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## Multiphase reaction of nitrate radicals with vanillic acid aerosols: kinetics and formation of light-absorbing particles

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Given that biomass-burning aerosol emissions have a direct radiative effect on the atmosphere, it is important to understand the chemistry that occurs within wildfire smoke that may change aerosol particle optical properties. To investigate night-time aging chemistry, this laboratory study explores the kinetics of the reaction between gas-phase nitrate radicals ( $\text{NO}_3$ ) and vanillic acid (VA), a functionalized phenol. As breakdown products of lignin, phenolic compounds are the commonly observed components of biomass burning smoke. They are also present in urban air pollution, formed by the oxidation of aromatic precursors. The study was conducted in an aerosol flow tube with a residence time of 15 minutes, where roughly 1.6 pptv of  $\text{NO}_3$  was formed by the reaction of  $\text{NO}_2$  (21 ppbv) and  $\text{O}_3$  (230 ppbv), and VA/ammonium sulfate (AS) solutions were atomized to form particles in the accumulation mode size range. The reaction was monitored by an aerosol mass spectrometer (AMS), which measured nitrated aerosol products, and by a 5-wavelength aethalometer, which observed the optical absorption of aerosol particles. The observed gas-surface kinetics are consistent with a  $\text{NO}_3$  reactive uptake coefficient to form a nitrated product of  $0.30 \pm 0.39$  and  $0.19 \pm 0.12$  at respectively  $\text{RH} = 25\% \pm 5\%$  and  $55\% \pm 5\%$  at 296 K. The aerosol particles became highly absorbing during the reaction in the near ultraviolet (375 nm) and visible (470, 528, and 625 nm) regions. While this change in absorptivity presumably arises *via* the nitration of the aromatic ring, the reaction drives stronger particle absorption, which extends much more deeply into the visible part of the spectrum than is characteristic of (mono) nitrovanillic acid (NVA), indicative of the formation of complex reaction products. These results demonstrate that night-time atmospheric aging of phenol-containing wildfire smoke and urban particulates will occur rapidly and significantly darken the particles throughout the visible part of the spectrum.

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### Environmental significance

The chemical aging of biomass burning aerosols is important for climate. However, most studies have focused on daytime processes involving light, ozone, or hydroxyl radicals. Herein, we studied a key nighttime chemical process, the reaction of nitrate radicals ( $\text{NO}_3$ ) with vanillic acid, a biomass burning particle surrogate. Using environmentally relevant  $\text{NO}_3$  mixing ratios, we found that the kinetics are extremely rapid (on the timescale of minutes), with about 30% of  $\text{NO}_3$  collisions with the particles forming nitrated products. For the first time, we document the changes in aerosol light absorption as a result of the reaction. The particles became substantially darker, with the increased absorption extending across all visible wavelengths. This is indicative of complex chemical aging processes.

## 1. Introduction

Biomass burning aerosol particles contain a diverse array of organic molecules, some arising from primary particulate emissions of the burning material and others *via* gas-to-particle partitioning and secondary processes. Many of these molecules

have their origins in the cellulosic component of plant material leading to, for example, small sugars. Similarly, the lignin component of biofuel is transformed into smaller molecules during burning, including to a large number of functionalized phenols.<sup>1,2</sup> The presence of this complex molecular mixture in the atmosphere has impacts on both health and climate. In addition, phenols are formed within urban environments *via* the oxidation of aromatic precursors.<sup>3,4</sup> In particular, aerosol molecules that absorb actinic radiation in the visible and ultraviolet parts of the spectrum are referred to as brown carbon (BrC) materials.<sup>5,6</sup> The contribution of BrC to the direct radiative

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effect is thought to be 25% of the radiative impact of black carbon particles.<sup>7–9</sup> This impact can be proportionally higher in regions of high wildfire impact, especially under smoldering fire conditions that produce a lot of particulate materials. Moreover, BrC is present in urban areas.<sup>10–12</sup>

