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Impact of the fluorination degree of ether-based electrolyte solvents on Li-metal battery performance†

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Electrolytes using fluorinated solvents have proven effective in improving the cycling life of Li-metal batteries, by forming a robust solid–electrolyte interphase through decomposition of anion and fluorinated solvent molecules. Herein, we modulated the fluorination degree of ether-based electrolyte solvents to investigate their performance in Li-metal batteries. We tuned the fluorination degree by installing a monofluoro substituent on one ethoxy group of 1,2-diethoxyethane (DEE) and varying the fluorination degree on the other one, providing three fluorinated DEE solvent molecules (*i.e.*, **F1F0**, **F1F1** and **F1F2**) with a relatively low fluorination degree. All three electrolytes showed improved solvation strength and ionic conductivities compared with previous highly fluorinated DEE electrolytes while retaining good oxidative stability. A full cell test using the Li-metal anode and nickel-rich cathode revealed that a higher degree of fluorination is beneficial to the cycling performance, and the cycling stability follows **F1F0** < **F1F1** < **F1F2**. Specifically, **F1F0** exhibited poor cycling stability due to its instability against both the anode and cathode. While **F1F1** and **F1F2** both showed good stability against the Li-metal anode, their relative long-term oxidative stability was responsible for the distinct performance, in which the cycle numbers at 80% capacity retention for **F1F1** and **F1F2** were ~20 and ~80, respectively. Finally, we demonstrated that **F1F2** was able to achieve 90 cycles before reaching 80% capacity retention in practical lithium iron phosphate (LFP) pouch cells. This work shows the importance of modulating the fluorination degree of electrolyte solvents, and this approach is suitable for various cathode materials.

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Introduction

The high number of transferred electrons per atomic mass and low electrochemical potential in the Li⁺/Li redox reaction render Li metal an ideal anode material for high-energy-density batteries.^{1–3} Despite these merits, the Li-electrolyte side reactions, inaccessible lithium (or called dead lithium) generated during the plating/stripping cycles^{4,5} and, thus, the poor coulombic efficiency (CE) and cyclability have significantly

impeded the practical implementation.⁶ A key factor enabling stable Li deposition is the formation of a robust solid–electrolyte interphase (SEI) that allows for efficient Li⁺ transfer and uniform Li deposition.^{7,8} Typically, this SEI layer is composed of species associated with electrochemical and chemical decomposition of salt and solvent molecules, and a SEI layer that is rich in inorganic components (*e.g.*, LiF, Li₂O and Li₃N) has been found beneficial.⁹

A variety of molecular engineering strategies for electrolytes have been explored in order to achieve robust SEI layers in Li-metal batteries,^{10,11} including additive-reinforced electrolytes (AREs),¹² high concentration electrolytes (HCEs),¹³ localized high concentration electrolytes (LHCEs),¹⁴ weakly solvating electrolytes (WSEs),^{15–22} electrolytes with fluorinated solvents,^{23–29} *etc.* In these approaches, the formation of a robust SEI layer is promoted through decomposition of either additive, anion or fluorinated molecules. In particular, the fluorinated solvents were found to simultaneously provide several merits in electrolytes, including (1) improved oxidative stability resulting from the high electron-withdrawing capability of fluorine that lowers the highest occupied molecular orbital (HOMO),^{30,31} (2)

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promotion of the anion-derived SEI layer due to the weakened solvation ability associated with the reduced electron density of binding atoms,³² (3) improved flame retardance,³³ and (4) enriched LiF component in the SEI layer through potential decomposition of solvent molecules.^{34,35} Notably, the strategy of solvent fluorination allows for a single-solvent low-concentration electrolyte system without compromising ionic conductivity.^{36–38}

Examples of using fluorinated molecules as a single electrolyte solvent include a series of long-chain fluorinated glymes,^{39,40} fluorinated 1,4-dimethoxybutane (FDMB),⁴¹ *N,N*-dimethylsulfamoyl fluoride (FSA),³⁴ *N,N*-dimethyltrifluoromethane-sulfonamide (DMTMSA),³¹ fluorinated-1,2-diethoxyethane (FDEE)³² and, more recently, 1,1,1-trifluoro-2,3-dimethoxypropane (TFDMP)⁴² and bis(2-fluoroethyl) ethers (BFE).⁴³ In addition to improved oxidative stability, all these electrolytes showed excellent CE and cyclability using nickel-rich high-voltage cathodes. We recently showed that an exciting family of electrolytes based on FDEE (Fig. 1 top row) can achieve Li-cycling CE as high as 99.9% and ~200 cycles of full battery cycling at high-loading capacity (4.8 mA h cm⁻²) under harsh cycling conditions (0.2C charge, 0.3C discharge).³² This series of electrolytes has a fluorine content of 3–6 fluorine atoms per molecule and shows moderate ionic conductivities, and a higher ionic conductivity is necessary for fast charging/discharging. Therefore, we sought to fine-tune the degree of fluorination of DEE in the lower fluorine regime (Fig. 1 bottom row) to optimize the ionic conductivity with the hope of not compromising their oxidative stability.

It is known that increased fluorination degree in ether molecules improves oxidative stability but simultaneously reduces the solvation/binding strength, resulting in the formation of larger size of salt-anion clusters and so reduced ionic conductivity.³² We therefore further reduced the fluorination degree of ether molecules, by applying the monofluoro-substitution on one ethoxy group of 1,2-diethoxyethane (DEE) and varying the number of fluorine substituents on the other one (Fig. 1 bottom row).

