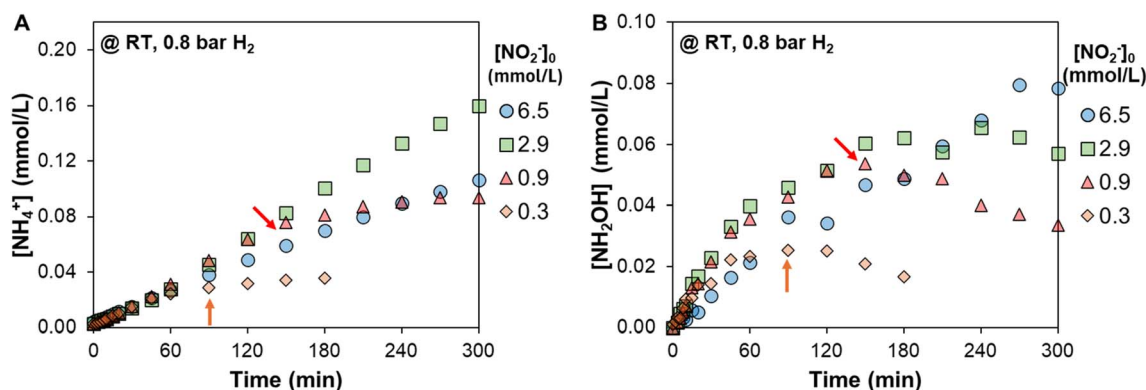


Fig. 3 NH_4^+ concentration (A) and NH_2OH concentration (B) at RT as a function of time at different initial NO_2^- concentrations. Arrows indicate the time of full NO_2^- conversion, if reached. Reaction conditions: 300 mL H_2O , 10 mg $\text{Pd}/\text{Al}_2\text{O}_3$, 80 : 10 : 10 mL min^{-1} H_2 : CO_2 : He, RT, 600 rpm.



remained ~ 0.2 while the NO_2^- hydrogenation activity is more sensitive to changes in the initial NO_2^- concentration at 40°C illustrated by a positive reaction order of 0.24 below 0.8 mmol L^{-1} NO_2^- and a negative reaction order of -0.47 above 0.8 mmol L^{-1} (SI, Fig. 4).

A typical concentration profile at 40°C is shown in the SI, Fig. 5. At 40°C , the NH_4^+ selectivity increases from 3–8% (RT, Fig. 2B) to 10–15% or even to 25% (0.6 bar , Fig. 4A) and the U-shape is less pronounced, or at 0.6 bar even disappeared entirely. In contrast, the maximum NH_2OH concentration at 40°C decreased by $\sim 50\%$ compared to RT and the maximum NH_2OH concentration is no longer observed near full NO_2^- conversion (Fig. 4B). Instead, the NH_2OH concentrations declined already before completion of NO_2^- hydrogenation. This indicates that elevated temperatures favor NH_2OH decomposition, lowering the measurable bulk NH_2OH concentration.

As NH_2OH primarily decomposes to NH_4^+ , faster NH_2OH decomposition explains the higher NH_4^+ selectivity at 40°C . Notably, the N_2 selectivity, calculated as the remainder of NH_4^+ and NH_2OH selectivity, is largely unchanged across most H_2 partial pressures at both RT and 40°C (Fig. 4C). Thus, the additional NH_4^+ at 40°C can be attributed to accelerated NH_2OH decomposition. Only at 0.6 bar of hydrogen the

nitrogen selectivity is substantially lower while NH_4^+ selectivity reaches a higher value, suggesting increased NH_4^+ formation from NO_2^- .

This kinetic study indicates that the formation of NH_4^+ can be suppressed under H_2 -deficient conditions, albeit at the expense of lower overall NO_2^- hydrogenation rates. The selectivity toward NH_2OH depends on both hydrogen partial pressure and temperature. At low H_2 partial pressures, the selectivity to hydroxylamine is low due to hydrogen starvation on the catalyst surface, which limits its formation rate. With increasing temperature, NH_2OH selectivity also declines because of its accelerated decomposition to ammonia. This intricate interplay between surface coverage and activation barriers for hydroxylamine formation and decomposition highlights the inherent difficulty in controlling the selectivity toward hydroxylamine and ammonia in this reaction.

3.3 NO_2^- hydrogenation on $\text{Pd}/\text{Al}_2\text{O}_3$ with NH_2OH co-feeding

To evaluate the effect of NH_2OH on the selectivity and the NO_2^- hydrogenation activity, NH_2OH was co-fed in concentrations ranging from 0.1 – 0.85 mmol L^{-1} under H_2 deficient (0.05 bar) and H_2 rich (0.8 bar) conditions at both RT and 40°C . As expected, higher NO_2^- hydrogenation rates were observed at

