

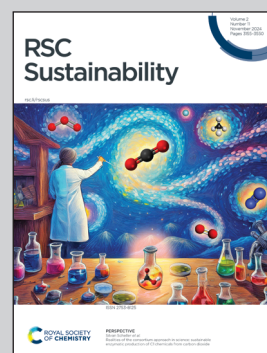


**Showcasing research from Professor Günther Rupprechter's laboratory, Institute of Materials Chemistry, TU Wien, Vienna, Austria.**

Bimetallic CuPd nanoparticles supported on ZnO or graphene for CO<sub>2</sub> and CO conversion to methane and methanol

Our work investigates the hydrogenation of CO<sub>2</sub> and CO to CH<sub>4</sub> and MeOH to reduce emissions and reliance on fossil fuels. It evaluates Cu, Pd, and CuPd nanoparticles on ZnO or graphene as catalysts under different operating conditions, demonstrating that lower Cu/Pd loadings favor CH<sub>4</sub> production, while higher Cu content boosts MeOH yield, offering valuable insights for sustainable fuel catalyst design.

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## PAPER

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[View Journal](#) | [View Issue](#)Cite this: *RSC Sustainability*, 2024, 2, 3276Bimetallic CuPd nanoparticles supported on ZnO or graphene for CO<sub>2</sub> and CO conversion to methane and methanol†Qaisar Maqbool,<sup>‡a</sup> Klaus Dobrezberger,<sup>ID ‡a</sup> Julian Stropp,<sup>a</sup> Martin Huber,<sup>ID a</sup> Karl-Leopold Kontrus,<sup>a</sup> Anna Aspalter,<sup>a</sup> Julie Neuhauser,<sup>a</sup> Thomas Schachinger,<sup>ID b</sup> Stefan Löffler<sup>b</sup> and Günther Rupprechter<sup>ID \*a</sup>

Carbon dioxide (CO<sub>2</sub>) and carbon monoxide (CO) hydrogenation to methane (CH<sub>4</sub>) or methanol (MeOH) is a promising pathway to reduce CO<sub>2</sub> emissions and to mitigate dependence on rapidly depleting fossil fuels. Along these lines, a series of catalysts comprising copper (Cu) or palladium (Pd) nanoparticles (NPs) supported on zinc oxide (ZnO) as well as bimetallic CuPd NPs supported on ZnO or graphene were synthesized via various methodologies. The prepared catalysts underwent comprehensive characterization via high-resolution transmission electron microscopy (HRTEM), energy-dispersive X-ray spectroscopy (EDX) mapping, electron energy loss spectroscopy (EELS), X-ray diffraction (XRD), hydrogen temperature-programmed reduction and desorption (H<sub>2</sub>-TPR and H<sub>2</sub>-TPD), and deuterium temperature-programmed desorption (D<sub>2</sub>O-TPD). In the CO<sub>2</sub> hydrogenation process carried out at 20 bar and elevated temperatures (300 to 500 °C), Cu, Pd, and CuPd NPs (<5 wt% loading) supported on ZnO or graphene predominantly yielded CH<sub>4</sub> as the primary product, with CO generated as a byproduct via the reverse water gas shift (RWGS) reaction. For CO hydrogenation between 400 and 500 °C, the CO conversion was at least 40% higher than the CO<sub>2</sub> conversion, with CH<sub>4</sub> and CO<sub>2</sub> identified as the main products, the latter from water gas shift. Employing 90 wt% Cu on ZnO led to an enhanced CO conversion of 14%, with the MeOH yield reaching 10% and the CO<sub>2</sub> yield reaching 4.3% at 230 °C. Overall, the results demonstrate that lower Cu/Pd loading (<5 wt%) supported on ZnO/graphene favored CH<sub>4</sub> production, while higher Cu content (90 wt%) promoted MeOH production, for both CO<sub>2</sub> and CO hydrogenation at high pressure.

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## Sustainability spotlight

The hydrogenation of carbon dioxide (CO<sub>2</sub>) to methane (CH<sub>4</sub>) or methanol (CH<sub>3</sub>OH) is a promising route to use CO<sub>2</sub> as feedstock, lowering its emissions and reducing dependence on fossil fuels. It aligns well with the UN's Sustainable Development Goals on energy, sustainability and climate. This study reports the synthesis of copper-based catalysts supported on zinc oxide or graphene, promoted by palladium. The nanoparticle catalysts demonstrate high efficiency in CO<sub>2</sub> and CO hydrogenation, favouring methane production at lower metal loadings but methanol production at higher copper content. This sustainable approach highlights the potential for reducing environmental impact by improving catalytic performance.

## Introduction

Carbon dioxide (CO<sub>2</sub>) is Earth's most abundant greenhouse gas responsible for absorbing and radiating heat.<sup>1</sup> As of April 2024, the atmospheric CO<sub>2</sub> concentration observed by the NOAA Global Monitoring Lab reached 425.38 ppm, marking a new

record.<sup>2</sup> This value surpasses any previous levels observed in human history and it is expected to increase to ≈500 ppm in the next 20 years, which is regarded as the point of no return.<sup>3</sup> Accordingly, the International Energy Agency (IEA) took the initiative of Carbon Capture, Utilization and Storage (CCUS)<sup>4</sup> and Net Zero Emissions by the 2050 (NZE)<sup>5</sup> Scenario. However, despite the existence of numerous strategies, effective solutions to this challenge remain elusive.

The increase in CO<sub>2</sub> concentration is largely attributed to burning fossil fuels for energy generation and use as feedstock for chemicals. The utilization of CO<sub>2</sub> as an alternative and sustainable carbon source has thus gained worldwide attention as a key aspect of CCUS.<sup>6</sup> The advancements in energy-efficient

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catalytic CO<sub>2</sub> conversion using renewable energy have the potential to mitigate CO<sub>2</sub> emissions and reduce reliance on fossil fuels.<sup>7</sup> One of the straightforward ways to utilize CO<sub>2</sub> is its hydrogenation to produce value-added products such as hydrocarbons (including olefins, liquid hydrocarbons, and aromatics), oxygenates (such as alcohols and dimethyl ether) or reaction gases such as CO (for syngas and Fischer–Tropsch processes) or methane.<sup>8,9</sup> The three primary catalytic methods for CO<sub>2</sub> hydrogenation include thermal catalysis,<sup>8–20</sup> electrocatalysis,<sup>21,22</sup> and photocatalysis.<sup>23–26</sup> Although thermal catalysis requires higher temperatures and pressures for CO<sub>2</sub> activation, it remains a widely applied process for rapid and efficient transformation of CO<sub>2</sub> (that could originate from carbon capture).

Due to thermodynamic limitations, hydrogenation to methanol (MeOH) demands high-pressure and elevated operating temperature to achieve favorable reaction kinetics, as well as an effective and active catalyst. In this regard, various catalytic materials including Pt, In, Ni, Ru, Zr, Rh, and Ga have been widely explored for CO<sub>2</sub> hydrogenation to MeOH.<sup>27–32</sup> However, Cu still stands out as the most utilized and studied metal<sup>16–18</sup> due to its high activity at lower temperatures, making it particularly suitable for the CO<sub>2</sub> hydrogenation reaction. Additionally, Cu offers advantages in terms of cost-effectiveness, as well as its multivalency (Cu<sup>0</sup>, Cu<sup>I</sup>, and Cu<sup>II</sup>).<sup>19</sup> Moreover, Cu maintains stable interaction with oxygen, preventing the formation of unstable intermediates or surface poisoning. The CO-induced mobility of Cu atoms may counteract sintering.<sup>33,34</sup> It also exhibits strong interactions with other materials, such as Zn, which improves stability, selectivity, and the ability to dissociate H<sub>2</sub>.<sup>35,36</sup>

Industrially, MeOH is mainly synthesized from a feed of CO<sub>2</sub>, CO, and H<sub>2</sub> at high pressure (100 bar), using Cu/ZnO/Al<sub>2</sub>O<sub>3</sub> catalysts.<sup>37,38</sup> The kinetics and thermodynamics of this reaction have been widely studied<sup>11,39–41</sup> along with the influence of water on catalyst performance.<sup>42–44</sup> There are three main reactions involved in the hydrogenation of CO<sub>2</sub>,

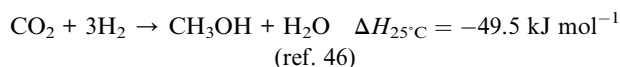
Reverse water gas shift (RWGS):



Methanation:



MeOH synthesis:



