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**ARTICLE TYPE** 

# Photocatalytic NO<sub>x</sub> abatement: Why the selectivity matters

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Titanium dioxide photocatalysis offers an excellent way to oxidise  $NO_x$  to nitrate and thus reduce air pollution. However, unmodified titanium dioxide also releases a significant amount of the toxic intermediate nitrogen dioxide in the process, a problem that is rarely discussed in previous literature. Herein, we highlight this issue by presenting systematic data on the activity and selectivity of a number of commercial titania powders. The photocatalytic performance of a previously developed W/N-codoped titanium dioxide is also reported which, for the first time, offers a way to eliminate this problem as it exhibits an exceptionally high selectivity towards nitrate. The selectivity appears to be solely dependent on the tungsten content, a concentration of 4.8 at.% is sufficient to induce a very high selectivity. Furthermore, the high selectivity could also be replicated by a W/N-codoped sample derived from the industrial sulphate synthetic process.

The increased selectivity comes at the expense of absolute activity, which is lower than in the reference titania samples. This raises the question of how to properly evaluate  $NO_x$  abatement photocatalysts when there are two factors to consider, activity and selectivity. To resolve this, we propose to define a new figure of merit for the evaluation of  $NO_x$  abatement photocatalysts by distilling total  $NO_x$  removal and selectivity into one value, the DeNOx index. It is derived by assigning a toxicity value to both NO and  $NO_2$  and then expressing the change in total toxicity rather than the concentration change of the individual nitrogen oxides.

Keywords: Photocatalysis, product spectrum, byproduct, doped titanium dioxide, nitrogen oxide toxicity, DeNOx index.

### 1 Introduction

21 Nitrogen oxides, commonly referred to as NO<sub>x</sub>, are a group <sub>22</sub> 2 of different compounds that play a major role in atmospheric 23 3 chemistry and air pollution. The term is usually used to refer 24 4 specifically to nitric oxide (NO) and nitrogen dioxide (NO<sub>2</sub>)  $_{25}$ 5 which are the two most common compounds of this group. 26 6 Although they are sometimes formed in natural processes 27 7 such as lightning the majority of NO<sub>x</sub> emissions are formed <sub>28</sub> 8 anthropogenically in high-temperature processes where both 29 9 oxygen and nitrogen are present, e.g., internal combustion 30 10 engines, gas- or oil-fired heating and industrial furnaces.<sup>1</sup> 31 11 They constitute a major environmental and health concern as 32 12 they are toxic compounds and also facilitate the formation of 33 13 ozone and acid rain.<sup>2,3</sup> As a consequence of this, increasingly <sub>34</sub> 14 stronger regulations and policies are in place enforcing actions 35 15 to reduce emissions and to lower the overall pollutant levels.<sup>4</sup> <sub>36</sub> 16 Apart from reducing the emissions directly by optimising 37 17 the combustion process for low-NO<sub>x</sub> formation rates, sev- $_{38}$ 18 eral other techniques have been developed to reduce the  $NO_{x_{39}}$ 19

emission of combustion processes.<sup>5</sup> Among the more widely adopted procedures are selective catalytic or non-catalytic reduction using a reducing agent such as ammonia to reduce the nitrogen oxides to molecular nitrogen. An alternative approach is to absorb and oxidise the nitrogen oxides in aqueous solutions.<sup>1,6</sup> All of these techniques have in common that they need external reagents and maintenance and are only effective when employed directly at the emission source. There are also recent reports questioning the efficacy of the strategy to reduce ambient NO<sub>x</sub> levels solely by reducing their emissions.<sup>7,8</sup> Semiconductor photocatalysis presents an appealing alternative capable of removing NO<sub>x</sub> and other air pollutants from the air once it has already been released and dispersed.<sup>9</sup> Additionally, photocatalysis needs neither maintenance nor external reagents, since the only required reagents are sunlight and molecular oxygen, which are both already present in outdoor conditions.

Owing to these advantageous properties, photocatalysis has been explored as a way to functionalise building materials to give them air cleaning properties.<sup>10–18</sup> Titanium dioxide based photocatalysts supported on cement-based construction materials for the reduction of nitrogen oxide pollution has been investigated extensively not just at the laboratory scale but also in several real-life pilot projects.<sup>19–23</sup> This highlights that this technology is on the verge of being employed on a large scale in the environment. However, the fundamental reaction mech-

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 $<sup>\</sup>ddagger$  Electronic Supplementary Information (ESI) available: XRD patterns of the synthesised samples. See DOI: 10.1039/b000000x/