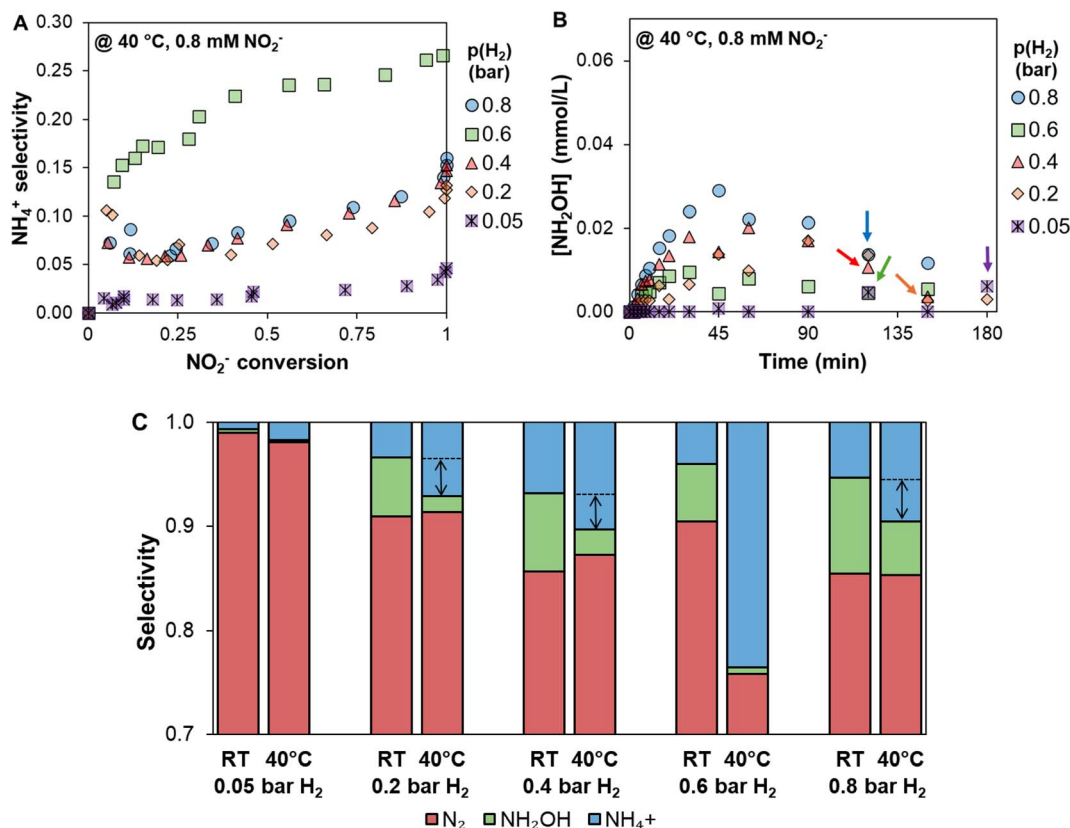


Fig. 4 NH_4^+ selectivity as a function of NO_2^- conversion (A), the NH_2OH concentration profile (B) both at 40°C and selectivity distribution at $\sim 50\%$ NO_2^- conversion at RT and 40°C and at different H_2 partial pressures (C). Arrows indicate full NO_2^- conversion (B) or the difference in NH_4^+ selectivity. Reaction conditions: $300\text{ mL H}_2\text{O}$, $10\text{ mg Pd}/\text{Al}_2\text{O}_3$, 0.8 mmol L^{-1} KNO_2 , 10 mL min^{-1} CO_2 , 5 – 80 mL min^{-1} H_2 and He to balance to 100 mL min^{-1} total flow, RT or 40°C , 600 rpm .



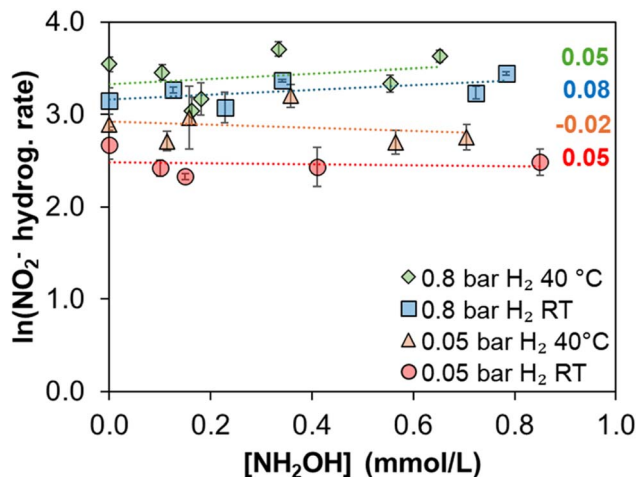


Fig. 5 Effect of NH_2OH on the NO_2^- hydrogenation rate on $\text{Pd}/\text{Al}_2\text{O}_3$ at different H_2 partial pressures and different temperatures. Reaction conditions: $0.8 \text{ mmol L}^{-1} \text{KNO}_2$, $300 \text{ mL H}_2\text{O}$, $10 \text{ mg Pd}/\text{Al}_2\text{O}_3$, $10 \text{ mL min}^{-1} \text{CO}_2$, 5 or $80 \text{ mL min}^{-1} \text{H}_2$ and He to balance to 100 mL min^{-1} total flow, RT or $40 \text{ }^\circ\text{C}$, 600 rpm .

elevated temperature and higher H_2 partial pressure. Surprisingly, the presence of co-fed NH_2OH did not affect the NO_2^- hydrogenation activity regardless of temperature or H_2 partial pressure as illustrated by apparent reaction orders close to zero (Fig. 5).

