

## PAPER

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## Valorisation of used lithium-ion batteries into nanostructured catalysts for green hydrogen from boranes†

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Cobalt-based Li-ion batteries are produced globally on a massive scale, but most are discarded to landfill at the end of their useful lifetime. In this work, an efficient cobalt catalyst for the hydrolysis of sodium borohydride to dihydrogen was prepared from lithium ion battery waste, providing a second life for valuable minerals. This material is composed of a mixed metal cobalt–aluminium oxide supported on graphene, as elucidated by a combined FTIR, Raman, SEM, scanning transmission electron microscopy with electron energy loss spectroscopy (STEM-EELS) and energy-dispersive X-ray spectroscopy (EDS) study. The obtained metal oxide material, which exhibits an average oxidation state for Co of 2.45, is a languid catalyst at room temperature, but rapid hydrogen production of up to 49 L(H<sub>2</sub>) min<sup>−1</sup> g<sup>−1</sup>(Co) was observed in catalytic runs heated to 70 °C. This carbon-supported cobalt catalyst is competitive with designed cobalt nanostructured catalysts prepared from pure precursors. This work is illustrative of the opportunities which arise when e-waste is utilised as a mineral resource within the scope of a circular economy.

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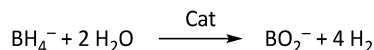
## Introduction

Energy storage technology plays a central role in enabling the movement towards decarbonising our world economy. In the pursuit of a green energy system, there is a steady increase in demand for lithium ion batteries (LIBs) to electrify the transportation sector and provide storage solutions for intermittently sourced renewable electricity.<sup>1</sup> Despite the massive scale of production of LIBs, only a small portion is ever recycled. In the USA, only 5% of spent LIBs are recycled and the remainder goes to landfill where they are hazardous to the environment. Mineral recovery is infrequent as the economics of current recycling processes are challenging.<sup>2</sup> There are ongoing efforts from both industry players and academia toward developing green, efficient processes to efficiently recover valuable elements such as Co, Li and Cu from battery waste.<sup>3–9</sup> Recently, biomaterials such as lignin have received high interest for the sustainable recovery of relevant metals from active electrode materials.<sup>5</sup>

Cobalt-containing oxides present in lithium ion battery cathodes are prominent in numerous other applications.

Cobalt oxides are catalysts for processes such as electrochemical water splitting,<sup>10–13</sup> or electrocatalytic water purification.<sup>14</sup> Complementary to technology aiming to recover materials are approaches that enable the development of new products directly from waste.<sup>15</sup> Relatively few studies have been conducted seeking to find new applications for battery waste. So far, it has been demonstrated that LiCO<sub>x</sub> from battery waste can be combined with graphene to prepare a highly efficacious lubricant additive,<sup>16</sup> that supercapacitor electrodes can be prepared from scrapped LIB cathode materials,<sup>17,18</sup> and that MnO<sub>2</sub> from Li–MnO<sub>2</sub> batteries is a potent catalyst for peroxy-monosulfate degradation.<sup>19</sup>

To explore the possibility of preparing materials relevant to energy transformation directly from e-waste, we have prepared cobalt catalysts for NaBH<sub>4</sub> hydrolysis using Co recovered from Li-ion battery cathodes. Hydrolysis of NaBH<sub>4</sub> solutions to release hydrogen is accomplished according to Scheme 1, yielding 4 equivalents of H<sub>2</sub> per NaBH<sub>4</sub> molecule, thereby releasing up to 10.8 wt% H<sub>2</sub>. While the hydrolysis of NaBH<sub>4</sub> is thermodynamically favourable, it is kinetically stable in alkaline solution. In other words, NaBH<sub>4</sub> is sufficiently stable in the given timeframe for potential application as a hydrogen



Scheme 1 Catalytic evolution of dihydrogen from sodium borohydride.

