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## Introduction

CO<sub>2</sub>/O<sub>2</sub> separations are of great interest for healthcare and industrial applications. For instance, artificial lungs for CO<sub>2</sub> and O<sub>2</sub> exchange are critical for blood oxygenation;<sup>1,2</sup> atmospheric CO<sub>2</sub> and O<sub>2</sub> compositions can be manipulated for storing and transporting vegetables and fruit to improve their shelf lifetime;<sup>3</sup> CO<sub>2</sub> capture from fossil fuel-derived flue gas has been proposed as a critical way to mitigate CO<sub>2</sub> emissions to the atmosphere, and the flue gas contains 4-16% O2 that needs to be separated from CO2.4,5 Membrane technology offers a cost- and energy-efficient approach for gas separations. However,  $CO_2$  has a kinetic diameter of 3.3 Å, very close to that of  $O_2$  (3.46 Å), and therefore, most polymers do not have sufficiently strong size-sieving ability to obtain high diffusivity selectivity and thus permeability selectivity. For example, Matrimid is widely investigated for membrane separations due to its strong size-sieving ability, and it showed a CO2/CH4 selectivity of 35 but a CO<sub>2</sub>/O<sub>2</sub> selectivity of only 3.8 at 35 °C.6

Gas separation properties can be often manipulated through interactions between polymers and targeted gases. For example, polymers containing poly(ethylene oxide) (PEO) demonstrate good  $CO_2/O_2$  separation properties because of their affinity towards  $CO_2$ , leading to excellent  $CO_2/O_2$  solubility selectivity.<sup>7-9</sup>

# Retarded $O_2$ transport in $Co^{2+}$ -coordinated supramolecular polymer networks for membrane $CO_2/O_2$ separations<sup>†</sup>

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Dissociated  $Co^{2+}$  ions in liquids and polymers have been demonstrated to reversibly react with  $O_2$  and increase  $O_2$  permeability. However, we find a series of  $Co^{2+}$ -coordinated supramolecular polymer networks (SPNs) with enormous  $O_2$  sorption but retarded diffusion, leading to superior  $CO_2/O_2$  separation properties. Specifically,  $Co(BF_4)_2$  is dissolved by cross-linked poly(ethylene oxide) (XLPEO), as validated by Fourier transform infrared (FTIR) spectroscopy, X-ray diffraction (XRD), and differential scanning calorimetry (DSC). The dissociated  $Co^{2+}$  ions increase  $O_2/CO_2$  solubility selectivity but decrease its diffusivity selectivity. For example, adding 6.4 mass%  $Co(BF_4)_2$  in XLPEO increases  $O_2$  solubility by 35 times and  $O_2/CO_2$  solubility selectivity from 0.12 to 5.0, but it decreases  $O_2/CO_2$  diffusivity selectivity from 0.40 to 0.0058, leading to a  $CO_2/O_2$  permeability selectivity of 35, above Robeson's upper bound and superior to that of state-of-the-art polymers. This study unravels an exciting platform of metal ion-coordinated supramolecular networks for various molecular separations by harnessing strong affinity but retarded diffusion despite their stability challenge.

PEO exhibited a  $CO_2/O_2$  selectivity of 18, though its  $CO_2/CH_4$  selectivity was only 20,<sup>8</sup> much lower than that of Matrimid.

 $Co^{2+}$  forms complexes with  $O_2$ , leading to high  $O_2$  sorption, and thus,  $Co^{2+}$ -based  $O_2$ -binding carriers have been reported, such as cobalt porphyrins,<sup>10</sup> cobalt(II) complexes,<sup>11</sup> cobalt(II)based metal-containing ionic liquid (MCIL),<sup>12,13</sup> and Co-based metal-organic frameworks (MOFs).<sup>14</sup> These carriers were incorporated into liquid membranes to improve  $O_2$ /gas separation performance,<sup>12,15,16</sup> as shown in Table 1. For example, introducing Co (3-MeOsaltmen) in dimethylacetamide (DMAc) increased  $O_2/N_2$  selectivity from 1.9 to 25 and achieved  $O_2$ permeability as high as 270 barrer (1 barrer =  $10^{-10}$ cm<sup>3</sup>(STP) cm cm<sup>-2</sup> s<sup>-1</sup> cm<sub>Hg</sub><sup>-1</sup>).<sup>11</sup> However, liquid membranes face instability challenges because of solvent evaporation, pressure-induced liquid loss, and carrier activity loss.