Reporting the NH_4^+ and NH_2OH selectivity in NH_2OH co-feeding experiments is complex as co-fed NH_2OH represents

an additional N-source resulting in an ill-defined denominator for the selectivity calculation. For instance, the NH_2OH selectivity could formally reach negative values and might therefore be misleading. To avoid this complexity, we report the NH_4^+ and NH_2OH concentrations as a function of time. Figures with the same data as a function of NO_2^- conversion deliver the same trends and are shown in the SI, Fig. 6.

At RT, the NH_2OH concentration remained essentially constant at its initial co-feed level regardless of the H_2 partial pressure (Fig. 6A for 0.8 bar and SI, Fig. 6 for 0.05 bar). Because NH_2OH formation and decomposition occur simultaneously, only the net concentration change can be tracked. Thus, from the concentration profile alone, it cannot be determined whether NH_2OH formation and decomposition are in balance or whether no NH_2OH is formed in the first place. The NH_4^+ concentrations, however, increase with increasing NH_2OH co-feed at RT as illustrated by the first two clustered columns in Fig. 6D. This suggests that NH_2OH is not a passive spectator but NH_2OH formation and decomposition are in balance with the NH_2OH decomposition contributing to increased NH_4^+ formation. Under H_2 -deficient conditions (0.05 bar), the NH_4^+ concentrations were consistently lower, as expected and discussed in Sections 3.1 and 3.2.

At $40 \text{ }^\circ\text{C}$ and low H_2 partial pressure the NH_2OH concentrations decrease over time resulting in slightly higher NH_4^+ concentrations (Fig. 6B and D (third clustered columns), respectively). The decrease in the NH_2OH concentration supports the earlier observations that the NH_2OH decomposition is promoted at elevated temperatures. At $40 \text{ }^\circ\text{C}$ and high H_2

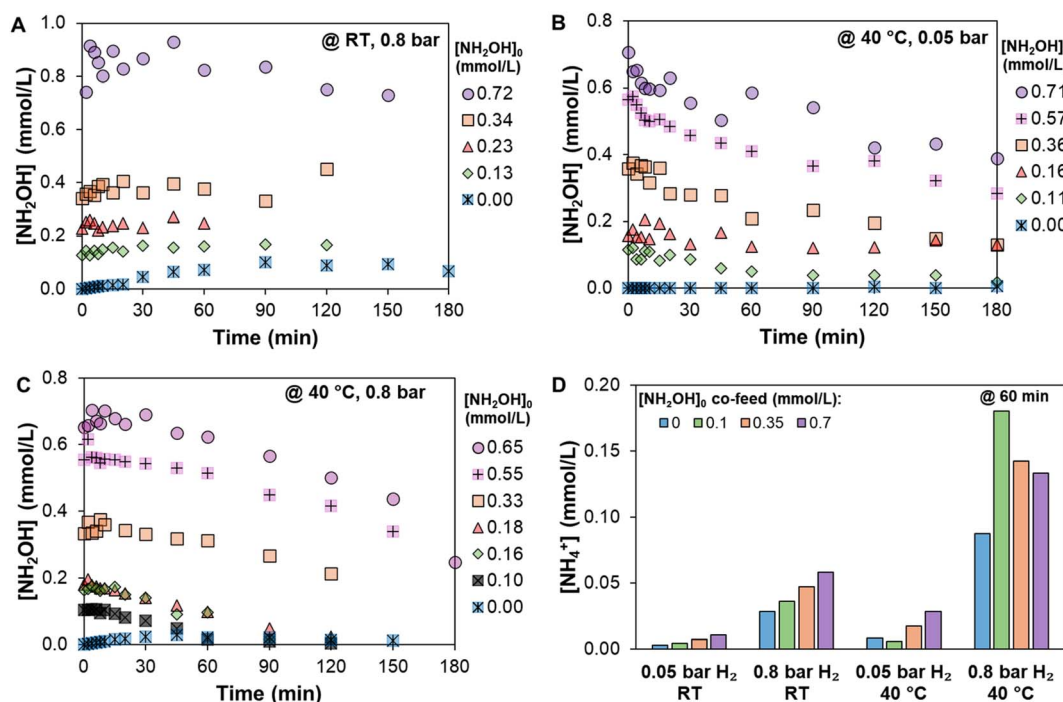


Fig. 6 NH_2OH concentration as a function of time at different NH_2OH co-feed concentrations at RT or $40 \text{ }^\circ\text{C}$ and at 0.8 or 0.05 bar H_2 (as stated in the chart, A–C) and the NH_4^+ concentration at different rounded NH_2OH co-feed concentrations after 60 min of reaction (D). Reaction conditions: $300 \text{ mL H}_2\text{O}$, $0.8 \text{ mmol L}^{-1} \text{KNO}_2$, $10 \text{ mg Pd}/\text{Al}_2\text{O}_3$, 80 or $5 \text{ mL min}^{-1} \text{H}_2$, $10 \text{ mL min}^{-1} \text{CO}_2$ and He to make up to 100 mL min^{-1} , RT or $40 \text{ }^\circ\text{C}$, 600 rpm .