Results and discussion

Synthesis and characterization of electrolytes

The fluorinated ether molecules (*i.e.*, **F1F0**, **F1F1**, and **F1F2**) are synthesized through S_N2 reactions and can be obtained on >10 g

scale (see the ESI†). Three single-solvent electrolytes were prepared by adding 1.2 mmol of lithium bis-(fluoromethanesulfonyl)imide (LiFSI) into 1 mL of each of the solvent molecules. We then performed ⁷Li NMR to analyze the solvation condition of salt in the electrolyte using LiCl in D₂O as an internal reference. As can be seen in Fig. 2a, the chemical shift of ⁷Li gradually moved upfield upon increasing the degree of fluorination. This increased electron shielding is attributed to more compact cation-anion interaction resulting from weakened solvation ability, as has been observed in other fluorinated solvents, HCEs, LHCEs and WSEs.^{16,32,43} Herein, consistent with our expectation, increasing the fluorination degree of ether solvent reduces its solvation ability; however, the impact on chemical shifts is not as pronounced as those of highly fluorinated FDEE electrolytes (Fig. 1, top),³² indicating improved salt solvation (or cation-anion dissociation) in our new electrolytes. Additional evidence from Raman measurement (Fig. 2b) showed that **F1F0** and **F1F1** electrolytes exhibit mainly solvent-separated ion pairs (SSIPs, 720 cm⁻¹), while trivial contact ion pairs (CIPs, 732 cm⁻¹) and aggregates (AGGs, 746 cm⁻¹).⁴⁴ In the case of **F1F2**, the broad shoulder peak indicated significant portions of CIPs and AGGs, suggesting the weakened solvation strength.

To evaluate the ionic conductivity, we infiltrated the electrolyte solution into a Celgard 2325 separator and used stainless-steel-sandwich configuration to mimic the conditions of coin-cell tests. As shown in Fig. 2c, all three electrolytes exhibited relatively higher ionic conductivities compared with previous FDEE counterparts (0.05–0.17 mS cm⁻¹),³² and they follow the trend **F1F0** > **F1F1** > **F1F2**, in alignment with the solvation strength. Interestingly, **F1F0** showed ionic conductivity that is even higher than that of the nonfluorinated DEE electrolyte. We reasoned that the F substituent increases the polarity of the molecule and provides an additional binding site to the Li⁺, giving rise to a less compact cation-anion cluster, as indicated by ¹⁹F NMR spectra (Fig. S1†) and some previous studies.^{43,45} Macroscopically, the molecular solvation is reflected in the electrolyte viscosities, where the viscosity trend follows: **F1F0** < **F1F1** < **F1F2** (Table S2†), and a relatively high viscosity leads to a lower diffusivity and so lower ionic conductivity.

Computation of solvation structures

We further performed molecular dynamics (MD) simulation to gain insight into the solvation behavior. Fig. 3a–c show the probability of coordinating O atoms as a function of distance from the Li⁺ center, or radial distribution function (RDF). We compared the O atom from both solvent and anion molecules. The first solvation shell peaked at *r*_(Li–O) ~0.22 nm, which indicates the length of the Li–O dative bond,⁴⁶ for both solvent and anion molecules in all three electrolyte systems.

Notably, the composition of solvating O atoms from solvent and anion molecules varied with the fluorination degree of the electrolyte solvents. The fraction of solvating O atoms from the FSI anion increases in the order **F1F0** < **F1F1** < **F1F2**, and that from solvent molecules decreases accordingly. This trend is consistent with the order of the solvation strength.

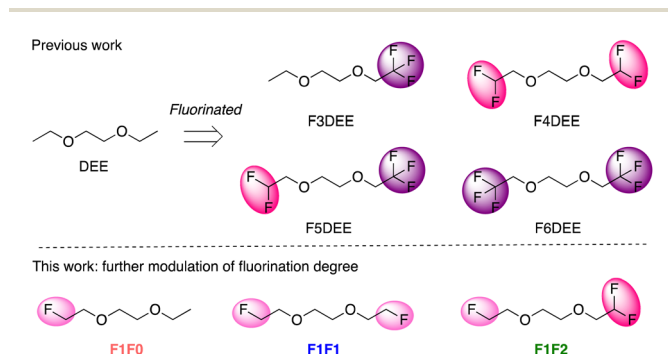


Fig. 1 Chemical structures of fluorinated 1,2-diethoxyethane solvent molecules.

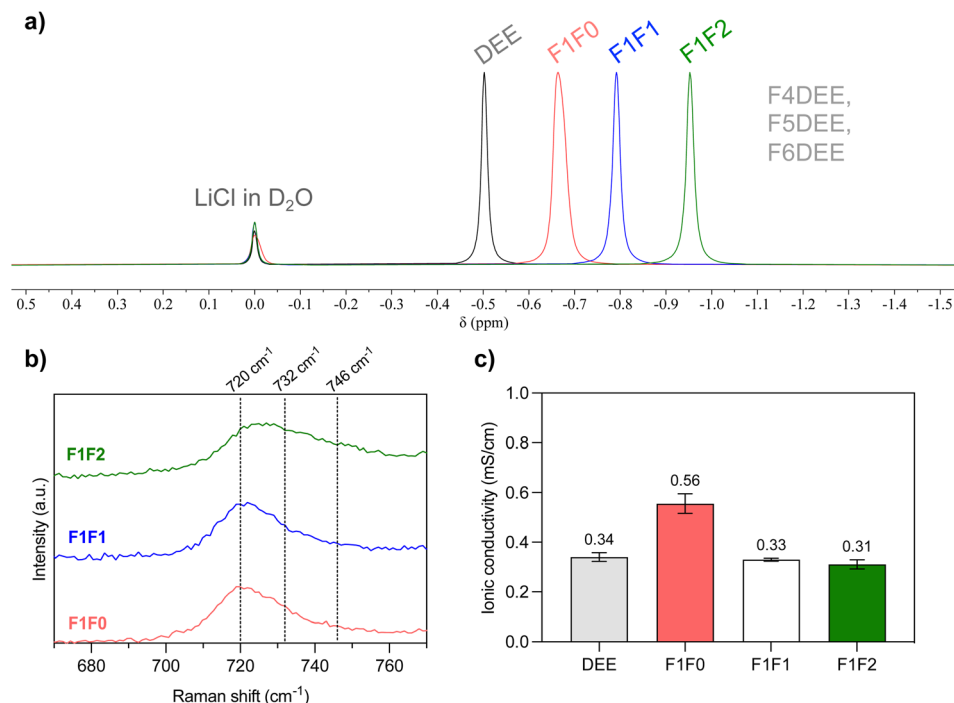


Fig. 2 (a) Overlay of normalized ^7Li NMR spectra of electrolyte solutions containing 1.2 mole L^{-1} of LiFSI salt, and LiCl in D_2O was applied as an internal standard. The pale blue region indicates the chemical shift of F4DEE, F5DEE and F6DEE electrolytes in the previous report. (b) Raman spectra of electrolytes in this study showing the solvation conditions of LiFSI salt. (c) Comparison of ionic conductivity in the stainless steel-separator-stainless steel sandwich structure using the Celgard 2325 trilayer separator. Each electrolyte was measured three times (see Table S3†).

