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# Synthesis of magnetic core–shell Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> nanoparticles from electric arc furnace dust for photocatalytic degradation of steel mill wastewater

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The study was undertaken to design magnetic core–shell Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> nanoparticles from electric arc furnace dust and evaluate its photocatalytic activity on organic pollutant degradation from steel industry wastewater. Different molar ratios of Fe<sub>3</sub>O<sub>4</sub> to TiO<sub>2</sub> were tested on Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> nanoparticles. The materials were characterized using X-ray diffraction, X-ray photoelectron spectroscopy, Fourier transform-infrared spectroscopy, scanning electron microscopy, energy-dispersive X-ray spectroscopy, and transmission electron microscopy, and a zeta potential analyzer and vibrating sample magnetometer. The behavior of Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> nanoparticles under different molar ratios of Fe<sub>3</sub>O<sub>4</sub> to TiO<sub>2</sub>, pH, photocatalyst dose and temperature was investigated. The apparent rate constant of organic pollutant degradation using Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> was found to be pH dependent as it influenced the surface properties and therefore the photocatalytic activity of Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub>, which was higher under acidic condition. The degradation of organic pollutants was as high as 96% at pH 3, 1 g L<sup>-1</sup> photocatalyst dose, 30 °C temperature, after 90 min reaction time, and the apparent rate constant was 0.043 min<sup>-1</sup>. The thermodynamic parameters of activation, estimated by the Eyring equation and based on transition state theory (TST), indicated a nonspontaneous process in nature with positive Δ<sup>‡</sup>G° values, an endothermic reaction with positive Δ<sup>‡</sup>H° and negative Δ<sup>‡</sup>S° values. High degradation rate and catalyst recovery were maintained after five consecutive recycling cycles.

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## 1. Introduction

Khuzestan steel company (KSC) is an iron and steel producer in the south west of Iran, established in 1973 and built on 3.8 km<sup>2</sup> in the vicinity of Ahwaz city. KSC is operated based on a direct reduction method and uses electric arc furnace (EAF) technology, which has an actual capacity of up to 3.6 million tons per year. KSC consumes 8 m<sup>3</sup> of water to produce a tonne of steel. The effluent of steel mill wastewater is transferred into pumping stations through gravity lines. At a predetermined point, the wastewater is pumped through a pressurized force main gravity pipe system that carries the wastewater to the wastewater treatment plant. However, an unfavorable event involving a common issue that impedes with the operation of pumping stations is the accumulation of fat, oil and grease (FOG), which may cause blockages, leading to wastewater spills and backups. Besides, EAF in KSC generate a considerable amount of undesirable wasting metals in the form of a fine dust (*i.e.*, EAF dust) during the melting process.<sup>1</sup> Compared to other wastes, it is difficult to pile up in the open space or landfill as it creates serious environmental problems. In KSC, six arc furnaces are assessed to generate about 60 000 tons of EAF dust

per year during the annual steel production of the aforementioned and approximated in the diameter range of 20–25 μm size of particles. The United States environmental protection agency (US EPA) in 1980 categorized the EAF dust as a hazardous industrial waste, due to its chemical and physical properties.<sup>2</sup> In general, disposal or recycling of these heavy metals from EAF is actually quite expensive and inefficient.<sup>3</sup> A previous study suggested that the most abundant elements in EAF dust were iron and some transitional metals.<sup>4</sup> In view of the above, it would be attractive to supply a process for the recovery of iron EAF dust by way of waste prevention and metal values that does not present a difficult solid/liquid extraction system and to cover an alternative application method of treatment and disposal of effluents of steel industries.

Among the oxidation methods, advanced oxidation processes (AOPs) are of great attention for the treatment of those wastewaters with high chemical strength and low biodegradability by conventional methods, due to their thermodynamic feasibility and high oxidative capability for the removal of organic pollutants of wastewater *via* precipitation of free radicals, mainly hydroxyl radicals (·OH).<sup>5,6</sup> AOPs can be categorized as homogeneous (Fenton, Fenton-like, O<sub>3</sub>/H<sub>2</sub>O<sub>2</sub>, UV/O<sub>3</sub>) and heterogeneous (ZnO/UV, TiO<sub>2</sub>/UV and others) processes in which highly reactive hydroxyl radicals are generated, with or without UV irradiation, to attack a great variety of organic compounds.<sup>7,8</sup> Among the wide applied AOPs, TiO<sub>2</sub> is the most

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used semiconductor for removing organic pollutants from the aqueous phase in heterogeneous process. It is well established that TiO<sub>2</sub> with a wide band gap (3.2 eV) and proper UV radiation wavelength ( $\lambda < 385$  nm) can generate electron/hole pairs ( $e^-/h^+$ ) that recombine a conduction band electron and a valence band hole to be able to interact with adsorbed electron acceptors and oxidize electron donors.<sup>9</sup> This catalyst elucidates efficient photocatalytic activity, strong oxidizing power, good chemical and optical stability, non-toxic and at a relatively low cost and long-term stability against photocorrosion and chemical corrosion.<sup>10,11</sup> To address the current complications of conventional TiO<sub>2</sub> catalysts as applied in practice, the main weakness of this process is the difficulty in removing the suspension photocatalyst from the treated wastewater at the outlet of the photocatalytic reactor<sup>12,13</sup> and separating such nanoparticles from large volumes of water involves additional cost. To overcome separation problem, immobilization of TiO<sub>2</sub> particles onto support materials (such as quartz, silica gel, alumina, zeolites, activated carbon, glass sphere *etc.*) provides loss of photocatalytic activity, low surface areas, low mass transfer limitation, and difficult to recover and reuse from the photoreactor.<sup>14</sup> Consequently, there is a great demand for ways to improve TiO<sub>2</sub> particles stability and reusability. Potential application of magnetic photocatalyst separation provides a suitable approach for removing and reusing magnetic nanoparticles by applying an appropriate external magnetic field. Using this approach, the agglomeration of the heterogeneous photocatalyst particles can be prevented in the recovery stage and the long-term durability of the photocatalysts may be improved. At present, this is the main technical disadvantages that associated with the application of the photocatalytic wastewater treatment processes.<sup>15</sup> Furthermore, the author has previously reported that the cost associated with a downstream separator may be reduced or may even eliminate a downstream separating unit for a large-scale energy, developing energy-saving technologies.<sup>16</sup> Consequently, TiO<sub>2</sub> photocatalyst has been coated onto the surface of several magnetic supports, for instance polymers,<sup>17</sup> carbon,<sup>18</sup> and silica,<sup>19</sup> zeolite<sup>20,21</sup> and other nanocomposites combining silica mesoporous structure materials with a high surface area and tunable pore size (2–50 nm) with magnetic nanoparticles<sup>22</sup> in order to enhance the photocatalytic ability of nanostructured TiO<sub>2</sub>. Xin *et al.*<sup>23</sup> have fabricated a separable Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> core-shell nanocomposite for photocatalytic degradation of Rhodamine B (RhB) solution. Wang *et al.*<sup>24</sup> have recently reported a separable Fe<sub>3</sub>O<sub>4</sub>@SiO<sub>2</sub>@mTiO<sub>2</sub> core-shell nanocomposite and an outer mesoporous TiO<sub>2</sub> (mTiO<sub>2</sub>) as the active layer for photocatalytic degradation of methylene blue (MB) solution. However, the major disadvantages of the aforementioned research studies are the relatively high cost of the iron salts (chloride and nitrate salts) and the release of large amounts of chloride and nitrate from iron chloride or iron nitrate, which adds additional cost to the process and would have deleterious to the environment. Therefore, a process to use iron-based EAF dust to produce magnetic photocatalyst compensate the above mentioned cost advantage.

Alongside the above background, for the first time, magnetic core-shell Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> nanoparticles were designed through

the preparation of magnetic core Fe<sub>3</sub>O<sub>4</sub> nanoparticles from an electric arc furnace dust from the steelmaking industry and TiO<sub>2</sub> shell, so the resulting nanoparticles could be easily separated from treated wastewater under the application of an external magnetic field. The characteristics of photocatalyst were analyzed by several techniques and the UV-light catalytic activity of the resulting nanoparticles was evaluated for the efficiency in the degradation of steel mill wastewater, which showed a low biodegradability, posing serious threats to the environment once released into natural water. The effects of different Fe<sub>3</sub>O<sub>4</sub> to TiO<sub>2</sub> ratio, solution pH value, Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> dose and temperature on COD removal were investigated. The recycling capability and reuse of the Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> nanoparticles were also studied. The Langmuir-Hinshelwood was applied to explain the kinetics of the photodegradation of organic pollutant of steel mill wastewater and the thermodynamic parameters of the photocatalytic reaction at various temperatures estimated by the Eyring equation based on the transition state theory.

## 2. Materials and methods

### 2.1. Materials

EAF dust, ethylene glycol (EG), sodium acetate anhydrous (CH<sub>3</sub>COONa, AcNa), tetraethylorthotitanate (TEOT), tetra-*n*-butylammonium hydroxide (TBAOH) and absolute ethanol were obtained from Merck. All these reagents were used as received without further purification.

### 2.2. Preparation of Fe<sub>3</sub>O<sub>4</sub> nanoparticles

The magnetic particles were synthesized through a solvothermal method Zhao *et al.*<sup>25</sup> with some modification. Table 1 shows the dry composition of EAF dust collected from KSC. The main components are 30.18% total Fe, 13.17% CaO and 7.90% Na<sub>2</sub>O, indicating that fine dust contains significantly larger amounts of iron. In a typical procedure, 10 g EAF dust was dissolved by HCl (4 mol) under vigorous stirring for 60 min. The solution was placed in a boiling water-bath for 60 min, and added ethylene glycol (40 mL) to form a clear solution and then

Table 1 Analysis of elemental composition of EAF dust and Fe<sub>3</sub>O<sub>4</sub> nanoparticles

Element	Value $\pm$ SD, wt%	
	EAF dust	Fe <sub>3</sub> O <sub>4</sub> nanoparticles
Total Fe	30.18 $\pm$ 5.09	—
FeO	6.26 $\pm$ 2.58	—
Fe <sub>2</sub> O <sub>3</sub>	27.24 $\pm$ 5.27	55.45 $\pm$ 3.48
SiO <sub>2</sub>	1.81 $\pm$ 0.30	16.83 $\pm$ 1.83
Al <sub>2</sub> O <sub>3</sub>	0.36 $\pm$ 0.14	3.162 $\pm$ 0.85
CaO	13.17 $\pm$ 3.06	3.427 $\pm$ 1.01
MgO	1.56 $\pm$ 0.59	1.92 $\pm$ 0.73
Na <sub>2</sub> O	7.90 $\pm$ 3.30	0.29 $\pm$ 0.08
K <sub>2</sub> O	6.985 $\pm$ 0.26	0.172 $\pm$ 0.04
SO <sub>3</sub>	0.26 $\pm$ 0.09	—
P <sub>2</sub> O <sub>5</sub>	0.22 $\pm$ 0.05	3.765 $\pm$ 1.03
L.O.I	21.03 $\pm$ 1.15	9.6 $\pm$ 1.94



sodium acetate (2.0 g) added to the solution at 60 °C under vigorous stirring for 60 min. The mixture was put into a Teflon-lined stainless-steel autoclave (50 mL), thereafter the autoclave was heated at 200 °C for 8 h in an oven and allowed to cool to room temperature. The black particles were collected with the help of a magnet, followed by washing with ethanol and deionized water several times, and then dried under vacuum at 60 °C overnight for further use.

### 2.3. Preparation of Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> nanoparticles

In preparation of Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub>, 5 mL of absolute ethanol was mixed with 5 mL of tetrabutylammonium hydroxide and stirred for 1 h by the magnetic stirrer. Then, 5.56 mL of tetraethylorthotitanate and 30 mL diluted water were added. Mixing was continued under heating conditions at 80 °C. After 1 h, 1 g of Fe<sub>3</sub>O<sub>4</sub> nanoparticle powder was added to the obtained white gel and was mixed for another 1 h. All the processes were conducted in a Teflon vessel and the mixture was then put in a stainless steel reactor that was kept at 180 °C for 4 days in an oven. The suspension was dried at 25 °C and then calcined at 400 °C for 3 h.