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source for fuel cells. Hydrolysis (correspondingly, hydrogen evolution) of alkaline borohydride solutions can be readily controlled by the addition and subsequent removal of a solid catalyst.<sup>20</sup>

Cobalt oxides,<sup>21</sup> borides,<sup>22</sup> borates<sup>23</sup> and Co-P materials (*i.e.*, phosphates, phosphides and mixed phase materials)<sup>24</sup> and mixed transition metal borides such as Co-M-B (M = W or Mo)<sup>25,26</sup> are potent candidates for heterogeneous earth-abundant metal catalysed hydrogen production from inorganic boranes. These catalysts can be single-phase or alternatively a complex core-shell structure.<sup>24</sup> Using a variegated cobalt precursor sourced from battery waste is expected to give rise to new structural diversity and potentially, catalytic properties contrasting those of systems prepared from pure precursors. These cobalt-based catalysts have proven to have similar efficacy at a much lower manufacturing cost point when compared to the precious metal catalysts initially investigated for this purpose. In this work, we have extended this principle by applying simple technology to recover cobalt from a potentially hazardous waste material. Direct treatment of the aqueous cobalt leachate with a sodium borohydride yields a useful catalyst for green hydrogen production. The catalytic and structural properties of this material are discussed herein.

## Experimental

### General comments

Graphene nanoplatelet aggregates (surface area = 500 m<sup>2</sup> g<sup>-1</sup>) were purchased from Alfa Aesar and used as received. Other chemicals were obtained from various commercial sources and used as received. HTC-BG32100 batteries were obtained from the internal battery recycling service at MMK, Stockholm University. ATR-IR spectra were collected using a Varian 610-IR FTIR spectrometer. Raman spectra were collected using a LabRAM HR 800 Raman microscope equipped with an Nd-YAG laser (532 nm). SEM micrographs were taken using a JEOL JSM-7000F scanning electron microscope, and samples were supported on carbon (sample 1) or copper (1C) tape. STEM (scanning transmission electron microscope) images, EDS (energy-dispersive X-ray spectroscopy) and EELS (electron energy loss spectroscopy) spectra were collected from samples mounted on a holey carbon grid using a Thermo Fisher Scientific™ Themis Z microscope equipped with a SuperX EDX detector operated at 300 kV in the scanning TEM mode, and a Gatan imaging filter (Quantum ER) for EELS. Thermal analysis was performed on a PerkinElmer TGA 7 under a dynamic atmosphere of synthetic air under a heating rate of 10 K min<sup>-1</sup>. Powder X-ray diffraction (PXRD) data was collected using a X-Pert PANalytical diffractometer equipped with a fixed divergence 1/2° slit, a Cu W/Si mirror and a 10 mm mask as incident optics and a parallel plate collimator and a proportional detector as diffracted beam optics. Spectrophotometric analysis of cobalt(II) as 4-(2'-pyridylazo)resorcinol complexes were conducted using a photocolormeter (WPA, S800) for point measurements at 500 nm in quartz cuvettes as described

elsewhere.<sup>27</sup> The elemental content of 1C was determined by ICP-OES (iCAP 7400 ICP-OES Duo, Thermo Fisher, Waltham, MA, USA) after microwave supported digestion treatment with nitric acid.

### Battery workup and preparation of recovery solution

A HTC-BG32100 mobile phone battery was discharged by immersion in 1 M NaCl solution for 30 minutes. The battery casing was then removed manually and cathode powder and some associated plastic was collected (4.5 g) (Fig. S1, ESI†). This material was added portion-wise to 200 mL of H<sub>2</sub>O, resulting in gas evolution. Given the construction of Li-based batteries and potential presence of lithium metal agglomeration, related reactive lithium species, and/or volatile electrolytes this step should be preferentially performed with care under the fume-hood. The resultant slurry was stirred magnetically for 30 m, after which the bubbling had ceased. 100 mL of 4 M HCl solution was added in 10 × 10 mL portions, accompanied by gas flow. The mixture was then heated to 80 °C. After 1 h, this mixture was filtered hot, to give a bright red solution. The cobalt recovery solution was made up to 300 mL with distilled water and stored for further experiments (Fig. S2, ESI†). Colourimetric assay; 11.4 g L<sup>-1</sup> Co.