The reaction selectivity is thus influenced by the reaction temperature, pressure, and the catalyst used. Additionally, the catalytic performance of Cu can be further improved by the addition of promoters (e.g. Mn, Zr, Zn, and Al)<sup>47,48</sup> and by various

supports (e.g. graphitic carbon, SiO<sub>2</sub>, CNTs, and MgO).<sup>49–52</sup> This can modulate active sites and the surface charge of Cu.<sup>53</sup>

Studies have shown that the use of Pd, either alone or as a promoter of Cu, both over ZnO, can enhance selectivity towards various products of CO<sub>2</sub> hydrogenation.<sup>54,55</sup> Siriworarat *et al.*<sup>56</sup> investigated the impact of Pd loading (5, 10, and 15 wt%) on a Pd–Cu–Zn catalyst, where Cu and Zn comprised 25 wt%. Conducted at 250 °C and 25 bar, the study demonstrated that the highest performance was achieved with the catalyst containing 15 wt% Pd, 25 wt% Cu, and 25 wt% Zn, yielding a MeOH space-time yield of 0.112 kg<sub>MeOH</sub> kg<sub>cat</sub><sup>−1</sup> h<sup>−1</sup>. In another study by Díez-Ramírez *et al.*,<sup>57</sup> 37.5 wt% Pd with CuZn/SiC exhibited the highest selectivity towards MeOH. In addition, Deetrakul *et al.*<sup>7</sup> found that 15 wt% CuZn(O) loading over a nitrogen-doped graphene aerogel achieved the highest MeOH production (0.095 kg<sub>MeOH</sub> kg<sub>cat</sub><sup>−1</sup> h<sup>−1</sup>) at a reaction temperature of 250 °C and a relatively low pressure of 15 bar. Collectively, the combination of Cu with Pd over ZnO or graphene as the support may present an intriguing avenue to enhance CO<sub>2</sub> hydrogenation to hydrocarbons, warranting further exploration through studies of monometallic Cu/ZnO, bimetallic CuPd/ZnO, or CuPd/Gr. Even more so, as one would rather avoid using noble metals.

To add to the current understanding, different preparation protocols were adapted to prepare ZnO-supported CuPd (bimetallic) and graphene-supported CuPd, as well as ZnO supported Cu or Pd (monometallic) catalysts, as summarized in Table 1. The reduction temperature of the catalysts (monometallic) was varied (*i.e.*, 200, 300, and 500 °C) to investigate its influence on catalytic activity, catalyst morphology, particle size, and composition. High resolution transmission electron microscopy (HRTEM) with electron energy loss spectroscopy (EELS) and energy-dispersive X-ray spectroscopy (EDX), high-angle annular dark-field scanning transmission electron microscopy (HAADF-STEM), and X-ray powder diffraction (XRD) were employed to analyze the size, distribution of metal particles, and the catalysts' composition. Furthermore, temperature-programmed reduction (TPR) provided insights into catalyst stability and metal-support interactions. Moreover, temperature-programmed desorption (TPD) revealed information about adsorption sites. On the reduced catalysts, the hydrogenation of CO<sub>2</sub> was carried out at atmospheric pressure and an elevated pressure of 20 bar in a continuous flow fixed-bed reactor, connected to a micro-gas chromatograph (GC) for kinetic measurements, with the reaction conducted at different temperatures. Selectivity and catalytic activity as a function of reaction temperature were compared for each catalyst.

## Results and discussion

### Catalyst synthesis and characterization

Fig. 1A illustrates the synthesis procedures for obtaining different types of catalysts using ZnO or graphene (Gr) as supports (Table 1; for details see the Experimental section). Following a redox method (denoted by r)<sup>58</sup> for 5 wt% Cu/Pd (3 : 2), H<sub>2</sub>-reduced Cu on ZnO or Gr was mixed with Pd salt under N<sub>2</sub> (Cu + Pd<sup>2+</sup> → Cu<sup>2+</sup> + Pd) forming (i) CuPd/ZnO-r or (ii) CuPd/Gr-r catalysts, respectively.



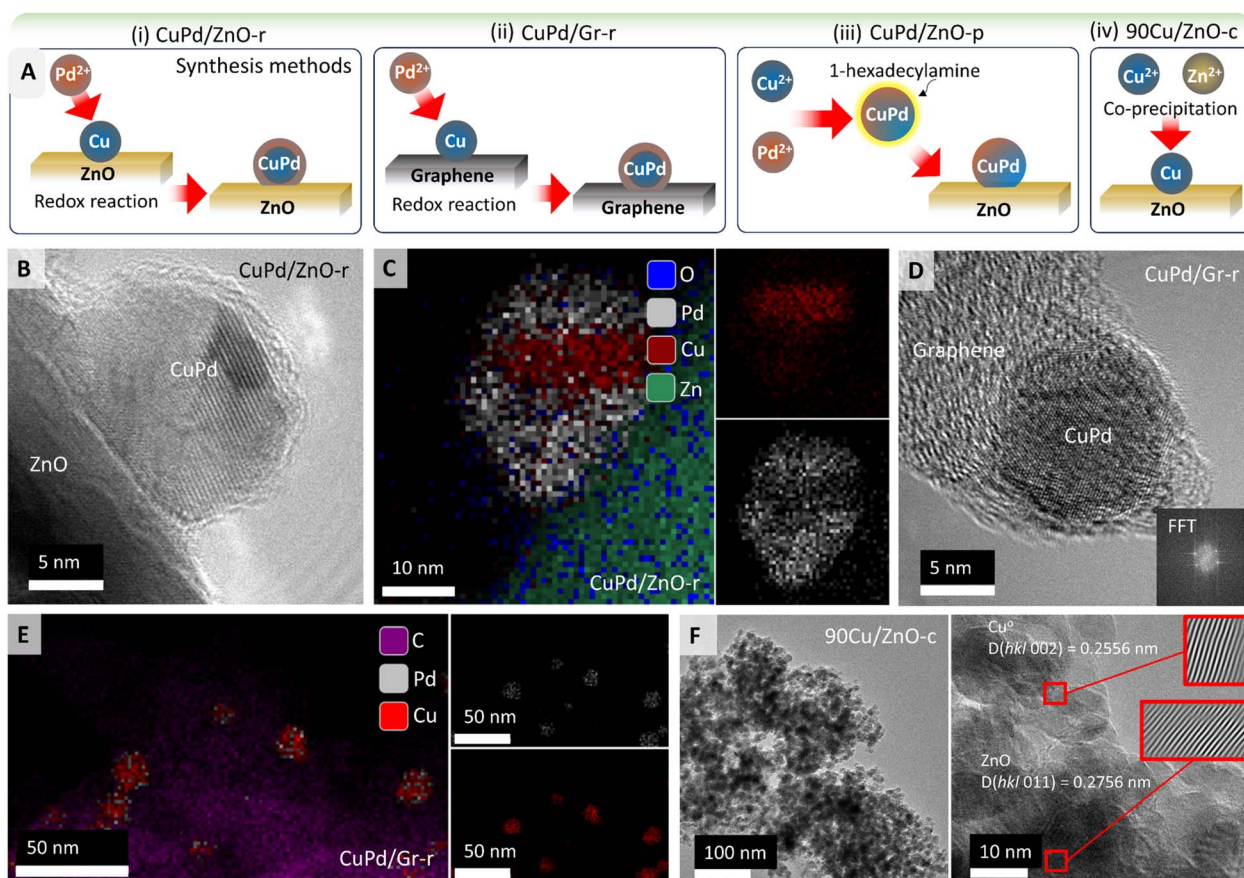
**Table 1** Catalysts examined in the current study (% refers to wt%)

Synthesized catalysts	Abbreviation
5% CuPd (3 : 2) on ZnO or graphene (reduction method)	(i) CuPd/ZnO-r (ii) CuPd/Gr-r
5% CuPd (3 : 2) on ZnO (polyol synthesis method)	(iii) CuPd/ZnO-p
90% Cu- and Zn-nitrates reduced with Na <sub>2</sub> CO <sub>3</sub> (co-precipitation method)	(iv) 90Cu/ZnO-c
5% Cu or Pd on ZnO (wet impregnation method)	(v) Cu/ZnO-i (vi) Pd/ZnO-i

In a polyol synthesis,<sup>59,60</sup> Pd<sup>2+</sup> and Cu<sup>2+</sup> ions were reduced with ethylene glycol and stabilized with 1-hexadecylamine as a ligand. The obtained CuPd alloy nanoparticles (NPs) were impregnated on the ZnO support forming (iii) CuPd/ZnO-p (p denotes polyol synthesis). Moreover, adopting a co-precipitation method,<sup>61</sup> 90 wt% Cu and Zn nitrates were reduced together with aqueous Na<sub>2</sub>CO<sub>3</sub>, dried, and calcined at 350 °C to obtain (iv) the 90Cu/ZnO-c catalyst (c denotes co-precipitation). (v) Cu/ZnO-i and (vi) Pd/ZnO-i were prepared by

wet impregnation (denoted by i). In the following, for simplicity %loading refers to wt%.

