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A pH-dependent microkinetic modeling guided synthesis of porous dual-atom catalysts for efficient oxygen reduction in Zn–air batteries†

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The oxygen reduction reaction (ORR) plays a crucial role in diverse energy conversion devices, such as zinc–air batteries (ZABs). Highly-efficient screening, rational design and precise synthesis of active and stable ORR electrocatalysts will advance ZAB technology for practical applications but they remain very challenging. Herein, we utilized a pH-field coupled microkinetic model to identify $\text{Fe}_1\text{Co}_1\text{-N}_6$ as the optimal dual-atom catalyst (DAC) for ORR in alkaline media. According to theoretical prediction, a $\text{Fe}_1\text{Co}_1\text{-N-C}$ DAC with a hierarchically porous structure was synthesized by a hard-template method following a CO_2 activation process. The prepared $\text{Fe}_1\text{Co}_1\text{-N-C}$ DAC exhibits superior ORR activity and stability to the benchmark Pt/C catalyst. More impressively, the $\text{Fe}_1\text{Co}_1\text{-N-C}$ based ZABs exhibit excellent performance including a high open-circuit voltage (1.51 V), a very high energy density ($1079 \text{ W h kg}_{\text{Zn}}^{-1}$), the best-ever rate capability (from 2 to 600 mA cm^{-2}), and ultra-long ZAB lifespan (over 3600 h/7200 cycles under 5 mA cm^{-2}). This work not only demonstrates that highly-efficient screening combined with rational design of DACs with optimal active sites and pore structures can boost their practical applications, but also presents a highly promising and effective way to synthesize different electrocatalysts for diverse applications.

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Broader context

Non-noble dual-atom catalysts (DACs) containing two adjacent metal active sites, which can optimize adsorption energies and improve catalytic kinetics, are a class of highly promising ORR catalysts. However, the low efficiency in the development of optimal DACs and unsatisfactory performance in practical energy devices hinder them from practical applications. Here, using pH-field microkinetic models, we rapidly identified and rationally synthesized an efficient $\text{Fe}_1\text{Co}_1\text{-N-C}$ ORR catalyst with desired $\text{Fe}_1\text{Co}_1\text{-N}_6$ dual metal atomic sites and hierarchically porous structures. The designed porous $\text{Fe}_1\text{Co}_1\text{-N-C}$ catalyst not only shows excellent ORR performance in a three-electrode system, but also exhibits outstanding performance in zinc–air batteries. This work provides insights for designing and constructing advanced catalysts for various high-performance energy conversion applications.

Introduction

The growing challenges of energy scarcity and environmental pollution from traditional fossil fuels require advanced energy devices and technologies.^{1–3} Rechargeable zinc–air batteries

(ZABs), with the merits of high theoretical energy density (1086 W h kg^{-1}), low cost, intrinsic safety and environmentally friendly nature, are considered some of the most promising power devices.^{2,4–6} The oxygen reduction reaction (ORR) involving multiple proton electron transfer at the air cathode plays a

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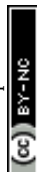
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vital role in ZAB performance, including discharge capabilities, cycling stabilities, and energy efficiencies; however, it suffers from sluggish kinetics.^{6–8} While platinum-based electrocatalysts, *e.g.*, Pt/C, are widely used as the benchmark catalysts with high activity for the ORR, the high cost, natural scarcity, and impurity poisoning limit their feasibility for large-scale practical applications.^{4,6,8} Therefore, the development of low-cost and high-performance ORR electrocatalysts is of great interest and highly desired.

During the past few decades, various non-noble metals/metal-free ORR electrocatalysts have been developed, including metal carbides,⁹ nitrides,¹⁰ oxides,¹¹ sulfides,¹² nitrogen doped carbon,^{13–15} and single-atom catalysts (SACs).^{7,16–18} Among them, SACs with atomically dispersed metal sites anchored on a substrate have attracted extensive attention, because of maximized atom utilization efficiency, unsaturated and tunable coordination environments, and unique electronic structures.^{19,20} In particular, metal–nitrogen–carbon (M–N–C, M = Fe, Co, Ni, Cu, and Mn) SACs have been widely reported as promising ORR catalysts with comparable catalytic activity to Pt-based materials.^{16,21–23} However, their performance is still lagging behind the apex of M–N₄–C SACs' Volcano plot, probably because their inherent electronic structures and symmetric electron distribution, as well as single-metal-atom active sites, have difficulty in breaking the linear scaling relationship among the adsorption energies of various ORR intermediates.²⁴

Recent studies have demonstrated that the construction of dual-atom catalysts (DACs) containing two adjacent metal active sites can optimize adsorption energies, thus effectively improving catalytic kinetics and enhancing the ORR activity of M–N₄–C SACs.^{25,26} DACs with diverse atom-pairs, such as Fe–Cu,²⁷ Cu–Co,²⁸ Fe–Ni,²⁹ Fe–Co,^{24,30,31} Fe–Mn,³² Co–Ni,³³ and Fe–Zn,³⁴ have been reported and exhibit very impressive ORR performance, even surpassing the benchmark Pt/C catalyst. Despite the great progress achieved in the synthesis and applications of DACs during the past few years, there are still some problems that need to be addressed in this field before their practical application. First, current studies mainly rely on the conventional trial-and-error method and lack precise theoretical guidance, which results in low efficiency for the development of optimal DACs. Second, most studies focus on the construction of different dual atom-pairs for performance enhancement and always ignore the creation of hierarchical pore structures, which is highly important for the transport properties of catalysis relevant species and can further improve DACs' catalytic performance in practical applications. Third, although some DACs exhibit superior ORR performance in traditional three-electrode tests, their performance in practical ZABs, such as rate performance and cycling stability, is still mediocre (stability time <1000 h and the maximum discharge rate <100 mA cm^{−2}), which severely hinders them from practical applications.^{6,8,35} Therefore, it is highly desired but still very challenging to develop a highly-efficient strategy for the construction of high-performance ORR DACs with optimal active sites and hierarchical pore structures for high-performance ZAB applications.

Here, we report a pH-field coupled microkinetic modeling guided synthesis strategy to construct desired ORR DACs with great practical application potential for ZABs. We firstly conducted theoretical analysis through a comprehensive pH-field coupled microkinetic model to quickly screen optimal DACs for the ORR, which clearly suggests that a DAC with Fe₁Co₁–N₆ structures as active sites is the most active ORR catalyst among SACs, transition metals (TMs), and DACs in alkaline media. Based on this theoretical understanding, we precisely synthesized DACs with Fe₁Co₁–N₆ structures as active sites, specifically Fe₁Co₁–N–C, and importantly, also created hierarchical pore structures on the DACs by a hard-template method following an activation process. The prepared porous Fe₁Co₁–N–C DAC displays an outstanding ORR performance, outperforming the benchmark Pt/C catalyst and reference Fe₁–N–C and Co₁–N–C SACs in a three-electrode system. *In situ* DRIFTS and Raman studies successfully revealed the main intermediate species in the 4e[−] ORR process over Fe₁Co₁–N–C DAC. Furthermore, the Fe₁Co₁–N–C DAC based ZAB shows excellent performance: it affords a very high energy density of 1079 W h kg_{Zn}^{−1}, the best-ever rate capability (from 2 to 600 mA cm^{−2}) as far as we know, and ultra-long ZAB cycling stability of over 3600 h/7200 cycles (150 days) at 5 mA cm^{−2}. The excellent ZAB performance of the Fe₁Co₁–N–C DAC demonstrates its great practical potential and the importance and advantages of the rational synthesis of DACs.

Results and discussion

pH-field coupled microkinetic modeling of DACs in the ORR

We first applied a pH-field coupled microkinetic model for theoretical analysis to enhance our mechanistic understanding and thereby guide the development of DACs. Fig. 1(a) presents the typical atomic configuration of SACs and DACs. The structure of a central metal atom bonded to four nitrogen atoms is widely recognized as an active and stable site for ORRs and is thus used as the typical configuration for SACs.^{3,7,19,20} As for DACs, previous studies by Yang *et al.*³⁶ and Karmodak *et al.*³⁷ have demonstrated that the M₁M₂–N–C catalysts depicted in Fig. 1(a) exhibit superior stability among various dual-atom structures. For this type of DAC, the metal atoms are similarly bonded to four nitrogen atoms, with two of these atoms shared between them. Next, we elucidated the reaction steps on M–N–C SACs and M₁M₂–N–C DACs (Fig. 1(b)). The conventional steps of the ORR proceed *via* a four-electron mechanism, involving the adsorption of O₂*, the formation of HOO*, the cleavage of the O–O bond within HOO*, and the elimination of HO*. The inter-metallic distance in DACs is approximately 2.3 Å, nearly double the length of the O–O bond in O₂ (1.24 Å) and HOO* (1.43 Å), suggesting that the cooperative effect of M₁ and M₂ may not directly facilitate the O–O bond cleavage in O₂ and HOO*.^{38,39} Consequently, the ORR is proposed to transpire independently at the two metallic sites (Fig. 1(b)). To investigate whether the O–O bond in O₂ and HOO* would break due to the presence of dual metal sites, we performed additional