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anism of the nitric oxide oxidation, as well as the spectrum and 95 46 fate of the reaction products, are still only poorly understood. 96 47 Up to now, the selectivity of the photocatalytic reaction has 97 48 only been of interest for applications in organic synthesis. <sup>24,25</sup> 98 49 In applications focused on the removal of pollutants from var- 99 50 ious sources, however, usually only the disappearance of the100 51 substrate was considered and the selectivity of the reaction101 52 and the spectrum of products largely ignored. More recently,102 53 the selectivity has attracted some attention and several authors103 54 have highlighted that one of the main aspects of the next gen-104 55 eration of photocatalysts should be their selectivity. 26-31 This105 56 is especially true in the case of photocatalytic removal of nitro-106 57 gen oxides from the air as during the eventual oxidation of the107 58 nitrogen oxides to nitrate there are several toxic intermediate108 59 products, the release of which could be detrimental to the air<sup>109</sup> 60 quality. An improvement in the air quality can only be guar-110 61 anteed by a selective catalyst which suppresses the formation111 62 and the release of these undesired intermediates. 112 63 Herein, we present a detailed description of the photocat-113 64 alytic nitric oxide oxidation, its possible intermediate products114 65 and their individual hazards. Moreover, a new figure of merit 66 for NO<sub>x</sub> abatement photocatalysts, the *DeNOx index* is intro- $_{115}$ 67 duced, which takes account of both activity and selectivity in 68 a single value. This index attempts to depict how a photo-116 69 catalyst will alter the overall air quality through the removal<sub>117</sub> 70 and formation of the various nitrogen oxides. We also present<sub>118</sub> 71 the NO<sub>x</sub> abatement performance of several commercial tita-119 72 nia powders as well as a recently developed W/N-codoped ti-120 73 tanium dioxide, which contrary to ordinary titanium dioxide<sub>121</sub> 74

# 76 2 Experimental Section

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exhibits exceptionally high selectivity.

### 77 Synthesis and characterisation

Samples of pristine, nitrogen- or tungsten-doped, and 126 78 tungsten-nitrogen-codoped titanium dioxide were prepared as127 79 already described previously.32 Briefly, for a typical syn-128 80 thesis, 10 mL of titanium isopropoxide (> 97 %, Sigma-129 81 Aldrich), were dissolved in 10 mL of anhydrous ethanol. Af-130 82 ter thoroughly mixing the solution, 5 mL of deionised water<sub>131</sub> 83  $(18 \text{ M}\Omega \text{ cm})$  were slowly added to the solution. The resulting<sub>132</sub> 84 white precipitate redissolved upon further stirring. In the next133 85 step, 20 mL of a pH 10 ammonia/ammonium chloride buffer134 86 (5% ammonia, Sigma-Aldrich) for the nitrogen containing 135 87 samples or 20 mL of deionised water for the nitrogen free sam-136 88 ples were added to the solution. Finally, the desired amount of 137 89 ammonium tungstate (BDH Chemicals) or tungstic acid (Hop-138 90 kin & Williams) was dissolved in 10 mL of warm deionised139 91 water and subsequently added to the solution. After thorough<sub>140</sub> 92 stirring for at least 4 h, the solution was filtered, washed sev-141 93 eral times with deionised water and then dried at 60 °C for<sub>142</sub> 94

4 h. The dry powders were ground in an agate mortar and then transferred into a crucible for calcination. The samples were calcined either at 400 °C or 600 °C for 4 h and ground again afterwards. Samples of Aeroxide P25 and P90 (Evonik Degussa, Germany), Hombikat UV100, PC50, PC105 and PC500 (Cristal Global), a pure rutile powder (Sigma-Aldrich) and a W/N-codoped titania (PC7A, Huntsman Pigments) were used as received. Brookite nanoparticles were prepared by a procedure reported by Kandiel et al.<sup>33,34</sup> Briefly, 22.2 mL of titanium bis(ammonium lactate) dihydroxide (TALH) aqueous solution (50%, Sigma-Aldrich) was mixed with 200 mL of  $6 \mod L^{-1}$  urea solution. The solution was transferred into a Teflon-lined steel autoclave and heated to 160 °C for 24 h after which it was cooled to room temperature in air. The resulting powder was separated by centrifugation, washed three times with deionised water and dried at 60 °C overnight. Finally, the powder was calcined at 400 °C for 4 h and ground in an agate mortar afterwards. This material was confirmed as 100 % brookite by X-ray diffraction with Rietveld refinement, cf. Figure S1.

### X-ray diffraction analysis

X-ray diffraction patterns were recorded in the range of 20 to 70°  $2\theta$  on a Siemens D5000 diffractometer in Bragg-Brentano geometry with CuK $\alpha_{1,2}$  radiation. The resulting patterns were subsequently used for Rietveld refinement using the software PowderCell 2.4. For the refinement anatase, rutile and brookite as well as hexagonal, triclinic and monoclinic tungsten trioxide were taken into account to calculate the phase composition. The XRD patterns can be found in the supporting information, Figure S1-4.