To overcome the instability of liquid membranes,  $\text{Co}^{2+}$ -based carriers were dissolved in solid polymers by ion coordination to form supramolecular polymer networks (SPNs) with good mechanical properties.<sup>20-22</sup> The dissociated  $\text{Co}^{2+}$  can reversibly bind O<sub>2</sub>, improving O<sub>2</sub>/N<sub>2</sub> separation properties (Table 1). For instance, adding 1 wt% cobalt(II) phthalocyanine (CoPc) in Pebax 1657 (a microphase-separated block copolymer containing PEO and nylon) increased O<sub>2</sub>/N<sub>2</sub> selectivity from 2.9 to 8.5.<sup>16</sup> Similar approaches have been adopted to develop Ag<sup>+</sup>-coordinated SPNs for olefin/paraffin separations. As Ag<sup>+</sup> forms complexes with olefins, AgBF<sub>4</sub> was dissolved in Pebax to dramatically increase ethylene/ethane selectivity from 1 to 30.<sup>23,24</sup>

In striking contrast, we report retarded  $O_2$  transport in the SPNs prepared from  $Co(BF_4)_2$  dissociated in crosslinked PEO

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Facilitated transport membranes

Table 1 Enhanced O<sub>2</sub> transport properties in conventional liquid membranes and polymers containing Co<sup>2+</sup>-based carriers

| Polymers/liquids            | Cobalt carriers              | Carrier content<br>(wt%) | Temp.<br>(°C) | Pressure<br>(bar) | O <sub>2</sub> permeability (barrer) | O <sub>2</sub> /N <sub>2</sub> selectivity |  |
|-----------------------------|------------------------------|--------------------------|---------------|-------------------|--------------------------------------|--|--|
| DMAc <sup>11</sup>          | Co (3-MeOsaltmen)            | 15                       | -10           | 0.19              | 270                                  | 25   |  |
| Pebax 1657 (ref. 16)        | CoPc                         | 1                        | 25            | 2                 | 224                                  | 8.5  |  |
| Polycarbonate <sup>17</sup> | CoSalen                      | 3                        | 5             | 3                 | 0.33                                 | 15   |  |
| PDMS <sup>18</sup>          | CoSalen                      | 20                       | 30            | 0.05              | $46^a$ a                             | 7.7  |  |
| PIM-1 (ref. 19)             | $mim_2Co$ (NCS) <sub>4</sub> | 2.0                      | 30            | 2                 | 113                                  | 5.3  |  |



Fig. 1  $Co^{2+}$ -coordinated SPNs with superior  $CO_2/O_2$  separation properties. (a) Schematic of  $O_2$ -retarded transport facilitating  $CO_2/O_2$  separation. (b) Schematic of XLPEO prepared from PEGDA and PEG-MEA and its interactions with  $Co(BF_4)_2$ . (c) Photos of XLPEO/salt films.

(XLPEO) synthesized from poly(ethylene glycol) methyl ether acrylate (PEGMEA) and poly(ethylene glycol) diacrylate (PEGDA) (Fig. 1). The Co ions complex with ether oxygens, enabling complete dissociation of the Co salts, as evidenced by transparent and uniform films obtained (Fig. 1c), leading to extremely high O<sub>2</sub> sorption. However, instead of improving O<sub>2</sub> permeability, increasing the Co(BF<sub>4</sub>)<sub>2</sub> content in XLPEO dramatically decreases O<sub>2</sub> permeability and increases CO<sub>2</sub>/O<sub>2</sub> selectivity. The effect of Co ions on the structures and CO<sub>2</sub>/O<sub>2</sub> transport properties of the SPNs is thoroughly investigated to derive structure and property relationships. This study unveils a new mechanism for harnessing strong binding capabilities with a penetrant to lower its diffusivity and permeability and enable its separation from other penetrants.