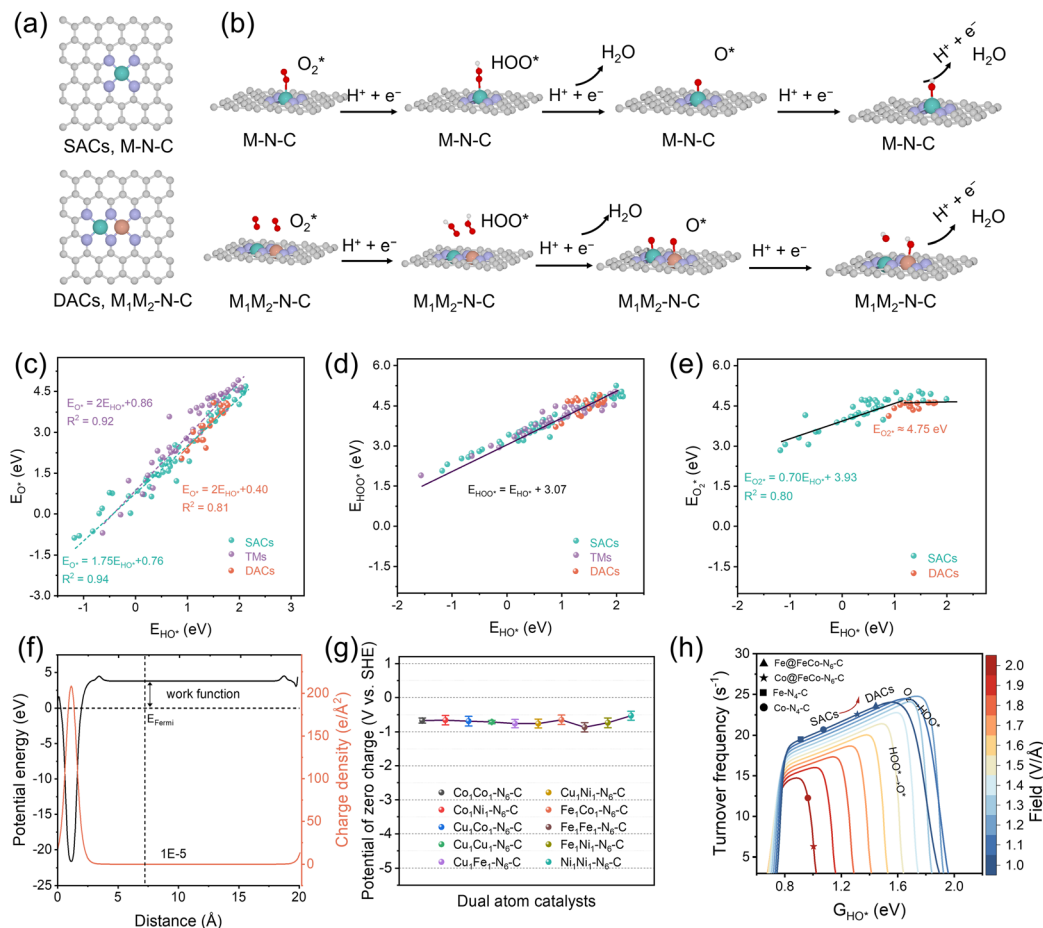


Fig. 1 pH-field coupled microkinetic modeling of DACs in the ORR. (a) The typical atomic configuration of SACs and DACs. The distance between the two metal atoms is approximately 2.3 Å in DACs. M = Mn, Fe, Co, Ni, or Cu. (b) ORR mechanisms on SACs and DACs. Both central atoms in DACs can concurrently undergo the ORR. The bond cutoff between metal atoms and oxygen was set to 2.2 Å. (c) E_{HO^*} vs. E_{O^*} scaling relationship on the above M-N-C catalysts. The slope of DACs is greater than that of SACs, mirroring the behavior observed with surfaces of TMs. (d) Universal scaling relationship of E_{HO^*} vs. E_{HOO^*} on SACs, DACs, and TMs. (e) E_{HO^*} vs. $E_{\text{O}_2^*}$ scaling relationship on SACs and DACs. (f) The work function of Fe₁Co₁-N₆-C determined via an implicit solvation model. (g) PZCs for various DACs with distinct metal centers. (h) pH-field activity volcano for DACs, highlighting enhanced positioning of the Fe/Co atop site towards peak activity in alkaline solutions. The electric field from 1.0 to 2.0 V Å⁻¹ corresponds to a pH from 13.4 to 1.3.

calculations using the Climbing Image Nudged Elastic Band (CI-NEB) method, as shown in Fig. S1, ESI†. For the adsorption of O₂ on the Fe₁-Co₁-N-C diatomic catalyst, the energy barrier for O-O bond cleavage from the initial molecular state to the final dissociated state is approximately 1.3 eV (Fig. S1a, ESI†), which is not thermodynamically spontaneous. In the case of HOO*, the energy barrier for its transition from the initial to the final state is around 0.75 eV. Additionally, for HOO* adsorbed on Fe-N-C, proton-electron transfer leads to direct O-O bond cleavage with an almost negligible energy barrier.⁴⁰ Based on these results, we conclude that O₂ and HOO* do not undergo direct O-O bond cleavage on the diatomic surface.

Next, to develop a microkinetic model, we initially calculated data to understand how the binding energies of different species (O*, HOO*, and O₂*) correlate with HO* across various materials, including TMs, SACs, and DACs (Fig. 1(c)-(e) and Table S1, ESI†). The relationship between O* and HO* on TMs reveals a slope of 2, a phenomenon coherently elucidated by d-band theory.⁴¹ For SACs, this ratio slightly drops to 1.75,

attributed to N coordination affecting d-electron states. Conversely, DACs exhibit a d-electron behavior very similar to that of TMs, with a ratio of 2, suggesting fundamentally different adsorption mechanisms between SACs and DACs. Another observed universal trend (HO* vs. HOO*) in DACs (Fig. 1(d)) shares a common intercept with TMs and SACs. In the case of O₂* and HO*, we previously identified a linear correlation for strong-binding surfaces on SACs.⁴² However, for SACs with an E_{HO^*} above 1.5 eV, O₂*'s binding energy stabilizes around 4.9 ± 0.2 eV, marking a shift from chemical to physical adsorption.^{42,43} This trend is similar to that observed in DACs. These correlations enable us to employ a single descriptor, E_{HO^*} , to create a more accurate activity volcano model, offering an advantage over traditional free energy diagrams.

We further calculated the potential of zero charge (PZC) for DACs to understand how pH levels affect the ORR performance of DACs (Fig. 1(f)). This step is crucial to theoretically determine the strength of the electric field around the catalyst. We used the vacuum level at a very low charge density (less than

$1 \times 10^{-5} \text{ e } \text{\AA}^{-2}$) to calculate the work function in a model that simulates the solvent environment (see the ESI† for more details). The PZCs stay around -0.70 V relative to the standard hydrogen electrode (SHE) (Fig. 1(g)). Using these PZC values and our established scaling relationships, we then modeled the ORR activity across different electric fields, ranging from 1.0 to $2.0 \text{ V } \text{\AA}^{-1}$ (Fig. 1(h)). This corresponds to pH levels from very acidic (1.3, shown with a red line) to very basic (13.4, shown with a blue line). The specific modeling approach can be found in the Methods section.

Our models show that in alkaline solutions, the turnover frequency (TOF) approaches the maximum ORR activity when the energy descriptor G_{HO^*} is about $1.65\text{--}1.70 \text{ eV}$. In all the DACs including $\text{Cu}_1\text{Ni}_1\text{-N}_6\text{-C}$, $\text{Cu}_1\text{Cu}_1\text{-N}_6\text{-C}$, $\text{Co}_1\text{Ni}_1\text{-N}_6\text{-C}$, $\text{Cu}_1\text{Fe}_1\text{-N}_6\text{-C}$, $\text{Ni}_1\text{Ni}_1\text{-N}_6\text{-C}$, $\text{Fe}_1\text{Co}_1\text{-N}_6\text{-C}$, $\text{Fe}_1\text{Fe}_1\text{-N}_6\text{-C}$, $\text{Co}_1\text{Co}_1\text{-N}_6\text{-C}$, $\text{Cu}_1\text{Co}_1\text{-N}_6\text{-C}$, and $\text{Fe}_1\text{Ni}_1\text{-N}_6\text{-C}$, the two metal sites in $\text{Fe}_1\text{Co}_1\text{-N}_6\text{-C}$ exhibit the most favorable binding free energies (Table S2, ESI†). This suggests that a $\text{Fe}_1\text{Co}_1\text{-N}_6\text{-C}$ catalyst performs better than SACs and other DACs in alkaline environments. To further understand the better performance of DACs, we analyzed the influence of metal atom proximities on the adsorption properties and charge transition. We find that the approaching of the M_1 and M_2 atoms significantly impacts the adsorption strength of the intermediates in the ORR. For instance, while the adsorption free energy G_{HO^*} on $\text{Fe}_1\text{-N-C}$ and $\text{Co}_1\text{-N-C}$ is calculated to be 0.61 and 0.94 eV , it significantly increases to approximately $1.56\text{--}1.66 \text{ eV}$ on $\text{Fe}_1\text{Co}_1\text{-N-C}$. This dual-metal configuration reduces the adsorption strength, thus modifying the ORR catalytic performance. In addition, we also analyzed the activity of M-pyrrolic-N and graphite-N (Fig. S2, ESI†). The adsorption free energies of HO^* on Fe-pyrrolic-N, Co-pyrrolic-N, and graphite-N are 0.67 eV , 0.87 eV , and 2.41 eV , respectively. According to the ORR volcano plot for M-N-C materials (Fig. 1(h)), the optimal adsorption free energy of HO^* for the most active reaction sites is approximately 1.6 eV . This suggests that while Fe-pyrrolic-N and Co-pyrrolic-N exhibit some ORR activity, their performance is inferior to the active sites in $\text{Fe}_1\text{-Co}_1\text{-N-C}$. In contrast, the ORR activity of graphite-N is significantly lower. More analyses on the differential charge densities and Bader charges of the interaction of two metal atoms in DACs can be found in the ESI† (Fig. S3 and Table S3). In acidic environments, our model aligns well with experimental observations; for instance, $\text{Fe}_1\text{Ru}_1\text{-N}_6\text{-C}$ demonstrates a G_{HO^*} of approximately 1.0 eV , indicating high performance in both alkaline and acidic solutions.³⁹ This underscores its reliability in screening DACs.