In order to determine the morphology, elemental composition, and metal-support interactions of the prepared catalysts, HRTEM, EDX, and EELS mapping were employed. CuPd/ZnO-r was examined after H<sub>2</sub> pretreatment (Fig. 1B) and after CO<sub>2</sub> hydrogenation, as shown in Fig. 1C and S1.† A notable aspect (EDX mapping in Fig. 1C) is the segregation of Cu and Pd within the NPs. Two potential reasons may account for CuPd/ZnO-r possessing a core-shell structure, formed during synthesis. As



**Fig. 1** (A) Schematics elaborating the synthesis of nanocatalysts through different methods, mainly (i) 5%Cu/Pd (3 : 2) over ZnO or (ii) graphene through the liquid reduction method, (iii) Pd<sup>2+</sup> and Cu<sup>2+</sup> reduction with ethylene glycol, stabilization with 1-hexadecylamine and deposition on ZnO to obtain CuPd/ZnO-p, and (iv) 90% Cu with Zn nitrates, reduced with aqueous Na<sub>2</sub>CO<sub>3</sub> to produce 90Cu/ZnO-c (for the details of synthesis see the Experimental section), (B) HRTEM image of the bimetallic CuPd/ZnO-r catalysts, (C) corresponding EDX mapping showing the distribution of 'Pd', 'Cu' and 'O' atoms in CuPd/ZnO-r, (D) HRTEM image of the CuPd/Gr-r catalysts, (E) EDX mapping showing the distribution of 'C', 'Pd', and 'Cu' atoms in CuPd/Gr-r and (F) HRTEM image of the 90Cu/ZnO-c catalysts, also showing the interplanar spacing of Cu ( $d = 0.256$  nm) and ZnO ( $d = 0.277$  nm).



shown in Fig. 1A, CuPd/ZnO-r is formed through the direct deposition of Pd *via* a redox reaction, with Cu/ZnO already in place while Pd coats the Cu, resulting in the development of layered NPs. Second, the layered structure may arise from reaction conditions, as CO can displace (mobilize) Cu atoms,<sup>33,62</sup> while the strong binding of CO to Pd drives its surface segregation. Given the layered morphology of the NP, the Cu : Pd ratio does not correspond to a specific phase. The line scan of a NP after CO hydrogenation (Fig. S2†) confirmed that Cu is predominantly present in the core, while Pd is mainly located on the outer shell, which is also consistent with CuPd/ZnO-r observed after CO<sub>2</sub> hydrogenation (Fig. S1†). Furthermore, the concentration of Zn within the particle increases in the vicinity of the ZnO support. Since there is no concurrent increase in oxygen within the particle, it suggests that Zn interacts with the particle, forming an interface alloy between the particle and support.

The bimetallic CuPd/ZnO-p catalyst was examined both before (Fig. S3†) and after CO<sub>2</sub> hydrogenation (Fig. S4†). The EDX maps in Fig. S3† suggest that the NPs were CuPd alloys, with Fig. S4† showing a nearly uniform distribution of Cu and Pd within the NPs. No metallic Zn was detected in the NPs, although XRD detected PdZn alloys (see below).

A HRTEM image of the reduced CuPd/Gr-r catalyst is presented in Fig. 1D. By performing fast Fourier transformation (FFT) of a small image area encompassing the NP, the lattice distance was determined. This analysis was conducted for four different NPs, yielding the results listed in Table S1.† The percentage of Cu was calculated using Vegard's rule, which assumes that an arbitrary mixture of two components (such as Cu and Pd) has the same face-centered cubic (fcc) crystal structure. Based on the lattice constant of Cu of 0.361 nm and that of Pd of 0.389 nm, successful incorporation of Cu into the Pd lattice can be assumed. Additionally, EDX analysis was applied for determining the elemental composition (Fig. 1E). EDX phase mapping clearly shows that the NPs mainly consist of Cu and Pd as assumed for Vegard's rule. The accompanying EDX plot (Fig. S5†) shows the quantification spectra of the NPs, with results listed in Table S2.† Similar to the results obtained *via* Vegard's rule, no discernible trend regarding the NP composition (Cu/Pd) ratio was observed.

In addition to EDX mapping, EDX line scans of the CuPd/Gr-r catalyst were acquired, depicted in Fig. S6.† Notably, the NP in the central image exhibited a much lower Pd percentage than the other NPs. In the left image, an apparent increase in carbon content inside the NP was observed nearer to the support. Given that the inclusion of carbon inside the NPs is unlikely, the signal rather originates from the graphene support under the NP. The line scan in the right image traverses two NPs, with Cu found between them, but no Pd. This suggests that sintering is initiated by the movement of Cu atoms,<sup>33</sup> leading to coalescence on the graphene support.

The catalyst obtained *via* the co-precipitation method, with 90% Cu over ZnO (90Cu/ZnO-c), exhibited an average particle size of 12 nm (Fig. 1F), with NPs uniformly dispersed. The interplanar spacing of Cu was  $d = 0.256$  nm, while for ZnO it was  $d = 0.277$  nm. The lattice constant of fcc Cu is 0.361 nm,

while ZnO exhibits a hexagonal crystal structure, with lattice parameters  $a = 0.32496$  nm and  $c = 0.52042$  nm. This confirms the assignment of the interplanar spacings and lattice structures to Cu and ZnO.

Similarly, the catalysts with low Cu or Pd loading (5%) over ZnO, obtained through a one pot wet-impregnation method, were also analyzed. The Cu/ZnO-i catalyst after reduction in H<sub>2</sub> showed a single Cu NP on ZnO (Fig. S7†). Benefitting from the high resolution, lattice planes were analyzed for phase identification, *i.e.* in the red square an FFT was generated. After inverse FFT, the image revealed individual lattice planes without interference from background signals. The distance between lattice planes was measured to be 0.251 nm. Fig. S7† illustrates the unit cell of Cu, focusing on (1 1 0) lattice planes marked in purple, where the distance between two Cu atoms was measured as  $d(\text{Cu-Cu}) = 0.25$  nm, as observed in the HRTEM image.

Additionally, Fig. S8† depicts a high-angle annular dark-field scanning transmission electron (HAADF-STEM) micrograph of the Pd/ZnO-i catalyst after H<sub>2</sub> reduction at 500 °C. Variations in intensity in HAADF images are attributed to differences in sample thickness or the atomic number. The red box surrounding the NP on the surface of the ZnO support (Fig. S8†) was chosen for EDX analysis revealing reduced Pd and Zn, with an overall composition of 46.6 at% Pd and 53.4 at% Zn.

Fig. S9 and S10† reveal the effect of high pressure (20 bar) and temperature (500 °C) on NP size in the course of the hydrogenation reaction. Bimetallic NPs (CuPd) showed significantly more sintering on graphene, increasing in size from 8.7 nm to 20 nm, than when supported on ZnO, for which the NP size only increased from 8.4 nm to 11 nm. In contrast, monometallic NPs of both Cu and Pd on ZnO even exhibited a slight reduction in size, likely due to CO-induced redispersion (Fig. S9†).

Fig. 2A and S11–S13† display the (area-averaged) X-ray diffraction (XRD) patterns of the as-prepared (calcined) and H<sub>2</sub>-reduced catalysts. For the CuPd/ZnO-r catalyst in the calcined state, CuO was identified, with no mixed CuPd oxide detected. Due to the small size of the metal particles, the Bragg peaks appear broader and blend into the background noise. Pd exhibits a higher affinity towards Zn, as a separate PdZn (1 1 1, 2 0 0) phase was detected after H<sub>2</sub> reduction at 500 °C, still with no signs of a CuPd alloy. This suggests that in CuPd/ZnO, Cu and Pd separate, also forming PdZn interfaces, in line with the locally resolved HRTEM studies (see Fig. 1B). The CuPd/ZnO-p catalyst showed similar XRD patterns before and after H<sub>2</sub> reduction, with peaks related to PdZn being less intense than the ones for CuPd/ZnO-r. Conversely, the CuPd/Gr-r catalyst (Fig. S11†) after H<sub>2</sub> reduction exhibited dominant diffraction from graphitic carbon (0 0 2), because of graphene calcination at elevated temperatures, in line with literature reports.<sup>63,64</sup> Furthermore, the XRD patterns of the Cu/ZnO-i and Pd/ZnO-i catalysts (Fig. S12 and S13†) after pretreatment in H<sub>2</sub> at different temperatures confirmed that PdO was reduced at 200 °C, while CuO reduction occurred at a higher temperature of 300 °C.