## Experimental

#### Materials

PEGDA (n = 13;  $M_n = 700$  g mol<sup>-1</sup>), PEGMEA (n = 9;  $M_n = 480$  g mol<sup>-1</sup>), 1-hydroxycyclohexyl phenyl ketone (HCPK), and Co(ClO<sub>4</sub>)<sub>2</sub>·6H<sub>2</sub>O were received from Sigma Aldrich Corporation

(St. Louis, MO).  $Co(BF_4)_2 \cdot 6H_2O$  was purchased from Thermo Fisher Scientific (Waltham, MA). Gas cylinders of O<sub>2</sub>, N<sub>2</sub>, and CO<sub>2</sub> (99.99%) were obtained from Airgas Inc. (Buffalo, NY).

#### Preparation of Co<sup>2+</sup>-coordinated SPNs

To prepare SPNs, PEGDA, PEGMEA, HCPK (0.1 mass% relative to PEGDA and PEGMEA), and Co salt were dissolved in water. The mass ratio of PEGDA to PEGMEA was set at 1:4 to obtain XLPEO with high gas permeability and good mechanical properties.<sup>25</sup> The prepolymer solution was sandwiched between two quartz plates and photopolymerized using UV light with a wavelength of 254 nm at 3.0 mW cm<sup>-2</sup> for 5 min.<sup>26</sup> The obtained solid films were vacuumed at  $\approx 23$  °C for three days or more to remove water and then kept under vacuum before use. The samples are named XLPEO/salt-*x*, where *x* represents the mass% of the salt in the dried films.

#### **Characterization of SPNs**

Film thickness was measured using a digital micrometer (Mitutoyo Corporation, Kanagawa, JP). An attenuated total reflection-Fourier transform infrared (ATR-FTIR) spectrometer (Vertex 70, Billerica, MA) was utilized at a resolution of 4 cm<sup>-1</sup> to investigate the conversion of PEGDA and PEGMEA and the salt state in XLPEO. The SPN structure was examined using an Ultima IV X-ray diffractometer (XRD, Rigaku Corporation, Tokyo, JP) with CuKa radiation (a wavelength of 1.54 Å) at  $\approx 23 \,^{\circ}$  C. Thermal transitions were obtained by Differential Scanning Calorimetry (DSC, Q2000, TA Instruments, New Castle, DE). Two heating cycles were carried out from -90 to 100 °C at 10 °C min<sup>-1</sup> in a N<sub>2</sub> atmosphere. Glass transition temperature ( $T_g$ ) was determined as the inflection point of a step change in the second heating cycle. SPN density,  $\rho_{SP}$  (g cm<sup>-3</sup>), was determined using an analytical balance equipped with a density kit.<sup>26,27</sup>

Pure-gas permeability of the SPN films was determined using a constant-volume and variable-pressure apparatus at different feed pressures (4.4, 7.9, and 11.3 bar) and 35 °C.<sup>28</sup> The measurement followed an order of N<sub>2</sub>, CO<sub>2</sub>, and O<sub>2</sub>. N<sub>2</sub> was also re-tested for some samples after O<sub>2</sub> to ensure that the samples remained intact after O<sub>2</sub> exposure. Gas permeability has an uncertainty of less than 10%, estimated using an error propagation analysis.<sup>29</sup> Pure-gas sorption in the SPNs (~2 g) was determined using a dual-volume and dual-transducer apparatus based on the pressure-decay method at 35  $^{\circ}C$  and three pressures (~4.5, ~7.9, and ~11.4 bar).^30