Table 2 Overview of the main trends of the NH_2OH co-feeding experiments with respect to NO_2^- hydrogenation activity, NH_2OH concentration and NH_4^+ formation under different reaction conditions

Effect of NH_2OH co-feeding	RT		40 °C	
	0.05 bar	0.8 bar	0.05 bar	0.8 bar
NO_2^- hydrog. activity	Constant		Activity unchanged	
$[\text{NH}_2\text{OH}]$	Increasing with $[\text{NH}_2\text{OH}]_0$		Decreasing	
NH_4^+ formation	Increasing with $[\text{NH}_2\text{OH}]_0$		Increased at high $[\text{NH}_2\text{OH}]_0$	Increasing non-linearly

partial pressure, substantially higher NH_4^+ concentrations are obtained than under all other conditions which underlines faster NH_2OH decomposition at elevated temperature and the need for sufficient H_2 . Interestingly, the NH_4^+ concentrations show a non-linear behavior with respect to the NH_2OH co-feed levels under these conditions. While all co-feed experiments deliver higher NH_4^+ concentrations than the baseline experiment without any NH_2OH co-feed, the increase in the NH_4^+ concentration was more pronounced at lower co-feed levels (Fig. 6D, last clustered columns). A possible explanation could be that at high NH_2OH concentrations the surface is increasingly covered with NH_2OH species. This may result in lower H-coverage at high NH_2OH co-feed than at low NH_2OH co-feed leading to higher N:H ratios and therefore more N-N coupling and less NH_4^+ formation. More broadly, this underscores the complex interplay of the different surface species and its relevance for the reaction mechanism.

As summarized in Table 2, these findings indicate that the NO_2^- hydrogenation activity is unaffected by NH_2OH co-feeding. Instead, the hydroxylamine co-feeding led to higher NH_4^+ formation rates, indicating that this intermediate regulates the product selectivity. This increased NH_4^+ formation correlates with faster NH_2OH decomposition, which is more pronounced at elevated temperatures.

3.4 Reviewing the NO_2^- hydrogenation reaction mechanism on $\text{Pd}/\text{Al}_2\text{O}_3$

Only very few studies propose a reaction mechanism considering elementary steps of the surface reaction and, to the best of our knowledge, none of them considers the desorption of NH_2OH .^{27,28,33} Thus, earlier published mechanistically relevant findings based on ATR-IR spectroscopy,^{29–31} DFT^{28,33–35} and reaction kinetics^{27,28} are critically discussed and a revised reaction mechanism under consideration of desorbed NH_2OH is provided. Mechanistic studies on NO_2^- over metals other than Pd ³⁶ or NO_3^- hydrogenation^{37–41} were not considered as the initial hydrogenation from NO_3^- to NO_2^- is the RDS of this

reaction and the surface coverages in NO_3^- and NO_2^- are thus not comparable.

3.4.1 Role of NH_2OH . Ebbesen *et al.* conducted ATR-IR studies on the decomposition of NH_2OH on $\text{Pd}/\text{Al}_2\text{O}_3$. They showed that in the absence of H_2 and NO_2^- , NH_2OH decomposes into NH_4^+ and another species that initially was assumed to be NH_2 .³¹ In following studies using isotope labelling, Rao *et al.* showed that this species contains oxygen and was therefore defined as NO_xH_y which represents HNO^* , NOH^* , NHOH^* and/or NH_2OH^* (unpublished work, SI, Fig. 7). The three species were indistinguishable from one another. Subsequent titration of the NO_xH_y^* species with H_2 in the ATR-IR cell showed that NO_xH_y^* is converted into NH_4^+ .³¹ Notably, NO^* was not observed in these experiments suggesting at least one irreversible reaction step from NO^* towards NO_xH_y^* on the Pd catalyst. In our latest work we reported NH_4^+ selectivity <100% in batch experiments converting NH_2OH . This indicates that N_2 or N_2O can be formed from NH_2OH even in the absence of NO_2^- and H_2 *via* catalytic disproportionation.¹⁷ Generally, these results suggest that there is a direct pathway from NH_2OH towards NH_4^+ , while NH_2OH can also merge into the mechanistic pathway that leads to N_2 , but NH_2OH cannot form NO^* .

3.4.2 Langmuir–Hinshelwood or Eley–Rideal mechanism for N_2 formation. Xu *et al.* formulated a NO_2^- hydrogenation mechanism based on extensive kinetic studies.²⁷ All possible Langmuir–Hinshelwood (LH) equations were derived and compared with the apparent reaction orders in a broad concentration regime. Four of these LH type reaction mechanisms match the observed reaction orders. Two of these mechanisms proceed *via* a N^* species (see SI, Fig. 8C and D) and were excluded as earlier work of Zhao *et al.* claimed N^* species to be kinetically irrelevant.²⁹ Zhao observed increasing NH_4^+ concentrations although NO_2^- was entirely converted and suggested N^* as strongly adsorbed surface species that only very slowly converts into NH_4^+ .²⁹ While this seemed a reasonable explanation as N^* species are IR inactive and could therefore not be observed in ATR-IR studies, it cannot be excluded that

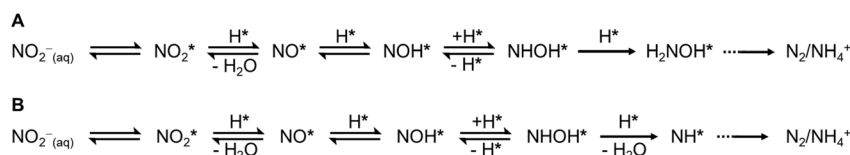


Fig. 7 Suggested NO_2^- hydrogenation mechanisms by Xu *et al.*²⁷



Huang *et al.*²⁸ suggested a co-limitation of the hydrogenation of NO* to HNO* and the consecutive hydrogenation of HNO* to HNOH* as the RDS based on their kinetic model.²⁸ DFT calculations in their work delivered lower activation barriers for HNOH* formation *via* HNO* than *via* NOH*. While NOH* might still form and couple with NH* to form N₂, we focus on HNO* for the subsequent pathway to HNOH*. Huang *et al.*²⁸ suggested that the degree of rate control shifts based on the reaction conditions but is under typical reaction conditions (RT, 0.8 bar H₂ partial pressure) at about 90% for the NO* hydrogenation to HNO*.

