


 Cite this: *Energy Adv.*, 2024, 3, 1265

 Received 3rd April 2024,  
 Accepted 19th May 2024

DOI: 10.1039/d4ya00218k

[rsc.li/energy-advances](https://rsc.li/energy-advances)

# Electrochemical-catalytic NH<sub>3</sub> synthesis from H<sub>2</sub>O and N<sub>2</sub> using an electrochemical cell with a Ru catalyst, Pd–Ag membrane cathode, and NaOH–KOH molten salt electrolyte at 250 °C†

 Raisei Sagara, Rika Hayashi, Aika Hirata, Shintaroh Nagaishi and Jun Kubota \*

Using sustainable energy-based electricity to synthesize NH<sub>3</sub> from H<sub>2</sub>O and N<sub>2</sub> to release O<sub>2</sub> not only contributes to making chemical fertilizer production carbon neutral, but also holds promise for the use of NH<sub>3</sub> as a fuel. NH<sub>3</sub> synthesis from water and nitrogen was conducted at around 250 °C and below 1.0 MPa by combining a molten salt electrolyte of NaOH–KOH, a Pd alloy hydrogen-permeable membrane cathode, a Ni anode, and a Ru-based catalyst on the cathode backside. The rate and current efficiency for NH<sub>3</sub> formation were obtained as 11 nmol s<sup>-1</sup> cm<sup>-2</sup> (38 μmol h<sup>-1</sup> cm<sup>-2</sup>) and 25%, respectively, at 30 mA cm<sup>-2</sup>, 1.0 MPa, and 250 °C. It was confirmed that the remaining percentage from the 100% current efficiency for NH<sub>3</sub> production was attributed to the current efficiency for H<sub>2</sub> production. The cell voltage was as low as 1.47 V at 30 mA cm<sup>-2</sup> and increased to 1.95 V at 100 mA cm<sup>-2</sup>. The potential of this electrochemical system is discussed.

## Introduction

Ammonia (NH<sub>3</sub>) not only supports human food production as a synthetic fertilizer itself or as its raw materials, but also holds promise as a carbon-free fuel when obtained from renewable energy sources.<sup>1–3</sup> At present, the most reliable methods for obtaining large amounts of renewable energy involve using photovoltaics, solar thermal, wind power, *etc.*<sup>4</sup> However, in advanced countries, surplus electricity from these sources is already being generated, leading to situations where it is shut down.<sup>5,6</sup> It is important to convert this electricity into chemical energy carriers and store it for use at times and places when humans need it.<sup>7,8</sup> Therefore, a huge number of research studies have been conducted on electrochemical reduction of nitrogen to produce NH<sub>3</sub><sup>9–13</sup> and electrochemical reduction of CO<sub>2</sub> to produce hydrocarbons.<sup>14,15</sup>

However, while the electrochemical reduction of CO<sub>2</sub> to CO is approaching practical efficiency,<sup>14</sup> the production of NH<sub>3</sub> *via* electrochemical reduction of N<sub>2</sub><sup>16</sup> and the production of hydrocarbons or alcohols *via* electrochemical reduction of CO<sub>2</sub><sup>15</sup> are not considered to have reached practical levels due to low current efficiency and significant overpotentials. The most promising electrochemical method for obtaining ammonia is the lithium-mediated method, but the use of metallic lithium is expected to require a very large overpotential.<sup>16,17</sup>

It is possible to produce NH<sub>3</sub> from electricity by utilizing water electrolysis for hydrogen production and the conventional Haber–Bosch process.<sup>18</sup> This approach has been attempted since the early stages of NH<sub>3</sub> synthesis.<sup>18</sup> However, large-scale chemical plants like the Haber–Bosch process face challenges in operating under fluctuating conditions, making it difficult to integrate with highly variable sources of energy, such as solar and wind power. As a result, complex and expensive systems including hydrogen storage become necessary. If NH<sub>3</sub> could be directly obtained from water and nitrogen within a single electrochemical device, not only would the thermodynamic energy requirements be reduced, but also the system could be operated solely with easy start–stop controls, eliminating the need for hydrogen storage.