### Nitric oxide oxidation

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Measurements of the photonic efficiency for the oxidation of nitric oxide were carried out in a glass flow-through reactor where the powder sample were placed on a glass frit inside the reactor so the pollutant gas has to pass through the sample, which is irradiated from above through an optical window. 0.3 g of the samples was uniformly distributed on the circular glass frit with an area of  $8.042 \times 10^{-4} \text{ m}^2$  inside the reactor. The pollutant gas, synthetic air with an nitric oxide concentration of 8 ppm and a volumetric flow rate of  $8.33 \times 10^{-7}$  m<sup>3</sup> s<sup>-1</sup> was then flowed through the reactor. The temperature was controlled using a water jacked around the reactor connected to thermostat and was monitored and kept constant at 27 °C. Prior to entering the reactor, the air was humidified and kept at a constant 42 % relative humidity. The concentrations of NO, NO<sub>2</sub> and total NO<sub>x</sub> in the outlet gas flow were monitored using a Thermo Scientific Model 42i-HL High Level NO-NO2-NOX Analyzer (Air Monitors Ltd., United Kingdom). Each

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8

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4

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0.

Concentration / ppm

Light on

sample was measured in the dark until an equilibrium concen-188 143 tration was reached and afterwards under illumination until189 144 steady state concentrations were observed. An Ultra-Vitalux<sub>190</sub> 145 300 W (Osram, Germany) light source was employed as the191 146 light source for irradiation. The resulting photon flux at the 147 position the powder was placed during the experiment was de-148 termined using ferrioxalate actinometry 35,36 and was found to 149 be  $5.268 \times 10^{-5}$  mol s<sup>-1</sup> m<sup>-2</sup>. Finally, the photonic efficiency 150  $\xi$ , which depicts the ratio of degraded molecules to imping-151 ing photons, was calculated according to eq. 1, where  $c_d$  is the 152 concentration under dark conditions,  $c_i$  the concentration un-153 der illumination,  $\dot{V}$  the volumetric flow rate, p the pressure, A 154 the irradiated area, R the gas constant, T the absolute temper-155 ature and  $\Phi$  the photon flux impinging the photocatalyst sur-156 face as determined by actinometry. The photonic efficiency 157 was determined separately for NO, NO<sub>2</sub> and total NO<sub>x</sub>. 158

$$\xi = \frac{(c_d - c_i) \cdot \dot{V} \cdot p}{\Phi \cdot A \cdot R \cdot T} \tag{1}$$

### 159 **3 Results**

In order to evaluate their suitability as NO<sub>x</sub> abatement pho-160 tocatalysts, several recently developed materials based on 161 W/N-codoped titanium dioxide were tested for their nitric ox-162 ide oxidation capabilities. A total of 24 formulations were 163 tested, ranging from 0 to 16.7 at.% tungsten concentration, 164 with and without nitrogen codoping and calcined at either 400 165 or 600 °C. The physico-chemical properties and band struc-166 ture of these materials have already been reported in detail<sup>195</sup> 167 elsewhere.<sup>32</sup> In order to put the obtained results into perspec-168 tive, validate them and to exclude effects originating from the 169 specific synthesis employed here, several commercially avail-170 able titanium dioxides were also measured and used as stan-171 dards. These include Aeroxide P25 and P90, UV100, PC50,<sup>200</sup> 172 PC105, PC500 and a pure rutile powder. 173

The complete oxidation of nitric oxide (NO) to nitrate 174 or nitric acid  $(NO_3^-/HONO_2)$  in a photocatalytic process is  $^{203}_{204}$ 175 a complex affair that involves several intermediate species 176 and has been previously described in a number of  $publi_{206}^{205}$ 177 cations.  $^{6,11,37-43}$  In principle, the photocatalytic oxidation 178 of nitric oxide to nitrate proceeds in three individual one- $\frac{207}{208}$ 179 electron transfer steps, via the intermediate species nitrous 180 acid (HONO) and nitrogen dioxide (NO<sub>2</sub>). Each step can be 181 realised by the direct reaction with valence band holes or me-182 diated via reactive oxygen species such as superoxide  $(O_2 \cdot \overline{})_{,212}^{211}$ 183 hydrogen peroxide  $(H_2O_2)$  or hydroxyl radicals ( $\cdot OH$ ): 184 213

$$\text{NO} \cdot \xrightarrow{\text{OH}} \text{HONO} \xrightarrow{\text{OH}} \text{NO}_2 \cdot \xrightarrow{\text{OH}} \text{HONO}_2 \qquad (2)_{215}^{214}$$

As shown by example in Figure 1, it sometimes takes sev-216 eral hours, depending on the surface area of the sample, for217 steady state conditions to appear. After reaching that state,218 however, the observed concentrations were constant for hours. Repeated experiments showed that after several cycles, steady state conditions are reached much faster but with the same final concentrations.