Additionally, we compared the binding strengths of metal atoms in $\text{Fe}_1\text{-N-C}$ and $\text{Co}_1\text{-N-C}$ SACs and $\text{Fe}_1\text{Co}_1\text{-N-C}$ DACs (Fig. S4, ESI†); DACs containing Fe and Co atoms exhibit a significant trend in stability. The binding energy decreases from -10.0 to -10.5 eV for Co-based structures and from -11.5 to -12.2 eV for Fe-based structures when transitioning from SACs to DACs. This consistent enhancement in binding strength suggests that the introduction of a second metal atom significantly improves the structural stability of the catalyst. Based on all the observations above, a DAC with $\text{Fe}_1\text{Co}_1\text{-N}_6$

structures as active sites is identified as the optimal choice for the ORR catalysts by our pH-field coupled microkinetic modeling, which not only possesses the best intrinsic ORR activity among TMs, SACs, and DACs, but also promises enhanced stability.

Synthesis and characterization of porous $\text{Fe}_1\text{Co}_1\text{-N-C}$ DAC

ORR catalytic performance is not solely determined by the active sites. Pore structures, which determine the accessibility of active sites and the transport properties of ORR-relevant intermediates, play an equally important role as active sites for ORR performance.^{44,45} Based on this understanding and our theoretical prediction, a DAC with $\text{Fe}_1\text{Co}_1\text{-N}_6$ structures as active sites and a porous structure for accessing of active sites is expected to possess an excellent ORR performance. Therefore, we developed a hard-template method following a CO_2 activation process for the construction of a porous $\text{Fe}_1\text{Co}_1\text{-N-C}$ DAC (Fig. 2(a), see the Methods section for details on the synthesis methods).⁴⁶ Briefly, the SiO_2 hard templates (that is, SiO_2 nanopowders) were first added into an aqueous solution containing Fe and Co ions, and *o*-phenylenediamine (*o*PD). Then ammonium peroxydisulphate ($(\text{NH}_4)_2\text{S}_2\text{O}_8$) was used to polymerize *o*PD to obtain the $\text{SiO}_2@\text{PoPD}$ composite. Next, the composites underwent pyrolysis, NaOH and H_2SO_4 etching to afford primary $\text{Fe}_1\text{Co}_1\text{-N-C}$. Finally, the prepared primary $\text{Fe}_1\text{Co}_1\text{-N-C}$ was subjected to a second heat treatment under CO_2 to further enhance the porosity, affording the hierarchically porous DAC (denoted as $\text{Fe}_1\text{Co}_1\text{-N-C}$). The optimized pyrolysis temperature was found to be 800°C , and the optimal CO_2 activation time was 20 min (Fig. S5 and Tables S4, S5, ESI†). The loading amounts of Fe and Co in $\text{Fe}_1\text{Co}_1\text{-N-C}$ were determined to be 1.0 and $1.4 \text{ wt\%}$, respectively, by inductively coupled plasma-mass spectrometry (ICP-MS; Table S6, ESI†).

We first used transmission electron microscopy (TEM) to investigate microstructures of $\text{Fe}_1\text{Co}_1\text{-N-C}$, which displays an interconnected vesicular structure with well-defined mesopores originating from SiO_2 nanotemplates (Fig. 2(b) and Fig. S6, ESI†). No nanoparticles or clusters can be observed for $\text{Fe}_1\text{Co}_1\text{-N-C}$. We further employed high-angular annular dark field scanning transmission electron microscopy (HAADF-STEM) to confirm the presence of atomically dispersed dual-atom sites within $\text{Fe}_1\text{Co}_1\text{-N-C}$. The high-resolution HAADF-STEM image (Fig. 2(c)) reveals the coexistence of a large number of dimers (marked by red rectangles) and a small number of single atoms. Statistical distances of adjacent dual-atom sites are about $2.3 \text{ \AA}$ (Fig. 2(d) and (e)), consistent with our modeled structure in Fig. 1(a). Considering that the distance of $2.3 \text{ \AA}$ is larger than that of direct bonding between dual-atom sites, it indicates that dual-atoms in $\text{Fe}_1\text{Co}_1\text{-N-C}$ are adjacent but not bonded. Statistical analysis showed that the dual-atom pairs account for *ca.* 74% of all discernible bright spots (Fig. 2(d)–(g) and Fig. S7, S8, ESI†). The energy-dispersive X-ray spectroscopy (EDS) mapping images (Fig. 2(h)) show homogeneous distributions of Fe and Co sites over the whole nitrogen doped carbon (N-C) support, suggesting the formation of Fe-Co dual-atom pairs. Moreover, powder X-ray diffraction (PXRD; Fig. 2(i)) reveals the graphitic