### Preparation of 1

10 mL of the cobalt recovery solution above (*ca.* 1.9 mmol Co) was treated with 1 M Na<sub>2</sub>CO<sub>3</sub> solution until pH 6 was achieved. An ethanolic NaBH<sub>4</sub> solution (700 mg, 18.7 mmol in 20 mL 70% EtOH/H<sub>2</sub>O) was added portionwise over 10 minutes, resulting in vigorous gas evolution. Although NaBH<sub>4</sub> is reasonably stable in ethanol or water, the reduction step should be performed with care since the reaction is exothermic and leads to bubbles evolving from the solution. The slurry was stirred for a further 5 minutes, then allowed to stand for 15. Much of the solution was decanted off, and the remainder mixed with 20 mL of 50–50 EtOH/H<sub>2</sub>O. The mixture was then centrifuged and the golden-brown powder collected by filtration, and dried overnight at 60 °C to give 1 (92 mg, 41% (Co atom basis)). SEM-EDS [Co] = 52 wt%.

### Preparation of 1C

10 mL of the cobalt recovery solution above (*ca.* 3.2 mmol Co) was treated with 1 M Na<sub>2</sub>CO<sub>3</sub> solution until pH 6 was achieved. After this, graphene nanoplatelet aggregates (50 mg) were introduced and the resultant slurry was stirred rapidly. An ethanolic NaBH<sub>4</sub> solution (700 mg, 18.7 mmol in 20 mL 70% EtOH/H<sub>2</sub>O) was added portionwise over 10 minutes, resulting in vigorous gas evolution (**caution** – exothermic reaction, see above). The slurry was stirred for a further 5 minutes, then filtered. The black filtrate was washed with water (2 × 25 mL) and EtOH (2 × 25 mL). The filtrate was dried overnight at 60 °C to give 1C (456 mg, 97% (Co atom basis)). ICP [Co] = 24.5 wt%.

### Hydrogen evolution experiments

A 50 mL round bottom flask (RBF) was heated to the appropriate temperature in an oil bath. Once the temperature had



stabilised, the RBF was loaded with 1 mg of the desired catalyst, and treated with either 1.45 mL or 10 mL of a freshly prepared aqueous solution of 0.5 M  $\text{NaBH}_4$  with 0.25 M  $\text{NaOH}$ . A gas adaptor was attached to the flask, and  $\text{H}_2$  was collected to an upturned measuring cylinder filled with water as described elsewhere. The experiments were filmed and then volume change with time was used to calculate the rates of catalysis in terms of  $V(\text{H}_2)/\text{time}/\text{mass}$  of catalyst.

## Results and discussion

A working solution of cobalt ions were obtained by digesting manually separated battery cathode materials from discarded HTC smartphone batteries in 5 M  $\text{HCl}$ . The resultant solution contained *ca.* 11 g  $\text{L}^{-1}$  Co, as determined by colourimetric methods. To obtain catalyst candidates for borohydride hydrolysis, we targeted cobalt oxide nanoparticles either unsupported or supported on graphene nanoplatelets. Previous studies have demonstrated synergy between carbon scaffolds and cobalt nanoparticles as catalysts for these reactions,<sup>28</sup> and have demonstrated that the reduction of cobalt salts with superstoichiometric borohydride leads to small particle sizes and corresponding high catalytic activity.<sup>29</sup> To prepare catalyst candidates, the battery extract solution was neutralised with  $\text{Na}_2\text{CO}_3$ , and the resultant solution was treated with an excess of sodium borohydride either with or without the addition of graphene platelets (with a surface area of 500  $\text{m}^2 \text{g}^{-1}$ ). Borate oxidation and ligand exchange in the absence of graphene yielded a small amount of an orange powder (**1**) consisting of metal oxide particles in a 46% yield on a Co atom basis. The addition of graphene substantially improved reaction yields; near quantitative precipitation of a black powder (**1C**) consisting of metal oxide particles supported on graphene plates was obtained (Scheme 2).