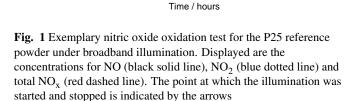
Light off

NO

NOx NO2

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All of the reference powders that are based on anatase exhibit a very similar behaviour, cf. Table 1. The highest degradation rates for nitric oxide are observed with the PC105 powder, closely following by UV100, PC500 and P25. The P90 and PC50 powders are less active by about 30 and 60%, respectively. When total NO<sub>x</sub> is considered rather than just nitric oxide, the removal rates are smaller by a factor of about 3.5 to 4, but the relative ranking remains the same. An exception is the pure rutile powder which shows the lowest activity by far of all the reference powders, only 2 and 8% of the activity of the worst anatase based catalyst PC50 for NO<sub>v</sub> and NO removal, respectively. A pure brookite powder was tested as well for a comparison and it performed comparable with the best anatase based powders in terms of NO removal but at least 30 % better than the best anatase based photocatalyst in terms of NO<sub>x</sub> removal, consistent with other reports of brookite's superior photocatalytic activity.<sup>33</sup> The surface area of the samples seems to have a negligible effect on the observed activity, as both the PC500 powder and the P25 powder exhibit approximately the same activity, even though their surface areas are drastically different  $(350 \text{ m}^2 \text{ g}^{-1} \text{ for PC500})$ versus  $50 \text{ m}^2 \text{ g}^{-1}$  for P25). This indicates that the activity is rate-limited by the photoreaction rather than the adsorption, as predicted by Dillert el al. for the concentrations applied here.<sup>39</sup>

Similar results were obtained when our own pure titanium dioxide powders were measured (W-0 series). However, af-

ter co-doping with tungsten and nitrogen, the observed pho-219 tocatalytic activity significantly decreased. The drop in activ-220 ity appears to be higher for higher tungsten loadings, stabil-221 ising after addition of about 1 at.% tungsten, after which no 222 further decrease in activity was observed, even when the tung-223 sten loading was as high as 16.7 at.%. Interestingly, however, 224 while the drop in nitric oxide oxidation efficiency ( $\xi_{NO}$ ) was 225 decreased by a factor of about 5 to 15, the efficiency in total 226 nitrogen oxide removal  $(\xi_{NOx})$  was only smaller by a factor of 227 about 3 to 6, indicating that the spectrum of the formed prod-228 ucts is significantly altered in the co-doped materials. 229

This highlights that absolute activity should not be the only factor to consider when evaluating photocatalyst performance. The photocatalytic oxidation of nitric oxide to nitrate involves several intermediate steps, most notably the formation of nitrogen dioxide before it is finally fully oxidised to nitrate. Nitrogen dioxide, however, is a strong environmental pollutant itself.

To account for this, nitrogen dioxide levels were also monitored during the photocatalytic reaction and catalyst selectivity for nitrate (S) is introduced as an additional parameter. The selectivity expresses the ratio of degraded NO that ends up as innocuous nitrate rather than toxic nitrogen dioxide and is derived according to eq. 3.

$$S = \frac{\xi_{NOX}}{\xi_{NO}}$$
 (3)<sub>263</sub>

As evident in Figure 2, the selectivity gradually rises with<sub>265</sub> 243 increasing tungsten content. This is true for both the samples<sub>266</sub> 244 doped with tungsten and the ones codoped with tungsten and<sub>267</sub> 245 nitrogen. A significant increase in the selectivity can first be<sub>268</sub> 246 observed at a tungsten loading of 2 at.%. At tungsten loadings<sub>269</sub> 247 of 4.8 at.% or higher, no significant further improvement  $in_{270}$ 248 the selectivity is observed, even when increasing the tungsten-271 249 doping ratio to 16.7 at.%. Instead, all of the samples with high 250 tungsten concentration display more or less the same high se-272 251 lectity of 82 to 91 %. 252 Furthermore, the results were empirically fit with an ex-274 253 ponential decay function (eq. 4, best fit:  $y_0 = 1.560 \times 10^{-4}$ , 275 254  $A_1 = 5.186 \times 10^{-4}, t_1 = 0.0038$ ) for the activity and an asymp-276 255 totic function (eq. 5, best fit: a = 0.91803,  $b = 0.71592_{,277}$ 256  $c = 2.101 \times 10^{-11}$ ) for the selectivity, respectively. With these<sub>278</sub> 257

empirical functions, a good fit for the experimental data was279
obtained with deviations within the expected experimental er-280
rOrs. 281

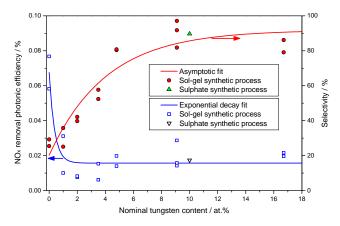
$$y = y_0 + A_1 \cdot e^{-x/t_1} \tag{4}_{284}$$