Our group has been addressing the synthesis of NH<sub>3</sub> from H<sub>2</sub>O and N<sub>2</sub> using phosphate-based electrolytes, a composite of CsH<sub>2</sub>PO<sub>4</sub> and SiP<sub>2</sub>O<sub>7</sub>, suitable for operation at temperatures between 200 and 250 °C.<sup>19,20</sup> In this temperature range, phosphate electrolytes are effective for synthesizing various molecules.<sup>21–25</sup> The distinguishing feature of our technology lies not in electrochemically reducing nitrogen, but in catalytically activating nitrogen, which is then hydrogenated by hydrogen obtained from water electrolysis.<sup>21</sup> Our goal is not to discover a new chemical phenomenon of direct electrochemical reduction of nitrogen as fundamental research, but to find out how to produce ammonia efficiently and easily from water and nitrogen using electricity. To achieve this, it is necessary to form a catalytic layer with two distinct functionalities: one portion exposed to the gas phase without being immersed in the electrolyte, and another portion

Department of Chemical Engineering, Fukuoka University, 8-19-1, Nanakuma, Jonan-ku, Fukuoka 814-0180, Japan. E-mail: [jkubota@fukuoka-u.ac.jp](mailto:jkubota@fukuoka-u.ac.jp)

† Electronic supplementary information (ESI) available. See DOI: <https://doi.org/10.1039/d4ya00218k>



that performs proton reduction in contact with the electrolyte. For this purpose, we devised an electrolysis cell with a Pd–Ag alloy hydrogen-permeable membrane interfacing with the electrolyte as the cathode, while a Ru-based catalyst for  $\text{NH}_3$  synthesis is placed on the backside of the Pd–Ag membrane.<sup>19,20</sup> The hydrogen-permeable membrane prevents the electrolyte from permeating into the Ru-based catalyst for  $\text{NH}_3$  synthesis, avoiding the absorption of the generated  $\text{NH}_3$  into the electrolyte and contamination of introduced steam into  $\text{NH}_3$ . Therefore, even unstable catalysts prone to dissolution when in contact with high-temperature electrolytes can be used reliably. Furthermore, mechanical support by the Pd–Ag alloy hydrogen-permeable membrane facilitates operation under pressure, up to 1.0 MPa. Even if spanning a two-step reaction pathway involving hydrogen formation and nitrogen hydrogenation, the production of  $\text{NH}_3$  and oxygen from water and nitrogen within a single-temperature electrochemical device maintains thermodynamic favorability similar to the electrochemical reduction of nitrogen.<sup>19,20</sup> In other words, the exothermic heat generated by the hydrogenation of  $\text{N}_2$  to form  $\text{NH}_3$  can be utilized for the endothermic process of water electrolysis. Furthermore, it offers practical advantages such as eliminating the need for hydrogen storage and simplifying device start–stop procedures. However, it has been noted that in systems operating at over  $60 \text{ mA cm}^{-2}$  with this  $\text{CsH}_2\text{PO}_4/\text{SiP}_2\text{O}_7$  electrolyte, the overpotential gradually increases, leading to degradation of the anode.<sup>20</sup>