Given the variegated composition of the battery extract, it was essential to thoroughly characterise **1** and **1C** to understand their chemical and morphological character. **1** and **1C** were characterised variously by SEM, STEM, PXRD, ICP-MS as well as FTIR and Raman spectroscopy. SEM micrographs (Fig. 1) reveal that **1** is composed of nanostructured particle  $\mu\text{m}$  clusters of a granular material, whereas **1C** is an array of stacked graphene platelets with a lateral size of 100–200  $\mu\text{m}$ , decorated with dispersed metal oxide particles. Based on the SEM images, it appears that metal oxide particles in **1C** and **1** are of quite a different morphology, with smaller, powdery

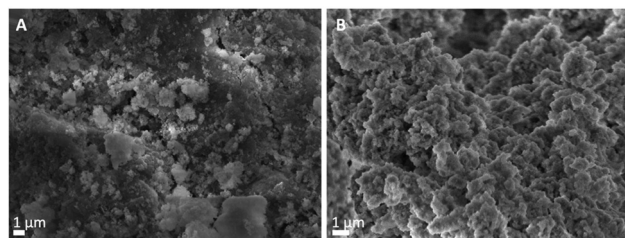


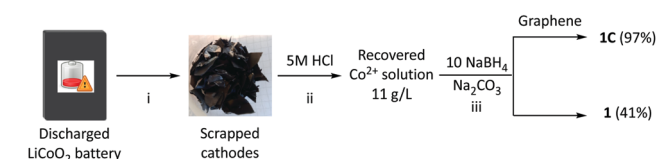
Fig. 1 SEM micrographs of (A) sample **1C** and (B) sample **1**.

clusters present in **1C**. ICP-MS analysis of a digested sample of **1C** showed that the bulk composition includes by weight: 24.5% Co, 7.8% B and 3.26% Al. Li, Mg, Mn, Fe, and Ni were also detected but were each present at <0.01 wt%. B is superstoichiometric to cobalt, the two are present in a 1.7:1 ratio. This is indicative of the presence of extensive borate phases, as are frequently observed in cobalt materials prepared by borohydride reduction of cobalt salts.<sup>23</sup>

To further elucidate the composition of **1C**, STEM EELS and EDS analysis were performed (Fig. 2). EDS indicated that the primary constituents of **1C** were cobalt, oxygen and carbon, with some aluminium and sodium also present. EELS is more accurate for the quantification of low Z elements on the surface of samples. EELS analysis indicated the presence of Co, Li and F. Relative elemental proportions of C, O, F, Na, Al, S and Co are presented in Table 1. A comparison of L2 and L3 edges of Co (Fig. S4, ESI†) using a method developed by Tan *et al.*,<sup>30</sup> *i.e.*, energy loss near edge structure (ELNES) fitting, indicated that the average oxidation state of Co is 2.45, indicating a mixture of  $\text{Co}^{2+}$  and  $\text{Co}^{3+}$  in **1C**.

Li is difficult to quantify by EELS in the presence of Co. The latter has an M edge at 60 eV, very close to the K edge of Li at 55 eV. As less than 0.1 wt% Li was detected by ICP-MS, EELS quantification of this element was not attempted. The relatively high portion of C detected arises from the necessity of choosing a site with only a very thin metal particle suspended on graphene. On an atom basis, the surface of **1C** contains Co:F in a 1:2 ratio, probably present in the form of Al-F or Co-F moieties. The origin of surface fluoride likely related to the reduction of residual  $\text{PF}_6^-$  electrolyte, or from polyvinylidene fluoride – a common binding agent in Li-ion battery cathodes.

Cobalt borates are topical catalysts for borohydride reduction,<sup>10,23</sup> so the presence of periodically related Lewis acidic Al sites in **1C** may lead to enhanced catalytic activity.



Scheme 2 Preparation sequence for **1** and **1C**. (i) Manual dismantling and separation of cathode materials. (ii) Dissolution in 5 M  $\text{HCl}$  at 80  $^\circ\text{C}$  for 1 h. (iii) neutralisation and treatment with 10 eq. of  $\text{NaBH}_4$  in ethanol, in the presence or absence of graphene.

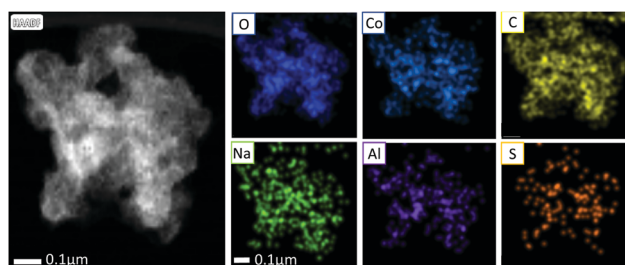


Fig. 2 STEM micrograph and EDS elemental mapping for **1C**.



