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## Introduction

Due to the need to change our fossil-based economy to a renewable based one,<sup>1–6</sup> methods to transform renewables with high selectivity are in demand. Thereby fatty acids can be considered as a broadly available raw material and selected methods for their transformation have been reported.<sup>7–9</sup> Although functionalised derivatives like  $\alpha$ -hydroxylated fatty acids serve as intermediates for the synthesis of  $\alpha$ -keto acids,<sup>10</sup>  $\alpha$ -amino acids,<sup>11</sup> as building blocks for bio-polyester<sup>12,13</sup> and to produce pharmaceuticals,<sup>14</sup> as antimicrobial agents and natural products,<sup>15</sup> their preparation is still challenging when starting from the non-functionalised fatty acid.

## Preparative regio- and stereoselective $\alpha$ -hydroxylation of medium chain mono- and dicarboxylic fatty acids<sup>†</sup>

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Regio- and stereoselective functionalisation reactions like C–H oxidation are of high importance for instance for the valorization of renewables like fatty acids by  $\alpha$ -hydroxylation. Here, peroxygenases were envisioned to be of high interest as they require common hydrogen peroxide as the only oxidant generating water as the sole side product. As the unspecific peroxygenase from *Hypoxylon* sp. (*Hsp*UPO) turned out to be not selective for  $\alpha$ -hydroxylation, various bacterial peroxygenases from the CYP152 family were tested for the stereoselective  $\alpha$ -hydroxylation of medium chain fatty acids (C6, C8, C10). The enzyme P450<sub>Exa</sub> proved to be highly suitable for the conversion of caproic acid (C6) (95% conv.) and showed high regioselectivity to give the  $\alpha$ -hydroxylated product ( $\alpha$  :  $\beta$ -selectivity = 14 : 1). Additionally, P450<sub>Exa</sub> successfully converted the dicarboxylic acids azelaic acid (C9) and sebacic acid (C10) exclusively to the corresponding  $\alpha$ -monohydroxylated product (up to >99% conversion). P450<sub>Spa</sub> hydroxylated the fatty acids C6, C8 and C10 preferentially in  $\alpha$ -position giving the optically pure or optically enriched (*S*)-enantiomer [ee 95–>99% (*S*)] with up to 99% conversion. Both enzymes were used for preparative synthesis of  $\alpha$ -hydroxylated fatty acids at up to 150 mM substrate concentration on 50 mL scale giving for instance 2-hydroxyoctanoic acid with 87% yield on gram scale (1260 mg) reaching TONs up to 42 000.

Using traditional chemical routes, functionalising saturated fatty acids bearing only a carboxylic acid group and many C-H bonds requires rather harsh conditions and is only moderately regioselective and not stereoselective, thus leading to the racemic product.<sup>16,17</sup> Although enzymes/biocatalysts are known to work under mild conditions in buffer and display high regio- and stereoselectivity,<sup>18-21</sup> C-H functionalisation is still a challenge. Typical enzymes for hydroxylation are P450 monooxygenases mediating e.g. the oxidation of aliphatic C-H bonds, aryl C-H bonds and C=C double bonds with a high degree of chemo-, regio- and stereoselectivity.<sup>22-25</sup> P450 peroxygenases and unspecific peroxygenases (UPOs) allow comparable oxy-functionalisation to P450 monooxygenases but are independent of reduced nicotinamide cofactors and electron transport chains, and rely on hydrogen peroxide as the only oxidant and source of oxygen.<sup>26-31</sup> Hydrogen peroxide can be considered as a green reagent,<sup>32</sup> as it is a stable oxidant and gives water as the only side product. The challenges with H<sub>2</sub>O<sub>2</sub>-driven biocatalysis are the inactivation of an enzyme at elevated peroxide concentration as amino acids may be oxidized,<sup>33,34</sup> or the heme group itself gets degraded.<sup>35–37</sup> Another challenge is the over-oxidation of desired products, like recently observed for the  $\alpha$ -hydroxylation of fatty acids

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leading to  $\alpha$ -keto acids,<sup>38</sup> which are sensitive to decarboxylation in the presence of H<sub>2</sub>O<sub>2</sub>. Consequently, various approaches have been developed to generate the H<sub>2</sub>O<sub>2</sub> *in situ* to keep the H<sub>2</sub>O<sub>2</sub> concentration low.<sup>39-45</sup>

Peroxygenases were mostly used for the hydroxylation of long chain fatty acids, and only few reports investigated medium chain fatty acids.<sup>10,11,35,38,46,47</sup> Nevertheless, the global supply of medium chain fatty acids like caproic acid, caprylic acid and capric acid relies on oils like coconut, corn and palm oil<sup>48</sup> and the global market of these medium chain fatty acids is expected to reach USD 2.03 Billion by 2028.<sup>49</sup> Consequently, our focus here is the regioselective hydroxylation of medium chain fatty acids (C6:0, C8:0 and C10:0) to identify a suitable enzyme and a reaction protocol which can then be used on preparative scale and also for dicarboxylic acids.