Similarly, we also prepared Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> nanocomposites with ratios of 1 : 0.25, 1 : 0.5, 1 : 1 and 1 : 2 of Fe<sub>3</sub>O<sub>4</sub> to TiO<sub>2</sub> and are denoted as FT0.25, FT0.5, FT1 and FT2, respectively.

### 2.4. Characterization

The elemental composition of EAF dust was determined by X-ray fluorescence (XRF, Philips, Spectrometer PW2404). The crystal structure of Fe<sub>3</sub>O<sub>4</sub> and Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> nanoparticles was examined by a Philips XPert MPD X-ray diffraction (XRD), using a Cu K $\alpha$  radiation ( $\lambda = 1.54056 \text{ \AA}$ ) in the range of 10–90° ( $2\theta$ ) at 40 kV and 30 mA. The Fourier transform infrared (FT-IR) spectra of Fe<sub>3</sub>O<sub>4</sub> and Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> were analyzed using the FT-IR spectrometer (Thermo Nicolet 360-FT-IR). The zeta potential of dispersed Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> was determined using a Zetasizer (Ver. 7.11, Malvern Instruments, UK) at room temperature. The measurements were performed with photocatalyst particles at a solid load of 0.1 wt%. Five suspensions with a pH of 2, 4, 6, 8 and 10 were prepared by adding either HCl 0.1 M or NaOH 0.1 M. The size and morphology of the as-synthesized particles were determined by a scanning electron microscope (SEM, KYKY-EM3200). The particle morphology was examined by a transmission electron microscope TEM (Philips CM120, 120 kV). The magnetization and hysteresis loop were measured in air at room temperature with a vibrating sample magnetometer (VSM, Lake shore, 7410). Chemical oxygen demand (COD) was determined for the SMW using a photometric analyzer (DR5000 spectrophotometer, Hach, Germany). X-ray photoelectron spectroscopy (XPS) analysis was employed by Specs model EA10 plus (Bestec Co, Germany) using the K $\alpha$  line energies of aluminium (AlK $\alpha = 1486/6 \text{ eV}$ ) as a radiation source and ultra-high vacuum (UHV) chamber at a pressure of 10<sup>-9</sup> Torr.

### 2.5. Wastewater characteristic

The steel industry wastewater was collected from the pumping stations of mill effluent sumps, the Khouzestan steel company (KSC), southwest of Iran. The wastewater was stored at 4 °C. The

characteristics of wastewater, including the chemical oxygen demand (COD), biological oxygen demand (BOD), total suspended solids and turbidity were determined according to standard methods for the examination of water and wastewater<sup>26</sup> as summarized in Table 2.

### 2.6. Photocatalytic experiments

Photodegradation experiments were carried out in a batch reactor. The cylindrical reactor of 1000 mL capacity was used by taking of 500 mL wastewater containing a certain amount of photocatalyst. Prior to the irradiation, the reaction mixture was purged with oxygen gas for 30 min to perform the reaction under dark condition. Photocatalytic removal efficiency of COD was evaluated to measure the optimum TiO<sub>2</sub> content of the photocatalyst for enhancing the photocatalytic activity of Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> while maintaining constant conditions of reaction temperature, dosage and pH. The Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> photocatalyst at the desired dosage was then used to degrade COD under different pH conditions (3, 4, 5, 6, 7 and 8) in order to verify the effect of pH on photocatalytic activity while maintaining constant conditions of reaction temperature and dosage. A low-pressure mercury vapor lamp (Philips, 9 W, Netherlands) placed in axial position inside a quartz sleeve was used as UV irradiation source. The photocatalytic removal efficiency of COD using Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> nanoparticles was computed by:

$$\text{Photocatalytic removal efficiency} = \frac{\text{COD}_0 - \text{COD}_t}{\text{COD}_0} \times 100 \quad (1)$$

### 2.7. Photocatalytic degradation kinetics

The Langmuir–Hinshelwood (L–H) model was applied to describe the initial rate of the photodegradation kinetics of the COD of SMW.

$$r_o = -\frac{dC_{\text{COD}}}{dt} = \frac{k_r K C_{\text{COD}}}{1 + K C_{\text{COD}}} \quad (2)$$

Table 2 The physicochemical characteristics of SMW

Characteristics	Average values $\pm$ SD
pH	7.6 $\pm$ 0.2
Total COD, mg L <sup>-1</sup>	1115.0 $\pm$ 107
Soluble COD, mg L <sup>-1</sup>	558.0 $\pm$ 62
Total BOD, mg L <sup>-1</sup>	550.0 $\pm$ 125
Oil and grease, mg L <sup>-1</sup>	21.8 $\pm$ 650
Total solids (TS), mg L <sup>-1</sup>	201.7 $\pm$ 37
Total dissolved solids (TDS), mg L <sup>-1</sup>	1001.7 $\pm$ 80
Total suspended solids (TSS), mg L <sup>-1</sup>	106.0 $\pm$ 10
Fixed suspended solids (FSS), mg L <sup>-1</sup>	51.3 $\pm$ 9.07
Volatile suspended solids (VSS), mg L <sup>-1</sup>	28.67 $\pm$ 6.81
Cl, mg L <sup>-1</sup>	9.9 $\pm$ 0.59
NO <sub>3</sub> -N, mg L <sup>-1</sup>	0.345 $\pm$ 0.102
TKN, mg L <sup>-1</sup>	34.9 $\pm$ 4.18
EC, $\mu\text{s cm}^{-1}$	1808.0 $\pm$ 137
DO, mg L <sup>-1</sup>	6.1 $\pm$ 0.404
Turbidity, NTU	70.0



where, where  $r_o$  is the initial rate of the disappearance of the COD concentration,  $C_{\text{COD}}$  the equilibrium bulk-solute concentration and  $t$  the reaction time,  $K$  the equilibrium constant for adsorption of COD onto the photocatalyst surface and  $k_r$  the limiting rate constant of the reaction at maximum coverage under the given experimental conditions. In the case of highly diluted solution, the term  $KC$  becomes less than 1, when the denominator of eqn (2) neglected and the reaction rate can be modelled by the apparent first-order kinetics as in the following equation:

$$r = -\frac{dC_{\text{COD}}}{dt} = k_r KC_{\text{COD}} = k_{\text{app}} C_{\text{COD}} \quad (3)$$

where,  $k_{\text{app}}$  the apparent first-order rate constant. The solution to differential eqn (3) with the boundary condition  $C = C_o$  at  $t = 0$  is:

$$\frac{\text{COD}_t}{\text{COD}_o} = e^{-k_{\text{app}}t} \quad (4)$$

where,  $\text{COD}_o$  and  $\text{COD}_t$  are the COD concentration at the initial time ( $t = 0$ ) and any time  $t$  ( $t = t$ ), respectively. Thus, by plotting  $\text{COD}_t/\text{COD}_o$  against  $t$ , the apparent rate constant can be computed from the nonlinear regression analysis.

## 2.8. Thermodynamic study

The reaction rate constant and removal efficiency increases with increasing the reaction temperature for  $\text{Fe}_3\text{O}_4/\text{TiO}_2$  photocatalyst decomposition. The activation energy, which is a minimum energy needed for the reaction to occur, can be expressed by the Arrhenius equation:

$$k_{\text{app}} = A e^{-\frac{E_a}{RT}} \quad (5)$$

where  $k_{\text{app}}$  is the apparent rate constant for the first order reaction ( $\text{min}^{-1}$ ),  $A$  the frequency factor ( $\text{min}^{-1}$ ),  $E_a$  the activation energy ( $\text{kJ mol}^{-1}$ )  $R$  the ideal gas constant which is equal to  $8.314 \text{ J K}^{-1} \text{ mol}^{-1}$  and  $T$  the temperature (K). The linear form of logarithm of eqn (5) can be written as:

$$\ln k_{\text{app}} = \ln A - \frac{E_a}{RT} \quad (6)$$

According to transition state theory (TST), the Henry Eyring equation can be used to deduce the temperature dependence of apparent rate constant:<sup>21</sup>

$$k_{\text{app}} = \frac{K_B T}{h} \exp\left(-\frac{\Delta^\ddagger G^\circ}{RT}\right) \quad (7)$$

where,  $K_B$  is the Boltzmann's constant which is equal to  $1.3805 \times 10^{-23} \text{ J K}^{-1}$ ,  $h$  is Planck's constant which is equal to  $6.6261 \times 10^{-34} \text{ J s}$  and  $\Delta^\ddagger G^\circ$  the standard Gibbs free energy change of activation ( $\text{kJ mol}^{-1}$ ). In the thermodynamic property of TST, the standard enthalpy change of activation ( $\Delta^\ddagger H^\circ$ ) and the standard entropy change of activation ( $\Delta^\ddagger S^\circ$ ) are brought together with the change in the standard Gibbs free energy of activation equation:

$$\Delta^\ddagger G^\circ = \Delta^\ddagger H^\circ - T\Delta^\ddagger S^\circ \quad (8)$$

Substitution of eqn (8) into eqn (7) gives:

$$k_{\text{app}} = \frac{K_B T}{h} \exp\left(\frac{\Delta^\ddagger S^\circ}{R}\right) \exp\left(-\frac{\Delta^\ddagger H^\circ}{RT}\right) \quad (9)$$

The linear form of the Eyring's equation can be expressed as follows:

$$\ln\left(\frac{k_{\text{app}}h}{K_B T}\right) = \frac{\Delta^\ddagger S^\circ}{R} - \frac{\Delta^\ddagger H^\circ}{RT} \quad (10)$$

Therefore a plot of dimensionless values of  $\ln(k_{\text{app}}h/K_B T)$  against  $1/T$  provides a straight line and  $\Delta^\ddagger H^\circ$  and  $\Delta^\ddagger S^\circ$  are obtained from the slope and the intercept, respectively. According to our previous publication, the following expressions give an additional method of estimating the frequency factor and activation energy can be computed:<sup>21</sup>

$$A = \frac{K_B T}{h} \exp\left(\frac{\Delta^\ddagger S^\circ}{R}\right) \quad (11)$$

$$E_a = \Delta^\ddagger H^\circ + RT \quad (12)$$

## 3. Result and discussion

### 3.1. Photocatalyst characterization

**3.1.1. XRD analysis.** Fig. 1 shows the XRD spectra pattern of  $\text{TiO}_2$ ,  $\text{Fe}_3\text{O}_4$  and  $\text{Fe}_3\text{O}_4/\text{TiO}_2$  core-shell nanoparticles. The diffraction peak in Fig. 1a shows the XRD pattern of the as-synthesized  $\text{TiO}_2$  particles and was found to associate to anatase of  $\text{TiO}_2$  (JCPDS no. 21-1272). The observed diffraction peaks in Fig. 1b can be indexed well with relative intensities of standard  $\text{Fe}_3\text{O}_4$  (JCPDS no. 19-629) indicating that the as-synthesized nanoparticles are the pure  $\text{Fe}_3\text{O}_4$  phase and single-phase of the face-centered-cubic spinel. By comparing Fig. 1a and b, it is found that the XRD diffraction peak intensities of  $\text{Fe}_3\text{O}_4$  decreased due to  $\text{TiO}_2$  coating. In addition, beside the crystal structure of  $\text{Fe}_3\text{O}_4$  lies in  $\text{Fe}_3\text{O}_4/\text{TiO}_2$  core-shell nanoparticles, the crystal structure of  $\text{Fe}_3\text{O}_4$  core-shell nanoparticles is as that of  $\text{TiO}_2$  nanoparticles, which is anatase and proves that dissolving  $\text{Fe}^{3+}$  from  $\text{Fe}_3\text{O}_4$  seeds in the preparation process does not cause the change of crystal structure. The crystallite or 0.1317 of anatase  $\text{TiO}_2$  and  $\text{Fe}_3\text{O}_4$  were estimated from the corresponding XRD peaks at  $2\theta = 25.42$  and  $35.50^\circ$ , respectively, by Scherrer's equation:

$$D = \frac{hk\lambda}{\beta \cos \theta} \quad (13)$$

where  $D$  is the crystallite size (nm),  $\lambda$  the wavelength of the X-ray radiation ( $\text{Cu K}\alpha = 0.1541874 \text{ nm}$ ),  $k$  the Scherrer constant (0.89),  $\beta$  the full width at the half-maximum of the (101) plane of anatase  $\text{TiO}_2$  and the (311) plane of  $\text{Fe}_3\text{O}_4$  and  $\theta$  the diffraction angle. The crystallite sizes of about 29.7 and 11.6 nm in pure anatase  $\text{TiO}_2$  nanoparticles and in  $\text{Fe}_3\text{O}_4/\text{TiO}_2$  nanocomposite and 15.64 and 32.66 nm for  $\text{Fe}_3\text{O}_4$  nanoparticles and  $\text{Fe}_3\text{O}_4$  in  $\text{Fe}_3\text{O}_4/\text{TiO}_2$  nanocomposite, respectively, were obtained.