**Table 1** Relative atomic abundance of elements in **1**, as determined by STEM, EELS and EDS measurements. Boron is not included, because its analysis by means of EDS is problematic due to inherent physical problems (peak overlap and low fluorescence yield)

Element	Atomic fraction (%)
C	32
O	49
F	10
Na	2.7
Al	2.7
S	0.2
Co	4.5

A dark field STEM micrograph of **1C** is presented in Fig. 2, alongside elemental mapping from STEM-EDS. From the elemental maps, it is evident that Al, Co and O are distributed across the graphene substrate in small clusters, consistent with the small metal-oxide particles observed under SEM (Fig. 1). Notably, the presence of Mn or Ni were detected by either EELS or EDS, confirming that Co is the dominant transition metal component on the surface of the sample. Based on EELS, EDS and ICP-MS analysis, **1C** can be described as mixed metal cobalt aluminium borate nanoparticles with fluoride decoration on the surface, supported on graphene.

Spectroscopic analysis was performed to better understand the chemical makeup of **1C**. The Raman spectrum of **1C** was collected between 1800–400  $\text{cm}^{-1}$ , and featured four main bands (Fig. 3). D and G bands of graphene are evident at 1566 and 1336  $\text{cm}^{-1}$ ; these correspond to aromatic in plane and out of plane vibration modes respectively.<sup>31</sup> The prominence of the G band (out of plane) is indicative of lattice defects, indicating some amorphous character to the carbon after treatment with the battery leachate and borohydride. Additional bands at 829 and 669  $\text{cm}^{-1}$  are tentatively assigned to various Co–O modes.

The PXRD pattern of **1C** (Fig. 4) features broad peaks centred at  $\theta = 23.7^\circ$  (002) and  $43.8^\circ$  (101), characteristic of graphitic plates with disordered stacking.<sup>32</sup> The position of the 002 peak corresponds to a interlayer  $d$ -spacing of 3.8 Å, signifying a lattice extension relative to pristine graphite (graphite features a  $d$ -spacing of *ca.* 3.3 Å). This is typical for graphene aggregates or reduced graphene oxide materials.<sup>33</sup> No XRD reflection

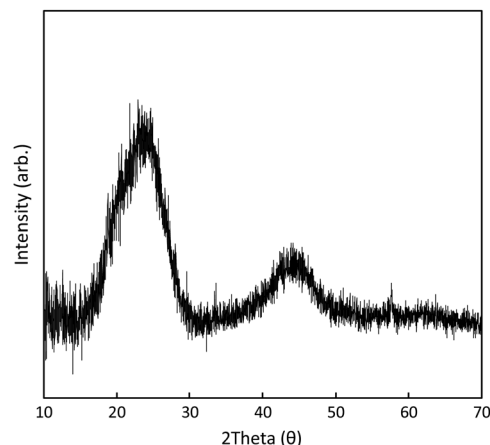


Fig. 4 PXRD pattern of **1C**.

peaks were able to be unambiguously assignable to metal oxide phases. This originates from the lack of long-range order due to the low temperature of the catalyst synthesis. Consequently, no reflection peaks of potential metal oxide phases can be observed in the XRD patterns.

The FTIR-ATR (Fourier transform infrared – attenuated total reflectance) spectra of **1** and **1C** are quite similar (Fig. 5). Both contain diagnostic bands arising from surface adsorbed water are evident at 3494 and 1640  $\text{cm}^{-1}$ , and doublets in regions associated with tetrahedral (1420–1320  $\text{cm}^{-1}$ ) and trigonal borates (1000–905  $\text{cm}^{-1}$ ),<sup>23</sup> indicating the presence of a  $\text{Co}_n(\text{B}_3\text{O}_6)$  species. The signal for trigonal borates is weaker in **1C** than in **1**. Shouldering at 850  $\text{cm}^{-1}$  may be associated with alumina species.<sup>34</sup>

### Borohydride hydrolysis

**1C** was evaluated as a catalyst for the hydrolysis of sodium borohydride in alkaline solutions (*vide supra*). We examined the performance of **1C** across a range of temperatures. High temperatures (60–100 °C) are realistic conditions for fuel cell vehicles being empowered by hydrogen technology.<sup>35</sup> The optimal rate of hydrolysis of borohydride to hydrogen with **1C** was noted at 70 °C.