As light-absorbing molecules, BrC aerosol materials are commonly electron-rich with a considerable degree of chemical unsaturation. These features make them prone to oxidative chemical transformations in the atmosphere. Field measurements on the rate at which BrC particles age in the atmosphere are challenging to conduct because the age of the fire or pollution plume needs to be known; nevertheless, there is an emerging consensus that aging affects the radiative impacts of BrC. In particular, significant whitening has been reported to occur far downwind of fire emissions, on a timescale as short as 24 hours.<sup>13–16</sup> Close to the fire source in the near-field, there is considerable variability in how BrC ages, with little indication of net whitening.<sup>17</sup> This could be because different darkening and whitening processes occur simultaneously.<sup>18</sup> The characteristics of the particles close to a fire are complex, with particle dilution and associated evaporation occurring simultaneously with secondary organic aerosol formation and multiphase chemical processing.<sup>19</sup>

Many laboratory studies have addressed the atmospheric chemical aging processes involving BrC aerosol particles,<sup>5,6,18</sup> including chemical transformations that occur in daylight hours *via* exposure to light and OH radicals.<sup>18,20–31</sup> These studies have illustrated that some wildfire materials initially become more absorptive in the near ultraviolet (UV) and visible parts of the spectrum, either *via* functionalization of reactive precursors or formation of higher molecular weight species, and then whitening occurs with additional aging.

However, considerably less work has been done on nighttime aging mechanisms, which will occur with the NO<sub>3</sub> radical. NO<sub>3</sub> is a ubiquitous, highly reactive oxidant, formed *via* reactions between NO<sub>x</sub> and ozone (O<sub>3</sub>). In particular, it can rapidly participate in addition reactions with electron-rich functional groups, such as aromatic rings and double bonds,<sup>32</sup> and it can also drive H-atom abstraction. Noting that NO<sub>3</sub> exists in a dynamic equilibrium with N<sub>2</sub>O<sub>5</sub>, its mixing ratios can range from many tens to hundreds of pptv in polluted environments, down to a few pptv in cleaner environments such as forests and marine environments.<sup>32</sup> Within near-field wildfire plumes, the formation rates of NO<sub>3</sub> can be high (up to 1 ppbv per hour), but the mixing ratios are generally quite low, well below the pptv level,<sup>33</sup> because of the high reactivity of NO<sub>3</sub> with gas phase constituents, such as phenolic molecules. NO<sub>3</sub> mixing ratios may be higher farther from the fires, as many of the reactive co-emitted species have already been depleted or diluted, reducing its loss pathways.

A study using a laboratory surrogate for tar balls has indicated that NO<sub>3</sub> oxidative transformations of BrC materials give rise to more absorption in the visible part of the spectrum, likely through the formation of –NO<sub>2</sub> groups (and perhaps –O–NO<sub>2</sub> groups) on aromatic rings,<sup>34</sup> with analogous chemistry of NO<sub>3</sub> observed in the aqueous phase<sup>35</sup> and with aqueous droplets.<sup>36,37</sup> NO<sub>3</sub> aging is consistent with some field observations of

nighttime aging.<sup>38</sup> Potential mechanisms for this chemistry, as illustrated in Scheme 1, involve NO<sub>3</sub> addition to the ring or H-abstraction from the phenolic OH group, with subsequent NO<sub>2</sub> addition to the free radical site on the ring to regain aromaticity.<sup>36,37,39–41</sup> We note that NO<sub>3</sub> chemistry may form products similar to those that are formed from OH chemistry in a NO<sub>x</sub>-rich environment when H-abstraction occurs, whereas O<sub>3</sub> oxidation more likely leads to ring-opening products.

Multiphase chemistry kinetic studies have largely focused on the interactions of gas-phase NO<sub>3</sub> with individual biomass burning materials, including phenolic substances such as catechol.<sup>36,37</sup> For example, by directly monitoring NO<sub>3</sub> decay, one study reports a reactive uptake coefficient of NO<sub>3</sub> with nitroguaiacol films on the order of 0.02 with no dependence on relative humidity up to 60%. A second study reports larger uptake coefficients, roughly 0.3, for reactions of NO<sub>3</sub> with syringaldehyde, vanillic acid, and coniferyl aldehyde using a relative rate technique and UV photoionization aerosol mass spectrometry;<sup>39</sup> both nitro- and di-nitro-products were observed. Such large uptake coefficients are consistent with the results of past studies showing that NO<sub>3</sub> reactivity with aromatic molecules in the form of polycyclic aromatic hydrocarbons is very efficient, with reactive uptake coefficients larger than 0.1.<sup>42,43</sup> Most recently, wood smoke particles have been shown to react on the timescale of minutes with part per trillion levels of NO<sub>3</sub>, forming nitrated products that absorb across the UV and visible parts of the spectrum.<sup>31</sup>