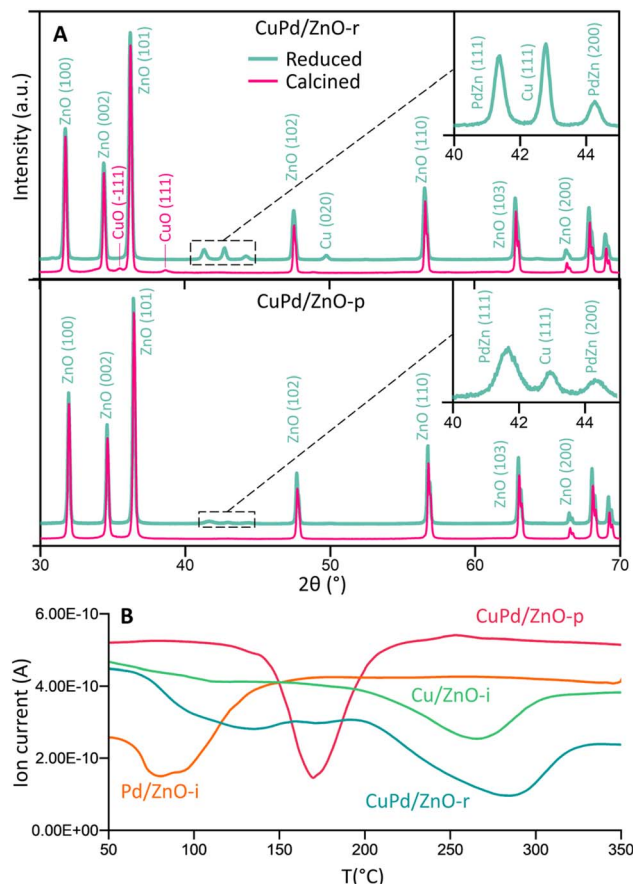


Fig. 2 (A) Crystal structure of calcined (500 °C) and  $\text{H}_2$ -reduced CuPd/ZnO-r and CuPd/ZnO-p catalysts. The crystal structure of other catalysts can be seen in Fig. S9–S11.† (B)  $\text{H}_2$ -temperature programmed reduction (TPR) profile of calcined (500 °C) CuPd/ZnO-r, CuPd/ZnO-p, Cu/ZnO-i and Pd/ZnO-i catalysts.

Temperature-programmed reduction (TPR) studies were thus carried out to monitor the  $\text{H}_2$ -induced reduction behaviour of the (calcined) catalysts in more detail (10%  $\text{H}_2$  in Ar). The mass spectrometer (MS) signals of  $\text{H}_2$  ( $m/z = 2$ ) were plotted against temperature, as shown in Fig. 2B and S14.† Pd/ZnO-i exhibited  $\text{H}_2$  consumption starting at a minimum temperature of 80 °C, while Cu/ZnO-i was reduced at 270 °C. In contrast, CuPd/ZnO-r and CuPd/ZnO-p displayed distinctly different profiles. For CuPd/ZnO-r, the minimum of Pd was slightly shifted to higher temperature (130 °C), while the minimum for Cu was at 290 °C. This again suggests that CuPd/ZnO-r consists of somewhat separate, but still connected Cu and Pd, likely within the NPs. The CuPd/ZnO-p profile exhibited only a single minimum at 170 °C, indicating the presence of alloyed CuPd NPs.

To evaluate the binding strength and distribution of  $\text{H}_2$  adsorption sites, hydrogen-temperature programmed desorption ( $\text{H}_2$ -TPD) was performed, which also shed light on metal-support interactions.  $\text{H}_2$ -TPD was performed for both catalysts (Cu and Pd/ZnO-i) for each reduction temperature ( $T_{200}$ ,  $T_{300}$ , and  $T_{500^\circ\text{C}}$ ). In Fig. 3A, the  $\text{H}_2$  desorption profile of the Cu/ZnO-i catalysts revealed desorption maxima at 390 and 393 °C for 200

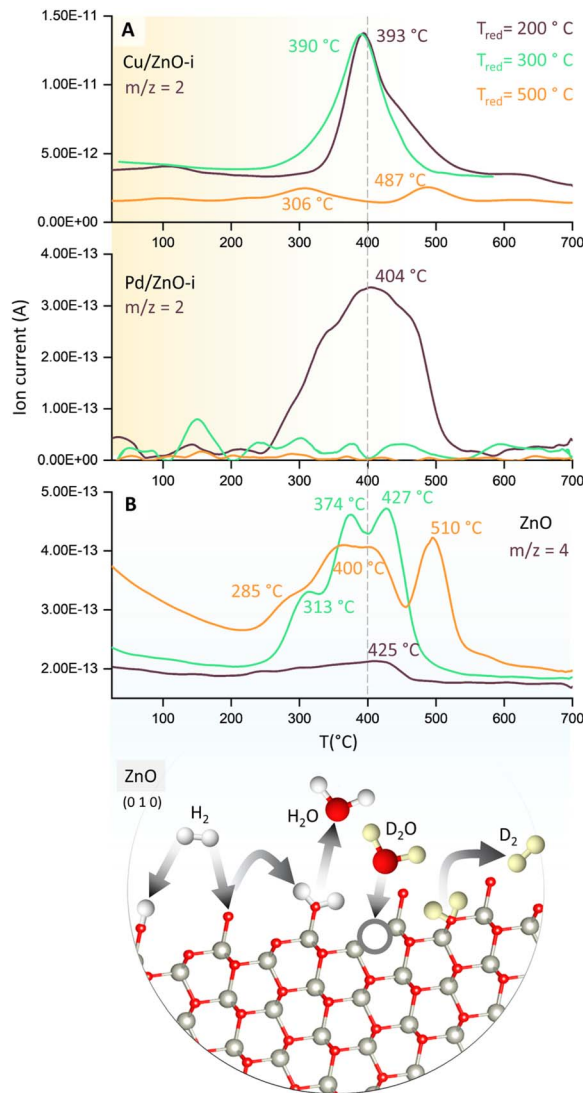


Fig. 3 Temperature programmed desorption (TPD) studies of catalysts. (A)  $\text{H}_2$ -TPD of Cu/ZnO-i and Pd/ZnO-i for different reduction temperatures with  $m/z = 2$  recorded and (B)  $\text{D}_2\text{O}$ -TPD of Cu/ZnO-i for different reduction temperatures with  $m/z = 4$  recorded. Structure of ZnO with possible reaction pathways of  $\text{H}_2$  and  $\text{D}_2(\text{O})$  on the ZnO surface.<sup>65</sup>

and 300 °C reduction temperatures, respectively. In contrast, the Cu/ZnO-i catalyst reduced at 500 °C did not exhibit a clear desorption peak, potentially due to the high-temperature reduction process leading to the formation of a CuZn alloy or sintering, which weakens the chemical bonding of  $\text{H}_2$  on the catalyst surface. Similarly, at higher reduction temperatures ( $T_{300}$  and  $T_{500^\circ\text{C}}$ ), the Pd/ZnO-i catalysts did not display the desorption maximum observed after  $T_{200^\circ\text{C}}$  (Fig. 3A) anymore. This again suggests that Pd can rather easily form an alloy with Zn at temperatures exceeding 200 °C.<sup>66–68</sup> Metallic Pd can absorb hydrogen into the NPs, which ceases upon forming a PdZn alloy. Analogously, previous studies with Pd–Pb alloys indicated a decreasing intensity of  $\text{H}_2$  desorption upon addition of Pb.<sup>69</sup> For the calculation of the binding energy of molecules on the catalyst's surface, the Redhead approximation was applied.<sup>70</sup>

The energy of desorption ( $E_{\text{des}}$ ) for Cu/ZnO-i was  $E_{\text{des}} = 169 \text{ kJ mol}^{-1}$  at  $T_{\text{max}} = 390 \text{ }^{\circ}\text{C}$ , while for Pd/ZnO-i, it was  $E_{\text{des}} = 174 \text{ kJ mol}^{-1}$  at  $T_{\text{max}} = 410 \text{ }^{\circ}\text{C}$ .