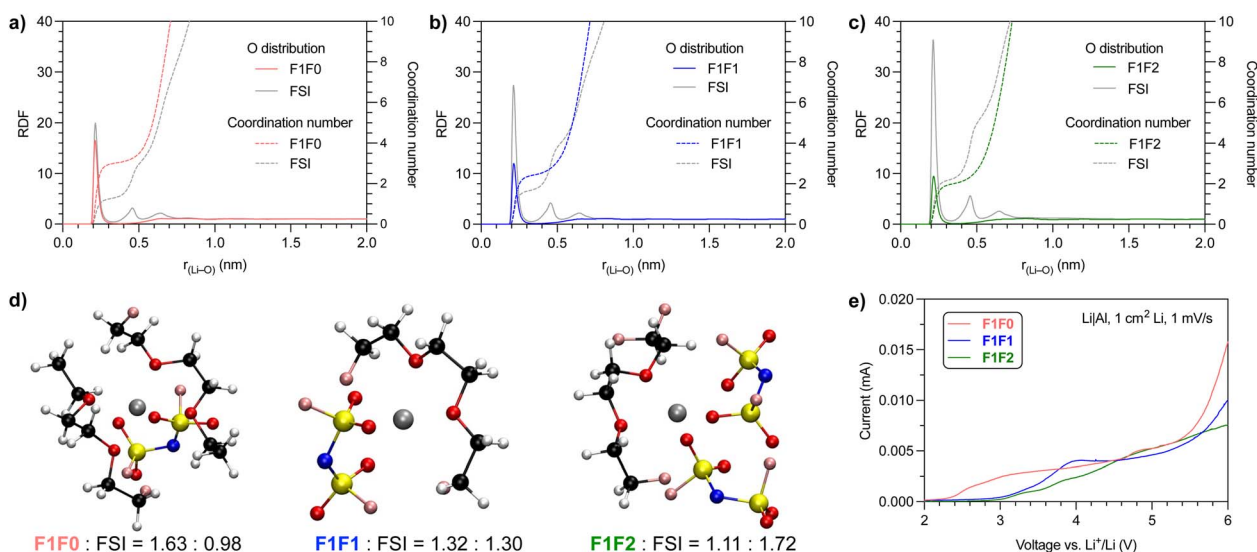


Fig. 3 Radial distribution function of O atoms of (a) F1F0, (b) F1F1 and (c) F1F2 solvent and anion molecules over the distance from the Li^+ cation center. (d) Representative solvation structure of electrolytes with 1.2 mol L^{-1} LiFSI salt, and the average numbers of solvent and anion molecules in the solvation structure are indicated at the bottom. (e) Oxidative stability of electrolytes against the Al current collector (scanning rate: 1 mV s^{-1}).

Consequently, the overall cation-anion interaction is stronger in less solvated electrolyte systems, as also evidenced by ^7Li NMR and Raman spectra analysis (Fig. 2a and b).

To present a quantitative picture of the solvation shell, we integrated the RDF to get the coordination number (CN) of O atoms from the solvent and FSI anion. The presence of a plateau

at $r_{(\text{Li}-\text{O})} \sim 0.36$ nm for both the solvent and FSI anion suggested the radius of the first solvation sheath, and the corresponding CN in the sheath was estimated. For F1F0 electrolyte, the CNs of O from the solvent and FSI anion are 3.03 and 1.34, respectively. The numbers became 2.46 and 1.76 for F1F1 electrolyte and 2.03 and 2.31 for F1F2 electrolyte. We further counted the number of

solvent and FSI anion molecules in the first solvation shell and found, on average, 1.63 solvent and 0.98 FSI in **F1F0** electrolyte, 1.32 solvent and 1.30 FSI in **F1F1** electrolyte, and 1.11 solvent and 1.72 FSI in **F1F2** electrolyte. It is worth noting that for electrolytes with 1.2 mmol of LiFSI in 1 mL solvent, the solvent/LiFSI molar ratios are 6.01, 6.03 and 5.78 for **F1F0**, **F1F1** and **F1F2**, respectively. Hence, there are both “binding” and “free” solvent molecules in the electrolytes. The above quantitative analysis is further highlighted by the typical solvation structures shown in Fig. 3d. Again, this observation is in alignment with the relative solvation strength of solvent molecules.

Previous work has found strong correlation between the solvation structure and the oxidative stability of electrolytes.^{13–29} We then scrutinized the impact of the fluorination degree of solvent on the oxidative stability and, hence, the feasibility to be used in high-voltage battery systems. Fig. 3e shows the screening of leakage current through linear sweep voltammetry of Li||Al half cells at a scanning rate of 1 mV s^{−1}. Interestingly, all three electrolytes exhibit a relatively small current (<5 μ A) at up to 5 V, and these observed low leakage currents are comparable to previous FDEE electrolytes.³²

Li-metal full battery performance

Encouraged by the improved ionic conductivity and retained anodic stability while reducing the fluorination degree, we performed Li||NMC811 full battery tests of the three electrolytes using the same conditions as reported for FDEE electrolytes, *i.e.*, pairing 50 μ m-thick Li foil (10.3 mA h cm^{−2}) with a high-

loading NMC811 cathode (4.8 mA h cm^{−2}) to yield a negative-to-positive electrode ratio (N/P) of $\sim$ 2.1; using an electrolyte-to-cathode ratio (E/C) of $\sim$ 8 g A^{−1} h^{−1}; and cycling at C/5 charging and C/3 discharging rates, for the purpose of comparison with previous studies and so evaluation of fluorination effects.