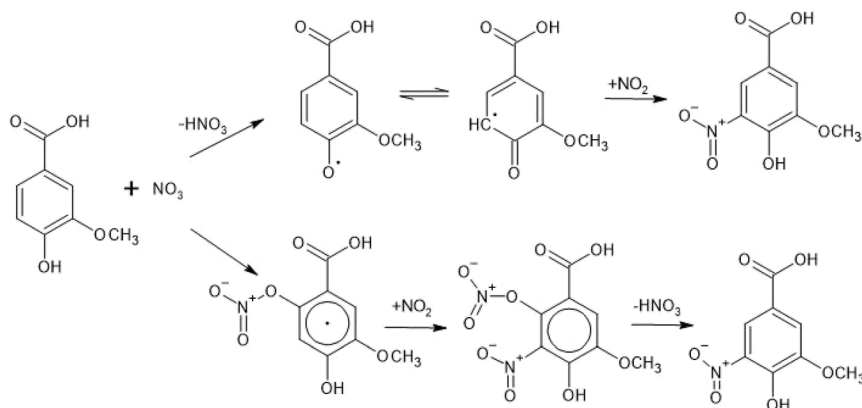
To advance our understanding of the chemistry involving nighttime aging of BrC wood smoke particles, our goals in this work are to measure the reaction kinetics for the addition of –NO<sub>2</sub> groups to a typical wood smoke condensed-phase aromatic compound – vanillic acid – while simultaneously observing the ability of the particles to absorb light in the near UV and visible parts of the spectrum. We chose vanillic acid as the surrogate molecule to study, given its prevalence in wood smoke,<sup>44,45</sup> low volatility ( $2 \times 10^{-8}$  atm),<sup>46</sup> which ensures that it is a particulate species, and aromaticity. We conducted the experiment in an aerosol flow tube with online instrumentation for monitoring changes in particle composition and optical properties. The experiments were performed with pptv-level, atmospherically relevant NO<sub>3</sub> mixing ratios.

## 2. Methods

### 2.1 Experimental

Experiments were conducted in a glass aerosol flow tube reactor (inner diameter 14.4 cm, length 200 cm, see Fig. 1) operated in a steady state manner at  $296 \pm 2$  K and atmospheric pressure. As described below, variable reaction times within the reactor were achieved by the introduction of gas-phase NO<sub>2</sub> *via* a movable injector, whereas aerosol particles and O<sub>3</sub> were injected at the upstream end of the flow tube. The sealed glass reactor was wrapped in aluminum foil, oriented vertically, and operated with a total flow of zero air, 1.6 SLM, which corresponds to a maximum residence time of 15 minutes. The relative humidity in the flow tube was raised by removing the dryers after the atomizer. The RH was measured using a probe (model RH-USB,





Scheme 1 Potential mechanisms for the reaction of  $\text{NO}_3$  with vanillic acid.



Fig. 1 Schematic of the experimental apparatus.

Omega Engineering Inc.) located on the flow exiting the reactor. It was steady to  $\pm 1.5\%$  for an individual experiment.

Instrumentation attached to the flow tube included a scanning particle mobility sizing (SMPS) system (Model 3034, TSI) for aerosol particle size determination, with the sheath at the same RH as the sample flow. Connected to the flow tube *via* conductive polymer tubing and stainless steel, the SMPS was operated with a sample flow of 0.3 SLM and a sheath flow of 3 SLM, with a scan rate of 4 minutes. A high-resolution aerosol mass spectrometer (HR-AMS) provided aerosol particle composition information *via* flash vaporization of aerosol particles at 600 °C, followed by electron-impact ionization of volatilized molecules.<sup>47</sup> The AMS sampled aerosol particles at a flow rate of 132 sccm through conductive polymer tubing and metal tubing. It was operated in V-mode and was calibrated with ammonium nitrate particles such that the aerosol masses presented in the paper are in nitrate-equivalent mass. The default relative ionization efficiency (*i.e.*, relative to nitrate, RIE) of 1.2 was applied to determine sulfate mass loadings. Both vanillic acid and nitrovanillic acid (a potential reaction product, see

Scheme 1) were calibrated directly using size-selected (300 nm), atomized particles. Their RIE values were 0.011 and 0.006, respectively.

