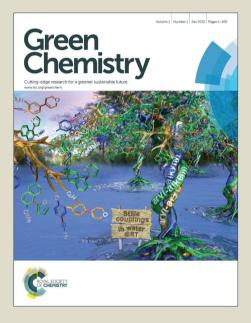
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Received 00th January 20xx, Accepted 00th January 20xx

DOI: 10.1039/x0xx00000x

www.rsc.org/

Direct C–C coupling of bio-ethanol into 2,3-butanediol by photochemical and photocatalytic oxidation with Hydrogen peroxide

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Theoretically, selective C–H manipulation in ethanol can result in a direct C–C coupling synthesis of 2,3-butanediol (2,3-BDO). However, this process is typically extremely difficult to achieve because of the high complexity of the involved chemical bonds. In this work, we determine that hydroxide radicals generated from the photolysis of H_2O_2 can selectively attack α -hydrogen atom in ethanol aqueous solutions and crack the C–H bond to produce hydroxyethyl radicals, which subsequently undergo C–C coupling as 2,3-BDO. This selective C–H breakage is determined by a reaction rate, which is primarily controlled by the local H_2O_2 concentration at a given irradiation intensity. At a moderate reaction rate of ethanol (37 mmol/h), 2,3-BDO selectivity reaching as high as 91% can be obtained. The introduction of catalyst can further increase ethanol conversion and enhance 2,3-BDO formation rate by controlling reaction rate. This result provides an environment-friendly approach to convert bio-ethanol directly to 2,3-BDO and to manipulate a single bond selectively in complex bonding situations.

Introduction

In the modern green chemical industry, selectively manipulating chemical bonds is a primary approach in organic chemistry and catalysis science that is becoming increasingly important.¹ Among them, the practical and selective functionalization of traditionally inert aliphatic C-H bonds have been developed as a powerful strategy to form new chemical bonds.^{2,3} However, one of the major challenges facing the continued advance of this field is requires the ability to manage single bond controllably in a compound containing many such bonds and an array of functional groups.⁴ With increasing demands for energy, concerns about anthropogenically caused global climate change, and depletion of fossil feedstock, more and more attempts have been focusing on alternative and renewable biomass sources for fuels and chemicals. Bio-ethanol, as an important biomass platform molecule, has great potential as a renewable alternative to petroleum, with the advantage of being compatible with current infrastructure.⁵ In the past decade, bio-ethanol production rapidly increased and the total annual capacity reached 100 billion L in 2013.⁶ The transformation of bioethanol into valuable chemicals or a high calorific value fuels is

of great interest in different countries owing to its availability as a feedstock. However, some limitations need to be overcome for the effective application of bio-ethanol. For example, bio-ethanol obtained by fermentation biomasses has large amounts of water (12% ethanol) and dehydration of it is very complex and need to consume large amounts of energy with higher cost due to ethanol-water azeotropic solution.^{7, 8} From the economic standpoint, development water phase reaction for ethanol conversion is very profitable. Moreover, ethanol has multifarious chemical bonds, including α -C-H, β -C-H, O-H, C-O, and C-C. These bonds provide ethanol with versatile functional properties, which has resulted in the current extensive ethanol industry system that produces aldehydes, acids, ethers, esters, olefins, etc.⁹ However, it make difficult to selectively cleave C-H bonds to form new C-C bonds, which is important and challenging in raising conversion efficiency and cleanness. Wang et al. found that the initial dissociation step of ethanol prefers to begin with its O-H bond cleavage leading to CH₃CH₂O and H species rather than the cleavage of other bonds.¹⁰ Davis et al. reported coupling reaction of ethanol into butanol over Hydroxyapatite and Magnesia, the products have ethane and acetaldehyde in addition to butanol.¹¹ The direct transformation of ethanol into ethyl acetate through acetaldehyde formation with bimetallic Pd/Zn catalytic membrane reactors was reported. In this process, it was main job how to avoid the transformation of ethanol to CO and CH₄.¹² Thus, it is very difficult to effectively selective cleaving C-H bonds of ethanol because two or more bonds may be broken normally.