A representative set of battery cycling results is provided in Fig. 4a (repeated results are provided in Fig. S4–S7[†]), and a clear trend of cycling life was observed: **F1F0** < **F1F1** < **F1F2**. The capacity of **F1F0** decayed quickly to near zero within 30 cycles, and its CE dropped significantly despite the presence of an excess Li reservoir, indicating the instability of **F1F0** against both the anode and cathode. Additionally, the decay pattern is in contrast to the DEE electrolyte (non-fluorinated electrolyte), which presents a steady capacity without significant reduction in the beginning 18 cycles and then drops quickly to 80% capacity in the following 37 cycles.¹⁶ Herein, the continuous capacity decay in **F1F0** suggested the negative impact of mono-fluorination on DEE. As for **F1F1**, the capacity remained almost unchanged in the first 20 cycles but then quickly reduced over cycles. In stark contrast, **F1F2** exhibited stable cycling without substantial capacity decay for $\sim$ 80 cycles, which is comparable to F3DEE and F6DEE but less than F4DEE and F5DEE in a previous report.³²

We further studied the charge/discharge curves at different cycles. Fig. 4b shows the charge/discharge curves of **F1F0** at the 1st, 10th and 20th cycles, where the overpotential at the start of charge/discharge remains nearly unchanged

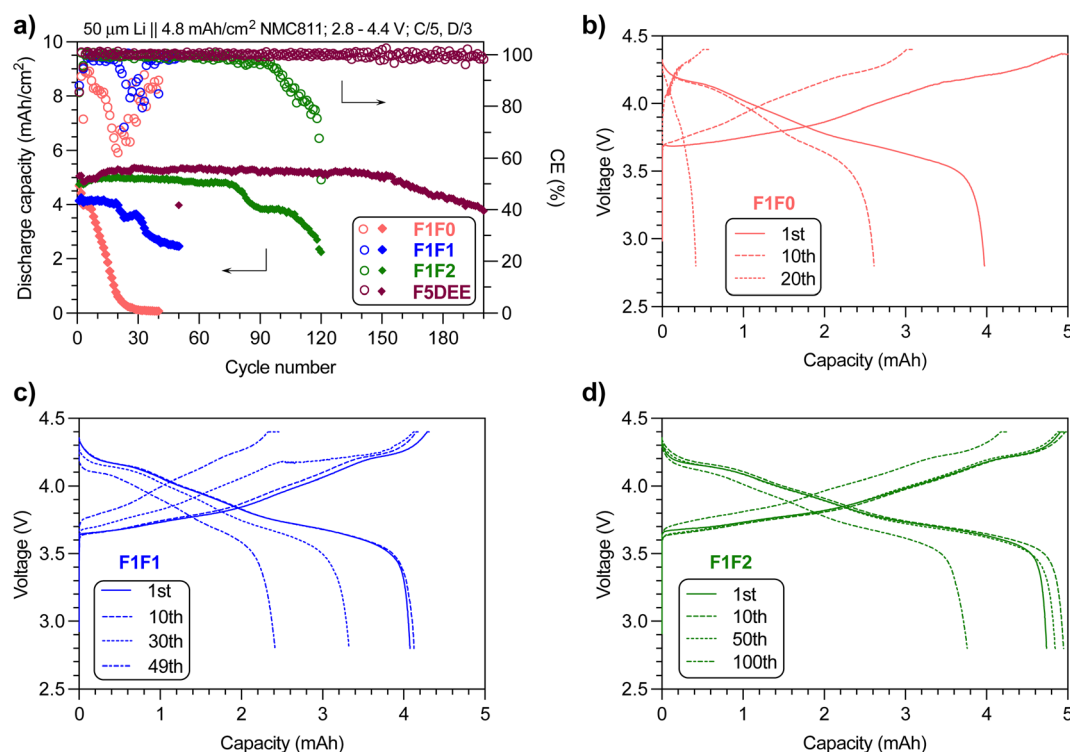


Fig. 4 (a) Capacity and CE retention of **F1F0**, **F1F1** and **F1F2** electrolytes over cycling numbers. The data of F5DEE were adapted from previous results.³² The charge/discharge curves of (b) **F1F0**, (c) **F1F1** and (d) **F1F2** at various cycles. Note: cycling of full cells was repeated and the results can be found in Fig. S4–S7.[†]

while the capacity fades quickly over cycles, indicating the retained bulk and interfacial resistance yet instability against electrodes. Specifically, the 10th discharge process only gave ~ 2.6 mA h, which corresponds to $\sim 84\%$ of the 10th charging capacity (~ 3.1 mA h). Because the high initial Li reservoir ($N/P \sim 2.1$) would guarantee the 3.1 mA h capacity when discharged at the 10th cycle, the observed capacity loss highly suggested the cathode degradation during the 10th discharge cycle. Indeed, the XRD analysis of the cathode after 10 cycles using **F1F0** electrolyte indicated significant layer disruption (Fig. S8†). This instability can be ascribed to the intrinsic low oxidative stability of **F1F0** (as will be discussed later), and the resulting side reactions deteriorate the cathode integrity. In contrast, **F1F1** showed slightly less capacity loss over cycles, but a substantial polarization (decrease in the initial discharge voltage or increase in charge voltage) implies the increased bulk and interfacial resistance. In the case of **F1F2**, the capacity loss is even less and the polarization over cycles is not as pronounced. Therefore, compared with **F1F0**, the improved oxidative stability of **F1F1** benefited the cathode performance but induced polarization, and **F1F2** overcame both drawbacks. We postulated that the combined compact Li^+ -anion pairs associated with weak solvation and improved oxidative stability resulting from the increased fluorination degree contributed to the overall improved cycling performance. Although the ionic conductivity values of **F1F1** and **F1F2** are similar, the polarization evolved distinctly and could be attributed to several factors, including the quality of the generated interphase layer at both the anode (SEI) and cathode (CEI) and their dissolution conditions, changes in electrolyte contents due to the interphase dissolution and the generated byproducts associated with electrochemical/chemical decomposition of solvent and/or salt.

Analysis of Li-metal half-cell cycling

We then examined the stability of Li metal cycling through $\text{Li}||\text{Cu}$ half cells. Typical evaluation of CE using the modified Aurbach method⁴⁷ indicated that the CEs for **F1F0**, **F1F1**, and **F1F2** are 75.8%, 96.3% and 98.7%, respectively (Fig. 5a). A close scrutinization of the overpotential curves reveals a “yielding” peak in the stripping cycle for all three electrolytes (Fig. 5b), which is ascribed to the transformation of interface kinetics.⁴⁸ Meanwhile, we noticed a significant capacity loss in the beginning cleaning cycle of **F1F0**, along with slowly increased stripping overpotential in the later cycles, indicating the cathodic instability of **F1F0** and impedance increase. Notably, the overpotential curve of the stripping cycle presents spike features, which could be related to the reconnection of “dead” Li upon stripping.⁴⁹ We therefore reasoned that **F1F0** presents poor electrochemical stability and unstable/nonuniform Li deposition. By contrast, **F1F1** and **F1F2** showed relatively high CE of 96.3% and 98.7%, respectively, and the average overpotentials of **F1F1** and **F1F2** under 0.5 mA cm^{-2} current are respectively 11 mV and 13 mV, both of which are lower than that of F5DEE (~ 20 mV)³² owing to their higher ionic conductivity.