To measure the ability of the particles to absorb light from the near ultraviolet to the near infrared parts of the spectrum, a 5-wavelength aethalometer (MA200, Aethlabs Inc., 375, 470, 528, 625, 880 nm) was used with measurements reported every minute. MA200 aethalometers operate by sampling aerosol particles onto a Teflon filter with a flow rate of 150 sccm, with the changes in light attenuation monitored continually. The standard correction provided by the supplier to account for the scattering effects on the filter ( $C_{\text{ref}} = 1.3$ ) was applied to obtain the mass absorption cross section at each wavelength.<sup>48</sup> The dual spot correction was employed to compensate for the reduction in light attenuation caused by the material accumulating on the filter, following the method from Virkkula *et al.*<sup>49,50</sup>

Aerosol particles were injected through a side-arm injector at the upstream end of the flow tube. The particles had a poly-disperse size distribution, formed *via* atomization of an aqueous solution of ammonium sulfate (0.005–0.007 M, AS) and vanillic acid (0.007–0.010 M). AS was used for three reasons: its environmental relevance, ability to add hygroscopicity to the particles, and utility as an unreactive aerosol component to act as an internal standard. The geometric mean diameter of the aerosol size distribution was approximately 95 nm and mass loadings in the reactor were approximately  $500 \mu\text{g m}^{-3}$ .

$\text{NO}_3$  was generated *in situ* within the flow reactor by the reaction of gas-phase  $\text{O}_3$  and nitrogen dioxide ( $\text{NO}_2$ ). In particular,  $\text{O}_3$  within a 250 sccm flow of zero air was added at the upstream end of the flow tube and  $\text{NO}_2$  was supplied as a 10 sccm flow from a cylinder (3 ppm  $\text{NO}_2$  in  $\text{N}_2$ ) *via* a movable, stainless steel injector (6.5 mm o.d., 210 cm long) configured with four exit ports aligned with the flow direction. In particular, the  $\text{NO}_2$  flowed through a 3 mm o.d. Teflon tube that lay inside the stainless-steel injector. The  $\text{O}_3$  was generated by passing 1000 sccm of zero air over a Hg lamp housed in a glass cell. The mixing ratios of  $\text{NO}_2$  and  $\text{O}_3$  in the flow tube were 21 ( $\pm 4$ ) and 230 ( $\pm 15$ ) ppbv, respectively, as measured continuously *via* gas monitors (Thermo NOx analyzer model 42i and 2B Tech, Model 202 Ozone Monitor) connected to the exit flow.



Sliding through an o-ring seal, the injector could be moved vertically within the flow tube to provide variable reaction times between the NO<sub>3</sub> (that forms from the reaction of NO<sub>2</sub> and O<sub>3</sub>) and aerosol particles within the main flow. The injector was electrically grounded to minimize the loss of particles on it.

In the kinetics determinations described below, we only used the data collected with a minimum residence time of roughly 2 minutes within the flow tube. There are two reasons for this. One, an estimate of the diffusive mixing time for the NO<sub>2</sub> exiting the injector within the carrier gas of the flow is a couple of minutes. Two, a kinetics model (see SI Text S1 and Fig. S2) predicts that NO<sub>3</sub> will achieve a quasi-steady state concentration in the flow tube on the timescale of less than 2 minutes.