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286

$$y = a - b \cdot c^x \tag{5}_{285}$$

These materials were produced using a lab-scale sol-gel<sub>287</sub> synthetic process which is expensive and difficult to scale up.<sub>288</sub>



**Fig. 2** Photocatalytic activity for the removal of  $NO_x$ , expressed as photonic efficiency (left axis, blue open squares) and the selectivity of the reaction with respect to nitrate formation (right axis, red filled circles) in relation to the nominal tungsten content of the material. Plotted are the tungsten-nitrogen co-doped TiO<sub>2</sub> samples as well as the purely tungsten doped one. In addition to the sol-gel derived samples there is also a sample synthesised using the sulphate process (PC7A, green and black triangle)

We were, however, able to obtain a W/N-codoped sample with 10 at.% W loading from Huntsman Pigments that was produced using the same sulphate synthetic process commonly used for large-scale  $TiO_2$  production. This sample, denoted PC7A, showed almost exactly the same behaviour in both activity and selectivity as the sol-gel derived samples with similar tungsten loading, proving that these materials can readily be scaled up and produced with established industrial processes.

In order to ascertain that the observed effects are not related to the photocatalyst surface being completely saturated with nitrate, the time at which such a saturation would occur was calculated. It has been shown that nitrate saturation occurs at approximately 2 molecules per square nanometre of photocatalyst surface and that nitrate can freely diffuse into layers not exposed to light so that saturation is only reached when the whole amount of photocatalyst is completely saturated at  $2 \text{ nm}^{-2}$ .<sup>44</sup> Under the conditions employed, this saturation would be reached at approximately  $1 \text{ hg m}^{-2}$  multiplied by the specific surface area of the material, assuming a complete conversion of all nitric oxide to nitrate. Considering that both, the specific surface area of the samples was at least  $10 \text{ m}^2 \text{ g}^{-1}$  and the conversion to nitrate was considerably less than 50% in all cases, it is highly unlikely that nitrate saturation did occur within the maximum of 20 h the experiments were conducted.

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**Table 1** Measured activity data for both, the reference materials and the ones synthesised in this work. Listed are the phase of the material as already reported elsewhere <sup>32</sup> (A = anatase, B = brookite, R = rutile), the photonic efficiencies for the removal of total NO<sub>x</sub> ( $\xi_{NOx}$ ) and NO ( $\xi_{NO}$ ) and the evolution of NO<sub>2</sub> ( $\xi_{NO2}$ ) as well as the calculated quantities nitrate selectivity (*S*) and DeNOx index ( $\xi_{DeNOx}$ )

Sample	Phase / %	S / %	$\xi_{DeNOx}$ / ppm	$\xi_{NOx}$ / ppm	$\xi_{NO}$ / ppm	ξ <sub>NO2</sub> / ppm
Aeroxide P25	75A/25R	27.8	-3689	878	3162	2284
Aeroxide P90	90A/10R	26.8	-3163	710	2647	1937
UV100	100A	27.2	-3928	900	3314	2414
PC50	100A	25.1	-2129	429	1708	1279
PC105	100A	29.1	-4090	1054	3627	2572
PC500	100A	28.8	-3543	897	3117	2220
Rutile TiO <sub>2</sub>	100R	6.9	-232	9	129	120
Brookite TiO <sub>2</sub>	100B	38.8	-2952	1374	3537	2163
W-0-400	70A/30B	27.8	-2273	541	1974	1407
W-0-600	28A/72R	7.5	-1823	77	1026	950
W-0-800	100R	6.3	-1218	42	672	630
WN-0-400	100A	29.3	-2940	768	2622	1854
WN-0-600	96A/4R	9.4	-3938	217	2294	2077
WN-0.1-400	100A	29.1	-1483	382	1315	933
WN-0.1-600	88A/12R	13.6	-1494	127	938	811
WN-0.5-400	100A	24.1	-1598	302	1251	950
WN-0.5-600	100A	24.7	-777	152	617	465
WN-1.0-400	100A	25.1	-500	101	401	301
WN-1.0-600	100A	25.0	-996	199	796	598
WN-2.0-400	100A	39.8	-168	83	208	128
WN-2.0-600	100A	42.1	-132	75	179	104
WN-3.5-400	100A	57.7	-72	153	266	112
WN-3.5-600	100A	52.4	-51	62	118	56
WN-4.8-400	100A	80.8	73	140	173	33
WN-4.8-600	100A	80.4	101	198	246	48
WN-9.1-400	100A	81.8	79	142	174	32
WN-9.1-600	100A	97.1	148	158	162	5
W-9.1-600	98A/2R	91.7	235	287	312	26
WN-16.7-600	100A	86.1	133	196	228	32
PC7A (10% W)	100A	89.7	134	174	194	20