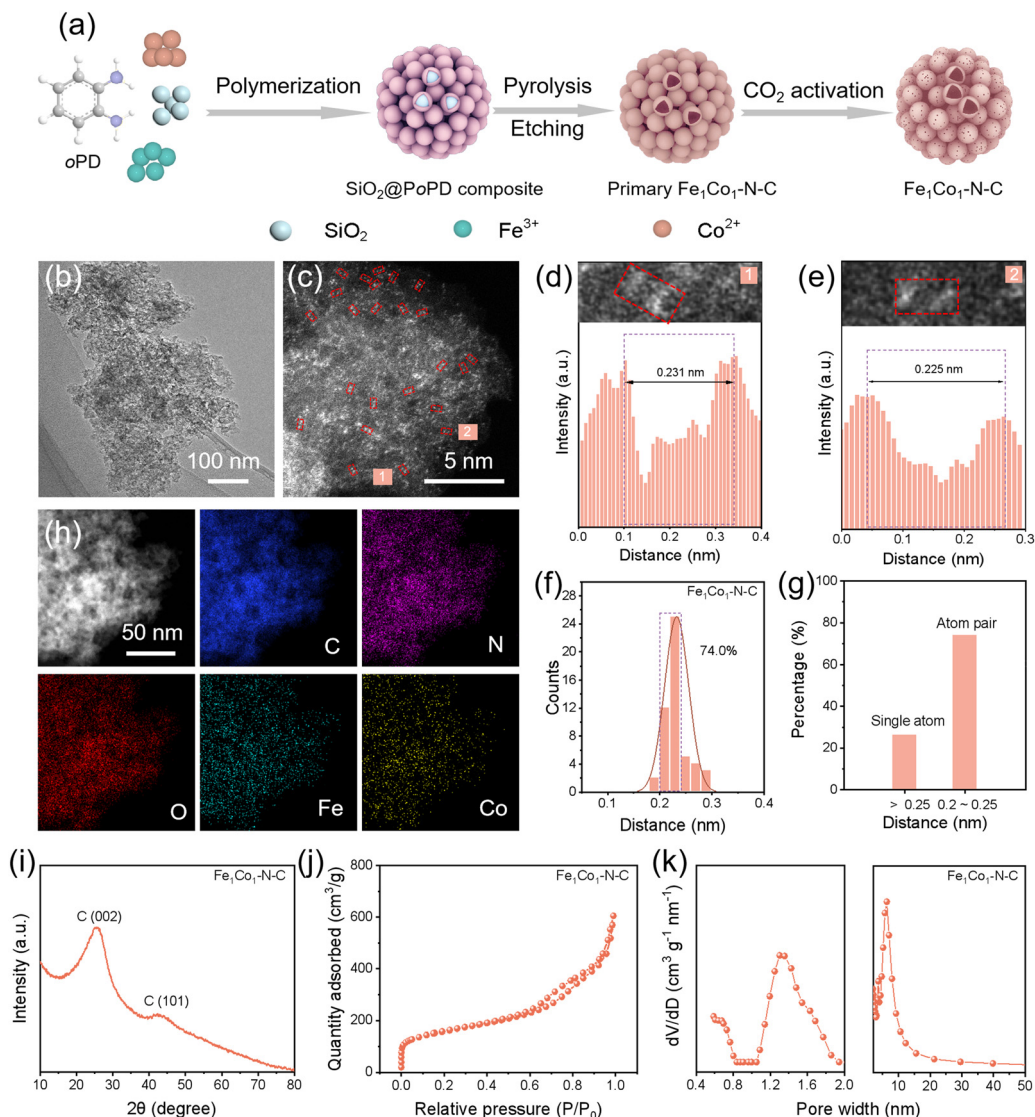


Fig. 2 Synthesis and characterization of $\text{Fe}_1\text{Co}_1\text{-N-C}$ DAC. (a) Illustration of the preparation procedures of the $\text{Fe}_1\text{Co}_1\text{-N-C}$. (b) TEM and (c) HAADF-STEM image of $\text{Fe}_1\text{Co}_1\text{-N-C}$ with dual atoms marked by red rectangles. (d) and (e) Upper parts are the randomly selected images in the red rectangles in (c), the lower parts are the intensity profiles of dual-atom sites. (f) Statistical distances in the dual-atom sites of $\text{Fe}_1\text{Co}_1\text{-N-C}$. (g) Statistical percentage of single atoms and dual atoms for at least 50 sites of $\text{Fe}_1\text{Co}_1\text{-N-C}$. (h) EDS mapping images of $\text{Fe}_1\text{Co}_1\text{-N-C}$. (i) XRD, (j) N_2 adsorption/desorption isotherms, and (k) pore size distribution curves of $\text{Fe}_1\text{Co}_1\text{-N-C}$. Note: a. u. means arbitrary units unless otherwise specified.

carbon structure for $\text{Fe}_1\text{Co}_1\text{-N-C}$, consistent with the Raman result (Fig. S9, ESI[†]). The PXRD pattern also confirms no obvious metallic particles or clusters in the $\text{Fe}_1\text{Co}_1\text{-N-C}$, which is also revealed by numerous TEM and HAADF-STEM observations. To demonstrate that our developed hard-template method following a CO_2 activation process can create hierarchically porous structures within the $\text{Fe}_1\text{Co}_1\text{-N-C}$ catalyst, we used the N_2 sorption method to analyze its pore structures. $\text{Fe}_1\text{Co}_1\text{-N-C}$ exhibits a type-IV isotherm characteristic for mesoporous materials (Fig. 2(j)); its Brunauer-Emmett-Teller (BET) surface area is $531.5 \text{ m}^2 \text{ g}^{-1}$ (Table S7, ESI[†]). The pore size distribution curves clearly indicate that the $\text{Fe}_1\text{Co}_1\text{-N-C}$ possesses abundant micropores and mesopores centered at 1.4 and 6.2 nm (Fig. 2(k)), respectively, suggesting that the hierarchical porous

structure has formed within our $\text{Fe}_1\text{Co}_1\text{-N-C}$ catalyst. In addition, we also synthesized $\text{Fe}_1\text{-N-C}$, $\text{Co}_1\text{-N-C}$, and N-C as control samples using the same method. All characterization techniques including TEM, HAADF-STEM, PXRD, Raman, EDS mapping, and N_2 sorption demonstrate that they possess similar structure properties to $\text{Fe}_1\text{Co}_1\text{-N-C}$ (Fig. S10–S18, Tables S6, S7 and Note S1, ESI[†]).

Atomic and electronic structural characterization of $\text{Fe}_1\text{Co}_1\text{-N-C}$ catalysts

We conducted X-ray photoelectron spectroscopy (XPS) and X-ray absorption spectroscopy (XAS) analysis to further reveal the atomic structures of our catalyst and explore the compositions and chemical states of the surface elements (Fig. 3). In the



XPS results (Fig. 3(a) and Fig. S19a, ESI†), the high-resolution Fe 2p spectra at 711.3, 722.5 eV and 713.9, 725.6 eV for Fe₁Co₁-N-C and Fe₁-N-C can be assigned to Fe²⁺ and Fe³⁺, respectively. Two peaks at 718.2 and 731.1 eV are the satellite peaks.^{30,32,47} Similarly, the prominent peaks of Co 2p_{3/2} (~780.9 eV) and Co 2p_{1/2} (~796.2 eV) with the corresponding satellite peaks (~786.2 and ~803.5 eV) appear in the Fe₁Co₁-N-C and Co₁-N-C (Fig. 3(b)) spectra.^{32,48} XPS results suggest that both Fe and Co elements are in the oxidative states in these catalysts. No obvious Si 2p XPS signal was detected for all the catalysts, suggesting that the SiO₂ templates had been completely removed (Fig. S19b, ESI†).⁴⁹ Meanwhile, the N 1s spectra of

all the catalysts show the presence of pyridinic N (397.8 eV), pyrrolic N (399.5 eV), graphitic N (400.9 eV), and oxidized N (404.1 eV) species (Fig. 3(c)).^{22,28,50}

In the Fe K-edge X-ray absorption near-edge structure (XANES) spectra, the near-edge absorption of Fe₁Co₁-N-C is located between Fe foil and Fe₂O₃ and is lower than Fe₁-N-C (Fig. 3(d)). The valence states of Fe in the Fe₁Co₁-N-C and Fe₁-N-C samples are between Fe⁰ and Fe³⁺.^{21,24,51,52} Furthermore, the Co K-edge XANES spectra (Fig. 3(g)) show the white line intensity and the pre-edge energy of Fe₁Co₁-N-C and Co₁-N-C are located between Co foil and Co₃O₄, suggesting the Co valence state is also positive.^{16,24,31,53} The XANES spectra results are consistent with the XPS analysis.