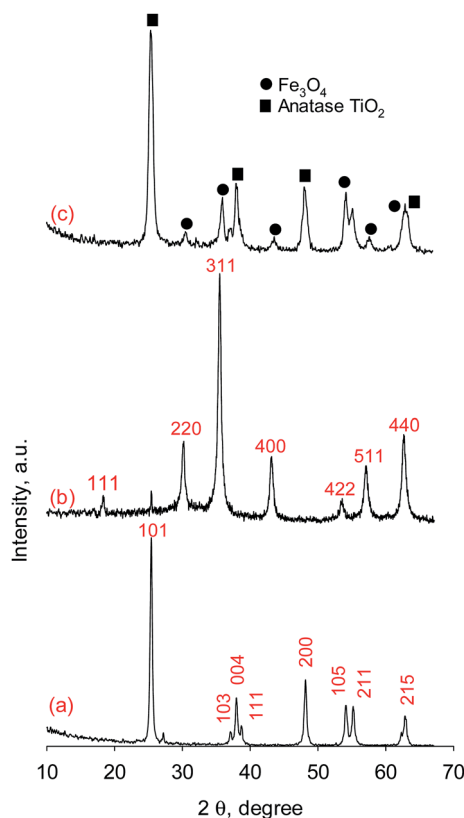


Fig. 1 XRD patterns of (a) anatase  $\text{TiO}_2$ , (b)  $\text{Fe}_3\text{O}_4$ , and (c)  $\text{Fe}_3\text{O}_4@/\text{TiO}_2$ .

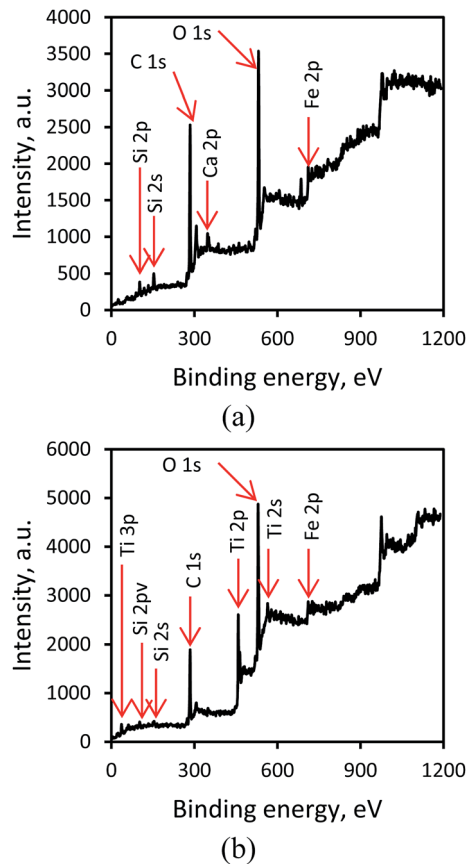


Fig. 2 Wide range XPS spectra of (a)  $\text{Fe}_3\text{O}_4$  and (b)  $\text{Fe}_3\text{O}_4@/\text{TiO}_2$ .

**3.1.2. XPS analysis.** X-ray photoelectron spectroscopy (XPS) analysis was employed to find stoichiometry and surface chemical composition of  $\text{Fe}_3\text{O}_4$  and  $\text{Fe}_3\text{O}_4@/\text{TiO}_2$ , as shown in Fig. 2a and b. Fig. 2a shows a total XPS spectrum that composed mainly of two peaks of carbon (C 1s 284.6 eV) and oxygen (O 1s 531.4 eV), deriving from the acetate coating on the surface and remaining carbon from EAF dust (Table 1), silicon (Si 2s 102.2 eV), silicon (Si 2p 153), calcium (Ca 2p 347.4 eV), and Fe (Fe 2p 685.4 eV), related to the oxidized surface of  $\text{Fe}_3\text{O}_4$ , while Fig. 2b shows a strong peak at 459.6 eV is assigned to the Ti 2p and another two weak peaks at the 39.4 and 564.3 eV are assigned to the Ti 3p and the Ti 2s, respectively, as well as a weak peak at a binding energy of about 61.8 eV is attributed to Fe 3p from  $\text{Fe}_3\text{O}_4@/\text{TiO}_2$ . Fig. 3a and b show the 2p electron orbit of Fe atoms in  $\text{Fe}_3\text{O}_4$  and  $\text{Fe}_3\text{O}_4@/\text{TiO}_2$  nanoparticles, indicating the peaks of Fe 2p<sub>1/2</sub> and Fe 2p<sub>3/2</sub> core-level electrons for the both  $\text{Fe}_3\text{O}_4$  and  $\text{Fe}_3\text{O}_4@/\text{TiO}_2$  samples that are located at a binding energy of 724 and 710.8 eV. According to quantum theory, the degeneracy energy level corresponding to each value of quantum number  $J$  is  $(2J + 1)$ .<sup>27</sup> As can be seen from Fig. 3a and b, of the two peaks, Fe 2p<sub>3/2</sub> peak is more intense than Fe 2p<sub>1/2</sub> peak, and the peak area ratio of Fe 2p<sub>3/2</sub> to Fe 2p<sub>1/2</sub> core level photoelectron of 2 to 1 is observed. This splitting energy of the XPS peaks ( $\Delta E$ ) was found to be 14.6 eV. Furthermore, the narrower and the larger peak area of Fe 2p<sub>3/2</sub> than Fe 2p<sub>1/2</sub> peak is due to spin orbit ( $J-J$ ) coupling. In addition, it is observed that Fe 2p<sub>3/2</sub> and Fe 2p<sub>1/2</sub> peaks for  $\text{Fe}_3\text{O}_4$  nanoparticles have two satellite peaks as presented in Fig. 3. The two satellite peaks are

located at 728.6 and 715.2 eV, which could also be corresponded to the oxidation state of  $\text{Fe}^{2+}$ . However, the peaks of Fe 2p for the two samples are located at the same positions. While in the Fe 3p spectra of  $\text{Fe}_3\text{O}_4$  and  $\text{Fe}_3\text{O}_4@/\text{TiO}_2$  nanoparticles, two peaks at 726.4 and 712.8 eV attributing to the binding energies of Fe 2p<sub>1/2</sub> and Fe 2p<sub>3/2</sub>, respectively, which is the characteristic of  $\text{Fe}^{3+}$  in iron oxide nanoparticles. While in the  $\text{Fe}_3\text{O}_4@/\text{TiO}_2$  nanoparticles, the peak positions of Fe 3p locates at the same binding energies as compared to  $\text{Fe}_3\text{O}_4$ . The positions of the satellite peaks for the Fe 3p<sub>1/2</sub> and Fe 3p<sub>3/2</sub> are centered at 729.8 and 720.6 eV in  $\text{Fe}_3\text{O}_4$ , respectively, which are assigned to the oxidation state of  $\text{Fe}^{3+}$  in  $\text{Fe}_3\text{O}_4$  nanoparticles. Compared with  $\text{Fe}_3\text{O}_4$ , the binding energy of the satellite peaks for the Fe 3p<sub>1/2</sub> and Fe 3p<sub>3/2</sub> of  $\text{Fe}_3\text{O}_4@/\text{TiO}_2$  nanocomposites exhibits a negative shift ( $\sim 1.5$  eV) and a positive shift ( $\sim 0.2$  eV), respectively. The XPS results confirm the formation of two compounds of magnetite and the results in the present study were consistent with previous findings.<sup>28</sup>

The XPS spectrum of the Ti 2p for the  $\text{Fe}_3\text{O}_4@/\text{TiO}_2$  photocatalyst is shown in Fig. 3c. The surface chemical composition in the nanoparticle photocatalyst showed that the Ti 2p peak involves four different peaks corresponding to two chemical states from doublet consisting of the Ti 2p<sub>3/2</sub> and the Ti 2p<sub>1/2</sub> occurred at binding energies of 457 and 463.1 eV ( $\text{Ti}^{3+}$ ) 458.8 and 464.6 eV ( $\text{Ti}^{4+}$ ), which designates the valences of Ti in the synthesized photocatalyst are +3 and +4. Clearly, the presence of



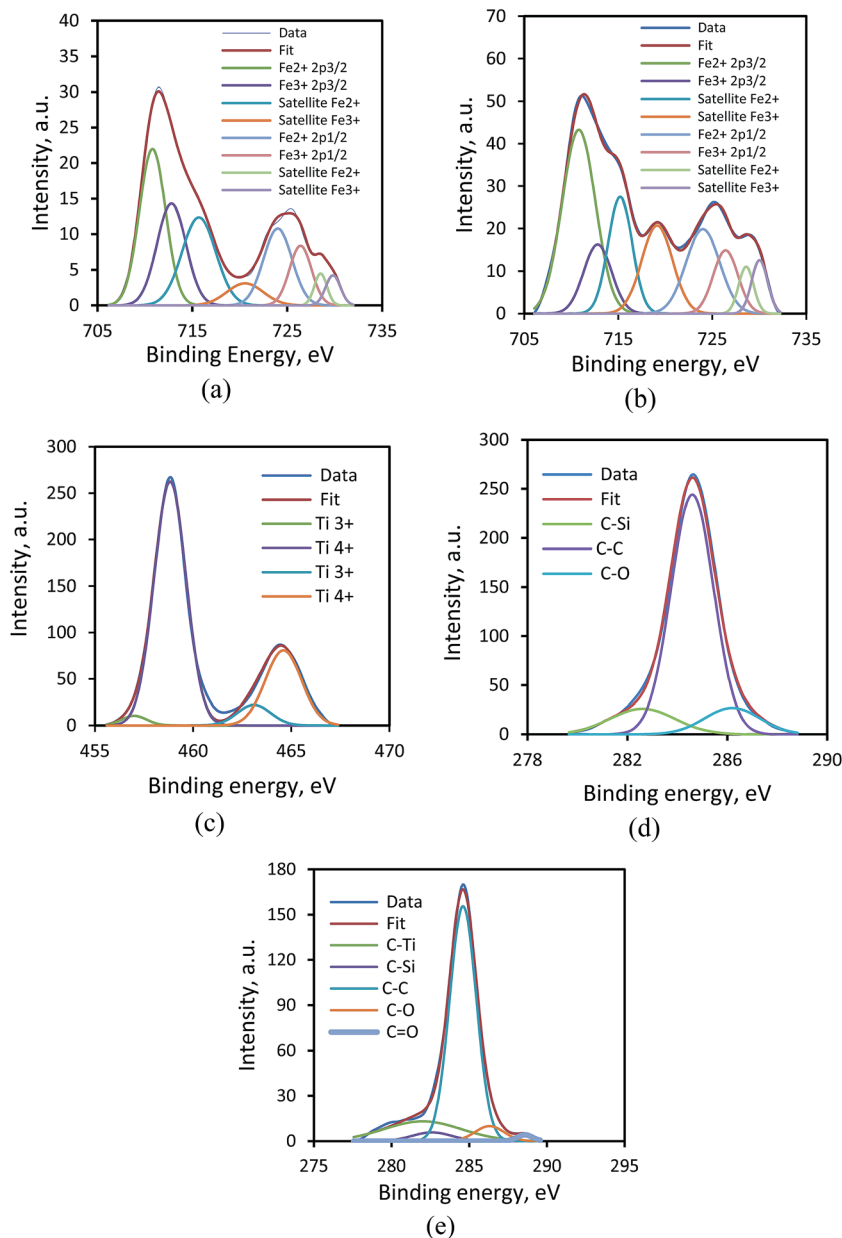


Fig. 3 XPS peak analysis of (a) Fe 2p peak on surface of  $\text{Fe}_3\text{O}_4$  and (b)  $\text{Fe}_3\text{O}_4@/\text{TiO}_2$ , (c) Ti 2p peak on surface of  $\text{Fe}_3\text{O}_4@/\text{TiO}_2$ , and (d) C 1s peak on surface of  $\text{Fe}_3\text{O}_4$  and (e)  $\text{Fe}_3\text{O}_4@/\text{TiO}_2$ .