#### Results and discussion

#### Medium chain fatty acid hydroxylation by an UPO (HspUPO)

In a first approach, the unspecific peroxygenase from Hypoxylon sp.  $(HspUPO)^{50}$  was investigated for the possible regioselective hydroxylation of the fatty acids caproic acid (C6:0, 1a), caprylic acid (C8:0, 1b) and capric acid (C10:0, 1c). The biotransformations were performed in phosphate buffer using acetonitrile (MeCN) as co-solvent and H<sub>2</sub>O<sub>2</sub> as oxidant. The enzyme had been produced by excretion using Pichia pastoris and was therefore a catalase free preparation. In contrast to methods for *in situ* generation of H<sub>2</sub>O<sub>2</sub> and also in contrast to batchwise addition of H<sub>2</sub>O<sub>2</sub>,<sup>11,46</sup> here the H<sub>2</sub>O<sub>2</sub> was supplied by continuous feeding of an H<sub>2</sub>O<sub>2</sub>-solution to supplement the reaction overall with (at least) stoichiometric amounts of oxidant. Using this approach, we expected to avoid elevated concentration of H<sub>2</sub>O<sub>2</sub>. Furthermore, the local H<sub>2</sub>O<sub>2</sub> concentration at the inlet was expected to be kept to a minimum by vigorous shaking or stirring.

Under the conditions employed, *Hsp*UPO converted caproic acid **1a** with 39% conversion (Scheme 1). Thereby the ( $\omega$ -1)-hydroxylated ( $\omega$ -1)-**2a** and the  $\beta$ -hydroxylated product  $\beta$ -**2a** were detected in a ratio of **1.8:1**. Alpha-hydroxylation was not



Scheme 1 Oxidative biotransformation of medium chain saturated fatty acids with *Hsp*UPO. Reactions were performed in 1.5 mL glass crimp vials. Reactions were analysed after derivatisation (BSTFA with 1% TMCS). Conversions [%] refer to the consumption of substrate and were determined by GC-MS using internal standard (ISD) in comparison to the sample at 0 hours. Ratios for mono-hydroxylated products were calculated based on GC-area (Fig. S9–S11†). Red circles illustrate that no  $\alpha$ -hydroxylation was observed.

observed at all. The same is true for octanoic acid **1b**, for which hydroxylation was primarily observed for the ( $\omega$ -1)-position but also detected in the  $\beta$ -,  $\gamma$ -, and  $\delta$ -positions. Also for capric acid **1c** the main mono-hydroxylation product had the alcohol-moiety in ( $\omega$ -1)-position, whereby hydroxylation was also observed in  $\beta$ - and  $\alpha$ -position in a ratio of ( $\omega$ -1): $\beta$ : $\alpha$  = 1.7:1.5:1. The incomplete mass balance detected for all three fatty acids by GC also indicated, that most likely also decarboxylation occurred, which fits to the observation, that the enzyme performed also  $\beta$ -hydroxylation.<sup>51</sup> The observed preferred ( $\omega$ -1)hydroxylation for the UPO is also in line with a very recent report describing the improvement of the ( $\omega$ -1)-preference by enzyme engineering of an UPO from another fungus (*Aae*UPO).<sup>27</sup>

Consequently, as the unspecific peroxygenase *Hsp*UPO was found to be indeed unspecific with respect to the position of hydroxylation of the fatty acids investigated and did not give  $\alpha$ -hydroxylation in significant amounts, we turned our attention to peroxygenases from the CYP152 family, expecting them to show higher specificity for  $\alpha$ -hydroxylation. Furthermore, we also considered to change the co-solvent MeCN, which is sometimes rated as not ideal in the solvent selection guides, <sup>52–54</sup> due to supply volatility, difficulties in dealing with MeCN waste and poor scoring with regard to life cycle management.<sup>55</sup> Consequently, biotransformations were performed using ethanol as an environmentally more preferable co-solvent.<sup>56</sup>