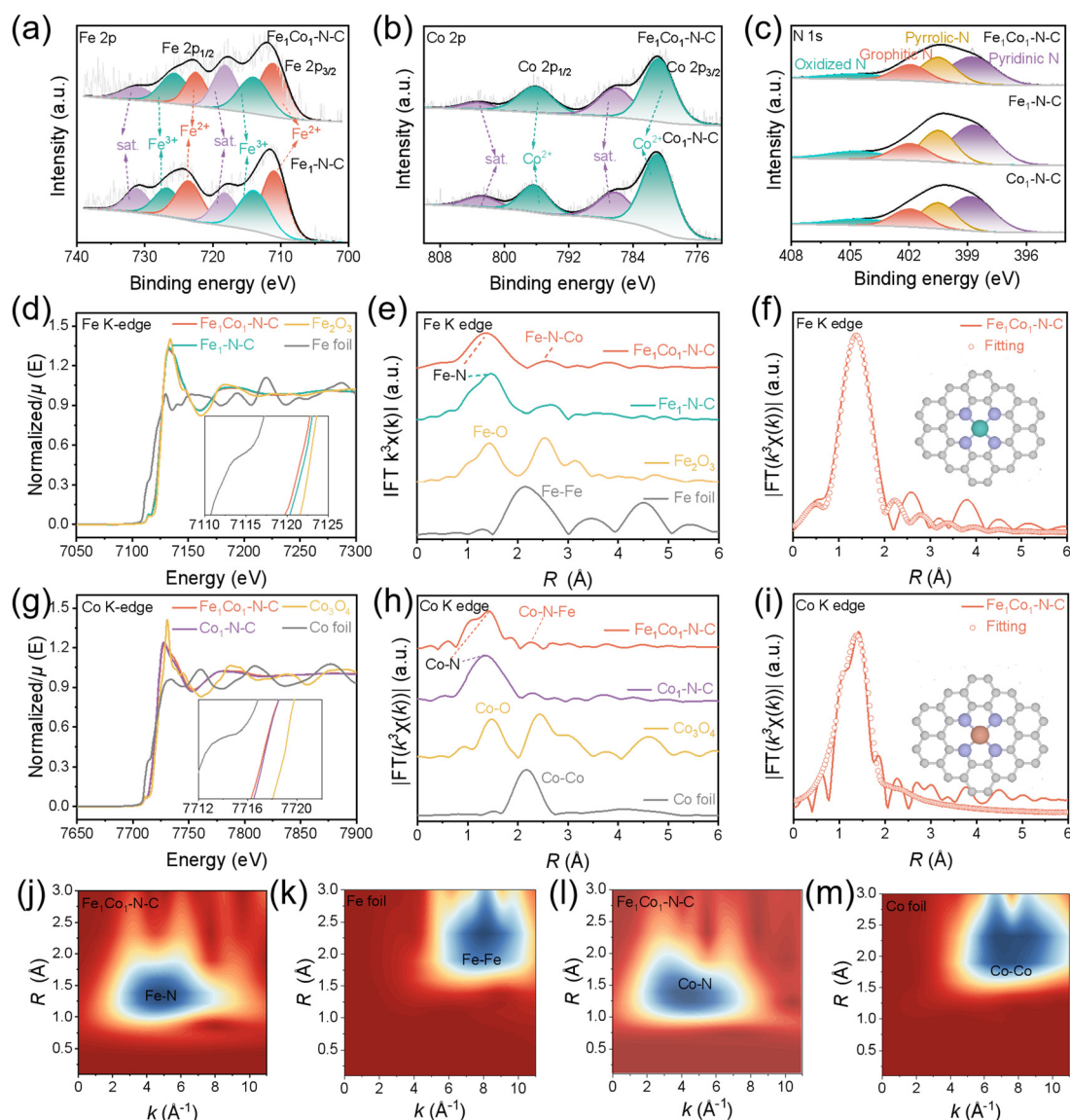


Fig. 3 Surface properties, atomic and electronic states of Fe₁Co₁-N-C and reference catalysts. High-resolution XPS spectra of (a) Fe 2p, (b) Co 2p, and (c) N 1s for Fe₁Co₁-N-C, Fe₁-N-C, and Co₁-N-C. (d) Fe K-edge XANES spectra of Fe₁Co₁-N-C, Fe₁-N-C, Fe₂O₃, and Fe foil. (g) Co K-edge XANES spectra of Fe₁Co₁-N-C, Co₁-N-C, Co₃O₄, and Co foil. FT EXAFS spectra at the R space of (e) Fe and (h) Co. (f) and (i) FT EXAFS spectra and the corresponding curve-fitting results of the Fe₁Co₁-N-C. Inset: Schematic models: Fe (green), N (purple), and C (gray), respectively. (j)–(m) WT of $\chi(k)$ of Fe and Co for Fe₁Co₁-N-C, Fe foil, and Co foil. R is the bond length; FT means Fourier transform; WT is Wavelet transform. In the Fe₁Co₁-N-C DAC, FeN₄ and CoN₄ sites mainly exist in the form of the Fe₂Co₁-N₆ model with a non-bonding Fe–Co path; in Fe₁-N-C and Co₁-N-C SACs, FeN₄ and CoN₄ structures are the metal active sites, respectively.



Fourier transformed (FT) *R*-spaced extended X-ray absorption fine structure (EXAFS) spectra of Fe₁Co₁-N-C show the prominent peaks at around 1.42 and 2.50 Å attributed to the first shell Fe-N and Fe-N-Co coordination scattering in Fe₁Co₁-N-C (Fig. 3(e)).^{54,55} No Fe-Fe scattering paths were found at 2.22 Å in Fe₁Co₁-N-C and Fe₁-N-C, indicating the absence of Fe clusters or nanoparticles in Fe₁Co₁-N-C and Fe₁-N-C. In the FT *R*-spaced EXAFS spectra at the Co K-edge (Fig. 3(h)), Fe₁Co₁-N-C and Co₁-N-C both exhibit the Co-N peak at around 1.48 Å with no Co-Co peak (2.1 Å), confirming the atomic-scale dispersion of Co species. Additionally, there is a small peak at 2.25 Å in the Co K-edge EXAFS of Fe₁Co₁-N-C, which can be attributed to Co-N-Fe.⁵⁴⁻⁵⁶ Considering the EXAFS results and HADDF-STEM observations, Fe₁Co₁-N-C with Fe-Co dual-atom pairs was successfully synthesized. To reveal the atomic structures of Fe₁Co₁-N-C DAC, Fe₁-N-C, and Co₁-N-C SACs, we performed fitting for the EXAFS spectra. The fitting of the Fe configuration for Fe₁Co₁-N-C, Fe₁-N-C, Fe foil, and Fe₂O₃ is shown in Fig. 3(f), Fig. S20a, S21a-c, S22a, b, S23a-c, and Table S8, ESI†. The coordinated numbers are both about 4, and the bond lengths between Fe and N are around 2.0 Å for both Fe-containing catalysts (the inset in Fig. 3(f)). Co K-edge EXAFS fitting results show that the Co site is also bonded with four contiguous N atoms to form a Co-N₄ structure in Fe₁Co₁-N-C and Co₁-N-C, and the average bond lengths of Co-N are 1.93 and 1.97 Å, respectively (Fig. 3(i), Fig. S20b, S21d-f, S22c-d, S23d-f, and Table S9, ESI†). Wavelet transform (WT) analysis was further performed to investigate the Fe, Co K-edge EXAFS oscillations of Fe₁Co₁-N-C (Fig. 3(j) and (k)). Fe₁Co₁-N-C demonstrates an intensity maximum at (4.80 Å⁻¹, 1.34 Å) with much smaller wave vector *k* and bond length *R* than Fe foil (8.02 Å⁻¹, 2.32 Å), indicating a lower coordinated atomic number and shorter bond length for Fe atoms in Fe₁Co₁-N-C. This could be attributed to the Fe-N bonding. Similar results for Co atoms were obtained from Co K-edge WT analysis (Fig. 3(l) and (m)). We also calculated the ratio of DACs and SACs by using the EXAFS spectrum and the peak fitting results from the XANES spectrum (Fig. S24, ESI†).⁵⁷ Combining the above HAADF-STEM observations and XAFS analysis, we can conclude that FeN₄ and CoN₄ sites mainly exist in the form of a Fe₁Co₁-N₆ model with a non-bonding Fe-Co path in Fe₁Co₁-N-C, which agrees well with our predicted structures with optimal performance. Additionally, FeN₄ and CoN₄ structures represent the metal active sites for Fe₁-N-C and Co₁-N-C, respectively.

ORR performance

With desirable Fe₁Co₁-N₆ active sites and porous structures, Fe₁Co₁-N-C DAC is expected to exhibit excellent ORR performance. Therefore, we carried out rotating disk electrode (RDE) tests in 0.1 M KOH to investigate its ORR performance. The reference catalysts including Fe₁-N-C, Co₁-N-C, and N-C as well as the benchmark Pt/C catalyst were also tested under the same conditions for comparison. The cyclic voltammetry (CV) curves in Ar- or O₂-saturated electrolyte were recorded in the potential range from 0 to 1.2 V (Fig. S25, ESI†). The cathodic peak occurring on Fe₁Co₁-N-C is more positive than those of

Fe₁-N-C, Co₁-N-C, N-C, and Pt/C catalysts, which indicated that the Fe₁Co₁-N-C DAC exhibits the best catalytic capability for the ORR among all the tested catalysts. We further evaluated the ORR catalytic activity by linear sweep voltammetry (LSV) (Fig. 4(a)). The Fe₁Co₁-N-C catalyst exhibits a more positive onset potential (*E*_{onset}, 1.00 V) and half-wave potential (*E*_{1/2}, 0.882 V) than those of benchmark Pt/C (*E*_{onset}, 0.97 V; *E*_{1/2}, 0.851 V), Fe₁-N-C (*E*_{onset}, 0.98 V; *E*_{1/2}, 0.847 V), Co₁-N-C (*E*_{onset}, 0.94 V; *E*_{1/2}, 0.848 V), and N-C (*E*_{onset}, 0.88 V; *E*_{1/2}, 0.772 V). Additionally, the kinetic current density (*J*_k) of Fe₁Co₁-N-C at 0.85 V (13.0 mA cm⁻²) is superior to Pt/C (3.88 mA cm⁻²), and also higher than Fe₁-N-C (4.6 mA cm⁻²), Co₁-N-C (4.5 mA cm⁻²), and N-C (0.1 mA cm⁻²) (Fig. 4(b)). The better ORR activity of Fe₁Co₁-N-C than those of SACs and TMs can be attributed to the fact that the Fe₁Co₁-N₆ dual metal sites in Fe₁Co₁-N-C exhibit the most favorable binding free energies for intermediates in the ORR process. Moreover, the fitted Tafel slope for Fe₁Co₁-N-C (60 mV dec⁻¹) is much lower than Fe₁-N-C (76 mV dec⁻¹), Co₁-N-C (79 mV dec⁻¹), and Pt/C (85 mV dec⁻¹), evidencing the Fe₁Co₁-N-C DAC has the most efficient ORR kinetics among all of the tested catalysts (Fig. 4(c)). In addition, the electrical double layer capacitance (*C*_{dl}) of Fe₁Co₁-N-C is up to 90.0 mF cm⁻², higher than SACs (Fe₁-N-C: 82.7 mF cm⁻², Co₁-N-C: 78.5 mF cm⁻²) and N-C (35.6 mF cm⁻²), indicating that the Fe₁Co₁-N-C has the largest accessible electrochemical surface area (ECSA, 884.1 cm²) (Fig. S26, ESI†). Of note, the ECSA normalized LSV curves show Fe₁Co₁-N-C still exhibits the best activity, which indicates its intrinsically highest activity,^{58,59} agreeing well with our simulation results (Fig. S27, ESI†).