Phosphate electrolytes have been studied with the expectation of being a practical electrolyte, given the commercialization of phosphoric acid fuel cells (PAFCs) operating at around  $200^\circ\text{C}$ .<sup>26,27</sup> However, large-scale water electrolysis predominantly utilizes alkaline water electrolysis (AWE) at temperatures below  $100^\circ\text{C}$ .<sup>28,29</sup> There is hope for the application of this electrolyte in  $\text{NH}_3$  synthesis by raising the temperature range to between  $200$  and  $250^\circ\text{C}$ .<sup>30–32</sup> NaOH and KOH form eutectic salts with a melting point of around  $160^\circ\text{C}$ , which allows them to be used as molten salt electrolytes at temperatures above  $200^\circ\text{C}$ .<sup>33–36</sup> With sufficient humidification, steam can undergo dissolution in the molten salt resembling a concentrated alkaline solution.<sup>33–36</sup> Phosphate electrolytes are in a semi-solid state at the operating temperatures, and while the usefulness of solid electrolytes is evident in fuel cells because the gas-phase network and three-phase interfaces for rapidly diffusing gaseous reactants to the electrode layer are crucial, their advantages seem not to be significant in water electrolysis. This is because the products are gaseous and are evolved as bubbles even in liquid electrolytes, and the superiority of solid electrolytes is not significant. Therefore, there is potential for liquid electrolytes such as molten salts as well. Unlike acidic ion exchange membranes used in proton exchange membrane electrolysis, alkaline electrolytes like NaOH–KOH allow for the use of non-noble metals such as Ni as electrode catalysts, which is another advantage.<sup>28,29</sup> In this study, we investigated  $\text{NH}_3$  synthesis using a Pd–Ag hydrogen-permeable membrane cell with an electrolyte consisting of NaOH–KOH. There were past attempts at  $\text{NH}_3$  synthesis using hydroxide molten salts, but none have reliably achieved nitrogen reduction.<sup>37,38</sup> Separating the functions of water electrolysis and nitrogen activation/hydrogenation, it is demonstrated that hydroxide melts can be

applied to  $\text{NH}_3$  synthesis in this work. The characteristics and practicality of  $\text{NH}_3$  synthesis from water and nitrogen using alkaline electrolytes were discussed.

## Experimental

The sectional drawing of a hydrogen-permeable membrane electrochemical cell for  $\text{NH}_3$  synthesis with an NaOH–KOH molten salt electrolyte is illustrated in Fig. 1. The main components of the electrochemical cell included a catalyst powder of Ru/Cs<sup>+</sup>/C weighing 0.20 g, a Pd–Ag membrane (3:1 atomic ratio) with a thickness of  $100 \mu\text{m}$ , an NaOH–KOH aqueous solution with a 1:1 molar ratio, and Ni foam with a diameter of 10 mm and a thickness of 1 mm on a Ni disk with a diameter of 10 mm and a thickness of 5 mm. The major differences from previous phosphate electrolyte electrochemical cells are that the material of the anode vessel has been changed from Ti to polytetrafluoroethylene (PTFE), and the material of the anode has been changed from Pt to Ni metal. The gap between the end faces of the cathode and anode was set to 3 mm. After assembling the anode and cathode vessels of the electrochemical cell, 5.0 mL of NaOH–KOH solution was introduced into the cell using a syringe with a narrow tube connected to the gas tube. The NaOH–KOH solution was a mixture of 0.20 mol of NaOH, 0.20 mol of KOH, and 20 mL of  $\text{H}_2\text{O}$ .

The cathode of the Pd–Ag membrane had a contacting area of  $3.1 \text{ cm}^2$  to the electrolyte, and the anode of the Ni foam disk had a geometric area of  $0.79 \text{ cm}^2$ . In this paper, the current density was defined relative to the cathode area, taking into account the uncertainty in the practical area of the Ni foam anode at the electrolyte interface. Due to length restrictions in the communication, the synthesis details of Ru/Cs<sup>+</sup>/C have been provided in our previous paper and the ESI,<sup>†</sup> for this article. Additionally, methods for detecting generated  $\text{NH}_3$  or  $\text{H}_2$ , cell heating techniques, gas supply methods, and ways to



Fig. 1 Sectional drawing of the hydrogen-permeable membrane electrochemical cell for  $\text{NH}_3$  synthesis with an NaOH–KOH molten salt electrolyte.



increase cell pressure can be referenced in our previous papers or the ESI† of this paper. It should be noted that the flow rate of N<sub>2</sub> was optimized for maximizing NH<sub>3</sub> production, resulting in an H<sub>2</sub>/N<sub>2</sub> ratio of 0.070 against current density.<sup>19,20</sup>