Furthermore, to detect surface defects in the ZnO support,<sup>71</sup> TPD was performed with deuterium oxide ( $\text{D}_2\text{O}$ -TPD). The desorption behaviour of  $\text{D}_2$  from  $\text{D}_2\text{O}$  adsorbed on the catalyst surface is indicative of the nature and density of surface defects or oxygen vacancies.<sup>72</sup> Specifically, the desorption temperature and intensity of  $\text{D}_2$  desorption peaks can reveal the availability and accessibility of surface defect sites. Higher desorption temperatures and/or broader desorption peaks may suggest stronger interactions between  $\text{D}_2\text{O}$  and defects, indicating vacancies in the ZnO support, which can influence the  $\text{CO}_2$  and CO hydrogenation reactions.<sup>73</sup>

In Fig. 3B,  $\text{D}_2$  desorption from the ZnO surface is displayed. After catalyst reduction at  $200 \text{ }^{\circ}\text{C}$  and  $\text{D}_2\text{O}$  dosing, only weak  $\text{D}_2$  desorption was observed. However,  $\text{D}_2$  desorption peaks were clearly visible for reduction at  $300$  and  $500 \text{ }^{\circ}\text{C}$ , with peak maxima ranging from  $313$  to  $427 \text{ }^{\circ}\text{C}$  and  $285$  to  $510 \text{ }^{\circ}\text{C}$ , respectively. A desorption peak at approximately  $370 \text{ }^{\circ}\text{C}$  is evident for every reduction temperature. Fig. 3B also illustrates potential processes involving the interaction of  $\text{H}_2$  and  $\text{H}_2\text{O}$ , or

$\text{D}_2$  and  $\text{D}_2\text{O}$ , with O vacancies on the ZnO surface. Due to the interaction of  $\text{D}_2\text{O}$  with the surface defects of ZnO, oxygen vacancies can be re-filled and  $\text{D}_2$  formed ( $m/z = 4$ ). The literature also reported the observations of surface defects in hydrothermally grown ZnO after exposure to  $\text{D}_2$  gas at elevated temperatures.<sup>74</sup>

### $\text{CO}_2$ and CO hydrogenation to methane or methanol

We then determined the  $\text{CO}_2$  hydrogenation performance of the various catalysts (Fig. 4A) at  $20 \text{ bar}$  pressure and temperatures from  $300$  to  $500 \text{ }^{\circ}\text{C}$ , including CuPd/ZnO-r, CuPd/ZnO-p, CuPd/Gr-r, 90Cu/ZnO-c, Cu/ZnO-i, and Pd/ZnO-i. Prior to each measurement, the catalysts were reduced in a hydrogen flow. The reaction mixture consisted of  $5\% \text{ CO}_2$  and  $20\% \text{ H}_2$  in helium.  $\text{CO}_2$  conversion increased with temperature, rising from about  $5\%$  at  $300 \text{ }^{\circ}\text{C}$  to  $>30\%$  at  $500 \text{ }^{\circ}\text{C}$ . Notably, for the bimetallic catalysts,  $\text{CO}_2$  conversion was at least  $3\%$  higher across all measured temperatures. CO and  $\text{CH}_4$  were detected as the main products of  $\text{CO}_2$  hydrogenation, with the CO yield increasing linearly with temperature, reaching  $20\%$  at  $500 \text{ }^{\circ}\text{C}$ . For both CuPd/ZnO-r and CuPd/ZnO-p, a significant increase was also observed in  $\text{CH}_4$  yield (from  $5.8\%$  to  $13\%$ ) as the

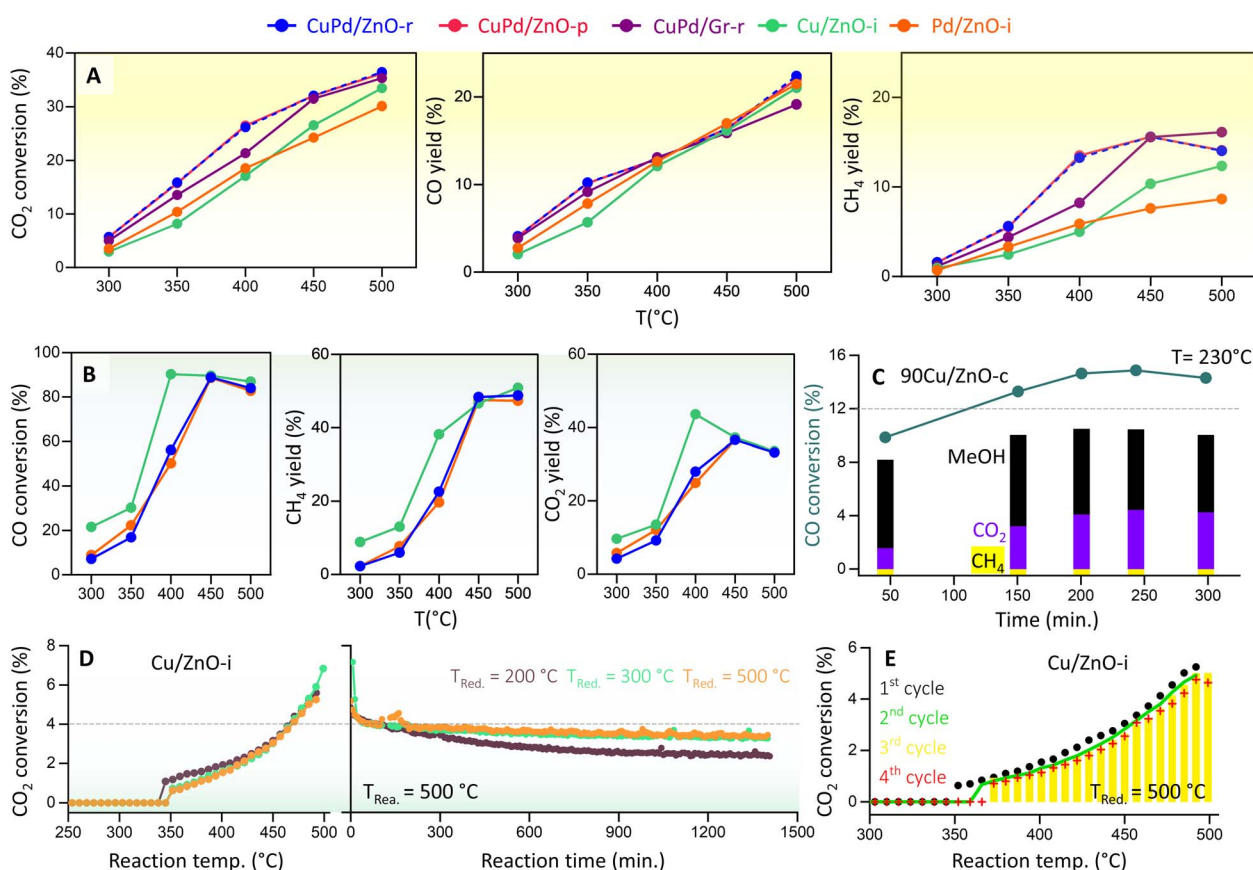


Fig. 4 Kinetic measurements of  $\text{CO}_2$  and CO hydrogenation. (A) Catalytic performance of CuPd/ZnO-r, CuPd/ZnO-p, CuPd/Gr-r, Cu/ZnO-i, and Pd/ZnO-i catalysts in terms of  $\text{CO}_2$  conversion and CO and  $\text{CH}_4$  yields at  $p = 20 \text{ bar}$  and  $T = 300\text{--}500 \text{ }^{\circ}\text{C}$ , and (B) CO conversion and  $\text{CH}_4$  and  $\text{CO}_2$  yields for CuPd/ZnO-r, Cu/ZnO-i, and Pd/ZnO-i at  $p = 20 \text{ bar}$  and  $T = 300\text{--}500 \text{ }^{\circ}\text{C}$ . (C)  $\text{CO}_2$  hydrogenation to MeOH (%) and  $\text{CO}_2$  (%) by 90Cu/ZnO-c catalysts at  $p = 20 \text{ bar}$  and  $T = 230 \text{ }^{\circ}\text{C}$  (for  $\text{CO}_2$  hydrogenation, see Fig. S15†), (D)  $\text{CO}_2$  conversion (%) to CO by Cu/ZnO-i catalysts reduced at different temperatures, at  $p = 1 \text{ bar}$  and  $T = 300\text{--}500 \text{ }^{\circ}\text{C}$ , and “reaction time” refers to the time on stream under constant conditions (for the Pd/ZnO-i catalyst, see Fig. S17†), and (E)  $\text{CO}_2$  conversion (%) to CO over multiple cycles (for the Cu/ZnO-i catalyst reduced at  $500 \text{ }^{\circ}\text{C}$ ).

temperature increased from 350 to 400 °C. At 500 °C, CuPd/ZnO-r exhibited the highest CH<sub>4</sub> yield (16%) as compared to CuPd/ZnO-p and CuPd/Gr, which both yielded 14%. The monometallic Cu/ZnO-i had a CH<sub>4</sub> yield of 12%, while Pd/ZnO-i showed the lowest yield of 8%.