The Koutecky-Levich (K-L) equation was used to further elucidate the ORR process. According to the K-L plots, the electron transfer number (*n*) is determined to be 3.9 for Fe₁Co₁-N-C (Fig. 4(d) and (e)), which is higher than other reference catalysts (Fe₁-N-C: *n* = 3.8; Co₁-N-C: *n* = 3.8; N-C: *n* = 3.3; Fig. S28, ESI†), demonstrating a four-electron pathway and high selectivity for reducing O₂ to OH⁻ over Fe₁Co₁-N-C. Moreover, we employed rotation ring-disk electrode (RRDE) tests to assess hydrogen peroxide (H₂O₂) production and determine the number of electrons transferred (*n*) during the ORR process (Fig. 4(f) and Fig. S29, ESI†). The H₂O₂ yield of Fe₁Co₁-N-C is less than 7% over wide potentials (0.2 to 0.8 V). The value of *n* is 3.9 and very close to commercial Pt/C (*n* ≈ 4.0), suggesting once again that Fe₁Co₁-N-C shows a high-efficiency 4e⁻ ORR pathway.

The stability plays a crucial role in practical applications. We thus investigated the stability of Fe₁Co₁-N-C for the ORR by chronoamperometry (*i*-*t*) and CV cycling tests. The *i*-*t* measurements (Fig. 4(g) and Fig. S30, ESI†) show that Fe₁Co₁-N-C well retains its pristine catalytic activity even with a slight increase after a 48 h test (at 0.6 V, in an O₂-saturated electrolyte, at 1600 rpm). The slight improvement in ORR performance for the Fe₁Co₁-N-C catalyst after the stability test should be attributed to the surface activation process during the stability test. The prepared Fe₁Co₁-N-C catalyst is a highly porous material. During the stability test process, more active sites were gradually exposed to O₂ dissolved in the electrolyte, resulting in



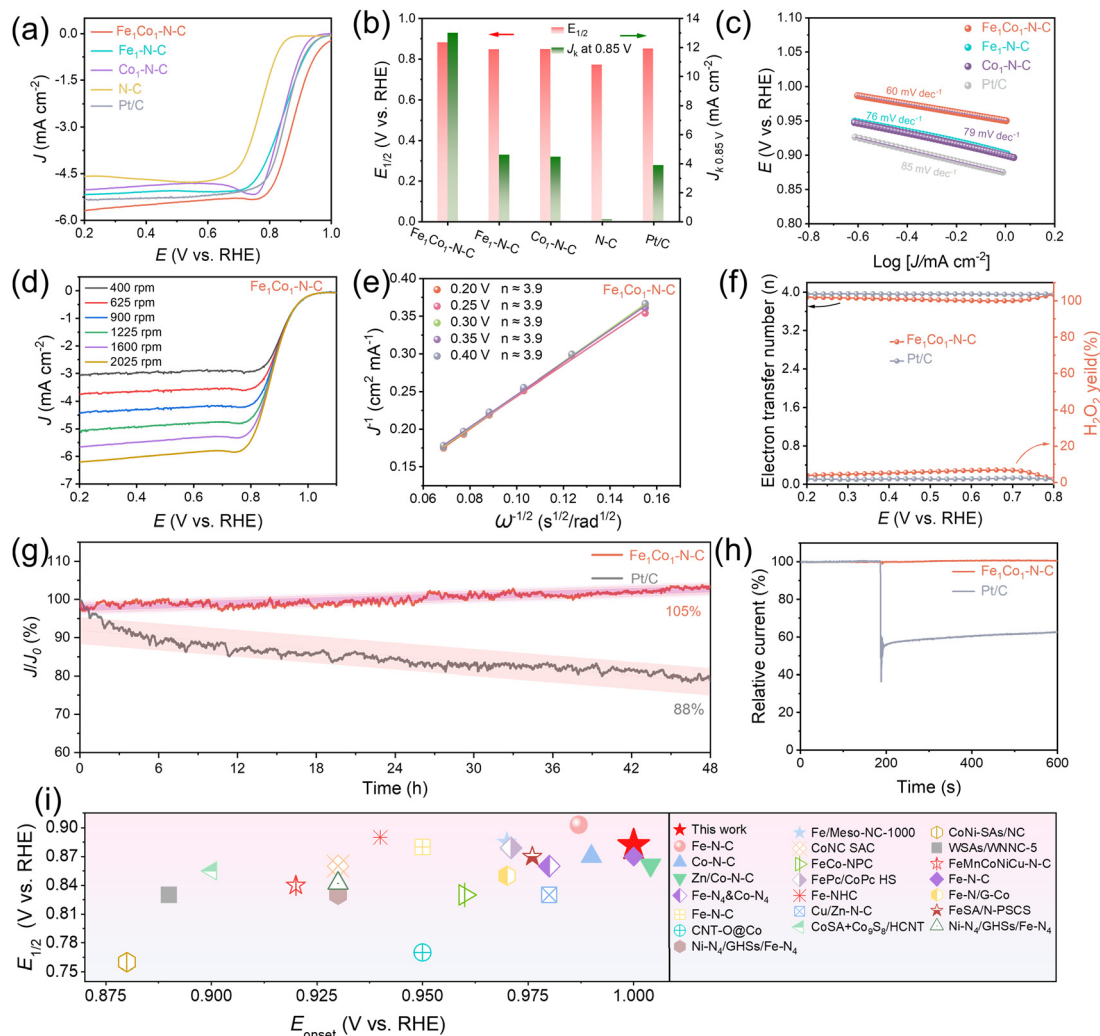


Fig. 4 Electrochemical ORR performance evaluated by RDE and RRDE tests. (a) LSV curves, (b) comparison of $E_{1/2}$ and J_k at 0.85 V, and (c) Tafel plots for $\text{Fe}_1\text{Co}_1\text{-N-C}$ and reference samples ($\text{Fe}_1\text{-N-C}$, $\text{Co}_1\text{-N-C}$, and Pt/C). (d) Polarization curves of $\text{Fe}_1\text{Co}_1\text{-N-C}$ at different rotation rates and (e) the K-L fitting lines at different potentials. (f) H_2O_2 yield and the electron transfer number (n) values for $\text{Fe}_1\text{Co}_1\text{-N-C}$ and Pt/C . (g) Normalized chronoamperometric curves of the ORR for $\text{Fe}_1\text{Co}_1\text{-N-C}$ and Pt/C during 48 h stability tests. (h) Chronoamperometric methanol resistance tests of $\text{Fe}_1\text{Co}_1\text{-N-C}$ and Pt/C . (i) Activity comparison of $\text{Fe}_1\text{Co}_1\text{-N-C}$ with other reported ORR catalysts. The $\text{Fe}_1\text{Co}_1\text{-N-C}$ exhibits a high ORR catalytic activity and excellent stability in the three-electrode system.

improved catalytic activity. This performance surpasses that of commercial Pt/C (88% retention) as well as SACs ($\text{Fe}_1\text{-N-C}$ with 96% retention; $\text{Co}_1\text{-N-C}$ with 98% retention). The poor stability of Pt/C catalysts in alkaline ORR is mainly due to three main factors: (1) surface reconstruction and dissolution of Pt ; (2) agglomeration of Pt nanoparticles during prolonged operation; and (3) corrosion of the carbon support. In addition, the excellent stability of $\text{Fe}_1\text{Co}_1\text{-N-C}$ was also confirmed by CV cycling tests; only a 2 mV negative shift on $E_{1/2}$ is observed for $\text{Fe}_1\text{Co}_1\text{-N-C}$ after 5000 continuous cycles (Fig. S31, ESI[†]), much lower than that of commercial Pt/C (20 mV). Importantly, we found the chemical properties of $\text{Fe}_1\text{Co}_1\text{-N-C}$ were well retained (Fig. S32, ESI[†]) after the stability test, further suggesting its excellent stability toward the ORR. In addition, $\text{Fe}_1\text{Co}_1\text{-N-C}$ also exhibits excellent methanol-poisoning resistance with negligible decay in the current density after injecting 3 M

methanol (Fig. 4(h)), superior to the Pt/C catalyst. Impressively, the ORR performance in terms of E_{onset} and $E_{1/2}$ of our $\text{Fe}_1\text{Co}_1\text{-N-C}$ is among the best of recently reported carbon-based SACs, DACs and other catalysts (Fig. 4(i) and Table S10, ESI[†]; all these literature data are also available in the Digital Catalysis Platform database for reliable comparison: <https://www.digcat.org/>).⁶⁰ Briefly, using the pH-field coupled microkinetic model, the $\text{Fe}_1\text{Co}_1\text{-N-C}$ DAC was synthesized with desired $\text{Fe}_1\text{Co}_1\text{-N}_6$ dual metal atomic sites and porous structures, which exhibits high ORR catalytic activity and excellent stability in a three-electrode system.