## **Results and discussion**

#### Physical and chemical properties of Co<sup>2+</sup>-coordinated SPNs

Fig. 2a exhibits FTIR spectra of XLPEO/Co $(BF_4)_2$  SPNs. The peak at 1096 cm<sup>-1</sup> representing C–O vibration in XLPEO redshifts with increasing Co $(BF_4)_2$  content, indicating the weakened C–O bonds caused by the interactions with  $\text{Co}^{2+}$ .<sup>26,31</sup> For example, adding 17 mass%  $\text{Co}(\text{BF}_4)_2$  lowers the C–O stretching frequency from 1097 to 1057 cm<sup>-1</sup>. By contrast, increasing the  $\text{Co}(\text{BF}_4)_2$ content has minimal impact on the C=O stretching at 1732 cm<sup>-1</sup>, indicating the absence of strong interactions with  $\text{Co}^{2+}$ . Similar behaviors have been observed for XLPEO/Co(Cl<sub>4</sub>)<sub>2</sub> (Fig. S1a<sup>†</sup>). Additionally, the SPNs exhibit a new peak at 623 cm<sup>-1</sup> characteristic of free ClO<sub>4</sub><sup>-</sup> anions, confirming the dissociation of Co(ClO<sub>4</sub>)<sub>2</sub> by XLPEO.<sup>31</sup>



Fig. 2 Physical properties of SPNs. (a) FTIR spectra and (b) XRD patterns of XLPEO/Co(BF<sub>4</sub>)<sub>2</sub>. (c) Correlation between  $\rho_{SP}$  and the salt content using eqn (1). (d) Correlation between  $T_g$  and the salt content using eqn (2).

**Table 2** Physical properties of XLPEO/Co(BF<sub>4</sub>)<sub>2</sub>-x including r (molar ratio of ether oxygens to Co<sup>2+</sup> ions),  $\rho_{SP}$ ,  $T_{g,SP}$ , and pure-gas permeability and selectivity at 35 °C

| x<br>(mass%) | r   | $ ho_{ m SP} ({ m g}  { m cm}^{-3})$ | $T_{ m g,SP}$ (°C) | P <sub>A</sub> (barrer) |       |        | Selectivity |            |           |
|--------------|-----|--------------------------------------|--------------------|-------------------------|-------|--------|-------------|------------|-----------|
|              |     |                                      |                    | $N_2$                   | $O_2$ | $CO_2$ | $CO_2/N_2$  | $CO_2/O_2$ | $O_2/N_2$ |
| 0            | _   | 1.149                                | -63                | 10                      | 26    | 510    | 51          | 20         | 2.6       |
| 2            | 259 | 1.179                                | -63                | 2.9                     | 2.2   | 109    | 38          | 50         | 0.76      |
| 3.4          | 150 | 1.182                                | -62                | 1.2                     | 0.82  | 33     | 28          | 40         | 0.68      |
| 6.4          | 77  | 1.224                                | -57                | 0.49                    | 0.40  | 15     | 31          | 38         | 0.82      |
| 17           | 26  | 1.282                                | -27                | 0.24                    | 0.14  | 8.4    | 35          | 60         | 0.58      |



Fig. 3 Enormous  $O_2$  sorption in XLPEO/Co(BF<sub>4</sub>)<sub>2</sub> SPNs at 35 °C. Effect of the Co(BF<sub>4</sub>)<sub>2</sub> loading on (a) CO<sub>2</sub> sorption isotherms, (b)  $O_2$  sorption isotherms, (c) CO<sub>2</sub> and  $O_2$  solubility, and (d) CO<sub>2</sub>/O<sub>2</sub> solubility selectivity.

Fig. 2b and S1b<sup>†</sup> show that both series of SPNs are amorphous at  $\approx 23$  °C, validating complete dissociation of the Co salts by XLPEO. Adding salts has a minimal effect on the *d*-spacing (4.2 Å). Fig. 2c shows that increasing salt content increases  $\rho_{\rm SP}$  (Tables 2 and S2<sup>†</sup>), which can be described using an additive model:<sup>31</sup>

$$\frac{1}{\rho_{\rm SP}} = \frac{w_{\rm P}}{\rho_{\rm P}} + \frac{w_{\rm S}}{\rho_{\rm S}} = \frac{1}{\rho_{\rm P}} + \left(\frac{1}{\rho_{\rm S}} - \frac{1}{\rho_{\rm P}}\right) w_{\rm s} \tag{1}$$