## Results and discussion

The rates of NH<sub>3</sub> and H<sub>2</sub> formation for NH<sub>3</sub> synthesis from H<sub>2</sub>O and N<sub>2</sub> with varying temperature are plotted in Fig. 2. The current efficiencies for the respective rates are also provided in Fig. 2. The current efficiencies for the formation of NH<sub>3</sub> and H<sub>2</sub>, CE<sub>NH<sub>3</sub></sub> and CE<sub>H<sub>2</sub></sub>, respectively, were defined as follows.

$$CE_{\text{NH}_3} = \frac{3Fr_{\text{NH}_3}}{j} \times 100 \text{ (\%)} \quad (1)$$

$$CE_{\text{H}_2} = \frac{2Fr_{\text{H}_2}}{j} \times 100 \text{ (\%)} \quad (2)$$

where  $r_{\text{NH}_3}$  and  $r_{\text{H}_2}$  are the rates of formation of NH<sub>3</sub> and H<sub>2</sub>, respectively, in mol s<sup>-1</sup> cm<sup>-2</sup>.  $F$  and  $j$  represent the Faraday constant of 96 485 C mol<sup>-1</sup> and current density in A cm<sup>-2</sup>. The product of the ratio of the thermoneutral potential of 1.32 V to the actual cell voltage and the current efficiency is the energy conversion efficiency, which is a critically important factor in energy conversion technologies.

The current efficiency for NH<sub>3</sub> synthesis was obtained as 4.0–4.2% at 230–250 °C. This efficiency was similar to our previous papers. The theoretical limit of current efficiency for NH<sub>3</sub> formation at 250 °C under this N<sub>2</sub> flow condition was derived as 6.4% from the thermodynamical equilibrium among NH<sub>3</sub>, H<sub>2</sub>, and N<sub>2</sub>.<sup>19,20</sup> The attainment of equilibrium was estimated to be 65% at 250 °C. The fact that there is little difference in the rate of NH<sub>3</sub> formation between 230 °C and 250 °C suggests that at 250 °C, the catalytic reaction is not limiting the rate, and the rate of NH<sub>3</sub> formation is constrained by the equilibrium. The decrease in NH<sub>3</sub> formation rate below 210 °C is attributed to insufficient catalytic reaction rates. The current efficiency for H<sub>2</sub> formation exceeded 100%, and when the sum of the current efficiencies of ammonia



Fig. 2 Rates and current efficiencies of NH<sub>3</sub> and H<sub>2</sub> formation for NH<sub>3</sub> synthesis from H<sub>2</sub>O and N<sub>2</sub> as a function of temperature. The current density was 10 mA cm<sup>-2</sup>, and pressure was 0.10 MPa in absolute pressure. The cathode and anode gases were 3.0 cm<sub>STP</sub><sup>3</sup> min<sup>-1</sup> of N<sub>2</sub> and 10 cm<sub>STP</sub><sup>3</sup> min<sup>-1</sup> + 10 μL min<sup>-1</sup> of Ar + H<sub>2</sub>O<sub>liq</sub>, respectively.



Fig. 3 Rates and current efficiencies of NH<sub>3</sub> and H<sub>2</sub> formation for NH<sub>3</sub> synthesis from H<sub>2</sub>O and N<sub>2</sub> as a function of current density. The absolute pressure and temperature were 0.10 MPa and 250 °C. The cathode and anode gases were 3.0 cm<sub>STP</sub><sup>3</sup> min<sup>-1</sup> of N<sub>2</sub> per 10 mA cm<sup>-2</sup> and 10 cm<sub>STP</sub><sup>3</sup> min<sup>-1</sup> + 10 μL min<sup>-1</sup> of Ar + H<sub>2</sub>O<sub>liq</sub>, respectively.

production and hydrogen production was calculated, it was approximately 100%.