$\text{TiO}_2$  ( $\text{Ti}^{4+}$ ) oxide layer on  $\text{Fe}_3\text{O}_4@/\text{TiO}_2$  is more obvious than  $\text{Ti}_2\text{O}_3$  ( $\text{Ti}^{3+}$ ), which indicates  $\text{Ti}^{4+}$  is in tetrahedral coordination with oxygen ( $\text{TiO}_2$ ). High-resolution spectra analysis reveals that the oxidation content of  $\text{Ti}^{4+}$  on the surface was about 90%. The separation energy of the XPS peaks ( $\Delta E$ ) was found to be 5.8 eV, which is proportional to the spin orbit coupling constant. The present study is in agreement with previous findings.<sup>29</sup>

The XPS spectra of C 1s binding energy region for the  $\text{Fe}_3\text{O}_4$  and  $\text{Fe}_3\text{O}_4@/\text{TiO}_2$  samples are shown in Fig. 3d and e. The surface chemical composition in the samples showed that the carbon adsorption reveals as a strong C–C bond (284.8 eV) and two weak C–Si (282.6 eV) and C=O (288.4 eV) peaks. In Fig. 3d, the peaks of C–Ti, C–Si, C–C, C–O and C=O are centered at 282, 282.6, 284.6, 286.3 and 288.6 eV, respectively. The shifting of the

binding energy values to slightly negative shift and positive shift can be attributed to the oxidation of  $\text{Fe}_3\text{O}_4$ . These results reveal that  $\text{TiO}_2$  and  $\text{Fe}_3\text{O}_4$  present mostly as separate phases in the  $\text{Fe}_3\text{O}_4@/\text{TiO}_2$  nanoparticle photocatalyst, which is in agreement with the previous study.<sup>30</sup>

**3.1.3. FT-IR analysis.** The  $\text{Fe}_3\text{O}_4@/\text{TiO}_2$  photocatalyst was also analyzed by FTIR in order to verify the presence of magnetic recovered by  $\text{TiO}_2$  (Fig. 4). The absorption peaks in the range of 1200 and 1460  $\text{cm}^{-1}$  are attributed to methyl and methylene groups bending, wagging, scissoring, rocking and twisting vibrations. An absorption band associated with C–H bond symmetric stretching are located at 2919  $\text{cm}^{-1}$  and an asymmetric stretching vibration at about 2850  $\text{cm}^{-1}$ . However, the absorption peak at 1698  $\text{cm}^{-1}$  is attributed to the presence of



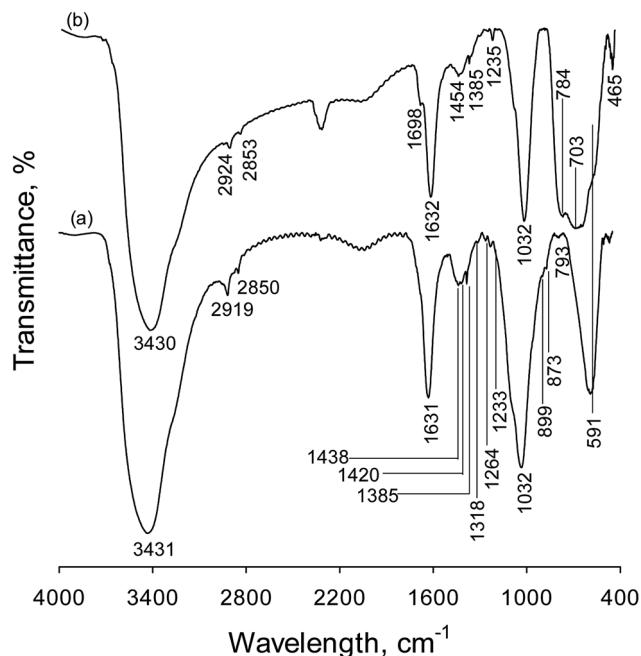


Fig. 4 FT-IR spectra of (a)  $\text{Fe}_3\text{O}_4$  and (b)  $\text{Fe}_3\text{O}_4@\text{TiO}_2$ .

C=O stretching vibration. These peaks belong to the acetate and ethyl alcohol that were used as the solvent in photocatalyst preparation. The absorbance peak centered at  $1032\text{ cm}^{-1}$  is attributed to a stretching vibration of C–O– functional group, with a shoulder peak at about  $1090\text{ cm}^{-1}$  corresponded to the Si–O– stretching vibration of the  $\text{SiO}_2$  layer in samples. In contrast to the FTIR spectra of  $\text{Fe}_3\text{O}_4$ , aforementioned peak intensities decrease in the spectrum of  $\text{Fe}_3\text{O}_4@\text{TiO}_2$ , indicating that the  $\text{TiO}_2$  nanoparticles is coated well on the surface of the  $\text{Fe}_3\text{O}_4$  nanospheres. In spectrum shown in Fig. 4a, the absorption peaks in  $1632$  and  $3431\text{ cm}^{-1}$  are attributed to H–O–H bending and O–H stretching vibrations, respectively, of the free water molecules and adsorbed water on the sample surface. The FT-IR spectra of  $\text{Fe}_3\text{O}_4$  show the characteristic band of magnetite, at  $591\text{ cm}^{-1}$ , which is assigned to the stretching vibration of the Fe–O functional group and remained in a fixed position in the magnetite lattice, as indicated by the vertical inspection line in Fig. 4. There is a clear difference in the FT-IR spectra of  $\text{Fe}_3\text{O}_4$  and  $\text{Fe}_3\text{O}_4@\text{TiO}_2$ . In  $\text{Fe}_3\text{O}_4@\text{TiO}_2$  sample (Fig. 4b), the magnetite peak overlaps with broad bands of the stretching mode of Ti–O–Ti group, confirming the presence of  $\text{TiO}_2$  layer. In addition, the peaks observed at  $703$  and  $784\text{ cm}^{-1}$  in spectrum in Fig. 4b are due to the Ti–O–Ti stretching vibration of the anatase phase of  $\text{TiO}_2$  layer. Also, XPS results confirm the formation of titanium oxide. In Fig. 4b, there is an O–H bond at  $3431\text{ cm}^{-1}$  and a Ti–O stretch at  $4650\text{ cm}^{-1}$  that are due to the stretching vibration of OH adsorbed on the surface ( $\text{TiOH}$  species) of nanoparticle and also a peak at  $1631\text{ cm}^{-1}$  due to the bending vibrations of adsorbed water.

**3.1.4. TEM and SEM analysis.** Fig. 5 shows TEM and SEM images of  $\text{Fe}_3\text{O}_4$  and  $\text{Fe}_3\text{O}_4@\text{TiO}_2$  nanoparticles. Fig. 5a demonstrates that TEM images of  $\text{Fe}_3\text{O}_4$  crystallites are ultra-fine and the diameter of the aggregated particle size is of

around 40 to 80 nm. Fig. 5b represents TEM image of a single core  $\text{Fe}_3\text{O}_4$  nanoparticle with a size of about 80 nm. Fig. 3b shows that the  $\text{Fe}_3\text{O}_4$  spherical shapes are composed of primary nanoparticles with a size of about 20 nm, which was comparable with the crystallite size of 15.64 nm in nanocrystalline bulk materials computed from the XRD pattern by using the Scherrer equation. Fig. 5c shows that the spherical shape of magnetite connects tightly to one another to form a sphere. According to Fig. 5d, the representative TEM image of a single core-shell  $\text{Fe}_3\text{O}_4@\text{TiO}_2$  nanoparticle with well-defined core-shell structure and with an average size of 80 nm and the average thickness of the shell is 15 nm. The dark and bright regions correspond to the  $\text{Fe}_3\text{O}_4$  and the shell, respectively. This phenomenon can be due to their different electron-absorbing abilities, *i.e.*, the electron binding ability of  $\text{Fe}_3\text{O}_4$  is higher than that of non magnetic  $\text{TiO}_2$ . Therefore, the cores can be identified as the darker region compared to the shell area.<sup>31,32</sup> From the TEM images, it can be seen that a uniform shell of  $\text{TiO}_2$  with a nanoscale thickness is coated on the  $\text{Fe}_3\text{O}_4$  surface to form a core-shell structure. On the other hand, Fig. 5d represents more closely that the spherical-like core-shell nanoparticles are formed onto the  $\text{Fe}_3\text{O}_4$  nanoparticle core and an anatase  $\text{TiO}_2$  nanolayer shell. Fig. 5e demonstrates SEM image of the spherical morphology of core-shell nanoparticles with some degree of agglomeration. From the particle size distribution obtained from SEM image, it is possible to identify particles with different size, ranging from small particles to particles with up to 100 nm; nevertheless, the particle sizes estimated from the SEM were in the range of 30 to 100 nm. Fig. 5f confirms the element composition by SEM with energy dispersive X-ray (EDX) spectroscopy analysis. Fig. 5g EDX peaks taken from the core-shell  $\text{Fe}_3\text{O}_4@\text{TiO}_2$  nanoparticle and spectra show strong Fe, Ti and O signals, which further confirms the formation of core-shell  $\text{Fe}_3\text{O}_4@\text{TiO}_2$  nanoparticles. Si peak was attributed to the EAF dust used as the Fe source and remained on the sample during photocatalyst preparation, as XPS results also confirm the presence of Si on the  $\text{Fe}_3\text{O}_4@\text{TiO}_2$  nanoparticles.