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2,3-BDO is a versatile platform chemical and a potential aviation fuel with a high calorific value (27,198 $\,$ J/g), which can be used to produce butadiene (a monomer of synthetic rubber), methyl ethyl ketone (an excellent organic solvent for resins and lacquers), acetoin, and diacetyl (a flavor enhancer) through dehydration or dehydrogenation reaction.13-15 The increasing annual demand for 2,3-BDO has become a valuable commercial opportunity.¹⁶ Generally, 2,3-BDO could be produced from carbohydrates (glucose, sucrose and glycerol etc.) by bacterial fermentation pathway. So far, the generation rate of 2,3-BDO from glucose is higher than other carbon source, which is not ideal for industrial production.^{17,18} Moreover, large-scale commercial production of 2,3-BDO using bacterial fermentation might be difficult in terms of safety regulations and the high cost of the feedstock. 19-21 Thus, developing a green, clean and high efficiency process based on using low-cost and renewable resources as substrates is imperative.

In this work, we reported one-step synthesis of 2,3-BDO from bio-ethanol via C-C coupling reaction at room temperature. In this process, we found hydroxyl radicals generated from the photolysis of H₂O₂ under UV irradiation can selectively attack α -hydrogen atom in ethanol aqueous solutions and crack the $\alpha\text{--}C\text{--}H$ bond to produce hydroxyethyl radicals (·CH(OH)CH₃), which subsequently undergo C-C coupling form 2,3-BDO. At a moderate ethanol reaction rate (37 mmol/h), 2,3-BDO selectivity can reach as high as 91%. Suzuki et al. also described the laser-induced selective synthesis of diols from methanol and ethanol in the presence of H_2O_2 .²² when ethanol was irradiated, the products were acetaldehyde and butanediol (including 2,3-, 1,3- and 1,4-butanediol). The acetaldehyde was major product and the selectivity was as high as 62%, which showed the O-H bond scission was main in this process, consistent with Wang et al. reported.¹⁰ Moreover, the selectivities of butanediol eg. 2,3-, 1,3-, 1,4-butanediol were 29%, 1%, 2%, respectively. For diols, they found that hydroxyl radicals competitively attacked α -C-H and β -C-H of ethanol to form α -hydroxyethyl radical (·CH(OH)CH₃) and β -hydroxyethyl radical (·CH₂CH₂OH), which subsequently dimerized to form 2,3- and 1,4-butanediol. However, the selectivity of diols was extremely low at 29%, which demonstrates that this technology is unsuitable for precisely manipulating single α -C-H bond breakage. Comparison with Suzuki et al. reported, Our advantages were mainly manifested on the following two aspects: (1) selectively manipulating $\alpha\text{--C--H}$ of ethanol; The hydroxyl radicals can selectively break the α -C-H of ethanol to form new C-C bond, which can be demonstrated by ERP and the high selectivity of 2,3-BDO (91%). Moreover, other butanediol (eg. 1,4 or 1,3butanediol) were not detected in our experiment. (2) Bioethanol instead of ethanol as raw material: we choose water as solvent to avoid the elimination of extensive water in bioethanol, which increase availability and decrease cost. For raising ethanol conversion rate, we investigated the influence of some catalysts on C-C coupling reaction efficiency. By experiment, we obtained that the introduction of catalyst can further accelerate ethanol conversion and enhance the

Results and discussion

To validate the selectivity of H_2O_2 in attacking the chemical bond of ethanol in aqueous solutions, the electron paramagnetic resonance (EPR) spin trapping technique was used. The reaction of H₂O₂ with bio-ethanol in UV irradiation in situ was investigated. The 5,5-dimethyl-l-pyrroline N-oxide (DMPO) spin trap was used in these experiments to detect radical intermediates. As shown in Fig. 1A, a four-line EPR signal from an apparent hydroxyl radical adduct with DMPO (DMPO/·OH, $a_N = a_H = 14.47$ G), which was formed by the photolysis of H₂O₂, could be observed. Furthermore, the other six-line EPR signal was characteristic of DMPO/·CH(OH)CH₃ with $a_N = 15.8$ G and $a_H = 22.6$ G, which was the result of the abstraction of the α -hydrogen atom of ethanol by \cdot OH. Fig. 1 (curve b) shows the computer simulation of the experimental spectrum at the third minute of illumination based on the coupling constants given for the DMPO spin adducts of ·CH(OH)CH₃, ·OH radicals. On the basis of the intensity ratio of these two adducts (9:1), we confirmed that ·CH(OH)CH₃ was the major intermediate radical for the reaction system. This result suggests that the hydroxyl radical from the photolysis of H_2O_2 can precisely crack the α -C-H of ethanol aqueous solutions into the \cdot CH(OH)CH₃ radical.