where *w* is the mass fraction, and the subscripts of *P* and *S* represent properties of XLPEO and the amorphous salt, respectively. The fittings yield a  $\rho_{\rm S}$  value of 3.84 g cm<sup>-3</sup> for amorphous Co(ClO<sub>4</sub>)<sub>2</sub> and 2.83 g cm<sup>-3</sup> for amorphous Co(BF<sub>4</sub>)<sub>2</sub>. However, there are no reported values for anhydrous crystalline or dissociated amorphous Co(ClO<sub>4</sub>)<sub>2</sub> or Co(BF<sub>4</sub>)<sub>2</sub> in the literature for comparison.

Fig. S1c and d<sup>†</sup> present the DSC thermograms of the SPNs. All samples do not show degradation at the temperatures ranging from -90 to 100 °C, indicating their potential applications for typical O<sub>2</sub> purification (~23 °C). XLPEO shows a crystallization peak at -36 °C and a melting peak at -7 °C, which disappear after adding Co(BF<sub>4</sub>)<sub>2</sub> because of the complexation between ethylene oxides and Co<sup>2+</sup>. The absence of melting peaks at around 0 °C also suggests the absence of water in these films.<sup>32</sup> Additionally, increasing salt loading increases  $T_{\rm g,SP}$  (Tables 2 and S2†), which can be described using an empirical equation:<sup>26,33</sup>

$$1/T_{g,SP} = 1/T_{g,P} - ac_S$$
 (2)

where  $T_{\rm g,P}$  is the glass transition temperature of XLPEO (K), *a* is an adjustable constant, and  $c_{\rm S}$  is Co<sup>2+</sup> content (kmol m<sup>-3</sup>). Fig. 2d shows that the best fit yields a value of  $8.1 \times 10^{-4}$  m<sup>3</sup> kmol<sup>-1</sup> K<sup>-1</sup>, close to that for XLPEO/Ni(BF<sub>4</sub>)<sub>2</sub> (9.3 × 10<sup>-4</sup> m<sup>3</sup> kmol<sup>-1</sup> K<sup>-1</sup>, Table S2†).<sup>26</sup>

#### Gas sorption properties of SPNs

To elucidate the effect of the salt content on gas transport properties,  $CO_2$  and  $O_2$  sorption isotherms for XLPEO/Co(BF<sub>4</sub>)<sub>2</sub> were obtained at 35 °C and are displayed in Fig. 3a and b.  $CO_2$ and  $O_2$  solubility can be calculated (Fig. 3c and Table S3†). Increasing Co(BF<sub>4</sub>)<sub>2</sub> loading decreases CO<sub>2</sub> solubility and significantly increases  $O_2$  solubility. For instance, adding 6.4 mass% Co(BF<sub>4</sub>)<sub>2</sub> in XLPEO increases  $O_2$  solubility from 0.19 to



Fig. 4 Pure-gas transport properties of the SPNs at 35 °C. Dependence of gas permeability on (a)  $Co(BF_4)_2$  loading and (b)  $Co(ClO_4)_2$  loading. Dependence of  $CO_2$ /gas selectivity on (c)  $Co(BF_4)_2$  loading and (d)  $Co(ClO_4)_2$  loading. Effect of the  $Co(BF_4)_2$  loading on (e)  $CO_2$  and  $O_2$  diffusivity and (f)  $CO_2/O_2$  diffusivity selectivity.



**Fig. 5** Superior  $CO_2/O_2$  separation properties in XLPEO/Co(BF<sub>4</sub>)<sub>2</sub> (x = 2, 3.4, and 17) compared with Robeson's upper bound,<sup>36,37</sup> and representative polymers, including Matrimid,<sup>6</sup> Pebax 1657 and 2533,<sup>9</sup> 6FDA-DAM,<sup>38</sup> PDMS,<sup>1</sup> and PIM-1.<sup>39</sup>