The mixing ratio of NO<sub>3</sub> in the flow reactor was measured using an indirect tracer method during independent experiments in the flow tube, *i.e.*, these experiments were not conducted at the same time as the NO<sub>3</sub>/VA/AS experiments. We added ozone and  $\alpha$ -pinene (2 ppbv initial mixing ratio) to the flow tube. A proton-transfer-reaction mass spectrometer (PTR-MS) monitored the change in  $\alpha$ -pinene signal, using the H<sub>3</sub>O<sup>+</sup> reagent ion at *m/z* 137,<sup>51</sup> with and without NO<sub>2</sub> present, *i.e.*, with and without NO<sub>3</sub> present. The NO<sub>3</sub> concentration was calculated from the following equation:

$$[\text{NO}_3] = -\frac{\ln([\alpha\text{-pinene}]_t/[\alpha\text{-pinene}]_0)}{k_x \times t} \quad (1)$$

where  $k_x$  is the rate constant of NO<sub>3</sub> with  $\alpha$ -pinene,  $t$  is the time in the reactor and  $[\alpha\text{-pinene}]_0$  and  $[\alpha\text{-pinene}]_t$  are the concentrations of  $\alpha$ -pinene before and after injection of NO<sub>2</sub> into the reactor. The  $\alpha$ -pinene was added *via* a cylinder containing a dilute mixture (21 ppmv) of the gas in N<sub>2</sub>. The particle loading and the O<sub>3</sub> and NO<sub>2</sub> mixing ratios were the same as during the VA kinetics experiments. Sufficiently little  $\alpha$ -pinene was added that its reaction with NO<sub>3</sub> did not represent a major sink relative to the loss of NO<sub>3</sub> *via* reactions with NO<sub>2</sub>, particles, and the walls of the reactor. Additional details on the measurements of the NO<sub>3</sub> concentrations are provided in the SI (Text S1, Fig. S1, S2 and Table S1).

Lastly, offline ultraviolet-visible spectra of stock solutions were measured with an Ocean Optics spectrometer (model USB 2000+) equipped with a deuterium tungsten halogen light source (DT-Mini-2, Ocean Optics). The light-absorption spectra were analyzed using the SpectraSuite (Ocean Optics) software with spectral data ranging between 250 and 850 nm. A water blank was measured prior to each measurement and subtracted from all spectra.

## 2.2 Data analysis

The reactive uptake coefficient expresses the probability that a reaction occurs upon collision of NO<sub>3</sub> with an aerosol particle. In this work, we define the reactive uptake coefficient as representing the probability that a condensed phase nitrated product forms from the reaction, as observed with the AMS. To do this, we use eqn (2) to calculate the uptake coefficient:<sup>52</sup>

$$\gamma_{\text{NO}_3} = \frac{-d([\text{VA}]_t/[\text{VA}]_0)}{d[\text{NO}_3]_t} \times \frac{V}{A} \times \frac{4RT}{\nu} \times [\text{reactant}]_0 \quad (2)$$

where the differential term is the slope of the linear fit of the decay of the particle mass concentration of reactive vanillic acid in the flow tube,  $[\text{VA}]$ , relative to the NO<sub>3</sub> exposure;  $V/A$  represents the particle volume to surface area ratio,  $\nu$  is the mean speed of nitrate radicals in the gas phase,  $R$  is the gas constant and  $T$  is the temperature. The initial molar concentration of reactive vanillic acid in the particles,  $[\text{reactant}]_0$ , was estimated using the following:

$$[\text{Reactant}]_0 = \frac{\rho_{\text{VA}}}{\text{MW}_{\text{VA}}} \times \left( \frac{[\text{NVA}]}{[\text{Org}]} \right)_\infty \quad (3)$$

where  $\rho_{\text{VA}}$  represents the density of vanillic acid,  $\text{MW}_{\text{VA}}$  is the molecular weight of vanillic acid (168.13 g mol<sup>-1</sup>),  $[\text{NVA}]_\infty$  and  $[\text{Org}]_\infty$  are the particle mass concentrations of nitrovanillic acid (NVA) and total organics in the flow tube, respectively, taken at infinite reaction time. Note that for this analysis, the AMS parent ion for NVA is used to indicate product formation. We extrapolate the kinetics data to infinite reaction time to provide an estimate of the maximum amount of product that can form. We note that higher-order products such as dinitrovanillic acid are also formed (see discussion below), it is likely that at least part of the mono-nitrovanillic ion signal in the AMS originates from the fragmentation of these compounds. We assume that the amount of reactive VA is equal to the total amount of NVA that forms, *i.e.*, some of the VA may be buried in the solid particle and cannot react. Although we are measuring reaction products (*i.e.*, NVA) with the AMS, eqn (2) requires knowledge of the amount of the reactive starting material ( $[\text{VA}]$ ):<sup>53</sup>

$$[\text{VA}]_t = [\text{VA}]_0 - [\text{NVA}]_t = [\text{NVA}]_\infty - [\text{NVA}]_t \quad (4)$$