While the observed reaction kinetics in this work are similar and therefore confirm the previous model not considering NH₂OH, the model cannot explain the RDS in the presence of NH₂OH sufficiently. If NO* hydrogenation was also the dominant RDS under NH₂OH rich conditions, all following steps were quasi-equilibrated and thus NH₂OH_(aq) was equilibrated with NH* according to the 0th law of thermodynamics. NH* can be coupled with NO* to form N₂ and NO* is easily formed from NO₂⁻ and surface abundant; thus an acceleration of the NO₂⁻ hydrogenation with increasing NH₂OH co-feed (NH₂OH reaction order > 0) would be expected. In other words, the NO* → NOH* RDS could be bypassed owing to the abundance of NH*. However, the observation is 0th order in NH₂OH; thus, there must be another RDS under NH₂OH rich conditions.

The H-assisted dissociation of the N–O bond in HNOH* to NH* can be a RDS based on the expected apparent reaction orders derived from the LH equations by Xu *et al.*²⁷ without considering NH₂OH. A similar derivation under NH₂OH rich conditions was derived (see the SI) and resulted in a reaction order range of [−1, 0] for NO₂⁻ and [−1, 1] for NH₂OH which covers the observed orders. Notably, in ATR-IR titration experiments of the surface abundant NO* and NO_xH_y* species it was observed that NO* is more quickly converted than NO_xH_y*^{29,30} supporting that HNOH* → NH* is a realistic RDS.²⁴ Controversially, if HNOH* → NH* is the RDS under NH₂OH rich conditions, one might expect the reaction to be accelerated with increasing NH₂OH concentration due to increased HNOH* coverage. However, if the surface is saturated with NH₂OH (and its equilibrated species including HNOH*), changes in NH₂OH in the solution would not affect the reaction rate. This surface saturation of NH₂OH species under NH₂OH rich conditions agrees with ATR-IR experiments that showed that NH_xO_y is a surface abundant species when feeding NH₂OH.^{30,31}

Thus, we suggest that the RDS varies even more on the surface coverages than reported by Huang *et al.*²⁸ In the absence of NH₂OH the RDS lies dominantly on the NO* → NOH* hydrogenation while it shifts to HNOH* → NH* under NH₂OH abundant conditions. In between these two extreme cases the degree of rate control shifts non-linearly and therefore accounts for intriguing trends such as decreasing NH₄⁺ formation with increasing NH₂OH co-feed (Fig. 6D) or higher NH₄⁺ formation at 0.6 bar H₂ and elevated temperature (Fig. 4C). NH* remains the last common reaction intermediate in the pathways towards N₂ and NH₄⁺. Thus, the surface coverage of H* and various N* species determines the probability whether NH* proceeds *via* the N₂ or NH₄⁺ pathway. Clearly, higher H-coverage increases

the probability for NH₄⁺ formation, which is consistent with increased NH₄⁺ selectivity at the beginning of a reaction and approaching full NO₂⁻ conversion and lower NH₄⁺ formation under H₂ deficient conditions as discussed in Section 3.1.

In conclusion, the recent discovery of NH₂OH as a desorbed reaction intermediate clearly highlights the need for the incorporation of NH₂OH into the NO₂⁻ hydrogenation mechanism. In our revised mechanistic scheme we (1) account for the adsorption equilibrium of NH₂OH, (2) include the hydrogenation equilibrium of HNOH* and NH₂OH* representing the possibility for NH₂OH to merge into the N₂ formation pathway, and (3) suggest a changing degree of rate control depending on the surface coverages with NO hydrogenation as the dominant RDS in the absence of NH₂OH and the H-assisted N–O dissociation of HNOH* to NH* as the RDS under NH₂OH rich conditions. This mechanism emphasizes that the selectivity is determined by NH* conversion, either reacting with H* to form NH₄⁺ or by coupling with an N-species to form N₂, depending on the surface coverage of H and HNO*/NOH* or NO*. Our proposed mechanism provides a coherent picture of the reaction mechanism consistent with the experimental data and previous results obtained from our group. Nonetheless, the dominant surface mechanism will inevitably depend on catalyst characteristics and operating conditions, and other mechanistic interpretations may also be reasonable.