The advantage of NaOH–KOH electrolyte is its ability to maintain stability and conduct long-term experiments at a relatively high current density of 100 mA cm<sup>-2</sup>. In our conventional system using phosphate electrolytes, when the current density exceeds 50 mA cm<sup>-2</sup>, the cell voltage starts to rise within a few hours, leading to deterioration. The rates of NH<sub>3</sub> and H<sub>2</sub> formation for NH<sub>3</sub> synthesis from H<sub>2</sub>O and N<sub>2</sub>, along with their current efficiencies, are depicted in Fig. 3 as a function of current density up to 100 mA cm<sup>-2</sup>. Exceeding a current density of 100 mA cm<sup>-2</sup> was not possible due to limitations in the capacity of the power supply. The rates of NH<sub>3</sub> and H<sub>2</sub> formation increased monotonically with increasing current density. Looking at the current efficiency, between 10 and 30 mA cm<sup>-2</sup>, both the current efficiency for NH<sub>3</sub> formation and for H<sub>2</sub> formation remain almost constant. However, when the current density is increased beyond 50 mA cm<sup>-2</sup>, it becomes evident that both the current efficiency for NH<sub>3</sub> formation and for H<sub>2</sub> formation decrease.

The decrease in current efficiency for NH<sub>3</sub> formation at high current densities can be understood as insufficient catalytic activity. In such cases, the current efficiency for H<sub>2</sub> formation must increase by the amount that the current efficiency for NH<sub>3</sub> formation decreases. The most likely cause of both the current efficiency for NH<sub>3</sub> and H<sub>2</sub> formation decreasing, resulting in a decrease in overall current efficiency, is the O<sub>2</sub> generated at the anode either being reduced at the cathode by passing through the electrolyte or the hydrogen reduced at the cathode being



unable to be absorbed by the Pd–Ag membrane and instead released as H<sub>2</sub> molecules in the electrolyte, subsequently oxidizing at the anode. The issue of such cross-leakage becoming problematic under high current densities was already recognized in our previous studies using phosphate electrolytes,<sup>20</sup> and it became pronounced even with NaOH–KOH electrolytes. Particularly in liquid electrolytes such as molten salts, cross-leakage poses a serious problem, as the evolved gases might pass through the electrolyte as bubbles or absorbed gases between the anode and cathode. Therefore, it seems necessary to explore measures such as optimizing the electrode spacing and installing separators with semi-permeable membranes.

Next, the results of time-dependent changes in cell voltage during NH<sub>3</sub> synthesis at constant current are shown in Fig. 4A for various current densities. At 10 mA cm<sup>-2</sup>, the cell voltage was about 1.28 V, which was between the equilibrium potential (1.16 V at 250 °C) and thermoneutral potential (1.32 V at 250 °C). With increasing current densities, cell voltage was increased to 1.96 V at 100 mA cm<sup>-2</sup>. At any current density, the cell voltage remained nearly constant over a period of 3 h, exhibiting remarkable stability. Fig. 4B shows the cell voltage changes in an operation for 3 weeks. While minor fluctuations in cell voltage were observed, there were no noticeable voltage increases indicative of degradation. The catalyst is inherently non-degrading, so consistent NH<sub>3</sub> production was observed at

any given point as long as water electrolysis continued at the stated current density. This was a highly favourable outcome compared to cells using phosphate electrolytes, as demonstrated in our previous papers, where an increase in cell voltage was observed within several hours at current densities exceeding 50 mA cm<sup>-2</sup>.

The synthesis of NH<sub>3</sub> by this system is strongly limited by chemical equilibrium, and theoretically, at a pressure of 0.10 MPa, temperature of 250 °C, and the present ratio between N<sub>2</sub> and current density, only up to 6.4% current efficiency of NH<sub>3</sub> can be expected. To relax the constraints of equilibrium, lowering the temperature while increasing the pressure is an option; however, as shown in Fig. 2, reducing the temperature shifts the limitation from equilibrium to kinetic, resulting in a decrease in the rate of NH<sub>3</sub> formation. Therefore, the results of investigating the rate of NH<sub>3</sub> formation when increasing the total pressure are shown in Fig. 5. At 1.0 MPa and 250 °C, the theoretical limit is estimated to be 36%.<sup>19,20</sup> As shown in Fig. 5, while the current efficiency for NH<sub>3</sub> formation was 4.76%, at 0.10 MPa, 10 mA cm<sup>-2</sup> and 250 °C, it was increased to 30% with elevating the pressure to 1.0 MPa. For 30 mA cm<sup>-2</sup> current density at 1.0 MPa and 250 °C, the current efficiency for NH<sub>3</sub> formation decreased to 25% because of insufficient catalytic activity.