Very differently, the catalyst containing 90 wt% Cu (90Cu/ZnO-c), prepared by co-precipitation and tested at 230 °C, exhibited selectivity towards MeOH rather than CH<sub>4</sub> (Fig. S15†). Despite a CO<sub>2</sub> conversion of 5.5%, the MeOH yield remained constant over time, with little CH<sub>4</sub> detected. Overall, the CO yield was 4%, while MeOH was recorded at 2%. A similar trend had been observed in previous studies, demonstrating improved MeOH selectivity/yield upon high Cu loading on ZnO<sup>10,75</sup> and observation of a volcano-like pattern in MeOH selectivity with respect to the Cu NP size.<sup>76</sup>

Furthermore, as RWGS may be followed by CO hydrogenation, the latter reaction was evaluated on Cu/ZnO-i, Pd/ZnO-i, and CuPd/ZnO-r under conditions similar to those of CO<sub>2</sub> hydrogenation, and only 5% CO was used instead of CO<sub>2</sub> (Fig. 4B). Notably, from 400 to 500 °C, CO conversion was at least 40% higher than CO<sub>2</sub> conversion. CH<sub>4</sub> (from methanation) and CO<sub>2</sub> (from WGS) were identified as the main products of CO hydrogenation, with the CO<sub>2</sub> yield increasing linearly with temperature, peaking at 37% at 450 °C and then dropping to 33% at 500 °C. The CH<sub>4</sub> yield reached its highest level of 48% at 450 °C and remained steady up to 500 °C. No significant differences were observed between monometallic or bimetallic catalysts for CO hydrogenation. Nevertheless, ethane (from FT) was detected as a side product ( $\approx$ 4%) at 400 °C (Fig. S16†). Interestingly, the 90Cu/ZnO-c catalyst showed a higher CO conversion of 14%, with a MeOH yield of 10% and a CO<sub>2</sub> yield of 4.3% at 230 °C (Fig. 4C). Overall, the MeOH yield remained constant at 8–10% over 300 minutes. This further confirmed that a CO/H<sub>2</sub> gas feed increases the MeOH yield ( $\text{CO} + 2\text{H}_2 \rightarrow \text{CH}_3\text{OH}$ ).<sup>20,41</sup> Indeed, for the best performance, a mixture of CO<sub>2</sub>/CO/H<sub>2</sub> (5%/20%/75%) is known to be required.<sup>77</sup> The conducted experiments confirm that the hydrogenation of CO yields more CH<sub>4</sub> or MeOH than CO<sub>2</sub> hydrogenation. Thus, for MeOH production at the industrial level using Cu/ZnO-based catalysts, CO serves as the major feed gas (20%) alongside CO<sub>2</sub> and H<sub>2</sub>.<sup>14</sup>

The catalytic performance of the best performing catalysts was further described by calculating the space-time yield (STY) (more details in the ESI†), which includes the amount of the catalyst (0.1 g) used during the reaction:

- For CO<sub>2</sub> hydrogenation to CH<sub>3</sub>OH over 90Cu/ZnO-c, the STY was 0.0836 g<sub>MeOH</sub> g<sub>cat</sub><sup>-1</sup> h<sup>-1</sup>, and for CO hydrogenation, its STY was 0.4811 g<sub>MeOH</sub> g<sub>cat</sub><sup>-1</sup> h<sup>-1</sup>.
- For CO<sub>2</sub> hydrogenation to CH<sub>4</sub>, CuPd/Gr-r showed the best performance with a STY of 0.2416 g<sub>CH<sub>4</sub></sub> g<sub>cat</sub><sup>-1</sup> h<sup>-1</sup>, while for CO hydrogenation, Cu-ZnO-i exhibited the best STY of 0.7618 g<sub>CH<sub>4</sub></sub> g<sub>cat</sub><sup>-1</sup> h<sup>-1</sup>.

A CuO/ZnO catalyst obtained through an ammonia-evaporation-induced synthetic method involving the impregnation of filament-like ZnO for CO<sub>2</sub> hydrogenation at 3 bars showed the best performance, with a MeOH STY of 0.55 g<sub>MeOH</sub> g<sub>cat</sub><sup>-1</sup> h<sup>-1</sup> and a selectivity of 78.2%.<sup>78</sup> Moreover, Han *et al.*<sup>79</sup> observed that doping Cu/ZnO catalysts with Pd, Pt, and Ru led

to the formation of electron-rich Cu sites due to partial electron transfer, greatly enhancing CO<sub>2</sub> activation. The Pd-doped catalyst demonstrated the highest MeOH STY of 0.52 g<sub>MeOH</sub> g<sub>cat</sub><sup>-1</sup> h<sup>-1</sup> with 100 hours of stability. In contrast, over a Cu<sub>0.5</sub>Ni<sub>0.5</sub>/γ-Al<sub>2</sub>O<sub>3</sub> catalyst at 5 bar pressure, Reddy *et al.*<sup>80</sup> reported CO<sub>2</sub> conversion not exceeding 30% to CO. During the reaction, the Cu core atoms migrated toward the surface, resulting in the restructuring of the Cu@Ni core-shell structure to a Cu-Ni alloy, which functioned as the active site by enhancing CO desorption.

To examine the effect of pressure, CO<sub>2</sub> hydrogenation was also studied at atmospheric pressure (1 bar) from 250 to 500 °C, using Cu/ZnO-i or Pd/ZnO-i catalysts, pre-reduced at different temperatures ( $T_{\text{red}} = 200, 300$ , and 500 °C) (Fig. 4D). CO was the primary product of both catalysts. The CO<sub>2</sub> conversion of Pd/ZnO-i was 11% higher than that of Cu/ZnO-i for every reduction temperature. A reaction temperature of about 300 °C was necessary for CO formation with the Pd/ZnO-i catalyst, whereas with Cu/ZnO-i amounts of CO were first detected at 380 °C. According to the literature,<sup>81–84</sup> the reaction mechanism involves the adsorption of CO<sub>2</sub> on the ZnO-supported Cu or Pd catalysts, leading to intermediate-carbonate formation.

To evaluate the catalysts' stability, a 24 hour reaction was carried out at 500 °C. Each catalyst underwent reduction pretreatment at 200, 300, or 500 °C before the long-term reaction. The Cu/ZnO-i catalyst reduced at 200 °C exhibited more pronounced deactivation than those pre-reduced at 300 or 500 °C (Fig. 4D). It appears that reduction at 200 °C was insufficient, with CuO still being present. During the reaction, the partly reduced sample was subjected to 500 °C and a gas flow of 20 vol% H<sub>2</sub>, leading to sintering of the remaining CuO NPs and final reduction to metallic Cu. The Cu/ZnO-i catalysts reduced at 300 and 500 °C displayed almost constant CO<sub>2</sub> conversion to CO over the 24 hour reaction period (Fig. 4D). In contrast, the Pd/ZnO-i catalyst exhibited some CO<sub>2</sub> conversion to CO at 200 °C, possibly due to metallic Pd already being present on the catalyst surface at this reduction temperature (Fig. S15†). The increase in reduction temperature resulted in surface alloy formation,<sup>55,85</sup> as indicated by the presence of a PdZn alloy in XRD (Fig. S11†). Additionally, cyclic and long-term reactions demonstrated the stability of both catalysts, with no signs of decreasing CO<sub>2</sub> conversion observed over multiple reaction cycles or for lower reduction temperatures (Fig. 4E and S17†).