**3.1.5. Magnetic characteristics.** The magnetic property of as-synthesized  $\text{Fe}_3\text{O}_4$  and  $\text{Fe}_3\text{O}_4@\text{TiO}_2$  nanoparticles were studied by a vibrating sample magnetometer (VSM) at room temperature. The magnetic hysteresis loop measured at 300 K is shown in Fig. 6. The magnetization–hysteresis curves show that both  $\text{Fe}_3\text{O}_4$  nanoparticles and  $\text{Fe}_3\text{O}_4@\text{TiO}_2$  catalyst are magnetic and  $\text{Fe}_3\text{O}_4$  have a magnetization saturation value of  $25.66\text{ emu g}^{-1}$  while that of  $\text{Fe}_3\text{O}_4@\text{TiO}_2$  catalyst is  $6.64\text{ emu g}^{-1}$ . The reduction of saturation magnetization is prevalently associated with the existence of nonmagnetic  $\text{TiO}_2$  shells on the surface of  $\text{Fe}_3\text{O}_4$  as shown in Fig. 6. This result also indicates that the  $\text{Fe}_3\text{O}_4@\text{TiO}_2$  nanocomposite remains magnetic after coating.<sup>33</sup> Due to the magnetic core-shell nanocomposite, the as-synthesized photocatalyst can be easily collected from aqueous solution by external magnetic field over a short period of time and then can be readily re-dispersed by slightly shaking it. The inset Fig. 6 shows the images obtained for dispersed aqueous solution (top inset) and separated from aqueous solution (down inset) by an external magnetic field. The



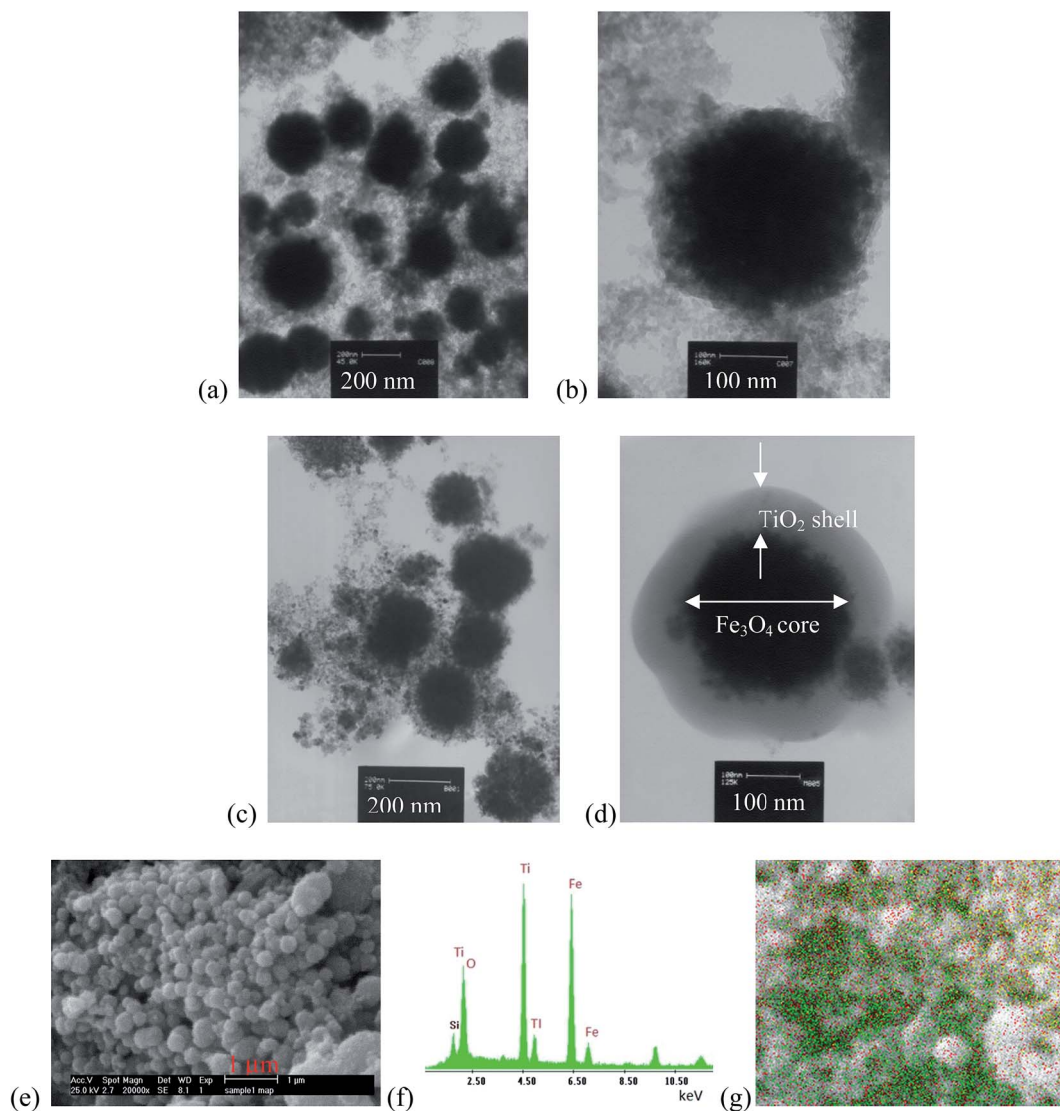


Fig. 5 TEM micrographs of (a)  $\text{Fe}_3\text{O}_4$  nanoparticles, (b) single core of  $\text{Fe}_3\text{O}_4$  nanoparticles (c)  $\text{Fe}_3\text{O}_4@TiO_2$  nanoparticles, (d) and single core-shell of  $\text{Fe}_3\text{O}_4@TiO_2$  (e) SEM, (f) EDX spectra of  $\text{Fe}_3\text{O}_4@TiO_2$  core-shell and (g) EDX point image taken from core-shell  $\text{Fe}_3\text{O}_4@TiO_2$  nanoparticle marked in the SEM images.

nanoparticles exhibited well magnetic behavior when they were magnetically separated from supernatant portion and redispersed in aqueous solution, suggesting the high potential sensitivity of as-synthesized magnetic photocatalyst.

### 3.2. Photocatalytic degradation

**3.2.1. Effect of different photocatalyst.** Fig. 7 shows the dark condition and adsorption under UV irradiation and the influence of five different photocatalysts (anatase  $TiO_2$  and FT0.25, FT0.5, FT1 and FT2) on the decomposition kinetics and removal of organic compound of steel mill wastewater. Fig. 7a shows that the COD concentration diminishes exponentially with increasing time in the presence of  $\text{Fe}_3\text{O}_4@TiO_2$  under UV irradiation. The apparent rate constant ( $k_{app}$ ) verifies the shape of exponential decrease. Under a dark condition, the rate of COD removal was found to be much lower than the case of UV irradiation. The experimental data showed that the amount of

COD adsorbed on the photocatalyst surface under a dark condition was found to be about 2.3% after 30 min (Fig. 7b), indicating a very low portion of the surface area of photocatalyst is accessible to COD adsorption. This means that the stereochemical structural limitations and its co-adsorbed with water molecules on the surface of photocatalyst are predominant for the reason that the water molecules are more abundant than COD molecules. At this operating condition, the rate constant of  $\text{Fe}_3\text{O}_4@TiO_2$  at pH 3 after 30 min was calculated as  $0.00067 \text{ min}^{-1}$ . Hence, the COD removal of  $\text{Fe}_3\text{O}_4$  magnetic nanoparticles under the UV light was about 7.7% after 30 min. The corresponding rate constant was calculated to be  $0.00082 \text{ min}^{-1}$ . From Fig. 7b, the results of our study showed that about 88.84% of the COD removal achieved in the presence of as-synthesized anatase  $TiO_2$  under UV light after 90 min. At this operating condition, the corresponding apparent rate constant was  $0.024 \text{ min}^{-1}$ . The decomposition and mineralization of



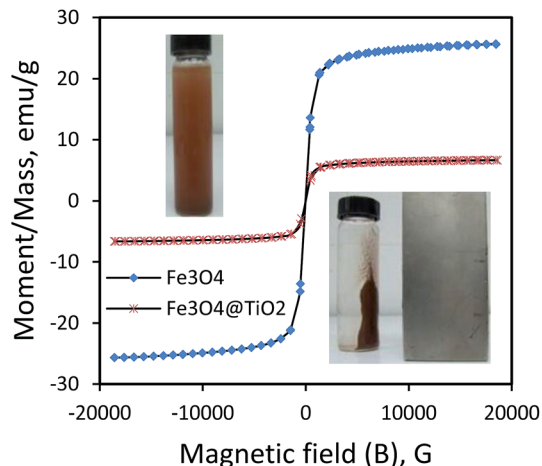
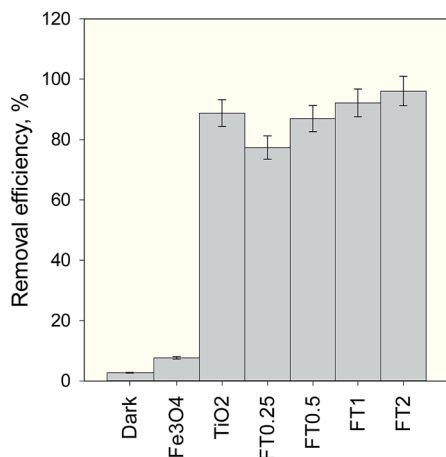


Fig. 6 Magnetization curves of  $\text{Fe}_3\text{O}_4$  and  $\text{Fe}_3\text{O}_4@TiO_2$  nanoparticles synthesized with molar ratio of 1 : 1 of  $\text{Fe}_3\text{O}_4$  to  $TiO_2$  (FT1).



(a)



(b)

Fig. 7 Degradation kinetic curves of organic compounds of SMW using anatase  $TiO_2$  and  $\text{Fe}_3\text{O}_4@TiO_2$  with different  $TiO_2$  loading ( $1\text{ g L}^{-1}$  photocatalyst dose,  $1070\text{ mg L}^{-1}$  initial COD, pH 3, 90 min reaction time and  $25\text{ }^\circ\text{C}$ ).

COD of steel mill wastewater enhanced more quickly and strongly in the presence of  $\text{Fe}_3\text{O}_4@TiO_2$  under UV light in comparison with anatase  $TiO_2$  photocatalysts. Fig. 7a also depicts the effect of adding  $TiO_2$  onto  $\text{Fe}_3\text{O}_4$  nanoparticles on the photocatalytic degradation kinetics of organic pollutants of wastewater. There was an improvement of COD removal efficiency with an increase in  $TiO_2$  coated onto  $\text{Fe}_3\text{O}_4$  surface to form nanocomposite of FT0.25, FT0.5, FT1 and FT2. In addition, our results showed when the ratio of  $\text{Fe}_3\text{O}_4$  to  $TiO_2$  increased, the photocatalytic degradation of the nanocomposite improved. This can be attributed to the large specific surface area and the more effective electron/hole pair separation. Wang *et al.*<sup>24</sup> have reported that the photocatalytic activity increased as the  $TiO_2$  loading increased. The maximum COD removal efficiencies of 77.37, 87, 92.19 and 96.12% were obtained for FT0.25, FT0.5, FT1 and FT2 at a photocatalyst dose of  $1\text{ g L}^{-1}$  after 90 min (Fig. 7b) and the corresponding rate constant was found to be 0.013, 0.020, 0.041 and  $0.057\text{ min}^{-1}$ . It is clear that the rate constant of degradation reaction is influenced by the amount of  $TiO_2$  coating onto  $\text{Fe}_3\text{O}_4$ , demonstrating the decomposition with the largest rate constant is the fastest. Fig. 8 compares photograph images of  $\text{Fe}_3\text{O}_4@TiO_2$  nanocomposite with various  $TiO_2$  loading onto magnetic  $\text{Fe}_3\text{O}_4$  in the aqueous solution. First, the magnetic nanoparticles were suspended in aqueous solution and were then applied to an external magnetic field. Fig. 8 shows that FT0.25, FT0.5 and FT1 samples separated completely from the aqueous solution, and there were no signs of suspension of the nanoparticles in the test beakers. However, the magnetic nanoparticles coated with  $TiO_2$  with a ratio of 2 : 1 onto  $\text{Fe}_3\text{O}_4$ , namely FT2, were not well separated from aqueous by external magnet, indicating some  $TiO_2$  particles have failed to coat on the magnetic core. For the photocatalytic activity of  $\text{Fe}_3\text{O}_4@TiO_2$  nanoparticles with four ratios of coating, we chose the one that has the biggest rate constant. In the case of the suspension of FT2, since sediments of  $\text{Fe}_3\text{O}_4@TiO_2$  nanoparticles became visible throughout the test beakers after 30 min and resuspending the aqueous solution, most of the  $\text{Fe}_3\text{O}_4@TiO_2$  nanoparticles were still suspended in the water (Fig. 8b). Therefore, with the comparison between the obtained results of the apparent degradation rate of the photocatalytic reaction of  $\text{Fe}_3\text{O}_4@TiO_2$  nanocomposite and the clear solution of photograph of FT1 (Fig. 8c), it is obvious that FT1 should be chosen as optimum photocatalyst, that can be used to obtain the apparent rate constants of other experimental conditions.