#### Fatty acid hydroxylation by members of the CYP152 family

Since the UPO turned out to be not suitable for hydroxylation in  $\alpha$ -position, six  $\alpha$ -hydroxylases from the CYP152 family  $(P450_{Sp\alpha}, {}^{57}P450_{CLA}, {}^{35}P450_{Bs\beta} {}_{F79L/G290F}, {}^{58}P450_{Ex\alpha}, {}^{59}CYP152K6^{60}$  and  $P450_{J\alpha} {}^{47}$ ) were selected from literature. Some of them (CYP152K6, P450<sub>Bs $\beta$  F79L/G290F</sub>, P450<sub>Ex $\alpha$ </sub>) have not been investigated for the transformation of medium chain fatty acids before, while for the others various challenges like overoxidation or expression issues have been reported.38 While CYP152s have often been reported to be difficult to express in soluble form or in sufficient quantities in E. coli, all the potential enzyme candidates were successfully expressed (ESI Fig. S1-S6<sup>†</sup>), whereby the choice of an appropriate expression construct was essential, especially in the case of P450<sub>Spg</sub> (see ESI Plasmids<sup>†</sup>). Since E. coli possesses catalase activity, which would disproportionate the H<sub>2</sub>O<sub>2</sub> reagent, the enzymes had to be purified. After purification,  $P450_{Exa}$  was obtained with the highest concentration of active enzyme as determined by CO titration [up to 228  $\mu$ M (10.9 mg mL<sup>-1</sup>)] (Table S5<sup>+</sup>).

Biotransformations with P450<sub>CLA</sub>, P450<sub>Spa</sub>, P450<sub>Exa</sub>, CYP152K6 and P450<sub>Bsβ F79L/G290F</sub> showed successful conversion using 10 mM of substrate to the corresponding α-hydroxylated fatty acids (Table 1). Remarkably, P450<sub>Exa</sub> was found to be an excellent candidate for the conversion of **1a** and exhibited good regioselectivity (14:1) for the α-position over the β-position, giving 7 mM of α-**2a** and only 0.5 mM of β-**2a**. The natural substrate for P450<sub>Exa</sub> has been described to be myristic acid.<sup>59</sup>

Furthermore,  $P450_{Sp\alpha}$  reached completion for the conversion of **1b** and **1c** (>99% conv.) giving the corresponding  $\alpha$ -hydroxylated products  $\alpha$ -2**b** and  $\alpha$ -2**c** with 8.9 mM and

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Table 1 α-Hydroxylation of medium chain fatty acids by CYP152s



Disastalast			Products <sup>b</sup> [mM]		$ee_{\alpha}{}^{c}[\%]$	
CYP152	FA	Conv. <sup><i>a</i></sup> [%]	α-ΟΗ β-ΟΗ			
P450 <sub>CLA</sub>	1a	44	3.0	n.d.	8 (S)	
$P450_{CLA}$	1b	>99	6.5	1.5	$48(S)^{d}$	
$P450_{CLA}$	1c	75	6.8	n.d.	62 $(S)^{d}$	
$P450_{Sp\alpha}$	1a	35	2.1	n.d.	>99 (S)	
P450 <sub>Spα</sub>	1b	>99	8.9	0.4	>99 (S)	
$P450_{Sp\alpha}$	1c	>99	8.5	0.6	>99 (S)	
P450 <sub>Exα</sub>	1a	95	7.0	0.5	81(S)	
$P450_{Ex\alpha}$	1b	>99	4.0	3.6	>99 (S)	
$P450_{Ex\alpha}$	1c	96	2.9	4.0	>99 (S)	
$P450_{J\alpha}$	1a	11	n.d.	n.d.	n.a. <sup>e</sup>	
$P450_{J\alpha}$	1b	11	n.d.	n.d.	n.a. <sup>e</sup>	
$P450_{J\alpha}$	1c	24	0.5	n.d.	n.a. <sup>e</sup>	
CYP152K6	1a	73	5.3	n.d.	93 (S)	
CYP152K6 <sup>f</sup>	1b	>99	6.3	1.3	>99 (S)	
CYP152K6	1c	92	5.9	2.2	>99 (S)	
P450 <sub>Bsβ F79L/G290F</sub>	1a	50	2.8	n.d.	58(S)	
P450 <sub>Bsβ F79L/G290F</sub> f	1b	>99	5.6	1.6	79(S)	
$P450_{Bs\beta\ F79L/G290F}$	1c	38	n.d.	1.3	n.a. <sup>e</sup>	

<sup>*a*</sup> Conversion [%] (*i.e.*, consumption of substrate **1a–c**) was determined by GC using an int. standard (lauric acid) after derivatisation (for GC traces see Fig. S12–14<sup>†</sup>). <sup>*b*</sup> Product concentrations were determined *via* calibration curves with an internal standard (Fig. S8<sup>†</sup>). The response factor for  $\beta$ -OH was assumed to be the same as for  $\alpha$ -OH. n.d. not detected. <sup>*c*</sup> Optical purity was measured after derivatisation of GC using a chiral phase. <sup>*d*</sup> ee values in literature are 36% ee (*S*)- $\alpha$ -**2b** and 71% ee (*S*)- $\alpha$ -**2c**.<sup>35 e</sup> n.a. = not applicable due to no product formation. <sup>*f*</sup>(*Z*)-2-Hydroxyoct-2-enoic acid (7% and 8% GC-area) was detected by GC-MS.