In situ studies

To reveal the ORR mechanism over the $\text{Fe}_1\text{Co}_1\text{-N-C}$ DAC, we first carried out *in situ* attenuated total reflection surface-enhanced infrared adsorption spectrum (ATR-SEIRAS) testing



during the ORR process (Fig. 5(a)). Three sets of *in situ* DRIFTS spectra are observed under different potentials (Fig. 5(b)–(d)). A characteristic C–N stretching vibration of $\text{Fe}_1\text{Co}_1\text{-N-C}$ is observed at 1338 cm^{-1} (Fig. 5(b)).⁶¹ During the negative potential scan, the intensity and frequency of the C–N peak remains nearly constant until 0.9 V; subsequently, the intensity begins to decrease, while the frequency shifts to a higher wavenumber until reaching 0.7 V; ultimately, both the intensity and frequency stay constant below 0.4 V. The meaningful transformations in intensity and frequency of the C–N peak during the ORR process matches very well with the electrochemical conversion behavior of O_2 , indicating a strong electronic interaction between O_2 and the $\text{Fe}_1\text{Co}_1\text{-N-C}$ during the ORR process.^{61,62} The peaks at 1440 and 1230 cm^{-1} belong to surface-adsorbed O_2^* and HOO^* species, respectively (Fig. 5(c) and (d)).^{63,64} To better illustrate the spectroscopic variations of intermediates during the negative potential scan, the area of 1440 and 1230 cm^{-1} peaks were plotted as functions of the potential (Fig. 5(e)). With the decreased potentials, the kinetics of the ORR is accelerated and the absorption peak of O_2^* begins to intensify until 0.8 V, after which the peak gradually diminishes; simultaneously, the HOO^* peak area is observed to weaken as the potential becomes more negative-going (Fig. 5(c)–(e)). This suggests the robust binding of $^*\text{OOH}$ to the electrode surface destabilizes the O–O bond, ultimately resulting in the complete reduction of O_2 . Furthermore, we also performed *in situ* Raman spectroscopy tests during electrochemical experiments (Fig. 5(f) and Fig. S33, ESI†). The peaks of O_2^* and HO^* adsorbed on the catalyst surface are found in 1112 and 714 cm^{-1} (Fig. 5(g)).^{65–67} As the potential

decreases from 1.0 to 0.8 V, the peak area of the O_2^* increases (Fig. 5(h) and Fig. S34, ESI†), which indicates that the adsorption of O_2 on the $\text{Fe}_1\text{Co}_1\text{-N-C}$ surface gradually reaches the maximum; after that, it diminishes gradually. Simultaneously, the peak area of the HO^* increases, reaching its peak at 0.6 V, and then gradually diminishes until it disappears completely. These experimental observations agree well with our theoretical model: at higher potentials, the rate-limiting step shifts from the reaction of O_2^* to HOO^* . However, as the potential decreases, the rate-limiting step transitions to the reaction from HOO^* to O^* . Consequently, in experiments, we observe that O_2^* and HOO^* progressively accumulate on the electrode surface as the electrode potential decreases and eventually form OH^- . Based on electron transfer number measurements and *in situ* tests, we can conclude that the $\text{Fe}_1\text{Co}_1\text{-N-C}$ catalyst participates in the typical $4e^-$ ORR pathways involving the adsorption of O_2^* , the formation of HOO^* , the cleavage of the O–O bond within HOO^* , and the elimination of HO^* , consistent with our proposed ORR mechanism (Fig. 1(b)).

ZAB performance

To evaluate the application potential of $\text{Fe}_1\text{Co}_1\text{-N-C}$ in energy conversion devices, a ZAB was assembled by applying $\text{Fe}_1\text{Co}_1\text{-N-C}$ as the catalyst for the air cathode and zinc foil as the anode with 6 M KOH + 0.2 M $\text{Zn}(\text{Ac})_2$ solution as the electrolyte (Fig. 6(a)). The $\text{Fe}_1\text{Co}_1\text{-N-C}$ based ZAB exhibits a higher open-circuit voltage (1.51 V) and a larger maximum peak power density (234 mW cm^{-2} , Fig. 6(b) and (c), Fig. S35, and Table S11, ESI†) than the ZABs based on Pt/C (1.47 V and 163 mW cm^{-2} , respectively). When normalized to the mass of

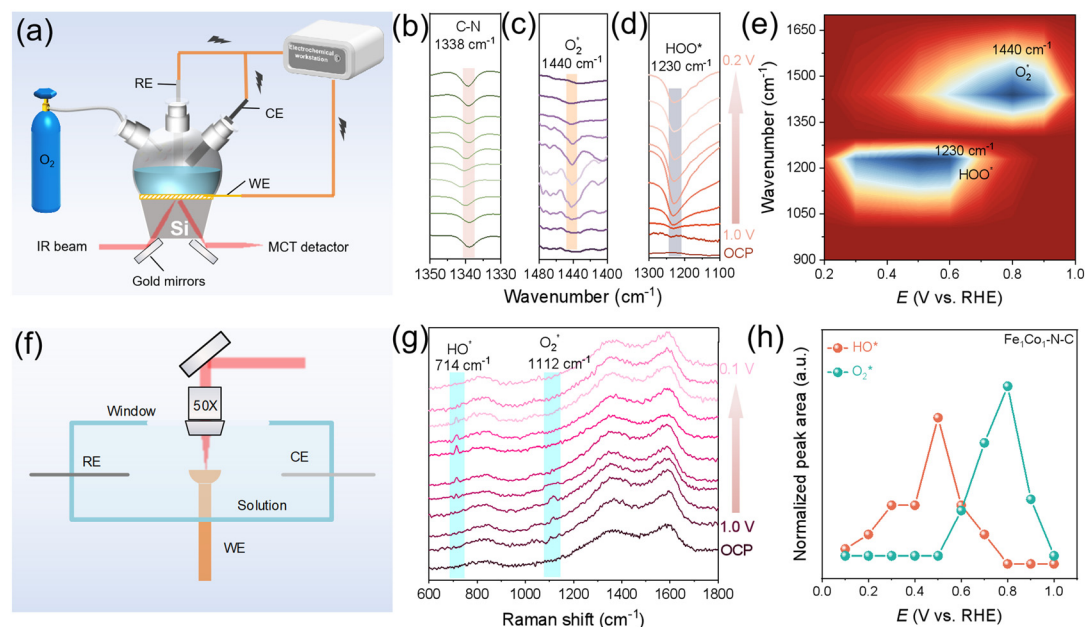


Fig. 5 *In situ* ATR-SEIRAS and *in situ* Raman studies for the ORR mechanism. (a) and (f) Scheme of the *in situ* ATR-SEIRAS and *in situ* Raman spectroscopy equipment. The working electrode, reference electrode, and counter electrode are abbreviated as WE, RE, and CE, respectively. (b)–(d) and (g) *In situ* ATR-SEIRAS and Raman spectra were recorded at different potentials for the $\text{Fe}_1\text{Co}_1\text{-N-C}$ catalyst during the ORR process. Peak area variations were taken from *in situ* (e) ATR-SEIRAS and (h) Raman spectra for $\text{Fe}_1\text{Co}_1\text{-N-C}$. Potential dependence of the normalized peak area of (e) *in situ* ATR-SEIRAS for O_2^* (1440 cm^{-1}) and HOO^* (1230 cm^{-1}), and (h) *in situ* Raman for O_2^* (1112 cm^{-1}) and HO^* (714 cm^{-1}).

zinc consumed, the specific capacity of the $\text{Fe}_1\text{Co}_1\text{-N-C}$ based ZAB is over $836.5 \text{ mA h g}_{\text{Zn}}^{-1}$ (corresponding to an energy density of *ca.* $1079 \text{ W h kg}_{\text{Zn}}^{-1}$) at a current density of 10 mA cm^{-2} , which corresponds to *ca.* 99.4% utilization of the theoretical energy density (*ca.* $1086 \text{ W h kg}_{\text{Zn}}^{-1}$). When the current density was increased to 20, 50, and 100 mA cm^{-2} , the specific capacity of the battery is 794.2, 750.1, and $436.4 \text{ mA h g}_{\text{Zn}}^{-1}$ (corresponding to an energy density of *ca.* 976.9, 817.6, and $405.9 \text{ W h kg}_{\text{Zn}}^{-1}$), respectively (Fig. 6(d)), indicating that the $\text{Fe}_1\text{Co}_1\text{-N-C}$ catalyst possesses outstanding ORR activity performance. In addition, we further tested the

rate capability of the $\text{Fe}_1\text{Co}_1\text{-N-C}$ based ZAB from 2 to 5, 10, 20, 50, 100, 300, 500, and 600 mA cm^{-2} , which has very high discharge voltages of 1.38, 1.34, 1.31, 1.27, 1.18, 1.07, 0.85, 0.63, and 0.40 V, exhibiting superior rate performance. Importantly, it also displays a superb reversibility for 11 cycles, which is much better than $\text{Fe}_1\text{-N-C}$, $\text{Co}_1\text{-N-C}$, N-C , and Pt/C based ZABs (Fig. 6(e) and (f), and Fig. S36 and S37, ESI†). As far as we know, the rate capability is the best one reported for ZABs to date (Table S12, ESI†). Impressively, the $\text{Fe}_1\text{Co}_1\text{-N-C}$ based ZAB can power a phone and light-emitting diodes (LEDs), affirming the great application potential of $\text{Fe}_1\text{Co}_1\text{-N-C}$ in energy devices