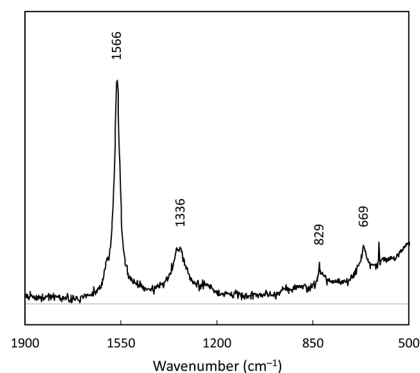


Fig. 3 Raman spectra of **1C**.

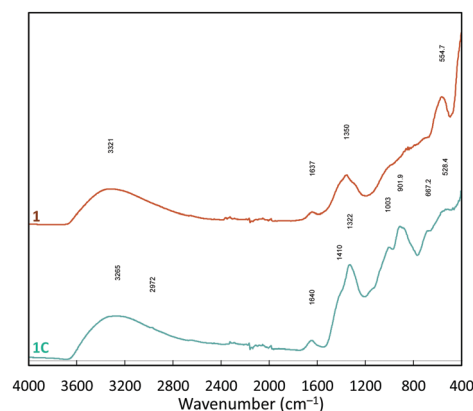
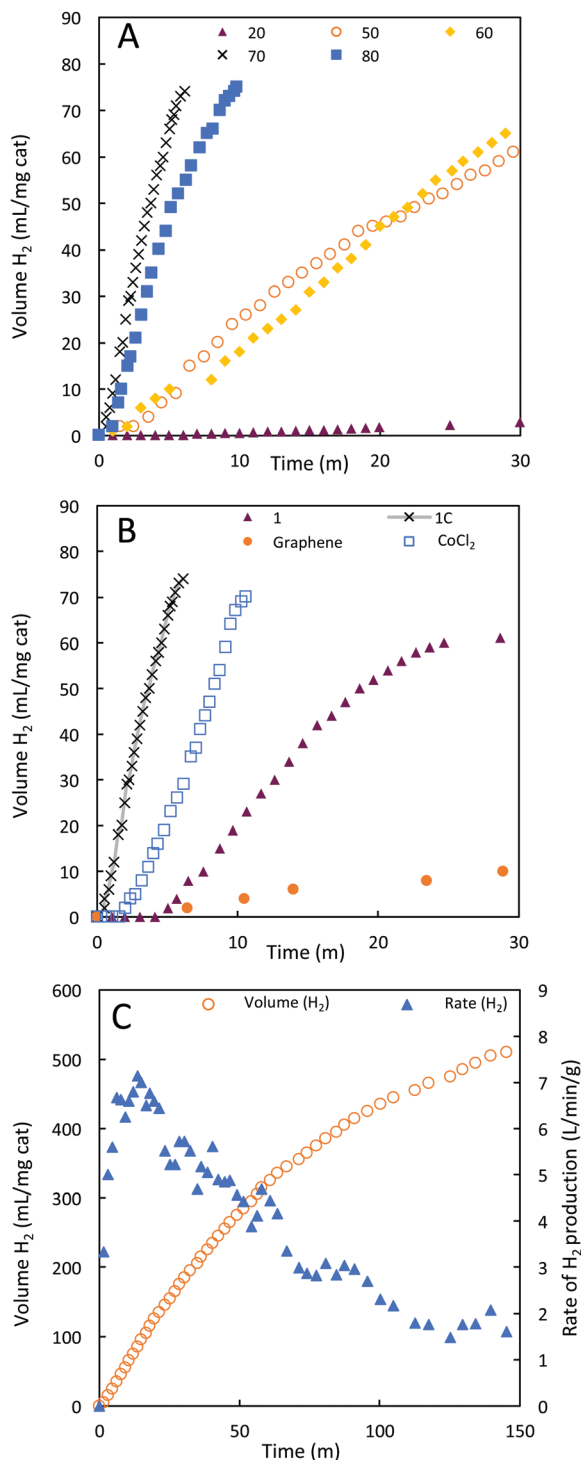


Fig. 5 FTIR-ATR (Fourier transform infrared – attenuated total reflectance) spectra of **1** and **1C**.