6.7 cm<sup>3</sup>(STP) cm<sup>-3</sup> atm<sup>-1</sup> because of the Co<sup>2+</sup>–O<sub>2</sub> complexation and decreases CO<sub>2</sub> solubility from 1.5 to 1.3 cm<sup>3</sup>(STP) cm<sup>-3</sup> atm<sup>-1</sup> due to the competitive interactions with XLPEO from the Co<sup>2+</sup> ions. More importantly, increasing the Co(BF<sub>4</sub>)<sub>2</sub> content decreases CO<sub>2</sub>/O<sub>2</sub> solubility selectivity and significantly increases O<sub>2</sub>/CO<sub>2</sub> solubility selectivity (Fig. 3d and e). In contrast, adding Co(ClO<sub>4</sub>)<sub>2</sub> has minimal impact on O<sub>2</sub> solubility (Fig. S2a†). Although the underlying mechanism for missing O<sub>2</sub> affinity in XLPEO/Co(ClO<sub>4</sub>)<sub>2</sub> is unclear, it is widely reported that anions and ligands can significantly influence the complexation between Co<sup>2+</sup> and O<sub>2</sub>. For example, Co<sup>2+</sup>-based carriers with different anions exhibited a wide range of O<sub>2</sub> sorption values between 0.06 and 0.90 mol O<sub>2</sub> per mol carrier at 16 cm<sub>Hg</sub>.<sup>11</sup> Similarly, when various silver salts were dissolved in PEO for C<sub>3</sub>H<sub>6</sub> sorption, the SPNs showed a molar ratio of C<sub>3</sub>H<sub>6</sub> to Ag<sup>+</sup> of 0.49 for AgBF<sub>4</sub>, 0.13 for AgCF<sub>3</sub>SO<sub>3</sub>, but only 0.03 for AgNO<sub>3</sub>;<sup>34</sup> anions of bis(trifluoromethylsulfonyl)imide (Tf<sub>2</sub>N) stabilized Ag<sup>+</sup> against H<sub>2</sub>, but not NO<sub>3</sub><sup>2-</sup> anions.<sup>35</sup>

#### Gas permeation properties of the SPNs

Fig. 4a and b present the effect of the  $Co(BF_4)_2$  and  $Co(ClO_4)_2$ content in XLPEO on pure-gas permeability at 35 °C (a typical temperature used for membrane applications), respectively. Increasing the salt loading decreases gas permeability because of the increased  $T_{g,SP}$ . For instance, adding 17 mass% Co(BF<sub>4</sub>)<sub>2</sub> decreases CO2 permeability by 98.4% from 520 to 8.4 barrer and O2 permeability by 99.5% from 26 to 0.14 barrer. Similar behaviors have been observed for XLPEO with the addition of LiClO<sub>4</sub>, Ni(BF<sub>4</sub>)<sub>2</sub>, and Cu(BF<sub>4</sub>)<sub>2</sub> were correlated with the increased  $T_{\rm g,SP}$ .<sup>26</sup> Increasing the salt content also decreases CO<sub>2</sub>/  $N_2$  selectivity because of the interactions between  $Co^{2+}$  and XLPEO, which reduce the favorable interactions between CO<sub>2</sub> and XLPEO. Importantly, XLPEO/Co $(BF_4)_2$  SPNs exhibit unexpected CO<sub>2</sub>/O<sub>2</sub> selectivity. For instance, adding only 3.4 mass%  $Co(BF_4)_2$  increases  $CO_2/O_2$  selectivity from 20 to 40, while adding Co(ClO<sub>4</sub>)<sub>2</sub> consistently decreases CO<sub>2</sub>/O<sub>2</sub> selectivity (Table S1<sup>†</sup>). Interestingly, XLPEO/Co( $BF_4$ )<sub>2</sub> SPNs even show  $O_2/N_2$ 

selectivity less than 1 (Fig. S2b†), which is very unusual for polymeric films.