3.5 NO₂⁻ hydrogenation on SnPd/Al₂O₃ – activity, selectivity and NH₂OH co-feeding

The same set of experiments, varying the NO₂⁻ concentration from 0.3–8 mmol L⁻¹ and the H₂ partial pressure from 0.05–0.8 bar, was conducted on a SnPd/Al₂O₃ catalyst. This catalyst was prepared from the previously tested Pd/Al₂O₃ by Controlled Surface Deposition (CSD), introducing Sn corresponding to 0.4 monolayers relative to the accessible Pd surface atoms. Remarkably, the overall NO₂⁻ hydrogenation activity remained largely unaffected by Sn doping. Since the activity was unchanged, we assume, as for Pd/Al₂O₃, that mass transport limitations are absent (SI, Fig. 1). The derived reaction orders are likewise similar to those observed for Pd/Al₂O₃: the order in NO₂⁻ remains close to zero (Fig. 9A), while the order in H₂ increases from 0.2 (Pd/Al₂O₃) to 0.5 (SnPd/Al₂O₃, Fig. 9B), indicating a higher sensitivity to changes in H₂ partial pressure. This can be rationalized by the partial blockage of Pd sites by Sn, which cannot dissociate H₂, thereby reducing the effective H availability. In NH₂OH co-feeding experiments, the NO₂⁻ hydrogenation activity also remained unchanged, resulting in an apparent reaction order in NH₂OH close to zero at both 0.8 and 0.05 bar H₂ (Fig. 9C).

The selectivity trends on SnPd/Al₂O₃ mirror those on Pd/Al₂O₃: NH₂OH concentrations increase over the course of the reaction, peaking near full NO₂⁻ conversion (Fig. 10B), while NH₄⁺ selectivity exhibits a U-shaped dependence on conversion (Fig. 10A) as discussed in Section 3.1. As for Pd/Al₂O₃, variations in the initial NO₂⁻ concentration have only minor effects on product distribution (SI, Fig. 9), and both NH₄⁺ and NH₂OH



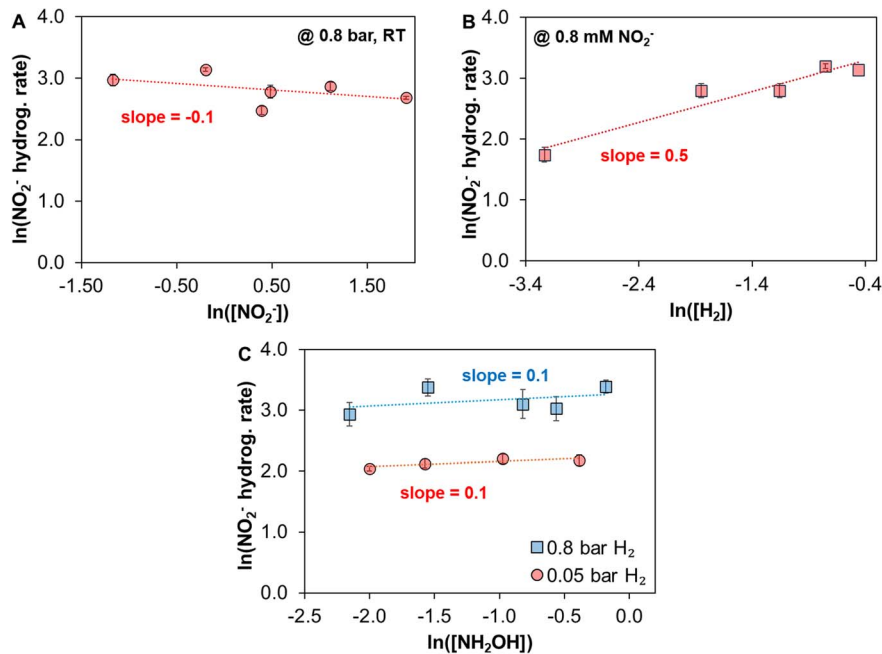


Fig. 9 Effect of NO_2^- (A), H_2 (B) and NH_2OH concentration (C) on the NO_2^- hydrogenation rate on $\text{SnPd}/\text{Al}_2\text{O}_3$. Reaction conditions: 300 mL H_2O , 10 mg $\text{SnPd}/\text{Al}_2\text{O}_3$, $10 \text{ mL min}^{-1} \text{CO}_2$, $5\text{--}80 \text{ mL min}^{-1} \text{H}_2$ and He to balance to 100 mL min^{-1} total flow, RT, 600 rpm.