**3.2.2. Effect of pH.** The pH of the solution is a major factor affecting the photocatalytic activity, because it dedicates the surface charge of the photocatalyst and the size of aggregates it forms.<sup>34</sup> It can be explained that the solution pH positively correlates with their photocatalytic performance, indicating that the organic wastewater compounds are to be differences in hydrophobicity, solubility and speciation behaviors. When a pH of a solution decreases below its  $pK_a$  value, an organic compound exists in a neutral form and it transfers from neutral to a negatively charged when the solution pH increases above its  $pK_a$  value. Accordingly, organic pollutants decomposition rate of photocatalytic reaction was increased significantly with



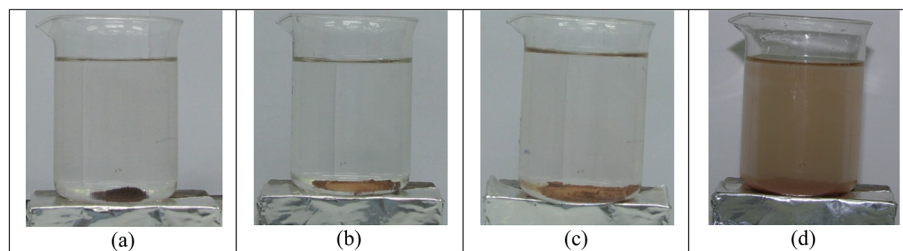
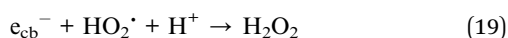
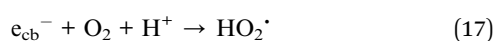
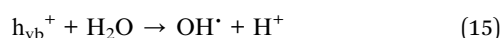
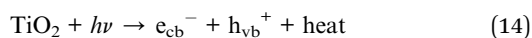
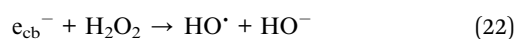
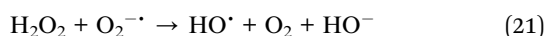


Fig. 8 Photograph comparing appearance of aqueous of magnetic nanoparticles coated with TiO<sub>2</sub>. (a) FT0.25, (b) FT0.5, (c) FT1, and (d) FT2 suspensions after 30 min.

increasing pH. The acidic solution favors degradation of organic compound onto TiO<sub>2</sub> surface. Thus, degradation efficiency increased. At this pH, there is also formation of OH<sup>•</sup> radicals, which react with organic molecules and increase the degradation level. This means that OH<sup>•</sup> radicals are formed on the surface of Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> by the reaction of gaps in the valence band ( $h_{vb}^+$ ) with adsorbed water molecules or hydroxide of surface titanol groups (TiOH). Furthermore, photogenerated electrons react with oxygen molecules to produce superoxide (O<sub>2</sub><sup>•-</sup>). This O<sub>2</sub><sup>•-</sup> can react with protons and O<sub>2</sub> to produce hydroperoxyl radicals (HO<sub>2</sub><sup>•</sup>). The formation of hydrogen peroxide (H<sub>2</sub>O<sub>2</sub>) can occur either by water oxidation (by holes) or by two conduction band electron reduction of the adsorbed water. Aforementioned processes are represented by the following equations:



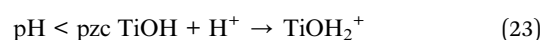
In addition, OH<sup>•</sup> radicals can be produced by cleavage of H<sub>2</sub>O<sub>2</sub> by one of the following reactions:



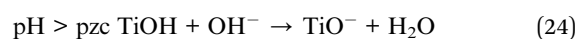
Finally, oxidation of organic compounds to CO<sub>2</sub> mineralization occurs in a solution saturated with activated oxygen species (O<sub>2</sub><sup>•-</sup>, HO<sub>2</sub><sup>•</sup>, H<sub>2</sub>O<sub>2</sub>, OH<sup>•</sup>), which may affect the yield of oxidation.

The experiments were carried out at pH 3, 4, 5, 6, 7, and 8 for 90 min reaction time (Fig. 9). Fig. 9a shows that anchored in the results of our experiments, decomposition of organic pollutants using Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> photocatalyst for steel mill wastewater follows the first-order kinetic. This figure shows that the decomposition rate of the organic compounds decreased with

increasing pH of the solution. The plot of COD<sub>t</sub>/COD<sub>0</sub> versus reaction time gives a good relationship ( $R^2 > 0.99$ ), which is supportive of the good agreement of fitting the reaction data in first-order kinetic and the apparent reaction rate constant of the photocatalytic decomposition at pH 3, pH 4, pH 5, pH 6, pH 7 and pH 8 were calculated as 0.043, 0.038, 0.036, 0.035, 0.034 and 0.030 min<sup>-1</sup>, respectively. As the pH of the solution is increased, the degradation of organic molecules onto catalyst surface decreased. Therefore, degradation rate constants were observed to be low at basic pH condition. Fig. 9b shows that neutral pH and moderate acidic pH conditions were appropriate for organic degradation of steel mill wastewater by Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub>. Fig. 9b shows that the maximum degradation of about 94% was observed at pH 3. This phenomenon could be led to obvious justification that degradation of organic compounds exhibited different behaviors with strong pH dependence of the solution.<sup>35,36</sup> To explain, electrostatic interactions and pH-dependent trend between the protonated surface of photocatalyst (TiOH<sub>2</sub><sup>+</sup>) and cations of organic compound of COD results to strong adsorption and subsequent efficient decomposition of organic pollutants:



The existing form of organic compounds and surface charges of Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> is also related to solution pH. Fig. 9c shows that the point of zero charge (pzc) for anatase TiO<sub>2</sub> used in this study was around pH = 4.1. Therefore, catalyst surface is positive in solution at moderate acidic (pH < 4.1) and negatively at basic condition.<sup>37</sup> Repulsions between same charged Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> surfaces prevent the agglomeration of the catalyst. Similar observations on the effect of pH for TiO<sub>2</sub> photocatalyst have been reported in photocatalytic decomposition of COD of some other pollutants.<sup>37,38</sup> At pH 8, TiO<sub>2</sub> particle surfaces should mainly be neutral. Minimum degradation of 85.24% was observed at pH 8 (Fig. 9b). To explain, basic pH electrostatic interactions between deprotonated surface of photocatalyst (TiO<sup>-</sup>) and organic compound of COD leads to adsorption and degradation of organic compounds:



However, the band hole position may be moved to more negative value with increasing pH, causing in a reduction of oxidation potentials. Consequently, the solution pH at

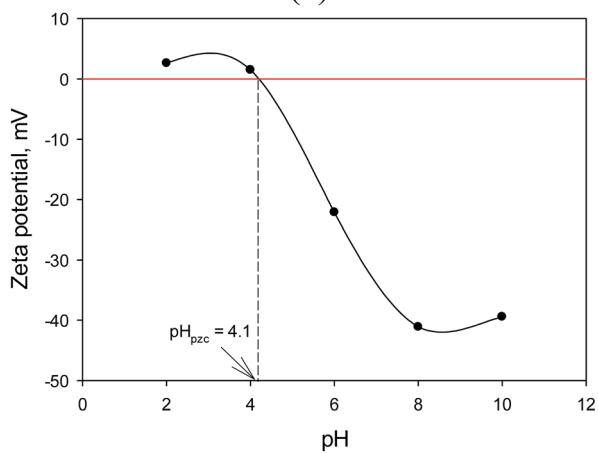




(a)



(b)



(c)

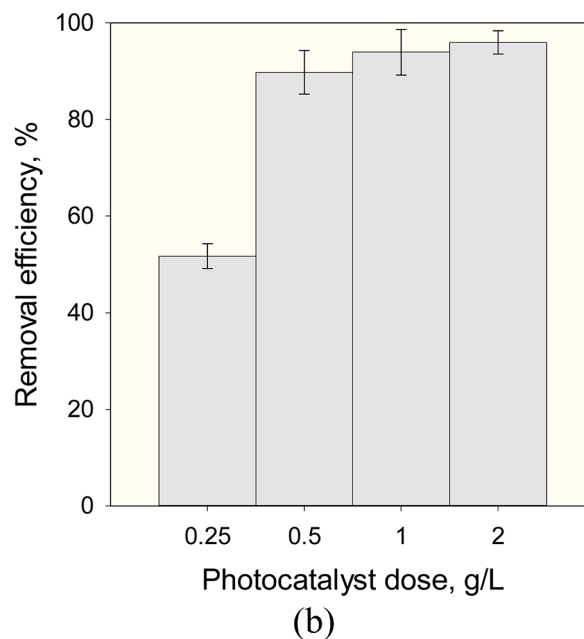
Fig. 9 (a) Kinetic curves, (b) removal efficiency of SMW with  $\text{Fe}_3\text{O}_4\text{@TiO}_2$  (FT1) at different pH ( $1 \text{ g L}^{-1}$  photocatalyst dosage,  $920 \text{ mg L}^{-1}$  initial COD, 90 min reaction time and  $30 \text{ }^\circ\text{C}$ ) and (c) zeta potential and the pzc of  $\text{Fe}_3\text{O}_4\text{@TiO}_2$ .

a suitable value, due to electrostatic attraction, would influence the degradation of organic compound of COD in wastewater and the adsorption on the surface of  $\text{Fe}_3\text{O}_4\text{@TiO}_2$  photocatalyst and thus it is found to favor efficient degradation rate of organic compounds.

**3.2.3. Effect of dose of photocatalyst.** For economic consideration and the penetration depth of light irradiation by the high turbidity suspension and light shadowing effects at high dose of photocatalyst, experiments were performed to optimize the dose of the  $\text{Fe}_3\text{O}_4\text{@TiO}_2$  photocatalyst in order to maximize the density of surface active sites and reactivity for the photocatalytic mineralization of organic pollutants. This part of the experiment was carried out under the following conditions: catalyst dose of 0.25, 0.5, 1 and  $2 \text{ g L}^{-1}$ , initial COD  $860 \text{ mg L}^{-1}$ , pH 7, temperature of  $30 \text{ }^\circ\text{C}$ , and 90 min reaction time. Fig. 10a depicts a good agreement of the nonlinear relationship of photodegradation kinetics with experimental data ( $R^2 > 0.97$ ) and the apparent rate constants of the photocatalytic degradation at 0.25, 0.5, 1 and 2 were calculated as 0.007, 0.033, 0.043 and  $0.058 \text{ min}^{-1}$ , respectively. The variations in COD removal efficiency obtained are illustrated in Fig. 10b. Correspondingly,



(a)



(b)

Fig. 10 (a) Kinetic curves, (b) removal efficiency of SMW with  $\text{Fe}_3\text{O}_4\text{@TiO}_2$  (FT1) at different photocatalyst dose (pH = 3,  $920 \text{ mg L}^{-1}$  initial COD, 90 min reaction time and  $30 \text{ }^\circ\text{C}$ ).



when the photocatalyst dose was increased from 0.25 g to 2 g, the COD removal efficiency was improved from 51.74 to 95.93%. It was speculated that excessive amount of the  $\text{Fe}_3\text{O}_4@\text{TiO}_2$  photocatalyst added to the solution has significant efficiency of photodegradation under UV radiation. However, a further increase in photocatalyst dose above the optimum level (up to  $3 \text{ g L}^{-1}$ ) led to irregular light intensity scattering, so that the reaction rate was lower with an increase in catalyst dosage (figure not shown). Our results showed that the decomposition rate of COD increases linearly with catalyst dose up to  $2 \text{ g L}^{-1}$  and then decreases due to increase in solution turbidity.