For MeOH production over Cu/ZnO catalysts, a formate pathway has been proposed in the literature.<sup>86</sup> A DFT study by Grabow and Mavrikakis<sup>87</sup> demonstrated that CO<sub>2</sub> hydrogenation over Cu/ZnO occurs *via* the formate pathway ( $\text{CO}_2^* \rightarrow \text{HCOO}^* \rightarrow \text{HCOOH}^* \rightarrow \text{CH}_3\text{O}_2^* \rightarrow \text{CH}_2\text{O}^* \rightarrow \text{CH}_3\text{O}^* \rightarrow \text{CH}_3\text{OH}^*$ ). Meanwhile, MeOH production from CO follows the sequence  $\text{CO}^* \rightarrow \text{HCO}^* \rightarrow \text{CH}_2\text{O}^* \rightarrow \text{CH}_3\text{O}^* \rightarrow \text{CH}_3\text{OH}^*$ . Nevertheless, it is well documented in the literature that methanation, particularly over Pd-based bimetallic catalysts (*e.g.*, CuPd), can follow either the formate or the reverse-water gas shift (RWGS) pathway.<sup>88</sup> Future studies employing *in situ* or *operando* techniques may provide confirmation of these intermediates, although the mechanism is still controversially discussed.<sup>84</sup>



## Conclusions

Not unexpectedly, the hydrogenation of CO<sub>2</sub> or CO to CH<sub>4</sub> and/or MeOH with catalysts of Cu, Pd, and PdCu NPs supported on ZnO or graphene has shown promise for reducing CO<sub>2</sub> emissions. Through comprehensive characterization involving various techniques such as HRTEM, EDX, HAADF-STEM, XRD, H<sub>2</sub>-TPR, H<sub>2</sub>-TPD, and D<sub>2</sub>O-TPD, as well as CO<sub>2</sub>/CO hydrogenation kinetics, it was observed that lower Cu or Pd loadings (5%) supported on ZnO or graphene favored CH<sub>4</sub> production from 300 to 500 °C and 20 bar pressure. CO was the major byproduct, indicating the occurrence of the reverse water gas shift (RWGS) reaction. The addition of the noble metal Pd to Cu had only a minor effect on performance. In contrast, higher Cu content (90%) strongly increased MeOH production in both CO<sub>2</sub> and CO hydrogenation at high pressure (20 bar).

CO<sub>2</sub> hydrogenation at ambient pressure (1 bar) and high temperature (300–500 °C) on both Cu and Pd on ZnO produced CO as the major product, corroborating that high pressure is essential for CH<sub>4</sub>/MeOH production.

For CO hydrogenation at 400 to 500 °C, CO conversion was at least 40% higher than CO<sub>2</sub> conversion, with CH<sub>4</sub> and CO<sub>2</sub> identified as the main products. Again, utilizing 90% Cu supported on ZnO led to an enhanced CO conversion of 14%, with a MeOH yield reaching 10% and a CO<sub>2</sub> yield reaching 4.3% at 230 °C.

The findings underline the significance of catalyst (NP) composition, affected by the corresponding synthesis methodologies, for optimizing CO<sub>2</sub> and CO hydrogenation processes for efficient methane or methanol production. This offers useful insights for advancing sustainable energy solutions.

## Experimental

### Synthesis of catalysts

The bimetallic catalysts were synthesized employing two distinct methods. For the first method (Fig. 1A), Cu was initially deposited on the support, followed by the addition of palladium salt to initiate a redox reaction and form alloyed NPs. The synthesis was conducted on both ZnO powder and graphene, with a total metal loading of 5 wt% and a Pd/Cu ratio of 2 : 3. Copper acetate monohydrate (0.19 g) was dissolved in distilled water under stirring, followed by the addition of 1.90 g ZnO (or graphene nanoplatelets), and the suspension was stirred overnight. The mixture was then heated to 130 °C to evaporate the water, and the solid was dried for 2 hours at 120 °C. Subsequently, the catalyst was calcined at 500 °C for 2 hours in air and then reduced with H<sub>2</sub> at 350 °C for 2 hours. In a separate step, a solution of palladium acetate in water was prepared, and the reduced copper catalyst was added to the solution under a flow of nitrogen. After evaporating the water and drying, the catalyst was calcined at 500 °C for 2 hours before reduction in the reactor prior to kinetic measurements. The prepared catalysts are named “CuPd/ZnO-r” and “CuPd/Gr-r”.

In the second method (Fig. 1A), 1-hexadecylamine (HDA) capped Pd–Cu nanoparticles were synthesized and then dissolved in toluene for impregnation on ZnO. The metal loading

was 5 wt%, with a Pd : Cu ratio of 2 : 3. In a round-bottom flask equipped with a magnetic stirrer, refluxing device, and nitrogen purging source, 80 mL of ethylene glycol was cooled with an ice bath and degassed for ten minutes under a stream of nitrogen. Copper acetate hydrate (0.95 g) and palladium acetate (0.43 g) were added to the flask, followed by the addition of 4.8 g of HDA to the ethylene glycol solution kept in the ice bath. The mixture was heated to 60 °C until HDA dissolved, resulting in a color change from blue to green. The solution was then heated to 160 °C and maintained at this temperature overnight. The color of the solution changed from deep blue/violet to green, then blue, and finally black, with a red layer, likely Cu<sub>2</sub>O, deposited on the inner wall of the flask. After cooling to room temperature, black NPs were separated by centrifugation and washed three times with ethanol to remove excess HDA and ethylene glycol. The NPs were dried overnight, resulting in a yield of approximately 58.7%. Subsequently, the nanoparticles were deposited on ZnO. The required amount of NPs for a metal loading of 5 wt% was calculated, and 0.1 g of NPs was suspended in toluene with 1.89 g of ZnO. After removing all toluene under vigorous stirring at about 150 °C, the precipitate was dried overnight at 125 °C, followed by calcination in air at 500 °C for 2 hours to completely remove HDA. The reduction of metal oxides was performed in the reactor before conducting kinetic measurements. The resulting catalyst weighed 1.77 g, representing a yield of 88.5%, named “CuPd/ZnO-p”.

Using a co-precipitation method,<sup>61</sup> copper nitrate (90%) and Zn nitrates (10%) were reduced with aqueous Na<sub>2</sub>CO<sub>3</sub>, dried, and calcined at 350 °C to obtain the “90Cu/ZnO-c” catalyst (Fig. 1A).

The monometallic Cu and Pd catalysts were prepared *via* the wet-impregnation (“-i”) method of a ZnO support. Each catalyst was synthesized by weighing 0.32 g of copper acetate monohydrate or 0.21 g of palladium acetate. The metal salt was then suspended in 30 mL toluene in a flask, ensuring complete dissolution by adding a few drops of ethanol. Subsequently, 1.90 g of ZnO powder was added, and the suspension was stirred overnight at room temperature. The solvent was evaporated by heating the mixture to 150 °C, and the resulting solid was dried for 2 hours in an oven at 120 °C. The calcination of the catalysts was performed in air at 500 °C for 2 hours, using a heating rate of 10 °C min<sup>-1</sup>. This calcination step was essential for removing the acetate from the catalyst and converting the metals into oxides. Prior to kinetic measurements, the catalysts underwent reduction in the reactor. The reduction was carried out using a 10 vol% hydrogen/He flow at three different temperatures: 200 °C, 300 °C, and 500 °C. The prepared catalysts were named “Cu/ZnO-i” and “Pd/ZnO-i”.

### Characterization of catalysts

The morphology and crystal structure of the catalysts were analyzed using an FEI TECNAI G2 F20™ at the University Service Center for Transmission Electron Microscopy (USTEM) at TU Wien. The microscope was equipped with a field emission gun (X-FEG) operated at an acceleration voltage of 200 kV. Additionally, an energy dispersive X-ray (EDX) silicon drift



detector (SSD) (EDAX Apollo XLT SSD™) was incorporated into the TEM. Catalyst samples were loaded onto a carbon-coated Cu grid and then inserted into the TEM's inlet system using a single tilt holder. Various TEM images, including high-angle annular dark field (HAADF) and high-resolution (HR) TEM images, were recorded for each catalyst both before and after the reaction. Structural alterations during the reaction were discerned through image comparison, with the high resolution of HRTEM images allowing for precise measurement of lattice planes to identify different phases. Additionally, energy dispersive X-ray spectroscopy (EDX) and electron energy loss spectroscopy (EELS) measurements were conducted to investigate alloy formation. Particle size and distribution were analyzed using DigitalMicrograph software (Gatan™).

The XRD measurements were primarily carried out to elucidate the atomic structure of various crystalline phases (metals, alloys, and oxides). Diffractograms were acquired using a PANalytical X'Pert Pro™ Bragg–Brentano™ powder diffractometer at the X-ray Center of TU Wien. Cu K $\alpha$  with a wavelength of 1.54 Å served as the radiation source. A small amount of each catalyst (including calcined catalysts and those subjected to three different reduction temperatures) was applied to a silicon wafer (Si (1 1 1) layer) fixed to a sample holder. The position (2 $\theta$  angle) of the measured reflexes was compared with diffractograms from a database (COD Crystallography Open Database™) to identify crystalline phases. Rietveld refinement was employed to quantify the different compounds present in the diffractograms. This technique utilizes the least squares method to fit a theoretical line profile to the observed reflexes until a satisfactory match is achieved. Furthermore, Rietveld refinement facilitated the calculation of the crystallite size of both the support and the metal particles (using HighScore Plus 4.1 – PANalytical software™).