Long-term cycling of $\text{Li}||\text{Cu}$ half cells was applied to further validate the Li cycling stability (Fig. 5c–e). Interestingly, **F1F0** showed an extremely low CE of $\sim 50\%$ in the first cycle, and it then increased and reached a plateau value of $\sim 88\%$ in the following 20 cycles. However, this value slowly decreased to $\sim 50\%$ after 100 cycles. It was found that the average CE of the initial 12 cycles is $\sim 75\%$, which is consistent with the CE value obtained from the modified Aurbach measurement that includes 12 cycles of Li plating/stripping. Herein, **F1F0** shows poor stability against Li cycling and thus cycling of a full battery. On the other hand, both **F1F1** and **F1F2** showed stable Li cycling over 200 cycles and average CE of 98.5% and 98.8%, respectively. It is worth noting that the CE of both **F1F1** and **F1F2**

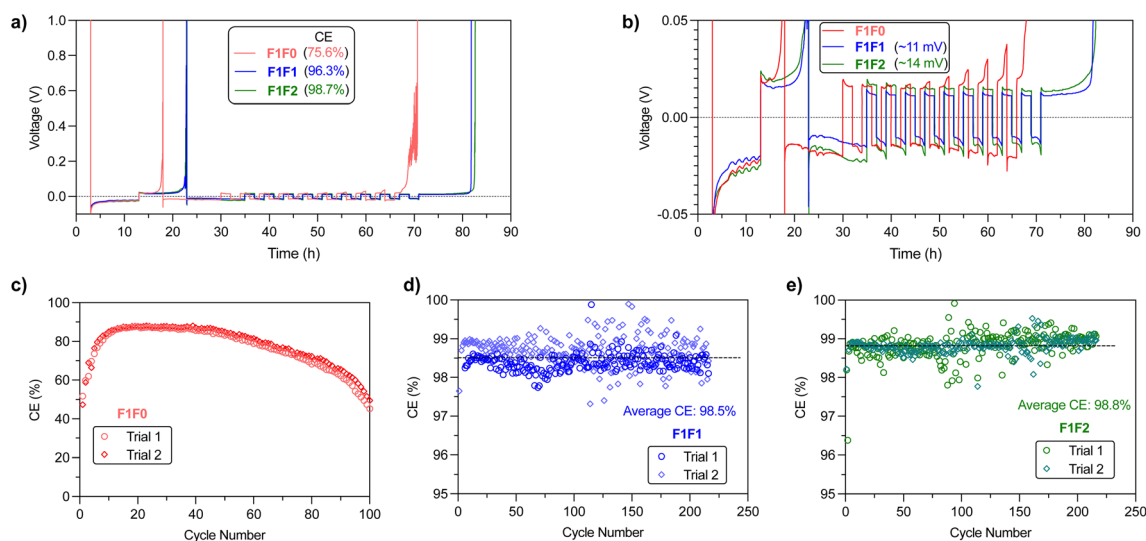


Fig. 5 (a) CE evaluation of $\text{Li}||\text{Cu}$ half cells using the modified Aurbach method. (b) Zoom-in view of voltage–time profiles in CE measurements. CE values of (c) **F1F0**, (d) **F1F1** and (e) **F1F2** electrolytes over long-term cycling of $\text{Li}||\text{Cu}$ half cells. The average CEs of **F1F1** and **F1F2** from two trials over >200 cycles are indicated in (d) and (e), respectively.

quickly reached stable values during the initial 3 cycles, which suggests a quick passivation and formation of robust SEI layers (Fig. S9†).

Despite the similar Li||Cu cycling performance of **F1F1** and **F1F2**, they showed different full battery performance. To understand the underlying mechanism, we compared the Li deposition morphology of **F1F1** and **F1F2**. However, no substantial difference in the grain size and morphology was found (Fig. S10†). Further, the SEI composition after one cycle was analyzed by X-ray photoelectron spectroscopy (XPS), which showed signals from LiOH, Li₂O, LiF, Li₂SO_x, Li₂S and organic species for both electrolytes (Fig. S11–S13†). While the species are similar, a closer comparison of the relative abundance of each element revealed that the O and F contents in **F1F1** are relatively higher than those of **F1F2** after the first cycle (27.1% vs. 10.8% and 17.8% vs. 4.5%, Fig. 6). The difference could be due to the higher electrochemical susceptibility of the mono-fluoride substituent than the difluoro one. It is worth noting that the observed SEI content by XPS is an evaluation of results from multiple factors: (1) the electrolyte solvation dictates the generated SEI composition; (2) the dissolution of the SEI in the corresponding electrolyte. Direct comparison of SEI contents between different electrolytes seems less meaningful in elucidating their relative performance, as the observed contents are the “stable” residue in the specific electrolyte.

We next scrutinized the SEI composition for each electrolyte at the 10th cycle. It was found that the O and F contents in **F1F1** slightly increased to 32.9% and 20.5%, respectively. Therefore, the potentially stable inorganic species of **F1F1** remained at a high level over cycles. Interestingly, the increase was more significant in **F1F2**, which showed 23.8% for O and 16.9% for F at the 10th cycle. The increase of O and F contents in **F1F2** over cycling indicated more accumulation of stable components (possibly Li₂O and LiF) in the SEI, which we hypothesized could be a consequence of less SEI dissolution over cycling,⁵⁰ and the dissolved SEI components could potentially migrate to the cathode side and affect the cathode performance.⁵¹

Long-term oxidative stability

The SEI composition and Li||Cu half-cell cycling performance of **F1F1** and **F1F2** are rather similar, and albeit thin, the Li metal foil in the full cell still provides excess Li reservoir. Therefore, with an average CE of >98% for Li plating/

stripping, the full cell performance is more limited by the cathode side. Because full cell cycling is a long-term process, the oxidation of electrolytes occurs in an accumulating manner and the side reactions could diminish the cathode integrity over time. We therefore performed chronoamperometry to understand the long-term oxidative stability of electrolytes under high voltage. Fig. 7 shows the leakage current of electrolytes under 4.4 V constant voltage over time using Li||Pt half cells. Significant leakage current was observed in **F1F0** and **F1F1** over long-term high voltage holding, and the situation devastated over time. By contrast, there was minimal leakage current in **F1F2**, and it remained steady over more than 18 h. Herein, compared with **F1F1**, the superior oxidative stability of **F1F2** is responsible for its much more stable cycling of full batteries.