**3.2.4. Effect of reaction temperature.** Fig. 11 shows the temperature effect on the COD degradation in the experiments at different temperature in the range of 30–55 °C, whereas the initial COD concentration, dose of photocatalyst, pH and contact time were fixed at  $1070 \text{ mg L}^{-1}$ ,  $1 \text{ g L}^{-1}$ , 3 and 90 min reaction time, respectively. Based on the experimental results, degradation of organic compounds in wastewater using heterogeneous  $\text{Fe}_3\text{O}_4@\text{TiO}_2$  catalysts follows pseudo apparent first-order kinetics (Fig. 11a). Over the examined range temperature, COD degradation was increased as the temperature rose (Fig. 11b). The maximum removal efficiency was obtained at a temperature of 55 °C. Fig. 11c illustrates that the Arrhenius equation demonstrates the effect of a change of temperature on the rate constant from 15 to 45 °C. The calculated  $E_a$  obtained for the photodegradation of organic pollutants in steel industry wastewater by heterogeneous  $\text{Fe}_3\text{O}_4@\text{TiO}_2$  and the corresponding frequency factor and  $R^2$  are presented in Table 3. This is to be stated that the activation energy of  $\text{Fe}_3\text{O}_4@\text{TiO}_2$  system is relatively less than the other reported in the literatures.<sup>21</sup> Fig. 11d shows the Eyring plot

of SMW with  $\text{Fe}_3\text{O}_4@\text{TiO}_2$  at different temperature and Table 3 provides results of the computations of Arrhenius and TST theories for heterogeneous photocatalytic decomposition of COD of steel mill wastewater using  $\text{Fe}_3\text{O}_4@\text{TiO}_2$  nanoparticles. The values of both  $\Delta^\ddagger H^\circ$  and  $\Delta^\ddagger G^\circ$  were found to be positive, while that of  $\Delta^\ddagger S^\circ$  was negative. The increasing value of  $k_{\text{app}}$  and the positive values of  $\Delta^\ddagger H^\circ$  with increasing temperature prove that the decomposition of COD using the  $\text{Fe}_3\text{O}_4@\text{TiO}_2$  is an endothermic process.<sup>21</sup> The endothermic nature of photocatalytic process is possibly due to the electrostatic interaction between the hydrophobic character of  $\text{TiO}_2$  on the photocatalyst surface and organic pollutants. The hydrophobic surface property of  $\text{Fe}_3\text{O}_4@\text{TiO}_2$  photocatalyst favors adsorption of organic pollutants onto charged  $\text{TiO}_2$  surface to achieve efficient photocatalytic degradation and decreases agglomerations of  $\text{Fe}_3\text{O}_4@\text{TiO}_2$  nanoparticles. In addition, the positive values of  $\Delta^\ddagger G^\circ$  increased with an increase in experimental temperature. At a given temperature the more positive value of  $\Delta^\ddagger G^\circ$  at the higher temperature demonstrates that the system will go in the direction of producing reactants (nonspontaneous process) and poor adsorption tendency of organic pollutants on  $\text{Fe}_3\text{O}_4@\text{TiO}_2$  or undesired photocatalytic degradations under given experimental temperatures. Finally, the negative value of standard entropy change of activation ( $\Delta^\ddagger S^\circ$ ) indicates that interactions of potential-determining ions with the active surface sites ( $\text{H}^+/\text{OH}^-$  ions and  $\text{TiO}_2$ ) are less hydrated at the solid/liquid interface.

### 3.3. Studies upon photocatalyst recycling

To examine the reusability and photocatalytic stability of  $\text{Fe}_3\text{O}_4@\text{TiO}_2$  nanocomposite, recycling experiments were also

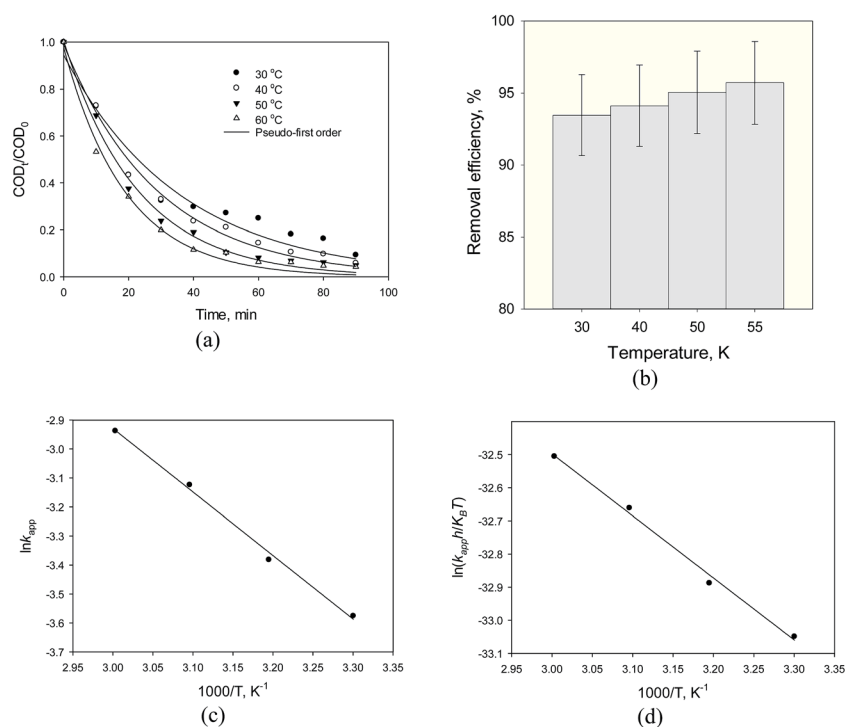


Fig. 11 (a) Kinetic curves, (b) removal efficiency, (c) the Arrhenius plot and (d) the Eyring plot of SMW with  $\text{Fe}_3\text{O}_4@\text{TiO}_2$  (FT1) at different temperature (photocatalyst dose  $1 \text{ g L}^{-1}$ , pH = 3,  $920 \text{ mg L}^{-1}$  initial COD, and 90 min reaction time).



Table 3 Kinetic and activation parameters for the photocatalytic degradation of organic pollutants in petroleum refinery wastewater<sup>a</sup>

T, K	$k_{app}$ , min <sup>-1</sup>	$\ln(k_{app}h/K_B T)$	Arrhenius theory			Transition state theory					
			$E_a$ , kJ mol <sup>-1</sup>	A, min <sup>-1</sup>	$R^2$	$\Delta^\ddagger H^\circ$ , kJ mol <sup>-1</sup>	$\Delta^\ddagger S^\circ$ , kJ K <sup>-1</sup> mol <sup>-1</sup>	$\Delta^\ddagger G^\circ$ , kJ mol <sup>-1</sup>	A, min <sup>-1</sup>	$E_a^a$ , kJ mol <sup>-1</sup>	$R^2$
303	0.028	-37.14	18.21	38.21	0.9957	15.57	-0.258	93.60	13.41	18.09	0.9942
313	0.034	-36.98						96.17	13.85	18.18	
323	0.044	-36.76						98.75	14.30	18.26	
325	0.053	-36.60						101.32	14.74	18.34	

<sup>a</sup>  $E_a = \Delta^\ddagger H^\circ + RT$ .

conducted under optimal conditions. At the end of the first step of decomposition reaction cycle, the Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> nanoparticles were separated from aqueous solution by external magnetic field for a period of 90 min and then the treated wastewater was discharged. The separated photocatalyst was then reused without any treatment. The advantage of the magnetic photocatalytic process of organic pollutant degradation is to be employed for a number of working cycles in order to maintain low cost and the good photocatalytic activity, the easy separation from the aqueous solution, the possibility of reuse. To test the possibility of reusing the photocatalyst Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub>, the experiments were immersed in steel industry wastewater at pH 3, a photocatalyst dose of 1 g L<sup>-1</sup> and 55 °C under exposure to ultraviolet radiation. Under these conditions, the degradation removal efficiency of the photocatalyst was obtained more than 95% within 90 min. When the organic pollutants were degraded, Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> photocatalyst were reused for further wastewater immersion for COD degradation measurement. The results showed that Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> nanoparticles by two and three cycles could degrade organic pollutant of wastewater by slight decreases in the COD removal of 0.90 and 1.40, respectively. The decrease in the removal efficiency of photocatalytic decomposition in the third cycle of the experiment was about 2.28% and 2.75 and 3.16% after the 4 and 5 cycles, respectively. This means that after the photocatalyst Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> was reused in five successive cycles, the degradation removal efficiency of wastewater of 92.54% was obtained, indicating its photocatalytic activity. Our results have demonstrated that the Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> photocatalyst offers great potential photocatalytic activity with a highly efficient degradation rate to be stable and reusable after several treatment cycles with a lower number of possible recycling cycles.

#### 3.4. Comparison of Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> with other photocatalyst

The comparison of maximum percentage removal of as-synthesized Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> photocatalyst by various photocatalyst with respect to different solution pH, different type of photocatalyst, photocatalyst dose and temperature was judged from the literatures. A study demonstrated that the reason for the variations in the photocatalytic activity of TiO<sub>2</sub>-SiO<sub>2</sub> composite are probably related on the effect of change in the molar ratio of Ti to Si.<sup>39</sup> The degradation efficiency of RhB under visible light after 40 min irradiation was about 98.6%, while that

of pure TiO<sub>2</sub> was only 11.9%. They have stated that the superoxide radicals and photogenerated holes are the key reactive species for the decomposition of RhB. Chládková *et al.*<sup>40</sup> have investigated the effect of pH (3–10) on the decomposition of Reactive Red 195 using a mixture of amorphous hydrated TiO<sub>2</sub> and crystalline TiO<sub>2</sub>. They stated that the degradation adsorption of RR195 was increased at the acidic pH compared to the alkaline pH, which was attributed to the strong electrostatic interaction between the catalyst surface and the dye molecules at lower pH values. Under the conditions tested, the degradation efficiency was reported to be at 76 and 66% for pH 3 and 10, respectively. A study<sup>20</sup> has shown that the percentage decomposition of photocatalyst increases with increasing photocatalyst dose and then decreases at high dose because of a decrease of light scattering and screening effects among photocatalyst particles. They reported that a maximum reduction of 80% COD for petroleum refinery wastewater using TiO<sub>2</sub>/Fe-ZSM-5 at pH of 4, a photocatalyst concentration of 2.1 g L<sup>-1</sup>, a temperature of 45 °C and UV exposure time of 240 min. In addition, the problem of particle agglomeration (particle-particle interactions) also increases at high dose of photocatalyst may result in the degradation efficiency of photocatalyst. Zhang *et al.*<sup>41</sup> compared the photocatalytic degradation of gaseous 1,2-dichlorobenzene (*o*-DCB) using ZnFe<sub>2</sub>O<sub>4</sub>/In<sub>2</sub>O<sub>3</sub> hybrid nanoheterostructures under visible light. After 8 h irradiation, the degradation efficiencies of In<sub>2</sub>O<sub>3</sub>, ZnFe<sub>2</sub>O<sub>4</sub> and ZnFe<sub>2</sub>O<sub>4</sub>/In<sub>2</sub>O<sub>3</sub> were reported to be 41.8, 56.7 and 68.7%, respectively. A possible reason stated was that the strong interaction formed at the intimate interfaces between In<sub>2</sub>O<sub>3</sub> and ZnFe<sub>2</sub>O<sub>4</sub> is the favorite for the migration and separation of charge carriers, resulting in long lived e<sup>-</sup>/h<sup>+</sup> pairs. It was found that effect of temperature on biodiesel (90% soybean oil and 10% lard) oxidation was evaluated by kinetic and thermodynamic data using sodium methoxide as catalyst.<sup>42</sup> However, few researches have studied temperature influence on photocatalytic degradation activity.<sup>21</sup> The kinetic parameters were calculated by the L–H model and the energy of activation for decomposition of COD in petroleum refinery wastewater obtained by Arrhenius equation which was reported at about 18.76 kJ mol<sup>-1</sup>. The thermodynamic activation parameters of the reactions, evaluated by the Eyring equation based on the TST, indicated nonspontaneous processes with a  $\Delta^\ddagger G^\circ$  value of 92.82 kJ mol<sup>-1</sup>, a  $\Delta^\ddagger H^\circ$  value of 16.26 kJ mol<sup>-1</sup> and a  $\Delta^\ddagger S^\circ$  value of -0.266 kJ K<sup>-1</sup> mol<sup>-1</sup> at optimum pH of 4, TiO<sub>2</sub>/Fe-ZSM-5 dose of