For large uptake coefficients, there can be a mass transfer limitation arising from the slow diffusion of NO<sub>3</sub> in the gas phase to the particle, which can be accounted for using a standard approach.<sup>54</sup> In particular, by calculating the Knudsen number characteristic for the system, one can correct an observed first-order rate constant for reactant loss for gas-phase diffusion. For the results presented below, the correction is less than 15%, which is within the estimated uncertainty in the uptake coefficient.

## 3. Results and discussion

### 3.1 Nitrate radical concentration

Fig. S1 illustrates typical data from which the concentration of NO<sub>3</sub> was determined. The average PTR-MS signal for  $\alpha$ -pinene was calculated when NO<sub>2</sub> (and so, also, NO<sub>3</sub>) was present in the flow tube and when it was absent. Considering the residence time of air in the flow tube (900 seconds for these experiments), eqn (1) was used to determine that the NO<sub>3</sub> concentration was 3.6 and 4.1 × 10<sup>7</sup> molecules per cm<sup>3</sup> at 25% ± 5% and 55 ± 5% RH, respectively, yielding an average value of 3.8 ± 1.9 × 10<sup>7</sup> molecules per cm<sup>3</sup> (*i.e.*, 1.6 ± 0.8 pptv at room temperature and pressure) across 7 experiments. See Text S1 for more details. The variability in RH values represents variations from experiment to experiment.



It is important to determine the timescale at which  $\text{NO}_3$  goes into a quasi-steady state within the flow tube, after  $\text{NO}_2$  and  $\text{O}_3$  react. The chemical reactions occurring in the flow tube include the following:



When (R1)–(R5) are implemented into a numerical model, the  $\text{NO}_3$  concentration temporal profile in Fig. S2 is generated. Most importantly,  $\text{NO}_3$  moves into steady state within about 100 seconds. As stated above, this is one reason that we do not use kinetic data collected within the first 20 cm of the flow tube, corresponding to 2 minutes of residence time after the  $\text{NO}_2$  and  $\text{O}_3$  mix.

The predicted concentration of  $\text{NO}_3$  is within a factor of 6 of the measured value, with the discrepancy likely due to neglecting  $\text{NO}_3$  and  $\text{N}_2\text{O}_5$  wall losses in the model. However, note that if reaction (R4) is not included in the model, the predicted  $\text{NO}_3$  concentration is roughly 30 times larger than the measured value. This is indirect confirmation that  $\text{NO}_3$  reacts rapidly with the aerosol particles.

### 3.2 Reaction kinetics between $\text{NO}_3$ and vanillic acid aerosol particles

Fig. 2 illustrates a typical time series of quantities monitored by the AMS during an experiment, as the injector was moved to change the  $\text{NO}_3$  residence time in the flow tube.  $\text{SO}_4^{2-}$  decreased somewhat at longer reaction times (upper horizontal axis), likely due to small fluctuations in the flow conditions or atomizer output. Given that ammonium sulfate is present in the atomizer alongside vanillic acid, VA and AS will be internally mixed within the same particles. Thus, we use  $\text{SO}_4^{2-}$  as an internal standard to correct for changes in the AMS particle collection efficiency that can occur with changing particle composition. After  $\text{SO}_4^{2-}$  normalization, the VA signal (observed at its molecular ion,  $\text{C}_8\text{H}_8\text{O}_4^+$ ) decreases with longer reaction times and the NVA signal ( $\text{C}_8\text{H}_7\text{NO}_6^+$ ) increases, indicative of a multiphase reaction of VA with  $\text{NO}_3$  to form NVA (and other products).