**Fig. 6** (A) Hydrogen production by 1 mg of **1C** at different temperatures from a 0.25 M  $\text{NaBH}_4^-$  solution. (B) Hydrogen production of **1C**, **1** and graphene at 70 °C from a 0.25 M  $\text{NaBH}_4^-$  solution. (C) Larger scale  $\text{H}_2$  evolution experiment at 70 °C using 1 mg of **1C**, the blue triangles indicate the rate of hydrogen production over time, and the orange circles indicate the cumulative volume produced.

At this temperature,  $12 \text{ L}(\text{H}_2) \text{ min}^{-1} \text{ g}_{\text{cat}}^{-1}$  (Fig. 6A and Table 2) of hydrogen gas was produced at a rate 130-fold higher than the rate observed at 20 °C ( $0.09 \text{ L}(\text{H}_2) \text{ min}^{-1} \text{ g}_{\text{cat}}^{-1}$ ). Adjusting for the

relatively small proportion of cobalt present in **1C**, the rate of hydrogen evolution can be expressed as  $49.3 \text{ L}(\text{H}_2) \text{ min}^{-1} \text{ g}_{\text{Co}}^{-1}$ , highlighting the efficiency of **1C** as a borohydride hydrolysis catalyst. Efficient performance at these temperatures is of critical importance, because prototyped engineered systems for borohydride hydrolysis operate above 60 °C.<sup>20,36</sup> The decay of catalytic activity at 80 °C indicates that the ideal temperature window is app. 70 °C and the loss in catalytic activity is most likely due to structural changes, *i.e.* decrease of active sites. An ideal temperature for a given reaction is a general phenomenon for both heterogeneous and homogeneous catalysts.

Hydrogen evolution from  $\text{NaBH}_4$  was then investigated in the presence of **1C**, **1**,  $\text{CoCl}_2 \cdot 6\text{H}_2\text{O}$  and graphene at 70 °C (Fig. 6B). Under these conditions, the run impregnated with graphene gave rise to very little hydrogen evolution, comparable to a blank run. **1** is less active than **1C**, despite containing a higher portion of cobalt by mass and only achieved 82% conversion of borohydride to hydrogen. The lower performance of **1** despite the significantly higher portion of cobalt present can be related to the large particle sizes observed by SEM. Large particles are typically associated with inferior catalytic performance. The improved durability of **1C** relative to **1** supports the postulate that the graphene platelets are effective at stabilising cobalt metal oxide nanoparticles.

The vast majority of studies on cobalt (and other) catalysts for the hydrolysis of borohydrides have investigated their efficacy only between 20–30 °C.<sup>20,24</sup> To determine if the more than hundred-fold improvement in hydrogen production rate at **1C** upon heating to 70 °C from room temperature is a general feature of cobalt catalysts, or idiosyncratic to this material, we examined the prototypical cobalt catalyst – cobalt chloride.<sup>40</sup> At 70 °C,  $\text{CoCl}_2$  turned over  $6.0 \text{ L}(\text{H}_2) \text{ min}^{-1} \text{ g}(\text{cat})^{-1}$  hydrogen,

**Table 2** Rate of  $\text{H}_2$  evolution from borohydride hydrolysis using a range of cobalt-based catalysts. It should be noted that there is no general standard in literature regarding the required reaction time for determining the catalytic performance