Moreover, we performed photochemical C–C coupling reaction in a 200 mL aqueous solution in argon atmosphere under UV irradiation at room temperature. The initial concentration of ethanol was 2.39 mol/L, whereas that of H_2O_2 was 0.25 mol/L. 2,3-BDO was produced as a major product, whereas acetaldehyde, acetic acid, carbon dioxide, carbon monoxide and methane were the minor products.

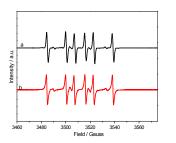


Figure 1 EPR spectrum of the CH₃CH₂OH-H₂O-H₂O₂-DMPO system at third minute of illumination. (a) Experimental spectrum; (b) spectrum for computer simulation with two species: I, DMPO/·OH; $a_N = a_H = 14.47$ G II, DMPO/·CH(OH)CH₃ with $a_N = 15.8$ G and $a_H = 22.6$ G

The conversion of ethanol was 14.2%, and the selectivity of 2,3-BDO was 84% after 5h (Fig. 2). On the basis of these preliminary data, 2,3-BDO could be selectively produced through the C-C coupling of bio-ethanol. We examined the photolysis of H_2O_2 , the conversion of ethanol, and the selectivity of products as a function of reaction time. As shown in Fig. 2A, the photolysis rate of H₂O₂ was extremely rapid in the beginning. However, as reaction time increased, the photolysis rate slowed down and the concentration of H₂O₂ decreased in the solution. The conversion of ethanol is basically consistent with the photolysis of H₂O₂. When the photolysis rate is fast, the quantity of ·OH is large, and the conversion of ethanol is high. When $H_2O_2\,decomposed$ completely, the conversion of ethanol approached equilibrium for approximately 5h. As shown in Fig. 2B, the selectivity of excessive oxidation products, namely, acetaldehyde and acetic acid, was high at the initial reaction stage. By contrast, the selectivity of 2,3-BDO was low. As the reaction progressed, the selectivity of acetaldehyde and acetic acid were evidently reduced, whereas the selectivity of 2,3-BDO gradually increased and then leveled off. The gas products, namely, CO, CO₂, and CH₄, did not evidently change in the entire reaction process. This outcome could be attributed to the high concentration of $\mathsf{H}_2\mathsf{O}_2$ that produced a large amount of $\cdot\mathsf{OH}$ during the early stage, which could not only attack the α -C-H of ethanol to form ·CH(OH)CH₃ radical, but could also further break down the other O-H, C-O, and C-C bonds of ethanol to form aldehydes, acids, or even CO₂. With the increment in time, H_2O_2 concentration and decomposition rate decreased to produce moderate ·OH radicals, which preferentially manipulated the a-C-H of ethanol in aqueous solutions. Thus, the selectivity of 2,3-BDO improved eventually. When ·OH disappeared, the quantity of 2,3-BDO became approximately constant.

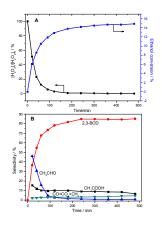


Figure 2 A): the conversion of ethanol and the photolysis of H_2O_2 as function of the reaction time. B): The selectivity of products as function of the reaction time (conduction: ethanol 0.479 mol, $H_2O_2(30\%)$ 0.05mol, 200 ml; 300 W high pressure Hg lamp)

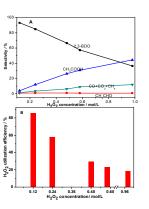


Figure 3 A): Effect of the H_2O_2 concentration on the selectivity of products B): H_2O_2 utilization efficiency as function of concentration (conduction: 298K, 5h, ethanol 0.479 mol, 200 ml; 300 W high pressure Hg lamp)

From the preceding data, we conjectured that H_2O_2 concentration might be one of the important factors that controlled the selectivity of 2,3-BDO. Thus, a series of comparative experiments was performed using a 2.4 mol/L ethanol aqueous solution with different H_2O_2 initial concentrations under a 300 W high-pressure mercury vapor lamp for 5 h. Moreover, the utilization efficiency of H_2O_2 was also investigated through comparative experiments, which can reflect how much H_2O_2 was used for effective coupling bioethanol to 2,3-BDO. Because the \cdot OH from the photolysis of H_2O_2 can not only crack the α –C–H bond to produce \cdot CH(OH)CH₃ (Eq.1-3), but can also occur a chain self-decomposition reaction with residual H_2O_2 to form O_2 (Eq.4-5).