Performance of anode-less pouch cells

To evaluate the application of these new electrolytes in practical cells, we performed the cycling test of a commercial multilayer anode-less LFP pouch cell with a relative high area loading of 2.1 mA h cm⁻². As shown in Fig. 8, ~80% capacity retention using **F1F1** electrolyte was achieved at ~55 cycles. With improved oxidative stability, **F1F2** was able to realize ~90 cycles. For comparison, the state-of-the-art electrolyte F5DEE achieved a high cycle number of ~110. Therefore, although it cannot outperform the F5DEE electrolyte, the **F1F2** electrolyte is suitable for research in practice cells.

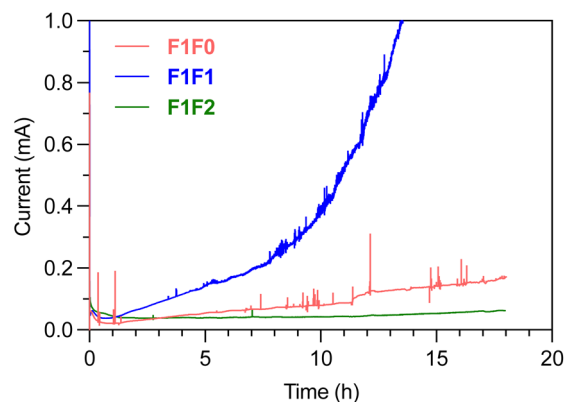


Fig. 7 The leakage current of electrolytes under 4.4 V constant voltage holding.

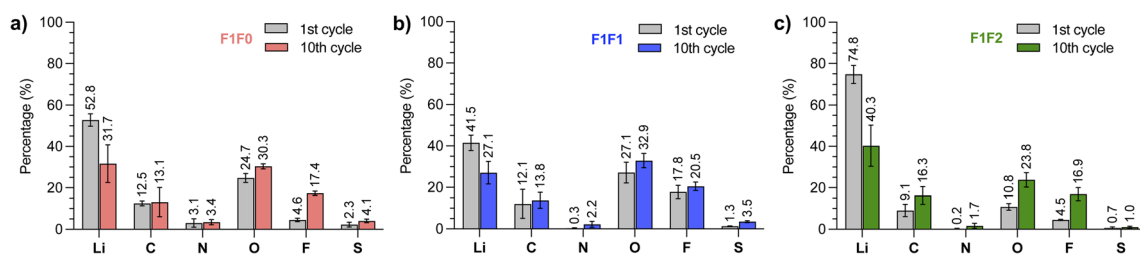


Fig. 6 XPS analysis of SEI composition of (a) **F1F0**, (b) **F1F1**, and (c) **F1F2** electrolytes at the 1st and 10th cycles of lithium deposition using Li||Cu half cells. The results were obtained by averaging the signals from 4 different sputtering times.

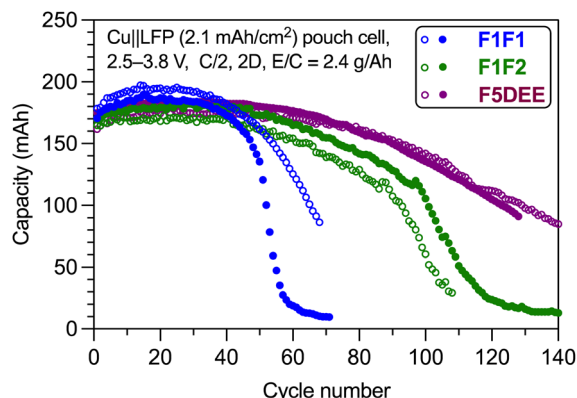


Fig. 8 Long-term cycling of anode-less Cu||LFP pouch cells using F1F1, F1F2 and F5DEE electrolytes. The cycling was performed at 0.5C charging rate and 2C discharging rate.

Conclusions

To conclude, the modulation of the fluorination degree in ether-based electrolyte solvents allows for fine-tuning of solvation strength and long-term oxidative stability. A general trend that a low degree of fluorination presents relatively strong solvation but poor oxidative stability and increasing fluorination degree improves the oxidative stability at the expense of solvation strength has been observed. Among these ether solvents with relatively low fluorination degrees, F1F0 exhibited particularly poor stability against both the Li-metal anode and NMC cathode. While F1F1 and F1F2 showed comparable cathodic stability, F1F2 possessed better anodic stability and, therefore, enhanced battery cyclability. While the performance of this series of electrolytes does not outperform our previous FDEE electrolytes, the improved ionic conductivity might be beneficial to high-current density ($>1 \text{ mA h cm}^{-2}$, Fig. S9†) charging of battery systems that possess relatively low overpotential.

The observed trade-off between ionic conductivity (or related solvation capability) and oxidative stability makes it challenging to design an ideal single solvent through solely tuning the fluorination degree. Strategies that can further enhance the electrolyte performance include increasing salt concentration, where there would be a point that provides optimal conductivity and improved oxidative stability, and adding diluent, as has been demonstrated recently by Ren and coworkers for the F1F1 solvent molecule.⁴⁵

Author contributions

Yangju Lin and Zhiao Yu contributed equally to this work. Yangju Lin: conceptualization, methodology, investigation, data curation, visualization, writing – original draft; Zhiao Yu: conceptualization, investigation, methodology, data curation; Weilai Yu: investigation, data curation, visualization; Sheng-Lun Liao: methodology, formal analysis; Elizabeth Zhang, Xuelin Guo, Zhuojun Huang, and Yuelang Chen: data curation; Jian Qin: supervision, discussion, writing – review and editing; Yi Cui: supervision, discussion, writing – review and editing;

Zhenan Bao: supervision, project administration, discussion, writing – review and editing. The manuscript was reviewed and edited by all the above authors. All authors have given approval to the final version of the manuscript.