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### 289 4 Discussion

The systematic testing of different titanium dioxide based pho-340 290 tocatalysts revealed that in addition to different rates of reac-341 291 tion, *i.e.*, photocatalytic activity, some catalysts also produce<sub>342</sub> 292 a different spectrum of products. This feature can be easily<sub>343</sub> 293 expressed as the selectivity of the reaction with respect to ni-344 294 trate formation. A high selectivity means that almost all NO<sub>345</sub> 295 is completely oxidised to nitrate before being released into the346 296 environment and that NO<sub>2</sub> release is strongly suppressed. The<sub>347</sub> 297 results of the pure titanium dioxide samples serve to highlight<sub>348</sub> 298 the discussed problem very well, as the main product of their<sub>349</sub> 299 photocatalytic reaction with NO is NO<sub>2</sub>. This is especially<sub>350</sub> 300 true for the samples containing rutile, suggesting that the pres-351 301 ence of this phase is detrimental to the selectivity. These find-352 302 ings are consistent with other reports on photocatalytic NO<sub>x 353</sub> 303 abatement<sup>28,45–55</sup> which also report significant NO<sub>2</sub> evolution<sub>354</sub> 304 upon NO oxidation, although the consequences of this obser-355 305 vation, that these catalysts could potentially increase the air356 306 toxicity rather than decrease it, are usually not discussed. 357 307

However, as illustrated in Figure 2, the increased selectivity is bought at the expense of activity which decreases in turns as the selectivity increases. In terms of conversion to nitrate  $(\xi_{NOx})$ , the activity at higher tungsten content drops to only about a third of its original value.

The existence of two individual parameters - activity on one363 313 side and selectivity on the other - makes an unambiguous eval-364 314 uation of the catalysts exceedingly difficult, especially in this<sup>365</sup> 315 case, where their trends work in conflicting directions. As a366 316 solution to this, we propose to introduce an alternative way to367 317 rate and evaluate photocatalysts in their nitrogen oxide abate-368 318 ment performance, the *DeNOx index* ( $\xi_{DeNOx}$ ). Rather than<sup>369</sup> 319 looking at the concentration changes of the individual nitrogen370 320 oxide species, this index assesses the change in total nitrogen<sup>371</sup> 321 oxide associated toxicity. However, in order to achieve this,372 322 relative toxicity values need to be assigned to the individual<sup>373</sup> 323 374 324 species.

### 325 Relative toxicity assessment of the NO<sub>x</sub> gases

Because both nitric oxide and nitrogen dioxide are very much 326 entwined in atmospheric chemistry, it is difficult to assign 327 exact values for their relative danger. Unfortunately, while375 328 there is information available on acute and chronic toxicity of<sub>376</sub> 329 both compounds at higher concentrations, there is virtually no<sub>377</sub> 330 significant data available on the long-term effects of ambient<sub>378</sub> 331 level exposure to NO and NO<sub>2</sub>. The danger of nitrogen oxides<sub>379</sub> 332 on human health at ambient concentrations is instead derived<sub>380</sub> 333 from epidemiological studies.<sup>56,57</sup> Thus, it is difficult to say<sub>381</sub> 334 how much more dangerous NO2 actually is when compared382 335 to NO in long term chronic exposure to low levels. Here, we<sub>383</sub> 336 arbitrarily assign a relative toxicity value of 1 to NO and 3 to384 337

Given the relative toxicity of 8 to 25 for higher concentrations and the additional risk of ozone formation, the assumption that NO<sub>2</sub> contributes three times as much as NO to the NO<sub>x</sub>-associated air toxicity seems a conservative estimate. The DeNOx index can then be calculated according to eq. 6 or eq. 7, where  $\xi_{NO}$  and  $\xi_{NO2}$  represent the photonic efficiencies of NO removal and NO<sub>2</sub> formation, respectively, and *S* the selectivity towards nitrate formation according to eq. 3.

$$\xi_{DeNOx} = \xi_{NO} - 3 \cdot \xi_{NO2} \tag{6}$$

$$\xi_{DeNOx} = \xi_{NOx} \cdot \left(3 - \frac{2}{5}\right) \tag{7}$$

This index is dimensionless and will be positive if the catalyst lowers the overall  $NO_x$  toxicity, according to the abovementioned weighing, and negative if the catalyst increases the toxicity level. The threshold for a positive index is a nitrate selectivity of at least 66.7 %. It should be noted that using the index in combination with a test that uses pure NO as the pollutant gas overemphasises the possible adverse effects since in real world conditions, there is always a mixture of both NO and NO<sub>2</sub> present, typically in roughly similar concentrations.<sup>8,60,61</sup> This means that while an unselective photocata-