CO<sub>2</sub> and O<sub>2</sub> diffusion coefficients ( $D_A$ , cm<sup>2</sup> s<sup>-1</sup>) can be calculated by using  $D_A = P_A/S_A$ , and the results are shown in Fig. 4e, f, S2c and Table S3.† Increasing the Co salt content decreases CO<sub>2</sub> diffusivity because of the decreased chain flexibility, as indicated by the increased  $T_{g,SP}$ . Importantly, adding 17 mass% Co(BF<sub>4</sub>)<sub>2</sub> increases CO<sub>2</sub>/O<sub>2</sub> diffusivity selectivity from 2.3 to 650, validating the retarded O<sub>2</sub> diffusion in the XLPEO/ Co(BF<sub>4</sub>)<sub>2</sub> SPNs. In contrast, adding 17 mass% Co(ClO<sub>4</sub>)<sub>2</sub> increases CO<sub>2</sub>/O<sub>2</sub> diffusivity selectivity only to 5.7 (Fig. S2c†).

#### CO<sub>2</sub>/O<sub>2</sub> separation properties

Fig. 5 exhibits superior  $CO_2/O_2$  separation properties of the XLPEO/Co(BF<sub>4</sub>)<sub>2</sub> SPNs in Robeson's upper bound plot.<sup>36,37</sup> All XLPEO/Co(BF<sub>4</sub>)<sub>2</sub> SPNs (x = 2, 3.4, and 17) exhibit  $CO_2/O_2$  separation properties above the upper bound.

Our preliminary data show that the SPNs may lose separation properties over time, as shown in Table S4.† After storage in a vacuum for ~4 months, a freestanding film (XLPEO/Co(BF<sub>4</sub>)<sub>2</sub>-5) was tested with CO<sub>2</sub> at 50 psig and O<sub>2</sub> at 100 psig alternatively for 9 days. CO<sub>2</sub> permeability decreased from 75 to 12 barrer, and CO<sub>2</sub>/O<sub>2</sub> selectivity decreased from 100 to 48, presumably because of the instability of Co<sup>2+</sup> ions. Though CO<sub>2</sub>/O<sub>2</sub> selectivity is still above the upper bound, the practical applications of these SPNs will need more investigation.

## Conclusion

We began this work with a hypothesis that Co<sup>2+</sup>-based carriers can be incorporated into XLPEO to increase O2 sorption and permeability because of the affinity of  $O_2$  towards  $Co^{2+}$ .  $Co(BF_4)_2$ at loadings as high as 17 mass% can be dissociated by XLPEO to form SPNs, as indicated by DSC and XRD results. As expected, increasing  $Co(BF_4)_2$  content increases  $T_{g,SP}$  and density and decreases gas permeability. Importantly, it dramatically increases O2 solubility and O2/CO2 solubility selectivity. Surprisingly, the XLPEO/Co(BF<sub>4</sub>)<sub>2</sub> SPNs exhibit extremely low O<sub>2</sub> permeability due to the retarded O2 diffusion and thus unexpectedly high CO<sub>2</sub>/O<sub>2</sub> permeability selectivity, surpassing Robeson's upper bound and current leading materials for CO<sub>2</sub>/ O<sub>2</sub> separation. This study unveils a new series of SPNs with the potential for CO<sub>2</sub>/O<sub>2</sub> separations, and the discovered retarded diffusion may be harnessed to design high-performance materials for various gas and vapor separations.

Interestingly, adding  $Co(ClO_4)_2$  into XLPEO does not improve  $O_2$  sorption and decreases  $CO_2/O_2$  permeability selectivity. We expect that the anion type influences the dissociation of the Co salts and the ability of  $Co^{2+}$  ions to interact with polymers and  $O_2$ . Additionally,  $Co^{2+}$  is subjected to oxidation and converted to  $Co^{3+}$  without affinity towards  $O_2$ . Therefore, experimental investigation and computational simulations will be needed to unravel the underlying mechanisms and determine the carrier stability. Future work should also focus on preparing thin-film composite membranes and evaluating them with real gas streams to determine long-term stability.

# Author contributions

T. A.: conceptualization, investigation, data curation, writing – original draft preparation; N. E.: data curation and discussion, writing-reviewing and editing; G. Z.: data curation and discussion, writing-reviewing and editing; H. L.: conceptualization, writing-reviewing and editing, supervision.

# Conflicts of interest

There are no conflicts to declare.

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