Conflicts of interest

Zhenan Bao, Yi Cui, Yangju Lin, Zhiao Yu and Yuelang Chen declare that this work is part of US Provisional Patent Application filed in 2021. The remaining authors declare no competing interests.

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References

- 1 Y. Guo, H. Li and T. Zhai, *Adv. Mater.*, 2017, **29**, 1700007.
- 2 D. Lin, Y. Liu and Y. Cui, *Nat. Nanotechnol.*, 2017, **12**, 194–206.
- 3 W. Xu, J. Wang, F. Ding, X. Chen, E. Nasybulin, Y. Zhang and J.-G. Zhang, *Energy Environ. Sci.*, 2014, **7**, 513–537.
- 4 C. Fang, J. Li, M. Zhang, Y. Zhang, F. Yang, J. Z. Lee, M. H. Lee, J. Alvarado, M. A. Schroeder, Y. Yang, B. Lu, N. Williams, M. Ceja, L. Yang, M. Cai, J. Gu, K. Xu, X. Wang and Y. S. Meng, *Nature*, 2019, **572**, 511–515.
- 5 P. P. Paul, E. J. McShane, A. M. Colclasure, N. Balsara, D. E. Brown, C. Cao, B.-R. Chen, P. R. Chinnam, Y. Cui, E. J. Dufek, D. P. Finegan, S. Gillard, W. Huang, Z. M. Konz, R. Kostecki, F. Liu, S. Lubner, R. Prasher, M. B. Preefer, J. Qian, M.-T. F. Rodrigues, M. Schnabel, S.-B. Son, V. Srinivasan, H.-G. Steinrück, T. R. Tanim, M. F. Toney, W. Tong, F. Usseglio-Viretta, J. Wan, M. Yusuf, B. D. McCloskey and J. Nelson Weker, *Adv. Energy Mater.*, 2021, **11**, 2100372.
- 6 X. B. Cheng, R. Zhang, C. Z. Zhao and Q. Zhang, *Chem. Rev.*, 2017, **117**, 10403–10473.
- 7 M. D. Tikekar, S. Choudhury, Z. Tu and L. A. Archer, *Nat. Energy*, 2016, **1**, 16114.
- 8 E. Peled and S. Menkin, *J. Electrochem. Soc.*, 2017, **164**, A1703.
- 9 X. B. Cheng, R. Zhang, C. Z. Zhao, F. Wei, J. G. Zhang and Q. Zhang, *Adv. Sci.*, 2016, **3**, 1500213.
- 10 S. Li, M. Jiang, Y. Xie, H. Xu, J. Jia and J. Li, *Adv. Mater.*, 2018, **30**, e1706375.
- 11 Y. Jie, X. Ren, R. Cao, W. Cai and S. Jiao, *Adv. Funct. Mater.*, 2020, **30**, 1910777.
- 12 H. Zhang, G. G. Eshetu, X. Judez, C. Li, L. M. Rodriguez-Martínez and M. Armand, *Angew. Chem., Int. Ed.*, 2018, **57**, 15002–15027.
- 13 Y. Yamada, J. Wang, S. Ko, E. Watanabe and A. Yamada, *Nat. Energy*, 2019, **4**, 269–280.