lyst evolves a lot of NO<sub>2</sub> by oxidising NO, it also oxidises<sub>415</sub> 385 some of the NO<sub>2</sub> already present, so the overall NO<sub>2</sub> concen-416 386 tration might not change considerably at all or at least not as417 387 much as the present studies on pure NO might suggest. This  $_{418}$ 388 behaviour is indicated by systematic studies on the photocat-419 389 alytic abatement of different NO/NO2-mixtures using P25 as420 390 a photocatalyst.<sup>46</sup> However, this does not change the fact that<sub>421</sub> 391 a more selective catalyst will still perform better in these con-422 392 ditions as it will both oxidise the already present NO<sub>2</sub> and the<sub>423</sub> 393 NO while avoiding to release any additional  $NO_2$ , resulting in<sub>424</sub> 394 an overall reduction in the NO<sub>2</sub>-level. 395 Many of the tested samples including all reference mate-426 396 rials exhibit a selectivity of 30% or less, reflecting an un-427 397 favourable, negative DeNOx index. Systems characterised by<sub>428</sub> 398 very high activity but inadequate selectivity (< 50%) could<sub>429</sub> 399 potentially increase the air toxicity by predominant formation<sub>430</sub> 400 of NO<sub>2</sub> rather than decreasing it. Only the samples with  $a_{431}$ 401 tungsten content of 4.8 at.% or more displayed a significantly<sub>432</sub> 402 higher selectivity, in the range of 80 to 100 %. Consequently,433 403 these samples should in general be preferred in real world ap-434 404 plications even though their absolute activity is lower than that<sub>435</sub> 405 of the unmodified photocatalysts. 406 436

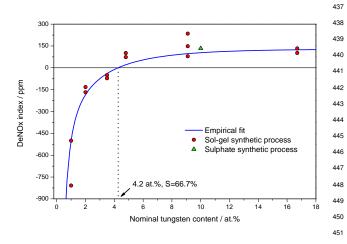


Fig. 3 The DeNOx index as calculated according to eq. 6 for the $^{452}$ W-doped and W/N-codoped titanium dioxide photocatalysts in $^{453}$ dependence of their tungsten content. Displayed are the measured $^{454}$ data points for the sol-gel derived samples (red dots) and the $^{455}$ W/N-codoped TiO2 derived from the sulphate process (PC7A, green456triangle) as well as the empirical fit from Figure 2 (blue line)

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Using the empirical fit functions for activity and selectivity,459 407 eqs. 4 and 5, the resulting DeNOx index can be calculated as460 408 well according to eq. 7 (see solid line in Figure 3) and the tung-461 409 sten content at which the DeNOx index turns positive  $(S \ge \frac{2}{3})^{462}$ 410 estimated at 4.2 at.%. This is in accordance with the experi-463 411 mental results where the samples with 3.5 at.% or less tung-464 412 sten have a negative DeNOx index but the ones with 4.8 at.%465 413 tungsten or higher are all positive. At high tungsten concen-466 414

trations the DeNOx index is virtually constant and no further improvement is observed upon addition of more than 9.1 at.% tungsten.

When the pure titanium dioxides are considered, it appears that all materials based exclusively on anatase exhibit a very reproducible selectivity of 24 to 29 %, independent of their particle size, surface area and synthesis method. This is also the case for the co-doped materials with a tungsten content low enough to not yet induce an increased selectivity, *i.e.*, < 1 %. Likewise, pure rutile powders show a much lower selectivity of 6 to 7%. These results suggest that the selectivity is a fundamental property of the material and that anatase is much more selective than rutile. When mixed phases are considered, a diverging behaviour is observed for some of the materials, as shown in Figure 4. The Aeroxide titanium dioxide particles exhibit the same selectivity as is seen for pure anatase, even though they also contain 10 to 25 % of rutile. However, when the co-doped powders with a low ( $\leq 1$  %) tungsten content are studied, those with even a very small amount of rutile show a drastically reduced selectivity, more in line with what was observed in the pure rutile powders. This may be a consequence of the different synthetic route, as the Aeroxides are produced by flame pyrolysis and the co-doped powders were obtained in a sol-gel synthesis. In fact, the atypical behaviour of the Aeroxides, mainly P25, has already been reported for several other properties, such as their unusually high photocatalytic activity.

It should also be noted that the brookite powder tested here for comparison displays a significantly higher selectivity than the other titanium dioxide phases, 38.8%. However, due to the difficulty in obtaining brookite as a pure phase and the unavailability of it as a commercial product, we were not yet able to confirm this value with different brookite powders.