The results of this study show that, unsurprisingly, the current efficiency of NH<sub>3</sub> production was very similar to the values obtained in our previous research, as the catalyst layer used was the same.<sup>19,20</sup> However, the significant advantage lies in the stable operation at higher current densities and the absence of observations such as electrode degradation. An important point not to overlook is that concentrated alkaline electrolytes, being strong alkalis, do not absorb NH<sub>3</sub>. In previous electrochemical cells using phosphate-based electrolytes, the use of a Pd–Ag membrane was imperative as it prevented the absorption of NH<sub>3</sub> by the protonic electrolyte and the subsequent neutralization of the electrolyte.<sup>19,20</sup> If the electrolyte does not absorb NH<sub>3</sub>, it might be possible to use hydrophobic filters instead of Pd–Ag membranes, as in the synthesis

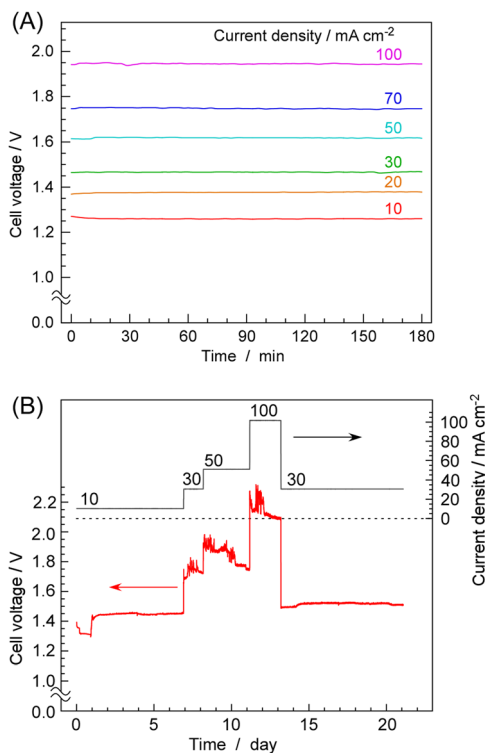


Fig. 4 Time courses of cell voltage for NH<sub>3</sub> synthesis from H<sub>2</sub>O and N<sub>2</sub> at various current densities and 250 °C. A summary of short-term current fluctuations (A) and the results obtained over a period of three weeks of operation (B). Note that (A) and (B) represent the experimental results from different cells that were reassembled, so the results do not perfectly match.

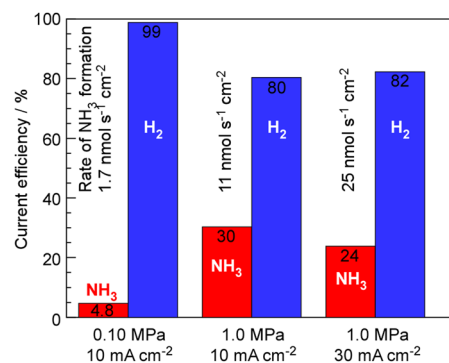


Fig. 5 Current efficiency of NH<sub>3</sub> and H<sub>2</sub> formation for NH<sub>3</sub> synthesis from H<sub>2</sub>O and N<sub>2</sub> at 250 °C with varying absolute pressure and current density. The rates of NH<sub>3</sub> formation are shown in this figure. The cathode and anode gases were 3.0 cm<sub>STP</sub><sup>3</sup> min<sup>-1</sup> of N<sub>2</sub> per 10 mA cm<sup>-2</sup> and 10 cm<sub>STP</sub><sup>3</sup> min<sup>-1</sup> + 10 μL min<sup>-1</sup> of Ar + H<sub>2</sub>O<sub>liq</sub>, respectively.





of methane from CO<sub>2</sub> and water using acidic phosphate electrolytes in this electrochemical system.<sup>22</sup> Alkaline water electrolysis conducted in aqueous solutions below 100 °C is considered crucial for hydrogen production in a hydrogen energy society. By increasing the operating temperature to around 250 °C, it is conceivable to synthesize NH<sub>3</sub> and produce various other fuel substances and useful materials.