- 14 X. Cao, H. Jia, W. Xu and J.-G. Zhang, *J. Electrochem. Soc.*, 2021, **168**, 010522.
- 15 J. Zhang, Q. Li, Y. Zeng, Z. Tang, D. Sun, D. Huang, Y. Tang and H. Wang, *ACS Energy Lett.*, 2023, **8**, 1752–1761.
- 16 Y. Chen, Z. Yu, P. Rudnicki, H. Gong, Z. Huang, S. C. Kim, J.-C. Lai, X. Kong, J. Qin, Y. Cui and Z. Bao, *J. Am. Chem. Soc.*, 2021, **143**, 18703–18713.
- 17 E. Park, J. Park, K. Lee, Y. Zhao, T. Zhou, G. Park, M.-G. Jeong, M. Choi, D.-J. Yoo, H.-G. Jung, A. Coskun and J. W. Choi, *ACS Energy Lett.*, 2023, **8**, 179–188.
- 18 H. Zhang, Z. Zeng, F. Ma, Q. Wu, X. Wang, S. Cheng and J. Xie, *Angew Chem. Int. Ed. Engl.*, 2023, **62**(21), e202300771.
- 19 T. D. Pham and K.-K. Lee, *Small*, 2021, **17**, 2100133.
- 20 R. Xu, J.-F. Ding, X.-X. Ma, C. Yan, Y.-X. Yao and J.-Q. Huang, *Adv. Mater.*, 2021, **33**, 2105962.
- 21 K. Ding, C. Xu, Z. Peng, X. Long, J. Shi, Z. Li, Y. Zhang, J. Lai, L. Chen, Y.-P. Cai and Q. Zheng, *ACS Appl. Mater. Interfaces*, 2022, **14**, 44470–44478.
- 22 Z. Li, H. Rao, R. Atwi, B. M. Sivakumar, B. Gwalani, S. Gray, K. S. Han, T. A. Everett, T. A. Ajantiwalay, V. Murugesan, N. N. Rajput and V. G. Pol, *Nat. Commun.*, 2023, **14**, 868.
- 23 N. von Aspern, G. V. Röschenthaler, M. Winter and I. Cekic-Laskovic, *Angew Chem. Int. Ed. Engl.*, 2019, **58**, 15978–16000.
- 24 Y. Zhao, T. Zhou, T. Ashirov, M. E. Kazzi, C. Cancellieri, L. P. H. Jeurgens, J. W. Choi and A. Coskun, *Nat. Commun.*, 2022, **13**, 2575.
- 25 Y. Zhao, T. Zhou, M. El Kazzi and A. Coskun, *ACS Appl. Energy Mater.*, 2022, **5**, 7784–7790.
- 26 J. Holoubek, M. Yu, S. Yu, M. Li, Z. Wu, D. Xia, P. Bhaladhare, M. S. Gonzalez, T. A. Pascal, P. Liu and Z. Chen, *ACS Energy Lett.*, 2020, **5**, 1438–1447.
- 27 Y. Zhao, T. Zhou, L. P. H. Jeurgens, X. Kong, J. W. Choi and A. Coskun, *Chem*, 2023, **9**, 682–697.
- 28 Y. Yang, D. M. Davies, Y. Yin, O. Borodin, J. Z. Lee, C. Fang, M. Olguin, Y. Zhang, E. S. Sablina, X. Wang, C. S. Rustomji and Y. S. Meng, *Joule*, 2019, **3**, 1986–2000.
- 29 J. Shi, C. Xu, J. Lai, Z. Li, Y. Zhang, Y. Liu, K. Ding, Y. P. Cai, R. Shang and Q. Zheng, *Angew Chem. Int. Ed. Engl.*, 2023, **62**, e202218151.
- 30 X. Fan, L. Chen, O. Borodin, X. Ji, J. Chen, S. Hou, T. Deng, J. Zheng, C. Yang, S.-C. Liou, K. Amine, K. Xu and C. Wang, *Nat. Nanotechnol.*, 2018, **13**, 715–722.
- 31 W. Xue, M. Huang, Y. Li, Y. G. Zhu, R. Gao, X. Xiao, W. Zhang, S. Li, G. Xu, Y. Yu, P. Li, J. Lopez, D. Yu, Y. Dong, W. Fan, Z. Shi, R. Xiong, C.-J. Sun, I. Hwang, W.-K. Lee, Y. Shao-Horn, J. A. Johnson and J. Li, *Nat. Energy*, 2021, **6**, 495–505.
- 32 Z. Yu, P. E. Rudnicki, Z. Zhang, Z. Huang, H. Celik, S. T. Oyakhire, Y. Chen, X. Kong, S. C. Kim, X. Xiao, H. Wang, Y. Zheng, G. A. Kamat, M. S. Kim, S. F. Bent, J. Qin, Y. Cui and Z. Bao, *Nat. Energy*, 2022, **7**, 94–106.
- 33 Z. Zhang, L. Hu, H. Wu, W. Weng, M. Koh, P. C. Redfern, L. A. Curtiss and K. Amine, *Energy Environ. Sci.*, 2013, **6**, 1806–1810.
- 34 W. Xue, Z. Shi, M. Huang, S. Feng, C. Wang, F. Wang, J. Lopez, B. Qiao, G. Xu, W. Zhang, Y. Dong, R. Gao, Y. Shao-Horn, J. A. Johnson and J. Li, *Energy Environ. Sci.*, 2020, **13**, 212–220.
- 35 W. Zhang, T. Yang, X. Liao, Y. Song and Y. Zhao, *Energy Storage Mater.*, 2023, **57**, 249–259.
- 36 X. Chen and Q. Zhang, *Acc. Chem. Res.*, 2020, **53**, 1992–2002.
- 37 Z. Li, Y. Chen, X. Yun, P. Gao, C. Zheng and P. Xiao, *Adv. Funct. Mater.*, 2023, **33**, 2300502.
- 38 Y. Wang, Z. Li, Y. Hou, Z. Hao, Q. Zhang, Y. Ni, Y. Lu, Z. Yan, K. Zhang, Q. Zhao, F. Li and J. Chen, *Chem. Soc. Rev.*, 2023, **52**, 2713–2763.
- 39 P. Ma, P. Mirmira and C. V. Amanchukwu, *ACS Cent. Sci.*, 2021, **7**, 1232–1244.
- 40 C. V. Amanchukwu, Z. Yu, X. Kong, J. Qin, Y. Cui and Z. Bao, *J. Am. Chem. Soc.*, 2020, **142**, 7393–7403.
- 41 Z. Yu, H. Wang, X. Kong, W. Huang, Y. Tsao, D. G. Mackanic, K. Wang, X. Wang, W. Huang, S. Choudhury, Y. Zheng, C. V. Amanchukwu, S. T. Hung, Y. Ma, E. G. Lomeli, J. Qin, Y. Cui and Z. Bao, *Nat. Energy*, 2020, **5**, 526–533.
- 42 Y. Zhao, T. Zhou, M. Mensi, J. W. Choi and A. Coskun, *Nat. Commun.*, 2023, **14**, 299.
- 43 G. Zhang, J. Chang, L. Wang, J. Li, C. Wang, R. Wang, G. Shi, K. Yu, W. Huang, H. Zheng, T. Wu, Y. Deng and J. Lu, *Nat. Commun.*, 2023, **14**, 1081.
- 44 Y. Yamada, M. Yaegashi, T. Abe and A. Yamada, *Chem. Commun.*, 2013, **49**, 11194–11196.
- 45 D. Ruan, L. Tan, S. Chen, J. Fan, Q. Nian, L. Chen, Z. Wang and X. Ren, *JACS Au*, 2023, **3**, 953–963.
- 46 O. C. Gagné and F. C. Hawthorne, *Acta Crystallogr., Sect. B: Struct. Sci., Cryst. Eng. Mater.*, 2016, **72**, 602–625.
- 47 B. D. Adams, J. Zheng, X. Ren, W. Xu and J.-G. Zhang, *Adv. Energy Mater.*, 2018, **8**, 1702097.
- 48 K. N. Wood, E. Kazyak, A. F. Chadwick, K.-H. Chen, J.-G. Zhang, K. Thornton and N. P. Dasgupta, *ACS Cent. Sci.*, 2016, **2**, 790–801.
- 49 K.-H. Chen, K. N. Wood, E. Kazyak, W. S. LePage, A. L. Davis, A. J. Sanchez and N. P. Dasgupta, *J. Mater. Chem. A*, 2017, **5**, 11671–11681.
- 50 P. Sayavong, W. Zhang, S. T. Oyakhire, D. T. Boyle, Y. Chen, S. C. Kim, R. A. Vilá, S. E. Holmes, M. S. Kim, S. F. Bent, Z. Bao and Y. Cui, *J. Am. Chem. Soc.*, 2023, **145**, 12342–12350.
- 51 H. Wu, H. Jia, C. Wang, J.-G. Zhang and W. Xu, *Adv. Energy Mater.*, 2021, **11**, 2003092.