Fig. 2 demonstrates that significant nitration of the particles is occurring, as indicated by the increase in the total nitrate signal with increasing reaction time in the flow tube. AMS total nitrate can arise from either inorganic nitrate (*i.e.*,  $\text{NO}_3^-$ ) or oxidized organic nitrogen (*e.g.*,  $\text{R-NO}_x$ ) particulate matter, which have different  $\text{NO}^+/\text{NO}_2^+$  ratios in the particle AMS mass spectra. In particular, in our instrument,  $\text{NH}_4\text{NO}_3$  particles yield a  $\text{NO}^+/\text{NO}_2^+$  ratio of 1.3, whereas higher values are typical of organic nitrate/nitro compounds.<sup>55</sup> Thus, the high ratios in Fig. 2 are indicative of oxidized organic nitrogen products. For

reference, we note that we measured the  $\text{NO}^+/\text{NO}_2^+$  ratio for nitrovanillic acid aerosol particles ( $\text{C}_8\text{H}_7\text{NO}_6$ ) to be 12.5 in our instrument.

While we clearly observed NVA formation, there was some evidence for the addition of two  $-\text{NO}_2$  groups to the VA aromatic ring (*i.e.*,  $\text{C}_8\text{H}_7\text{NO}_6^+$  and  $\text{C}_8\text{H}_6\text{N}_2\text{O}_8^+$ ). However, the di-nitro product signal was weaker than the mono-nitro signal (see Fig. S3), so only the mono-nitro product signal is plotted in Fig. 2. We note that the AMS employs electron impact as its ionization mechanism, which induces considerable ion fragmentation. Thus, the signal plotted in Fig. 2 for the mono-nitro product may also have some mass spectral intensity arising from fragmentation of larger parent ions. The ratio of the mono- to di-nitro signals did not vary during the course of the reaction. Note that the same two products were observed in the only prior study of this reaction, which used a softer ionization technique.<sup>39</sup>

The normalized signal of the product  $\text{C}_8\text{H}_7\text{NO}_6^+$  in Fig. 2 is plotted in Fig. 3a *versus* residence time in the flow tube, clearly indicating that the product intensity grows with increasing reaction time. Note that there is curvature in the growth curve, with slower growth at long reaction times. We attribute the slowing of the reaction at long times to the depletion of VA available for reaction at the surface of the solid VA/AS particles. To support this claim, we can estimate the number of VA molecules available for reaction at the surface of the particles. In particular, this quantity is calculated to be approximately from  $0.7$  to  $1.4 \times 10^{10}$  molecules per  $\text{cm}^3$ , obtained by multiplying the particle surface area density in the flow tube ( $6.8 \times 10^{-5} \text{ cm}^2 \text{ cm}^{-3}$ ) by a typical monolayer molecule coverage for molecules the size of VA ( $\approx 1$  to  $2 \times 10^{14}$  molecules per  $\text{cm}^2$ ). We can also estimate the number of reactive collisions per unit volume ( $\approx 6 \times 10^9$  reactions per  $\text{cm}^3$ ) that particles experience when passing through the flow tube by multiplying eqn (S1) by the steady state  $[\text{NO}_3]$  and the total reaction time (1000 s), assuming the reactive uptake coefficient is 0.3 (see below for calculation of the uptake coefficients). The fact that these two quantities are calculated to be so similar to each other says that there is enough  $\text{NO}_3$  in the flow tube, and that it has sufficiently high reactivity, that it can react with every VA molecule present at the surfaces of the particles during the reaction time in the flow tube; this makes us believe that the reaction is only occurring at the surface of the particles.

In Fig. 3b, we plot the kinetics data in Fig. 3a *versus*  $\text{NO}_3$  exposure, *i.e.*, the product of  $[\text{NO}_3]$  and reaction time. The y-axis of Fig. 3b is the quantity  $[\text{VA}]$  at time  $t$ , divided by the initial concentration of VA available for reaction, as calculated *via* eqn (4), where the value of  $[\text{VA}]_0$  is determined by fitting the data in Fig. 3a with a non-linear, least squares, exponential growth curve.