Temperature programmed reduction (TPR) served as a standard method for gathering insights into the reducibility of a material. The H<sub>2</sub> TPR analysis was conducted in a continuous fixed bed quartz tube reactor. Approximately 50 mg of catalyst was loaded into the reactor tube, which was then positioned in a heating furnace. Gas flows of argon and H<sub>2</sub> (the reducing gas) were carefully regulated using calibrated mass flow controllers. A total flow of 100 mL min<sup>−1</sup> with 10 vol% H<sub>2</sub> in Ar was passed through the sample. During the experiment, the furnace underwent heating from room temperature to 500 °C at a rate of 10 °C min<sup>−1</sup>. The quartz tube reactor was linked to a quadrupole mass spectrometer (Balzers Prisma™), which recorded the mass signals of H<sub>2</sub> ( $m/z$  = 2) and H<sub>2</sub>O ( $m/z$  = 18) over time as a function of temperature. These experiments were carried out for both synthesized catalysts and the pure ZnO support.

Temperature programmed desorption (TPD) provided insights into the binding energy of adsorbed molecules. The experiments were conducted within a solid quartz tube reactor in conjunction with a quadrupole mass spectrometer (Balzers Prisma™). Each catalyst, weighing 50 mg, was fixed with quartz wool and loaded into the reactor tube. To facilitate the adsorption of gas molecules on the surface, the catalyst was exposed to a gas mixture containing probe molecules such as H<sub>2</sub> or D<sub>2</sub>O (100 or 10 mbar gas pressure, respectively). The Redhead

approximation (eqn (1))<sup>70</sup> can be applied for calculating the binding energy of molecules on the catalyst's surface:

$$E_{\text{des}} = R \times T_{\text{max}} \times \left[ \ln \left( \frac{\nu \times T_{\text{max}}}{\beta} \right) - 3.46 \right] \quad (1)$$

$E_{\text{des}}$  is the activation energy of desorption,  $T_{\text{max}}$  is the temperature at the peak maximum,  $\beta$  is the heating rate (dT/dt),  $n$  is the order of desorption and  $\nu$  is the frequency factor.

In general, the Redhead equation is valid for first-order desorption (single step desorption). As an approximation, eqn (1) was used with a frequency factor of  $\nu = 10^{13} \text{ s}^{-1}$ .

Moreover, D<sub>2</sub>O TPD of ZnO was carried out after reduction at various temperatures, and  $m/z$  = 4 signals were recorded. This experiment provided insights into possible vacancies within the support. Due to the interaction of D<sub>2</sub>O with the surface defects of ZnO, D<sub>2</sub> was formed and detected by the mass spectrometer ( $m/z$  = 4). The same preparation and measurement steps as those used for H<sub>2</sub> TPD were applied, with a partial pressure of 10 mbar D<sub>2</sub>O utilized for adsorption.

## CO<sub>2</sub> and CO hydrogenation

The kinetic measurements were conducted using a PID Eng&Tech Microactivity Effi Reactor™, a 30 cm long stainless-steel tubular reactor with an internal diameter of 9.91 mm, in a temperature range of 25 to 800 °C and pressures up to 20 bar. Feed gases including H<sub>2</sub>, O<sub>2</sub>, CO, CO<sub>2</sub>, and He were introduced into the reactor, with flow rates regulated by calibrated mass flow controllers. Online product analysis was performed *via* a micro-GC system (Inficon™; 300 Micro GC, runtime < 2 min), equipped with a molecular sieve, a plotQ column™ and a Thermal Conductivity Detector (TCD). The molecular sieve effectively separated small molecules such as H<sub>2</sub>, O<sub>2</sub>, and N<sub>2</sub>, while the plotQ column facilitated the separation of carbon-containing compounds. Kinetic measurements were conducted for CO<sub>2</sub> and CO hydrogenation at 20 bar (or ambient pressure) and various temperatures ranging from 230 to 500 °C. Each temperature step was held constant for 8 hours, with average values taken for further calculations. This duration allowed the catalyst to reach a quasi-stationary state, minimizing the effects of transient behaviour. The total gas flow was maintained at 10 mL min<sup>−1</sup> (corresponding to a flow of  $6.81 \times 10^{-6} \text{ mol s}^{-1}$ ), comprising 5% CO<sub>2</sub> or CO and 20% H<sub>2</sub> in helium. Following each reaction period at a specific temperature, a reactivation treatment was applied. For this, the catalyst underwent oxidation with 10% O<sub>2</sub> in He at 500 °C to remove carbonaceous deposits, followed by reduction with 10% H<sub>2</sub> in He.

The TCD was calibrated prior to the experiments using standard gas mixtures to ensure accurate quantification of the detected species. Calibration curves were generated by plotting the peak areas against the known concentrations of the standards (CO<sub>2</sub>, CO, and H<sub>2</sub>, respectively). Linear regression was used to determine the relationship between the peak area and concentration. During the experiments, the peak areas corresponding to the different reactants and products were recorded. These peak areas were then used to determine the



concentrations of the molecules present. The calibrated peak areas from GC chromatograms were then utilized for the calculation of, *e.g.*, the conversion<sub>CO<sub>2</sub></sub> (%), as given in eqn (2),

$$\text{Conversion}_{\text{CO}_2}(\%) = \frac{A_{\text{CO}_2}^{\text{in}} - A_{\text{CO}_2}^{\text{out}}}{A_{\text{CO}_2}^{\text{in}}} \times 100 \quad (2)$$

where  $A_{\text{CO}_2}^{\text{in}}$  = peak area of CO<sub>2</sub> entering the reactor and  $A_{\text{CO}_2}^{\text{out}}$  = peak area of CO<sub>2</sub> exiting the reactor.

Analogously, for CO hydrogenation, the CO GC peak areas were utilized for the calculation of the CO conversion.

The selectivity of the catalysts for producing MeOH selectivity<sub>MeOH</sub> (%) was determined using eqn (3),

$$\text{Selectivity}_{\text{MeOH}}(\%) = \frac{A_{\text{MeOH}}}{A_{\text{MeOH}} + A_{\text{CH}_4} + A_{\text{CO}_2}} \times 100 \quad (3)$$

where  $A_{\text{MeOH}}$  = peak area of MeOH,  $A_{\text{CH}_4}$  = peak area of CH<sub>4</sub> and  $A_{\text{CO}_2}$  = peak area of CO<sub>2</sub>.

Similarly, the CH<sub>4</sub> selectivity<sub>CH<sub>4</sub></sub> (%) was determined using eqn (4)

$$\text{Selectivity}_{\text{CH}_4}(\%) = \frac{A_{\text{CH}_4}}{A_{\text{CH}_4} + A_{\text{MeOH}} + A_{\text{CO}_2}} \times 100 \quad (4)$$

With conversion (eqn (2)) and selectivity (eqn (3) or (4)), the yield of MeOH, CH<sub>4</sub>, or CO can be calculated using eqn (5)–(7),

$$\text{Yield}_{\text{MeOH}}(\%) = \frac{\text{Conversion}_{\text{CO}_2} \times \text{Selectivity}_{\text{MeOH}}}{100} \quad (5)$$

$$\text{Yield}_{\text{CH}_4}(\%) = \frac{\text{Conversion}_{\text{CO}_2} \times \text{Selectivity}_{\text{CH}_4}}{100} \quad (6)$$

$$\text{Yield}_{\text{CO}}(\%) = \frac{\text{Conversion}_{\text{CO}_2} \times \text{Selectivity}_{\text{CO}}}{100} \quad (7)$$

For CO hydrogenation, yields were calculated analogously.

For the Gas Hourly Space Velocity (GHSV), Residence Time ( $\tau$ ), and Space Time Yield (STY) calculations, refer to Note 1 of the ESI.†

## Data availability

The data supporting this article have been included as part of the ESI.†

## Author contributions

QM: conceptualization, methodology, validation, software, formal analysis, investigation, data curation, writing – original draft, and writing – review & editing. KD: conceptualization, methodology, validation, and formal analysis. JS: data curation and writing – review & editing. MH: methodology, validation, formal analysis, investigation, and writing – review & editing. KKL, TS, SL, AA, and JN: formal analysis, data curation, validation, and writing – review & editing. GR: conceptualization, validation, resources, writing – review & editing, and supervision.

## Conflicts of interest

There are no conflicts of interest to declare.

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