## Conclusions

With KOH–NaOH eutectic molten salt electrolytes, an electrochemical-catalytic cell for NH<sub>3</sub> synthesis from nitrogen and water was studied at 250 °C and 1.0 MPa. The current efficiency for NH<sub>3</sub> formation was achieved to 30%, and the residue was used for H<sub>2</sub> formation. The cell voltage was extremely stable up to 100 mA cm<sup>-2</sup>, and no corrosion of the electrodes or components was observed, suggesting that this study shows significant potential for obtaining ammonia from water and nitrogen using electricity.

## Author contributions

Sagara primarily contributed to the investigation, which included experimental work, analysis of the obtained data, and paper writing. Hayashi, Hirata, and Nagaishi were primarily involved in practical experimental works and data analysis. Kubota played multifaceted roles including supervision in this study.

## Conflicts of interest

There are no conflicts to declare.

## Acknowledgements

This article is based on results obtained from a project, JPNP14004, “Highly-efficient NH<sub>3</sub> electrochemical synthesis technology from renewable energy electricity (FY2022-2023)”, commissioned by the New Energy and Industrial Technology Development Organization (NEDO), Japan.

## References

- 1 CO<sub>2</sub> free ammonia as an energy carrier: Japan's insights, ed. K. Aika and H. Kobayashi, Springer Nature, Singapore, 2023.
- 2 International Energy Agency, *Ammonia Technology Roadmap*, 2021.
- 3 International Renewable Energy Agency, *Innovation Outlook: Renewable Ammonia*, 2022, ISBN: 978-92-9260-423-3.
- 4 International Energy Agency, *Renewables, 2023, Analysis and forecast to 2028*, 2023.
- 5 California ISO, *Wind and solar curtailment totals by month*, <https://www.caiso.com/informed/Pages/ManagingOversupply.aspx>.
- 6 D. Kim, Z. Wang, J. Brugger, D. Blum, M. Wetter, T. Hong and M. A. Piette, *Appl. Energy*, 2022, **321**, 119343.
- 7 R. Daiyan, I. MacGill and R. Amal, *ACS Energy Lett.*, 2020, **5**, 3843–3847.
- 8 J. Gong, N. J. English, D. Pant, G. R. Patzke, S. Protti and T. Zhang, *ACS Sustainable Chem. Eng.*, 2021, **9**, 7179–7181.
- 9 C. R. Santhosh and R. Sankannavar, *Appl. Energy*, 2023, **352**, 121960.
- 10 B. Wang, T. Li, F. Gong, M. H. D. Othman and R. Xiao, *Fuel Process. Technol.*, 2022, **235**, 107380.
- 11 G. Qing, R. Ghazfar, S. T. Jackowski, F. Habibzadeh, M. M. Ashtiani, C.-P. Chen, M. R. Smith III and T. W. Hamann, *Chem. Rev.*, 2020, **120**, 5437–5516.
- 12 A. J. Martín, T. Shinagawa and J. Pérez-Ramírez, *Chem*, 2019, **5**, 263–283.
- 13 I. A. Amar, R. Lan, C. T. G. Petit and S. Tao, *J. Solid State Electrochem.*, 2011, **15**, 1845–1860.
- 14 S. Garg, M. Li, A. Z. Weber, L. Ge, L. Li, V. Rudolph, G. Wang and T. E. Rufford, *J. Mater. Chem. A*, 2020, **8**, 1511–1544.