According to eqn (2), the slope of the linear least squares fit to the data in Fig. 3b yields the reactive uptake coefficient for the formation of nitrated VA. For the data in this figure, the uptake coefficient is determined to be  $0.10 \pm 0.02$ , where this uncertainty arises from the precision of the straight line fit to the data. Additional uncertainties in the uptake coefficient are larger, arising largely from the estimate of the value of



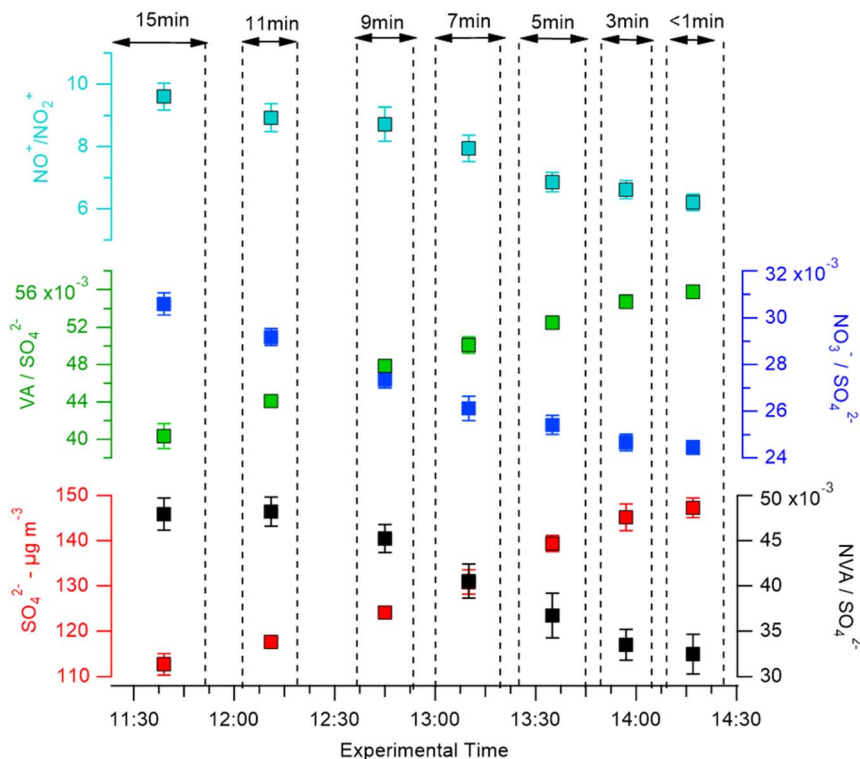


Fig. 2 Data collected during a typical experiment ( $RH = 25\%$ ), where experimental time on the lower horizontal axis is the real time at which the measurements were conducted in the laboratory, plotted in the hh:mm format. The times on the upper horizontal axis (*i.e.*, <1 to 15 min) correspond to the variable reaction times of  $\text{NO}_3$  and particles in the flow tube, dependent on the injector position, where the first time bracket at 15 min represents the maximum exposure time, which decreases as the injector is pushed into the flow tube. Traces shown include aerosol sulfate ( $\text{SO}_4^{2-}$ ),  $\text{NO}^+/\text{NO}_2^+$ , and  $\text{SO}_4^{2-}$ -normalized vanillic acid (VA), nitrate (indicative of both inorganic and organic nitrates), and NVA.

$[\text{reactant}]_0$  ( $\pm 50\%$ ) and a systematic error in the concentration of  $\text{NO}_3$  in the flow tube ( $\pm 50\%$ ). A summary of all the uptake coefficient measurements is provided in Table 1. The errors listed in the table are one standard deviation precision errors. The relatively large precision errors are likely a result of a variety of factors, including relatively weak AMS signals arising from

products only forming on the surface of the solid particles, as well as variability in the aerosol flow tube conditions.

The overall conclusion is that this multiphase reaction occurs rapidly, with reactive uptake coefficients larger than 0.1. This high reactivity is consistent with most past studies of related systems for the reactions of  $\text{NO}_3$  with aromatic, electron-



Fig. 3 (a) For the data in Fig. 2, the nitro-vanillic acid-to-sulfate ratio for different reaction exposure times in the flow reactor, and (b) variation in vanillic acid mass loading at each time normalized to the initial vanillic acid mass loading, as a function of  $\text{NO}_3$  exposure in the flow tube. Note that the nitro-vanillic acid data are baseline corrected by the signal with zero reaction time. Only the red data points are used in the kinetics analysis, whereas the grey points at early times are not included in the fits (since the first 2 minutes are required for  $\text{NO}_3$  to reach steady state).







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