$2 H_2O_2 + hv \rightarrow 2 \cdot OH$	(1)
2 ·OH + 2 CH ₃ CH ₂ OH → 2·CH(OH)CH ₃ + H ₂ O	(2)
$2 \cdot CH(OH)CH_3 \rightarrow CH_3CH(OH)CH(OH)CH_3$	(3)
$\cdot OH + H_2O_2 \rightarrow HO_2 \cdot + H_2O$	(4)
$\cdot OH + HO_2 \rightarrow H_2O + O_2$	(5)

The H₂O₂ utilization efficiency was defined as the ratio of the amount of H_2O_2 used to produce 2,3-BDO with the total amount of H_2O_2 consumed in the reaction, as reported by Wang et al.²³ As H₂O₂ dosage increased, the selectivity of acetic acid improved from 3.9 % to 44.3%, and the gas products increased slightly from 1.3% to 11.8%; aldehyde did not change evidently. However, the selectivity of 2,3-BDO decreased from 93.1% to 36.5% (Fig. 3A). Furthermore, H₂O₂ utilization efficiency was reduced from 85.5% to 19.6% with the increase of H_2O_2 concentration (Fig. 3B). Assuming that extensive H₂O₂ was consumed during excessive oxidation or during its self-decomposition to decrease utilization efficiency is reasonable. These results are consistent with the conclusion in Fig. 2. When H₂O₂ quantity is low, the selectivity of 2,3-BDO is high, and H₂O₂ utilization efficiency is increased. However, the conversion of ethanol is low. Thus, the means to achieve high efficiency in both ethanol conversion and 2,3-BDO formation must be determined.

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From the preceding question, we conjectured if 2,3-BDO formation and ethanol conversion could be improved by the successive addition of H_2O_2 . The successive addition method may control the local concentration of H₂O₂ through the flow rate to avoid the excessive oxidation of ethanol and the ineffective self-decomposition of H₂O₂. Thus, we compared the different addition methods of H₂O₂ through simultaneous and successive addition. The initial concentration of ethanol was 4.8 mol/L. As shown in Fig. 4A (curve a), the conversion of ethanol increased linearly with the successive addition of H₂O₂ at 2 mL/h for 5 h. During simultaneous addition (Fig. 4A, curve b), the conversion of ethanol steeply increased at the initial reaction stage and became nearly constant after 5 h. Compared with simultaneous addition, the successive addition method of H₂O₂ improved the ethanol conversion rate from 24.9 mmol/h to 37.2 mmol/h, the selectivity of 2,3-BDO from 74.0% to 91.3%, and the utilization efficiency of H_2O_2 from 46.3% to 84.9%. Moreover, for the successive addition of H_2O_2 , the selectivity of 2,3-BDO remained basically constant at 91% during the entire irradiation time, and the amounts of aldehyde and acetic acid were minimal (Fig. 4B). The 2,3-BDO formation amount and ethanol conversion were significantly higher in the successive addition of H_2O_2 than in the simultaneous addition. These results verified that the selective manipulation C-H of bio-ethanol could be achieved successfully by controlling local H₂O₂ concentration.

In order to further enhance ethanol conversion rate, we consider if it can be achieved via accelerating the decomposition of H_2O_2 . It was reported that photocatalysts _ can catalyze H_2O_2 decomposition into \cdot OH by accepting the conduction band electrons, thus we investigated the influence of TiO₂ photocatalysts on ethanol coupling reaction (Entry 2-5, Table 1).²⁴⁻²⁶ We found that Rutile – TiO₂ can accelerate the