3 g L<sup>-1</sup> and 45 °C. The heterogeneous photocatalytic decomposition of phenol in aqueous solution was studied using TiO<sub>2</sub> photocatalyst under UV light irradiation in an annular type photoreactor.<sup>43</sup> The kinetic parameters were modelled by the L-H model and the apparent reaction rate constant and removal efficiency for phenol degradation corresponding to the flow rate of 10 L h<sup>-1</sup> and 0.4 g L<sup>-1</sup> TiO<sub>2</sub> dose was found to be 0.00288 min<sup>-1</sup> and 36%, respectively. Abbasi and *et al.*<sup>44</sup> synthesized Fe<sub>2</sub>O<sub>3</sub> nanoparticles *via* a microwave method and Fe<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub> nanocomposites by a sonochemical-assisted procedure. Under UV light irradiation, the photocatalytic activity of Fe<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub> nanocomposites was assessed by measuring the decomposition of MB in aqueous media. The maximum degradation efficiency of MB was achieved about 81% after 100 min synthesis of carboxymethyl-β-cyclodextrin-functionalized Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> (CMCD-Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub>) core-shell nanoparticle was prepared for photocatalytic ability to degrade bisphenol A (BPA) and dibutyl phthalate (DBP) from aqueous solution.<sup>45</sup> They reported that the degradations of BPA and DBP in the presence of CMCD-Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> and Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> using a Hg vapor lamp were obtained to be complete for BPA within 60 min, whereas it was incomplete for DBP even after 180 min of illumination. They also studied the photocatalytic activity of the CMCD-Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> nanoparticles for multiple usages. It maintained 90% of efficiency after 10 cycles compared to the first use efficiency.

In summary, the catalytic mechanism of Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> nanocomposites in mineralization of organic compounds is known by the researchers in the field of environmental photocatalysis and especially they can easily be recycled and reused by external magnetic field due to their strong magnetic response. Moreover, our results demonstrated that the greater reactivity of the as-fabricated photocatalyst is more pronounced than for P25 TiO<sub>2</sub>. However, Fe<sub>3</sub>O<sub>4</sub> core and TiO<sub>2</sub> shell in the nanocomposite core-shell structure play a key role in the photocatalytic degradation process. The active sites on the surface of TiO<sub>2</sub> shell layer can act as adsorbent for photocatalytic function in mineralization of the organic compounds under UV light irradiation and the magnetite particle with about 25 nm crystalline Fe<sub>3</sub>O<sub>4</sub> core allows for the magnetic separation function from the dispersion once yields CO<sub>2</sub> and water, *i.e.*, complete mineralization.

## 4. Conclusion

The experimental data of this study demonstrated that Fe<sub>3</sub>O<sub>4</sub> nanoparticles were successfully synthesized by solvothermal reaction using EAF dust reaction substrate, sodium acetate as a reducer and ethylene glycol as solvent. The core-shell Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> nanocomposites were synthesized by the sol-gel method. The characterization results showed that samples presented a high degree of superparamagnetism and the particle size of Fe<sub>3</sub>O<sub>4</sub> obtained was about 100 nm. The second major finding was that the photocatalytic activity for the decomposition of COD of steel mill wastewater was higher in the acidic pH. In addition, Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> nanoparticles can be reused several times without significant decrease of their efficiency of the oxidation process which indicates that they are

suitable candidates for the practical use in the industrial wastewater treatment. Returning to the question posed at the beginning of this study, it is now possible to state that, using EAF dust is a good alternative to minimize the costs of preparation of photocatalyst, which is considered as an environmentally friendly method, because no salts are volatile or harmful that can be easily recycled. In other words, the Fe<sub>3</sub>O<sub>4</sub> nanoparticles derived in this study could help to reduce the burden on the environment from EAF dust, increase the improvement of the source nanomaterial and reduce the cost of raw materials. Finally, the findings of this study have an important suggestion for future work that other metal oxide nanoparticles could be synthesized from the precursor reacting with HCl in aqueous solution by hydrothermal precipitation with NaOH.

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## References

- 1 G. Salihoglu, V. Pinarli, N. K. Salihoglu and G. Karaca, *J. Environ. Manage.*, 2007, **85**, 190–197.
- 2 T. Sofilić, A. Rastovčan-Mioč, Š. Cerjan-Stefanović, V. Novosel-Radović and M. Jenko, *J. Hazard. Mater.*, 2004, **109**, 59–70.
- 3 S. Smith, X. Zhou and C. Nassaralla, *Iron Steelmaker*, 2000, **27**, 69–76.
- 4 J. O. Edwards and R. Curci, in *Catalytic Oxidations with Hydrogen Peroxide as Oxidant*, Springer, 1992, pp. 97–151.
- 5 C. Huang, C. Dong and Z. Tang, *Waste Management*, 1993, **13**, 361–377.
- 6 O. Legrini, E. Oliveros and A. Braun, *Chem. Rev.*, 1993, **93**, 671–698.
- 7 W. H. Glaze, J.-W. Kang and D. H. Chapin, *Ozone: Sci. Eng.*, 1987, **9**, 335–352.
- 8 G. V. Buxton, C. L. Greenstock, W. P. Helman and A. B. Ross, *J. Phys. Chem. Ref. Data*, 1988, **17**, 513–886.
- 9 J. M. Herrmann, *Top. Catal.*, 2005, **34**, 49–65.
- 10 S. Malato, P. Fernández-Ibáñez, M. Maldonado, J. Blanco and W. Gernjak, *Catal. Today*, 2009, **147**, 1–59.
- 11 J. Blanco-Galvez, P. Fernández-Ibáñez and S. Malato-Rodríguez, *J. Sol. Energy Eng.*, 2007, **129**, 4–15.
- 12 R. J. Watts, S. Kong and W. Lee, *J. Environ. Eng.*, 1995, **121**, 730–735.
- 13 P. Fernández-Ibáñez, J. Blanco, S. Malato and F. De Las Nieves, *Water Res.*, 2003, **37**, 3180–3188.
- 14 V. Loddo, G. Marci, L. Palmisano and A. Sclafani, *Mater. Chem. Phys.*, 1998, **53**, 217–224.



- 15 S. Suresh and D. Ramesh Raja, *Int. J. Chem., Environ. Pharm. Res.*, 2011, **5**, 349–360.
- 16 S. Xuan, W. Jiang, X. Gong, Y. Hu and Z. Chen, *J. Phys. Chem. C*, 2009, **113**, 553–558.
- 17 T. Arai, T. Sato, H. Kanoh, K. Kaneko, K. Oguma and A. Yanagisawa, *Chem.–Eur. J.*, 2008, **14**, 882–885.
- 18 S. Xuan, W. Jiang, X. Gong, Y. Hu and Z. Chen, *J. Phys. Chem. C*, 2008, **113**, 553–558.
- 19 X. W. Lou and L. A. Archer, *Adv. Mater.*, 2008, **20**, 1853–1858.
- 20 Z. Ghasemi, H. Younesi and A. A. Zinatizadeh, *Chemosphere*, 2016, **159**, 552–564.
- 21 Z. Ghasemi, H. Younesi and A. A. Zinatizadeh, *J. Taiwan Inst. Chem. Eng.*, 2016, **65**, 357–366.
- 22 M. Shokouhimehr, Y. Piao, J. Kim, Y. Jang and T. Hyeon, *Angew. Chem.*, 2007, **119**, 7169–7173.
- 23 T. Xin, M. Ma, H. Zhang, J. Gu, S. Wang, M. Liu and Q. Zhang, *Appl. Surf. Sci.*, 2014, **288**, 51–59.
- 24 D. Wang, J. Yang, X. Li, J. Wang, H. Zhai, J. Lang and H. Song, *Phys. Status Solidi A*, 2017, **214**, 1600665.
- 25 J. Liu, Z. Sun, Y. Deng, Y. Zou, C. Li, X. Guo, L. Xiong, Y. Gao, F. Li and D. Zhao, *Angew. Chem., Int. Ed.*, 2009, **48**, 5875–5879.
- 26 APHA, *Standard Methods for the Examination of Water and Wastewater*, American Public Health Association, Washington, DC, 1998.
- 27 P. Atkins and J. de Paula, *Physical Chemistry*, W. H. Freeman, 2002.
- 28 F. Meng, W. Wei, X. Chen, X. Xu, M. Jiang, L. Jun, Y. Wang and Z. Zhou, *Phys. Chem. Chem. Phys.*, 2016, **18**, 2510–2516.
- 29 Y. Fu, H. Du, S. Zhang and W. Huang, *Mater. Sci. Eng., A*, 2005, **403**, 25–31.
- 30 X. Qiao, Y. Luo, A. Sun, C. Wang, J. Zhang, C. Chu, J. Guo and G. Xu, *RSC Adv.*, 2015, **5**, 6489–6493.
- 31 S. C. Xu, Y. Q. Yang, Y. S. Liu, H. Miao, M. Dong, J. Yang, J. M. Zhang, Z. Dai, G. Zheng and B. Sun, in *Advanced Materials Research*, Trans Tech Publ, 2011, pp. 216–219.
- 32 X. Shen, Y. X. Wang, L. Q. Lu, Y. L. Chen, Y. Xia and Y. H. Li, *J. Sol-Gel Sci. Technol.*, 2010, **54**, 340–346.
- 33 R. E. Dunin-Borkowski, M. R. McCartney, R. B. Frankel, D. A. Bazylinski, M. Pósfai and P. R. Buseck, *Science*, 1998, **282**, 1868–1870.
- 34 W. Bahnemann, M. Muneer and M. M. Haque, *Catal. Today*, 2007, **124**, 133–148.
- 35 D. Chen and A. K. Ray, *Water Res.*, 1998, **32**, 3223–3234.
- 36 S. Sakthivel, B. Neppolian, M. Shankar, B. Arabindoo, M. Palanichamy and V. Murugesan, *Sol. Energy Mater. Sol. Cells*, 2003, **77**, 65–82.
- 37 M. Vohra and K. Tanaka, *Environ. Sci. Technol.*, 2001, **35**, 411–415.
- 38 W. Z. Tang and H. An, *Chemosphere*, 1995, **31**, 4157–4170.
- 39 Z.-Y. Yang, G.-Y. Shen, Y.-P. He, X.-X. Liu and S.-J. Yang, *J. Porous Mater.*, 2016, **23**, 589–599.
- 40 B. Chládková, E. Evgenidou, L. Kvítek, A. Panáček, R. Zbořil, P. Kovář and D. Lambropoulou, *Environ. Sci. Pollut. Res.*, 2015, **22**, 16514–16524.
- 41 F. Zhang, X. Li, Q. Zhao and D. Zhang, *ACS Sustainable Chem. Eng.*, 2016, **4**, 4554–4562.
- 42 D. Borsato, D. Galvan, J. L. Pereira, J. R. Orives, K. G. Angilelli and R. L. Coppo, *J. Braz. Chem. Soc.*, 2014, **25**, 1984–1992.
- 43 R. Kar, O. Gupta, K. Mandol and S. Bhattacharjee, *J. Chem. Eng. Process Technol.*, 2013, **4**, 143.
- 44 A. Abbasi, D. Ghanbari, M. Salavati-Niasari and M. Hamadani, *J. Mater. Sci.: Mater. Electron.*, 2016, **27**, 4800–4809.
- 45 R. Chalasani and S. Vasudevan, *ACS Nano*, 2013, **7**, 4093–4104.