Catalyst	$T$ (°C)	Rate of $\text{H}_2$ evolution	
		$\text{L min}^{-1} \text{ g}_{\text{cat}}^{-1}$	$\text{L min}^{-1} \text{ g}_{\text{Co}}^{-1a}$
<b>1C</b>	20	0.09	0.38
<b>1C</b>	50	1.8	7.5
<b>1C</b>	60	2.0	8.1
<b>1C</b>	70	12	49.3
<b>1C</b>	80	7.6	31.1
<b>1</b>	70	2.0	—
$\text{CoCl}_2 \cdot 6\text{H}_2\text{O}$	70	6.0	24
Graphene	70	0.34	—
Blank <sup>b</sup>	70	0.13 <sup>b</sup>	—
$\text{CoCl}_2 \cdot 6\text{H}_2\text{O}^{37}$	20	0.57	2.3
$\text{Co-B/C}_{\text{black}}^{28}$	30	—	23.94
$\text{Co-O-P}^{24}$	20	2.81	—
$\text{CoO nanocrystals}^{21}$	30	5.89	—
$\text{CoCl}_2/\text{Al}_2\text{O}_3^{38}$	20	8.9	45.4
$\text{Pt/C (10 wt\%)}^{39}$	25	23	176 <sup>c</sup>

<sup>a</sup> Using 4.5% Co determined by STEM EDS analysis, or as calculated in the literature by authors. <sup>b</sup> In the un-catalysed run, 4 mL of  $\text{H}_2$  evolved over 30 minutes, the rate is expressed w.r.t. 1 mg catalyst in line with the other results. <sup>c</sup> Value given is relative to Pt atoms.



indicating a 14-fold improvement compared to previous literature reports at 20 °C. The improvement in rate here is an order of magnitude less than that observed for **1C**, which is also ten times more active than  $\text{CoCl}_2$  at 70 °C on a Co atom basis.

To study the long-term stability of **1C**, we performed a longer catalytic run (Fig. 6C). In this run, the maximum turnover rate was noted after 15 minutes at  $7 \text{ L min}^{-1} \text{ g}_{\text{cat}}^{-1}$ , which then gradually declined to *ca.*  $2 \text{ L min}^{-1} \text{ g}_{\text{cat}}^{-1}$ , a rate still comparable with many literature catalysts. The reaction proceeded to completion with a turnover number of at least  $1.2 \times 10^7$  in terms of molecules of  $\text{H}_2$  produced per Co atom in the catalyst.

Most cobalt (and other non-precious metal) systems for borohydride hydrolysis have been benchmarked around room temperature to facilitate straightforward comparison to other systems. The activity of cobalt systems at elevated reaction temperatures is poorly characterised, obfuscating comparisons between literature catalysts and **1C**. Developing an understanding of how cobalt catalysts function over long time periods and at elevated temperatures is important if they are to find applications in hydrogen fuel cells. Our results emphasize that valorisation can be considered as sustainable recycling of used Li-ion batteries.<sup>41</sup>

## Conclusions

The mixed cobalt–aluminium borate catalyst **1C** was prepared from scrapped Li-ion battery cathodes with the addition of a graphene support. The preparation of **1C** was straightforward and green, involving treatment of a deconstructed battery with hydrochloric acid, neutralisation of the extract with sodium carbonate and finally reduction of the catalyst with sodium borohydride in the presence of graphene.

**1C** is an effective catalyst for the alkaline hydrolysis of sodium borohydride, achieving an optimal production rate of  $49.3 \text{ L(H}_2\text{) min}^{-1} \text{ g}^{-1} \text{ Co}$  at 70 °C, and a turnover number of at least  $1.2 \times 10^7$  molecules of  $\text{H}_2$  per Co atom. A similar catalyst, **1**, prepared without a carbon support gave poor turnover and exhibited a relatively lower activity. SEM and STEM analysis showed that metal oxide nanoparticles with smaller particle sizes were obtained in **1C** compared to **1**, which may explain how the presence of carbon can improve mass activity.

The dramatic improvement in activity of **1C** upon heating highlights the need to examine both cobalt and precious metal catalysts over a wide temperature range, as this data will better inform applications in hydrogen on demand systems. Furthermore, this work is illustrative that new possibilities for materials abound when chemists turn their attention to waste as a raw material. Future developments of this system will pursue an optimised synthesis, and seek conditions where long term stability is maximised so that up-cycled cobalt materials such as **1C** can be practical components of hydrogen on demand energy systems.

## Conflicts of interest

There are no conflicts to declare.

## Acknowledgements

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