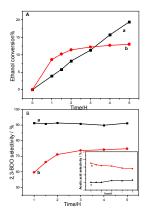


Figure 4 the effect of H_2O_2 addition method on ethanol conversion and 2,3-BDO selectivity (curve a: H_2O_2 was added by successive addition at 2ml/h; curve b: H_2O_2 was added by simultaneous addition); (Reaction conduction: 298K, ethanol 0.959mol, H_2O_2 (30%) 0.1mol, 200 ml; 300 W high pressure Hg lamp)

decomposition of H_2O_2 to increase the instantaneous concentration of ·OH radical, which improved ethanol conversion rate from 37.2 mmol/h to 40.6 mmol/h. After Pt cocatalyst was loaded on Rutile, the ethanol conversion rate was further enhanced to 47.9 mmol/h. when using the highly active P25-TiO₂ instead of Rutile as photocatalyst, the ethanol conversion rate can reach maximum value 55.1 mmol/h and the conversion was 31.4%. However, speeding up H_2O_2 decomposition lead to the selectivity of 2,3-BDO decrease and excessive oxide products increase because of high ·OH radical instantaneous concentration (Table S1). As shown Fig.S2, the generation amount of by-products enhanced obviously with the increase of the reaction rate. The improvement of ethanol conversion rate and maintaining constant selectivity of 2,3-BDO were contradictory, however, in general, the formation rate of 2,3-BDO can be enhanced by accelerating reaction rate. For example, the formation rate of 2,3-BDO increased from 15.3 mmol/h to 18.3 mmol/h using 0.2% Pt/Rutile as photocatalyst. Thus, controlling and choosing moderate reaction rate was very important to improve ethanol conversion rate with high 2,3-BDO formation rate.

Table 1. Experimental date for the photocatalytic C-C coupling of ethanol^a

\longrightarrow OH + H ₂ O ₂ \xrightarrow{hv} OH \rightarrow OH \rightarrow OH + H ₂ O						
Entry	Catalyst	Ethanol conversion (%)	Conversion rate ^b of ethanol (mmol h ⁻¹)	2,3-BDO Selectivity (%)	Formation rate ^c of 2,3-BDO (mmol h ⁻¹)	
1	No catalyst	19.4	37.2	91.3	15.3	
2	Rutile	22.4	40.6	86.1	17.5	
3	0.2%Pt/Rutile	24.9	44.9	81.4	18.3	
4	1%Pt/Rutile	26.8	47.9	61.9	14.9	
5	1%Pt/P25	31.4	55.1	36.5	10.1	
6	SiO ₂	25.0	42.4	75.5	16.0	
7	SBA-15	27.9	49.6	72.5	18.0	
8	γ -Al ₂ O ₃	32.1	55.4	68.6	18.9	

^a Reaction condition: 298K, ethanol 0.959mol, H_2O_2 (30%) 0.1mol was added by successive addition at 2ml/h, 0.2g of catalyst with 0.2% or 1% of Pt co-catalyst, 200 ml; 300 W high pressure Hg lamp, 5h of irradiation time. ^b The rate was calculated on the basis of the converted ethanol.^c The rate was calculated on the basis of the generated 2,3-BDO.

Moreover, based on the decomposition of H_2O_2 catalyzed by ceramic oxides (eg. Al_2O_3 and SiO_2),²⁷ we investigate the effect of some oxides (eg. SiO_2 nanopowers, SiO_2 mesoporous molecular siere (SBA-15) and γ - Al_2O_3) on bio-ethanol coupling reaction (Entry 6 - 8, Table 1). The results were similar to the above Rutile-based catalyst, both ethanol conversion rate and 2,3-BDO formation rate were improved. In coupling reaction, γ - Al_2O_3 displayed the highest ethanol conversion rate (55.4 mmol/h) and 2,3-BDO formation rate (18.9 mmol/h). Both the improvement of ethanol conversion and the increase of 2,3-BDO formation rate can be realized successfully by the introduction of catalyst. In the previous work, yang et al. reported that sacrificial ethanol can be selectively oxidized to 2,3-BDO during the water splitting reaction using pt/TiO₂ as photocatalyst, which discovered the hydroxyl radicals of TiO₂

surface played important role in selective oxidation process. Through fluorine substitution OH groups of Degussa P25 surface, the 2,3-BDO selectivity enhanced from approximately 2.6% to approximately 65%.²⁸ However, this process showed slightly low 2,3-BDO selectivity and long reaction time (24h). In this work, we utilized directly the ·OH radical from the photolysis H₂O₂ to selectively oxidize bio-ethanol to 2,3-BDO, which accelerated ethanol conversion rate to shorten reaction time with relatively high 2,3-BDO selectivity. Moreover, our strategy displayed higher controllability for aliphatic C–H breakage than Suzuki et al. reported. In a word, this result does not only provide an environment-friendly approach to convert bio-ethanol to 2,3-BDO but also provide a promising channel for selectively manipulating inert aliphatic C–H.