- 15 M. Gattrell, N. Gupta and A. Co, *J. Electroanal. Chem.*, 2006, **594**, 1–19.
- 16 S. Z. Andersen, V. Čolić, S. Yang, J. A. Schwalbe, A. C. Nielander, J. M. McEnaney, K. Enemark-Rasmussen, J. G. Baker, A. R. Singh, B. A. Rohr, M. J. Statt, S. J. Blair, S. Mezzavilla, J. Kibsgaard, P. C. K. Vesborg, M. Cargnello, S. F. Bent, T. F. Jaramillo, I. E. L. Stephens, J. K. Nørskov and I. Chorkendorff, *Nature*, 2019, **570**, 504–508.
- 17 M. I. Ahmed, A. Assafiri, D. B. Hibbert and C. Zhao, *Small*, 2023, **2305616**.
- 18 A. Valera-Medina, F. Amer-Hatem, A. K. Azad, I. C. Delouse, M. de Joannon, R. X. Fernandes, P. Glarborg, H. Hashemi, X. He, S. Mashruk, J. McGowan, C. Mounaim-Rouselle, A. Ortiz-Prado, A. Ortiz-Valera, I. Rossetti, B. Shu, M. Yehia, H. Xiao and M. Costa, *Energy Fuels*, 2021, **35**, 6964–7029.
- 19 K. Imamura and J. Kubota, *Sustainable Energy Fuels*, 2019, **3**, 1406–1417.
- 20 S. Nagaishi, R. Hayashi, A. Hirata, R. Sagara and J. Kubota, *Sustainable Energy Fuels*, 2024, **8**, 914–926.
- 21 E. Christensen, R. W. Berg, R. Krüger and N. J. Bjerrum, *J. Electrochem. Soc.*, 2023, **170**, 014502.
- 22 J. Kubota, T. Okumura and R. Hayashi, *Sustainable Energy Fuels*, 2022, **6**, 1362–1372.
- 23 N. Fujiwara, S. Tada and R. Kikuchi, *iScience*, 2022, **25**, 105381.
- 24 Y. Yuan, S. Tada and R. Kikuchi, *Sustainable Energy Fuels*, 2022, **6**, 458–465.
- 25 G. Qing, R. Kikuchi, S. Kishira, A. Takagaki, T. Sugawara and S. T. Oyama, *J. Electrochem. Soc.*, 2016, **163**, E282–E287.
- 26 T. F. Fuller and K. G. Gallagher, in *Phosphoric acid fuel cells, Materials for Fuel Cells*, ed. M. Gasik, Elsevier B.V., 2008, ch. 6.
- 27 P. M. Parker, *The 2023 Report on Phosphoric Acid Fuel Cells: World Market Segmentation by City*, ICON Group International, Inc., 2022.
- 28 S. Kumar and H. Lim, *Energy Rep.*, 2022, **8**, 13793–13813.
- 29 K. Zeng and D. Zhang, *Prog. Energy Comb. Sci.*, 2010, **36**, 307–326.
- 30 K. Kawaguchi, K. Goto, A. Konno and T. Nohira, *J. Electrochem. Soc.*, 2023, **170**, 084507.
- 31 F. P. Lohmann-Richters, S. Renz, W. Lehnert, M. Müller and M. Carmo, *J. Electrochem. Soc.*, 2021, **168**, 114501.



- 32 S. D. Ebbesen, S. H. Jensen, A. Hauch and M. B. Mogensen, *Chem. Rev.*, 2014, **114**, 10697–10734.
- 33 E. Al-Muslih, P. J. Iredale and J. K. Maund, *J. Chem. Eng. Data*, 1983, **28**, 245–246.
- 34 *Solubility Data Series, Gases in Molten Salts*, ed. J. W. Lorimer, International Union of Pure and Applied Chemistry (IUPAC), Pergamon Press, 1989, vol. 45/46.
- 35 H. W. Otto and R. P. Seward, *J. Chem. Eng. Data*, 1964, **9**, 507–508.
- 36 J. Yang, H. Muroyama, T. Matsui and K. Eguchi, *J. Power Sources*, 2014, **245**, 277–282.
- 37 S. Licht, B. C. Cui, B. H. Wang, F. F. Li, J. Lau and S. Z. Liu, *Science*, 2014, **345**, 637–640.
- 38 G. Chehade and I. Dincer, *Int. J. Energy Res.*, 2020, **44**, 7183–7197.