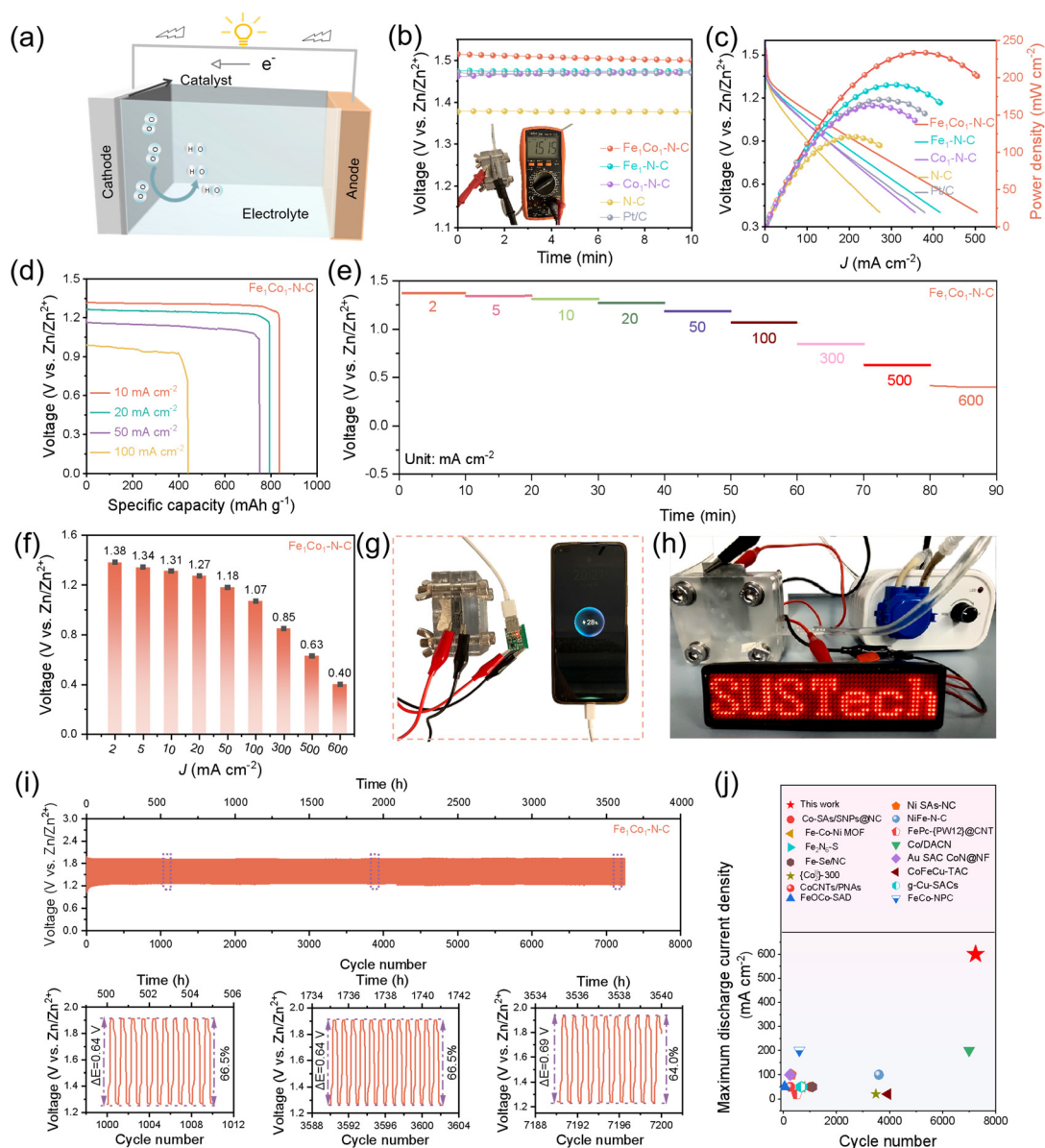


Fig. 6 ZAB performance. (a) Schematic illustration of a ZAB. (b) The OCV plots of the ZABs based on $\text{Fe}_1\text{Co}_1\text{-N-C}$ and reference catalysts ($\text{Fe}_1\text{-N-C}$, $\text{Co}_1\text{-N-C}$, N-C , and Pt/C). (c) Discharge polarization plots and corresponding power density plots of the ZABs. (d) Specific capacities of the ZAB based on $\text{Fe}_1\text{Co}_1\text{-N-C}$ at various current densities (10, 20, 50, and 100 mA cm^{-2}). (e) and (f) Discharge curves at current densities from 2 to 5, 10, 20, 50, 100, 300, 500, and 600 mA cm^{-2} for the $\text{Fe}_1\text{Co}_1\text{-N-C}$ based ZAB, and voltage values corresponding to each current density. (g) and (h) Optical images of a phone and an LED light powered by the $\text{Fe}_1\text{Co}_1\text{-N-C}$ based ZAB. (i) Cyclic stability at a current density of 5 mA cm^{-2} for the $\text{Fe}_1\text{Co}_1\text{-N-C}$ based ZAB. (j) Recently reported ZAB performances in terms of their corresponding maximum discharge current density and cycle time.



(Fig. 6(g) and (h), and Video S1, ESI†). In order to further carry out long-term galvanostatic discharge–charge cycling, $\text{Fe}_1\text{Co}_1\text{-N-C}$ was mixed with RuO_2 ,⁶⁸ a typical oxygen evolution reaction (OER) catalyst, and used as the catalyst for the air cathode. Two independent ZABs were assembled simultaneously and both demonstrate excellent and repeatable cycling stability over 3200 h (Fig. 6(i) and Fig. S38, ESI†). In particular, one ZAB displays an ultra-long stability for over 3600 h/7200 cycles with a 30 min per cycle period, which represents one of the most stable ZABs reported in the literature (Fig. 6(j) and Table S12, ESI†). The charge–discharge curves and battery round-trip energy efficiencies at 1000 cycles, 3600 cycles, and 7200 cycles are presented in the inset of Fig. 6(i). When the ZAB was cycled for 1000 cycles, the discharge and charge segment voltages were 1.26 and 1.90 V with a voltage gap of 0.64 V, and the related round-trip energy efficiency is calculated as 66.5%. When it was cycled to the end (7200 cycles), the discharge and charge voltages were 1.23 V and 1.92 V with a voltage gap of 0.69 V, and the corresponding round-trip energy efficiency is 64%. The mean capacity decay rate is only *ca.* 0.0003% per cycle. However, the Pt/C + RuO_2 based ZAB only cycled for less than 360 cycles (180 h) (Fig. S39, ESI†), and the charge–discharge voltage gap was more than 0.76 V after 180 h (initial: 66.0%; final: 58.2%; capacity decay rate of *ca.* 0.02% per cycle). All the ZAB performances strongly demonstrate that $\text{Fe}_1\text{Co}_1\text{-N-C}$ is a very promising candidate as an ORR electrocatalyst in ZABs and highlight the great potential of our $\text{Fe}_1\text{Co}_1\text{-N-C}$ DACs for future practical applications.

Conclusion

In summary, using a pH-field microkinetic model, we have rapidly identified and rationally synthesized an efficient $\text{Fe}_1\text{Co}_1\text{-N-C}$ ORR catalyst with desired $\text{Fe}_1\text{Co}_1\text{-N}_6$ dual metal atomic sites and hierarchically porous structures. Benefiting from the synergistic effect of neighboring Fe and Co dual-active centers and unique porous structures, the $\text{Fe}_1\text{Co}_1\text{-N-C}$ ORR DAC exhibits excellent performance in alkaline electrolyte and great practical application potential in ZABs. *In situ* DRIFTS and *in situ* Raman spectroscopy confirm the ORR pathway used in our pH-field microkinetic model. This work not only presents a highly efficient and rational strategy for the synthesis of high-performance ORR DACs with great practical potential, but also paves the way for designing and constructing advanced catalysts for various high-performance energy conversion applications.

Author contributions

Tingting Li: catalyst synthesis, conducted the catalytic tests, catalyst characterization, the related data processing and writing. Di Zhang: DFT calculations, theoretical modelling, and writing. Yun Zhang: catalytic tests, catalyst characterization and the related data processing. Danli Yang: validated catalyst synthesis and ORR performance data. Runxin Li: TEM and HAADF-STEM tests. Fuyun Yu: catalytic tests, catalyst

characterization and the related data processing. Kengqiang Zhong: catalytic tests, catalyst characterization and the related data processing. Xiaozhi Su: XAS tests. Tianwei Song: catalytic tests, catalyst characterization and the related data processing. Long Jiao: helped in catalyst characterization. Hai-Long Jiang: helped in catalyst characterization. Guo-Ping Sheng: helped in catalyst characterization. Jie Xu: TEM and HAADF-STEM tests. Hao Li: supervised the project, performed the DFT calculations, theoretical modelling, and writing. Zhen-Yu Wu: supervised the project and writing.

Data availability

The data supporting this article have been included as part of the ESI.† The key results of the data, all the computational structures, and the pH-dependent microkinetic model are also available in our Digital Catalysis Platform (DigCat: <https://www.digcat.org/>).

Conflicts of interest

There are no conflicts to declare.

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