Conclusions

We determined that the α –C–H bond of bio-ethanol could be selectively attacked to achieve direct C-C coupling synthesis of 2,3-butanediol with hydroxide radicals from the photolysis of H₂O₂ at room temperature. This selective C-H breakage was determined by the reaction rate, which was primarily controlled by the local H₂O₂ concentration at a given irradiation intensity. The low H_2O_2 local concentration was favorable for selectively cleaving the α –C–H of alcohols. Under a moderate reaction rate of ethanol (37 mmol/h), 2,3butanediol selectivity could reach 91%. The introduction of catalyst can further increase ethanol conversion rate from 37.2 mmol/h to 55.4 mmol/h and enhance the formation rate of 2,3-BDO from 15.3 mmol/h to 18.9 mmol/h via accelerating H₂O₂ decomposition. Comparison with previous synthetic method of 2,3-BDO, our strategy displays shorter reaction time, higher 2,3-BDO selectivity and faster ethanol conversion rate. This approach is a rational strategy to manipulate a single bond selectively in alcohols and to help explain C-C formation in natural photosynthesis.

Experimental Section

All chemical reagents were analytic-grade reagents and used without further purification. SiO₂ nanopowders (15 nm, 99.5%) and γ -Al₂O₃ (40-60 mesh) were purchased from Aladdin. Particle surface areas were determined on a Quantachrome Autosorb 1 analyzer using nitrogen adsorption and desorption at equilibrium vapor pressure and the Brunauer-Emmet-Teller (BET) method of surface area calculation. Specific surface areas of SiO₂ nanopowders, SiO₂ mesoporous molecular siere (SBA-15) and γ -Al₂O₃ particles were 124.3, 712.0 and 209.6 m²/g, respectively. The adsorption average pore diameter of SiO₂ nanopowders, SBA-15 and γ -Al₂O₃ particles were 11.2, 5.52 and 8.24 nm, respectively.

Rutile-TiO₂ was synthesized by a calcination method with commercial TiO₂ powder in a muffle furnace in air at 800° C for 8h. SBA-15 was synthesized according to the method reported elsewhere.²⁹

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Photochemical experiments were conducted in a 250 mL inner irradiation-type Pyrex reactor. A 300 W high-pressure mercury vapor lamp was used as the incandescent light source and was cooled by water to maintain the reactions at room temperature. All the photochemical tests were performed in a 200 mL aqueous solution of reactants and were magnetically stirred to achieve full dispersion, with pure Ar continuously bubbling. Before the photochemical reaction, Ar was purged into the reactor for 30 min to remove the air thoroughly. The reaction course was monitored by periodically sampling the liquid and gas from a sampling valve. Liquid samples were analyzed using a gas chromatograph (Haixin; GC-950) equipped with a flame ionization detector (FID). Gaseous samples were analyzed using a gas chromatograph (Fuli; GC-9790) equipped with a thermal conductivity detector (TCD), a FID. Quantities of the products and reactants were calculated from the peak areas of the compounds using calibration curves.

All the photocatalytic tests were carried out using 0.2g of catalyst, 200 mL of 0.959 mol ethanol aqueous solution and H_2O_2 (30%) (0.1mol) was added by peristaltic pump at 2ml/h for 5h, an appropriate amount (0.2% and 1% Pt) of chloroplatinic acid ($H_2PtCl_6\cdot 6H_2O$), was added to the solution. Before the photocatalyst reaction, Ar was purged into the reactor for 30 min to remove the air thoroughly. The other reaction course was similar to above photochemical experiment.

EPR spectra were recorded using a Bruker EMXplus-10/12. The typical parameters were as follows: sweep width = 100 G, EPR microwave power = 10 mW, modulation amplitude = 0.8 G, time constant = 40.96 ms, and sweep time = 167.77 s. The values of the g-tensor were calculated using Bruker's WIN-EPR SimFonia 2.3 program, which allowed control of the Bruker EPR spectrometer, data acquisition, automation routines, tuning, and calibration programs on a PC with a Windows operating system. The exact g-values of the key spectra were determined by comparing with the 2,2-diphenyl-1picrylhydrazyl (DPPH) standard.

Acknowledgements

This research was financially supported by the National Natural Science Foundation of China (21173250 and U1510108) and the Knowledge Innovation Project of the Chinese Academy of Sciences (KGCX2-EW-311).

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