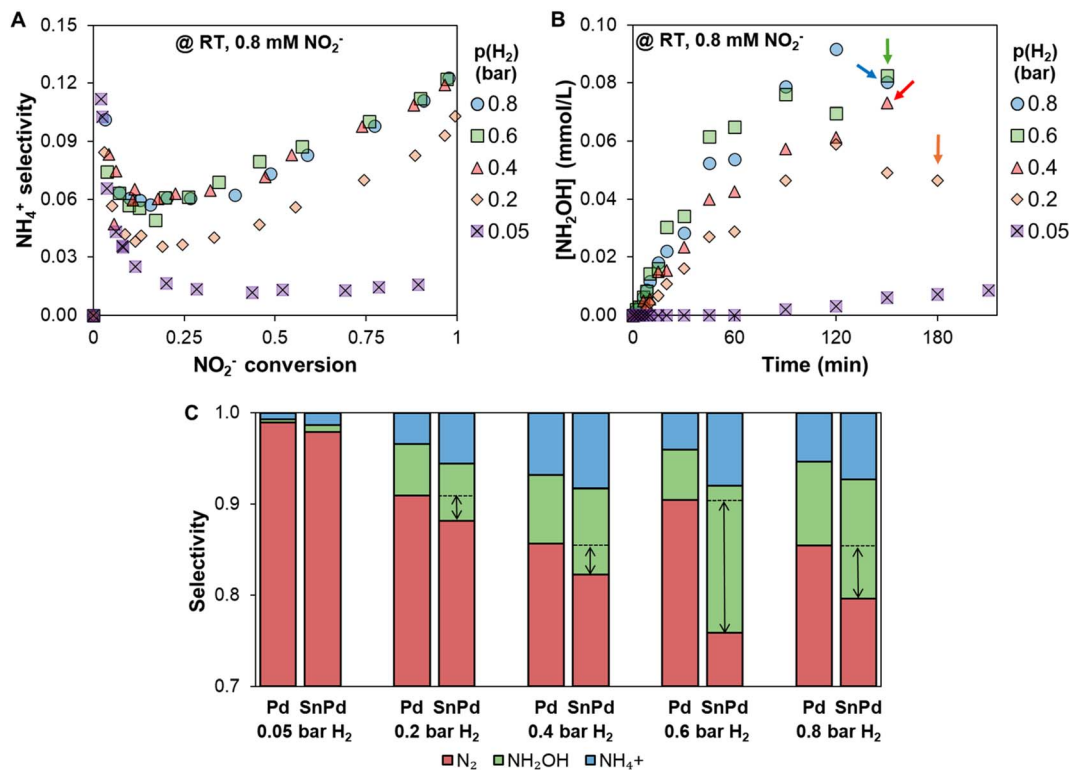


Fig. 10 NH_4^+ (A) and NH_2OH (B) concentrations as a function of NO_2^- conversion and time, respectively, and selectivity distribution at $\sim 50\%$ NO_2^- conversion on Pd and SnPd at different H_2 partial pressures (C). Pd data are the same as in Fig. 4 and replotted for intuitive comparison. The arrows in (C) indicate the difference in N_2 selectivity. Reaction conditions: 300 mL H_2O , 10 mg $\text{SnPd}/\text{Al}_2\text{O}_3$, $10 \text{ mL min}^{-1} \text{CO}_2$, $5\text{--}80 \text{ mL min}^{-1} \text{H}_2$ and He to balance to 100 mL min^{-1} total flow, RT or 40°C , 600 rpm.



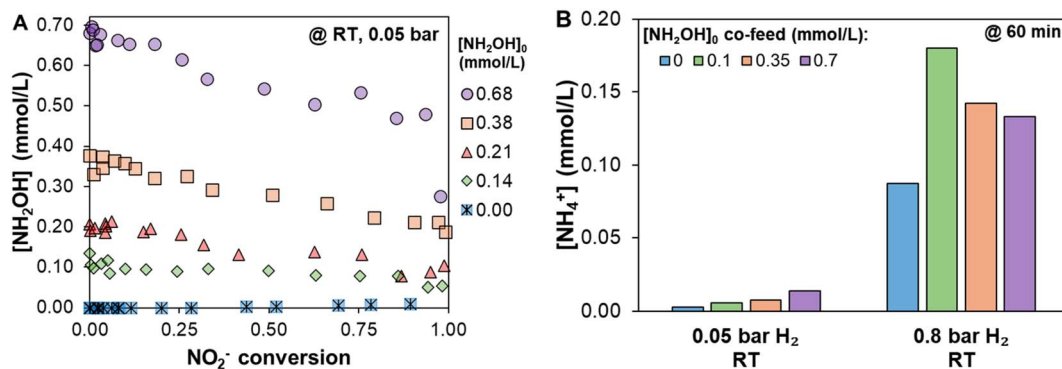


Fig. 11 NH_2OH concentration as a function of NO_2^- conversion at different NH_2OH co-feed concentrations at 0.05 bar H_2 (A) and the NH_4^+ concentration at different rounded NH_2OH co-feed concentrations after 60 min of reaction (B). Reaction conditions: 300 mL H_2O , 0.8 mmol L^{-1} KNO_3 , 10 mg $\text{SnPd}/\text{Al}_2\text{O}_3$, 80 or 5 mL min^{-1} H_2 , 10 mL min^{-1} CO_2 and He to make up to 100 mL min^{-1} , RT, 600 rpm.

concentrations are lower under H_2 -deficient conditions (Fig. 10).

Notably, the NH_2OH and NH_4^+ selectivity are mildly increased on $\text{SnPd}/\text{Al}_2\text{O}_3$ for all H_2 pressures ≥ 0.2 bar resulting in 4–16% lower N_2 selectivity upon Sn doping (Fig. 10C). While this appears contradictory to the notion of reduced H coverage caused by Sn blocking of Pd sites, this suggests that Sn also shifts the balance of surface reactions away from N–N coupling and towards NH_4^+ formation. Formation of N_2 requires N–N bond formation *via* coupling between a reduced N adsorbate (e.g., NH^*) and a more oxidized N adsorbate (e.g., $\text{NO}^*/\text{NOH}^*/\text{HNOH}^*$), which therefore requires co-adsorption of these intermediates in close proximity on Pd ensembles. Introducing Sn partially dilutes Pd, reducing the probability for such coupling configurations and thus slightly suppressing the N_2 pathway.⁴² In contrast, sequential hydrogenation steps toward NH_4^+ rely primarily on H^* availability and are less sensitive to the availability of larger Pd ensembles.⁴² This is consistent with the much higher mobility (lower diffusion barrier) of H^* on Pd compared with N-species,³⁴ which favors hydrogenation when coupling upon Pd dilution. The same argumentation applies to NH_2OH formation, since it does not require N–N coupling but follows from stepwise hydrogenation. However, we cannot rule out that the presence of Sn modifies the electronic structure of neighboring Pd surface atoms, increasing the rate of hydrogenation to NH_4^+ .