The selectivity of the reaction is most likely a property of both the photocatalyst and the experimental setup used. Our results presented herein show that the selectivity of a given material, e.g., anatase or rutile, is reproducible within a very small experimental error and no dependence on the surface area, particulate size or absolute photocatalytic activity was observed. In the experimental setup, parameters such as initial concentration of the pollutant gases, gas flow rate and residence time, mass of catalyst used and the irradiance of the light source are expected to have an influence on the selectivity. However, while not showing the exact same value, the low selectivity of ordinary anatase photocatalysts was observed without exception in the variety of different experimental setups that have been reported, including that of the widely used ISO 22197-1 standard. <sup>11,27,43,45-55</sup> Consequently, the selectivity must be a feature attributable mainly to the material used as photocatalyst.

At present, we do not yet understand the mechanism of the increased selectivity. Possible causes should be investigated 515

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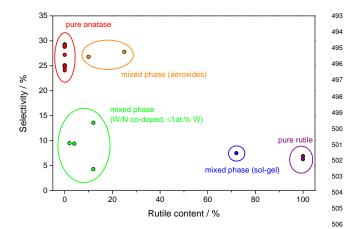


Fig. 4 The selectivity of the photocatalytic reaction with respect to<br/>nitrate formation versus the rutile content in the phase composition.508Plotted are all reference materials and all of the W/N codoped<br/>materials with a tungsten content of 1 at.% or less. The data points<br/>are coloured according to their compositions: pure anatase in red,<br/>pure rutile in purple, mixed phase (Aeroxides, P25 and P90) in<br/>orange, mixed phase (W/N-codoped) in green and mixed phase<br/>(sol-gel, no doping) in blue509

in the different properties of the modified materials and will
be the focus of future studies. These include an altered surface chemistry and acidity, compositional heterogeneity, including surface concentration of specific phases, conduction
band position and electron transfer reactions and changes in
the adsorption capabilities.

# 473 **5** Conclusions

It has been known and reported for some time that while tita-526 474 nium dioxide has the potential to photocatalytically oxidise ni-527 475 tric oxide to nitrate, it also releases a significant amount of the528 476 toxic intermediate nitrogen dioxide in the process. Even so,529 477 the implications of this observation are usually not discussed.530 478 Instead, most authors only report activity as the sole figure of 479 merit and do not mention or discuss selectivity at all. How-480 ever, a poorly selective photocatalyst has the potential to in-531 481 crease the adverse effects of air pollution rather than decrease 482 it by releasing vast amounts of the toxic nitrogen dioxide - this<sup>532</sup> 483 is why the selectivity matters and cannot be ignored. As a pos-533 484 sible solution to the problem, the photocatalytic performance<sup>534</sup> 485 of a previously developed W/N-codoped titanium dioxide is 486 reported which has the potential to eliminate this unwanted  $_{525}$ 487 side-effect. 488

It was shown that several of the novel compositions sig-<sup>536</sup>
 nificantly outperform conventional photocatalysts in terms of <sup>537</sup>
 their nitrate selectivity. The selectivity appears to be solely de-<sup>539</sup>
 pendent on the tungsten doping ratio and independent of nitro-<sup>540</sup>

gen codoping or calcination temperature. A tungsten concentration of 4.8 at.% is sufficient to induce a high selectivity and is not further improved by adding even more tungsten. The high selectivity could also be replicated by a W/N-codoped sample derived from the industrial sulphate synthetic process.

The mechanistic pathway for the increased nitrate selectivity has not as yet been elucidated and will be the focus of future studies on these materials. This is considered to be the first report of selective photocatalytic oxidation of nitric oxide to nitrate using titanium dioxide based materials. Minimising the production of NO<sub>2</sub> in the catalytic process has significant environmental and public health implications and has not been specifically addressed previously in the photocatalytic literature. This property highlights a significant differentiator between the novel W/N-doped catalysts and conventional TiO<sub>2</sub>based catalysts.

However, this increased selectivity is accompanied by a decrease in absolute photocatalytic activity by a factor of about 3. This raises the question of how to properly evaluate  $NO_x$  abatement photocatalysts when there are two figures of merit to consider, activity and selectivity.

By distilling total NO<sub>x</sub> removal and selectivity into one value, we propose to define a DeNOx index ( $\xi_{DeNOx}$ ) for the evaluation of NO<sub>x</sub> abatement photocatalysts. It is derived by assigning a toxicity value to both NO and NO<sub>2</sub> and then expressing the change in total toxicity rather than the change in the individual nitrogen species. The DeNOx index represents the relative change in nitrogen oxide associated air toxicity, defined by the weighing factors of 1 and 3 for NO and NO<sub>2</sub>, respectively, that is caused by the photocatalyst upon illumination. At this point this is an arbitrary assignment since exact toxicity data for long term chronic exposure at the low ambient concentrations are not available, but given the relative toxicity at higher concentrations this seems a conservative estimate. Not only does this new index allow for a better evaluation of the NO<sub>x</sub> removal properties of photocatalysts, it also reduces the amount of data to process, allowing for a clearer picture of the situation.

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