The NH_2OH co-feeding experiments at high H_2 partial pressure (0.8 bar) on $\text{SnPd}/\text{Al}_2\text{O}_3$ reproduce the trends observed on $\text{Pd}/\text{Al}_2\text{O}_3$: the NH_2OH concentration remains essentially constant, while more NH_4^+ is formed when NH_2OH is co-fed (SI, Fig. 10 and 11B). Interestingly, the same non-linearity is observed in decreasing NH_4^+ formation with increasing NH_2OH co-feed concentration, as on Pd at elevated temperature. Under H_2 -deficient conditions, NH_2OH depletion is more pronounced on SnPd than on Pd (Fig. 11A and SI, Fig. 6F) and the NH_4^+ concentration increases with increasing NH_2OH co-feed concentration (Fig. 11B). The NH_2OH co-feeding results can be rationalized by the ability to disproportionate into NH_4^+ and N_2 without net consumption of H_2 . Under H_2 -deficient conditions this disproportionation pathway gains relative

importance, because pathways that rely on H_2 uptake are suppressed. On $\text{SnPd}/\text{Al}_2\text{O}_3$ this is more pronounced; thus the presence of Sn facilitates the NH_2OH decomposition. This is in line with the enhanced N–O bond activation ability of Sn also allowing to break the first N–O bond in NO_3^- . As a result, NH_2OH is more readily consumed on $\text{SnPd}/\text{Al}_2\text{O}_3$ than on $\text{Pd}/\text{Al}_2\text{O}_3$, consistent with the stronger decrease in the NH_2OH concentration observed at low H_2 partial pressure.

In conclusion, $\text{SnPd}/\text{Al}_2\text{O}_3$ exhibits NO_2^- hydrogenation activity and selectivity trends very similar to $\text{Pd}/\text{Al}_2\text{O}_3$. The main differences are a higher sensitivity to H_2 in both activity and selectivity, likely due to lower H affinity on SnPd . Also, the NH_2OH and NH_4^+ selectivities are increased resulting in a lower N_2 selectivity on SnPd .

In the bigger picture, these results show the demanding challenges for NO_3^- hydrogenation aiming for high N_2 selectivity. The NO_3^- hydrogenation requires a bimetallic catalyst such as $\text{SnPd}/\text{Al}_2\text{O}_3$ for the initial NO_3^- hydrogenation to NO_2^- which represents the RDS of this reaction. As a result, NO_2^- is commonly detected in traces or not detected in the liquid bulk at all. Thus, the surface coverage of N-species in the NO_3^- hydrogenation on the Pd sites is lower and shifts the coverage towards higher H : N ratios favoring NH_4^+ and NH_2OH formation. This in combination with the higher NH_4^+ production affinity of SnPd itself highlights the fundamental challenges of selective NO_3^- hydrogenation for drinking water purification.

4 Conclusion

In this study, we have demonstrated that NH_2OH is a key intermediate in the catalytic hydrogenation of NO_2^- . The selectivity towards NH_4^+ is strongly conversion-dependent, with both NH_2OH and NH_4^+ formation substantially suppressed only under H_2 -deficient conditions, albeit at the expense of lower overall NO_2^- hydrogenation activity. Elevated temperature accelerates NH_2OH decomposition, thereby lowering the NH_2OH concentration. However, rather than enhancing N_2 formation, this shift promotes NH_4^+ selectivity leaving N_2 selectivity largely unaffected. Co-feeding experiments confirmed that the presence of NH_2OH does not influence the



intrinsic NO₂⁻ hydrogenation rate and that NH₂OH formation and decomposition are balanced. The latter suggests that a continuous process could in principle be designed in a way that NH₂OH would not excessively accumulate due to its intermediary nature. The activity and selectivity patterns for Pd/Al₂O₃ and SnPd/Al₂O₃ were very similar with higher NH₂OH and NH₄⁺ formation on SnPd/Al₂O₃ being the main differences.

We critically reviewed the NO₂⁻ hydrogenation mechanism and provided a revised LH-based scheme including NH₂OH as desorbed species. The revised mechanism highlights that NH₂OH can merge into the N₂ formation pathway and suggests the RDS to be strongly dependent on the surface coverages.

Author contributions

J. Betting: methodology, investigation, writing – original draft; Y. Preedawichitkun: investigation; T. Sooknoi: funding acquisition, writing – review & editing; J. Faria Albanese: funding acquisition, supervision, writing – review & editing; L. Lefferts: supervision, writing – review & editing.

Conflicts of interest

There are no conflicts to declare.

Data availability

The data supporting this article have been included as part of the supplementary information (SI). Supplementary information is available. See DOI: <https://doi.org/10.1039/d6ta00106h>.

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