8.5 mM, respectively. Only small amounts of  $\beta$ -hydroxylation product were detectable ( $\beta$ -2b and  $\beta$ -2c with 0.4 and 0.6 mM, respectively) corresponding to an  $\alpha$ :  $\beta$  ratio of 22:1 and 14:1, respectively. Incomplete mass balances are most likely due to undesired oxidative decarboxylation, which was in general not significant, except for  $P450_{I\alpha}$  for which decarboxylation to the alkene has been reported before.47 Furthermore 1-alkene formation has been observed for  $P450_{CLA}$ ,  $P450_{Sp\alpha}$  and  $P450_{Ex\alpha}$  at elevated H<sub>2</sub>O<sub>2</sub> concentrations.<sup>47,59</sup> The enzyme CYP152K6 has been described as α-hydroxylase for substrates like lauric acid, tetradecanoic acid and palmitic acid.<sup>60</sup> Nevertheless, our study showed that this biocatalyst exhibits also good regioselectivity for medium chain fatty acids leading in general to the  $\alpha$ -hydroxylated product, whereby for **1a** the  $\alpha$ -product was detected exclusively without any β-product and in case of 1b and **1c**, the ratios of  $\alpha$ :  $\beta$ -hydroxylation were 4.8:1 and 2.7:1, respectively. The variant  $P450_{Bs\beta F79L/G290F}$  produced actually only  $\alpha$ -2a, although at moderate conversion and low recovery, while the same enzyme gave only the  $\beta$ -product when transforming the C10 fatty acid 1c.

It is worth to mention, that for most enzymes and transformations no over-oxidation *e.g.* to the corresponding carbonyl compound, thus the  $\alpha$ -keto acid, was detected which has been identified as a major issue in previous work.<sup>27,38</sup> Only in the case of **1b** with CYP52K6 and P450<sub>Bsβ</sub> <sub>F79L/G290F</sub> some  $\alpha$ -keto acid was detected. The successful minimization/avoid-ance of the over-oxidation product can most likely be attributed to the continuous addition of the oxidant circumventing sudden high concentrations.

Analysing the chirality and optical purity of the  $\alpha$ -hydroxylated products revealed that all six CYP152 enzymes investigated formed preferentially the (*S*)-enantiomer (Fig. S15–17†). Thereby the biocatalysts P450<sub>Spa</sub>, P450<sub>Exa</sub> and CYP152K6 gave access to optically pure (*S*)-products (>99% ee) in most cases. In contrast,  $\alpha$ -hydroxylation by P450<sub>CLA</sub> was in general poorly enantioselective with ee values in the range of 8–62%.

From these results,  $P450_{Sp\alpha}$  and  $P450_{Ex\alpha}$  were chosen as the most suitable enzymes for  $\alpha$ -hydroxylation, due to the high conversion, regio- and stereoselectivity and amounts of products achieved.

#### Conversion of dicarboxylic acids with $P450_{Sp\alpha}$ and $P450_{Ex\alpha}$

Since the hydroxylation of mono-carboxylic acids was successful, the two best performing  $\alpha$ -hydroxylating enzymes P450<sub>Sp $\alpha$ </sub> and P450<sub>Ex $\alpha$ </sub> were investigated for the hydroxylation of selected dicarboxylic acids. While the dicarboxylic acids azelaic acid **3a** (C9) and sebacic acid **3b** (C10) were accepted by P450<sub>Ex $\alpha$ </sub> (Scheme 2 and Fig. S18†), P450<sub>Sp $\alpha$ </sub> did not transform these substrates.

The substrate azelaic acid is produced by ozonolysis of oleic acid<sup>61,62</sup> and sebacic acid is obtained by the alkaline cleavage of castor oil.<sup>63</sup> The market for azelaic acid is expected to reach USD 1.6 billion by 2025<sup>64</sup> and USD 313 million by 2026 for sebacic acid.<sup>65</sup> Both are building blocks of high interest for industrial applications<sup>66</sup> due to their bio-based nature<sup>67</sup> and biodegradability.<sup>68</sup>

Although one might expect that the dicarboxylic acids could be hydroxylated twice in the  $\alpha$ -positions of the two carboxylic acid moieties, P450<sub>Ex $\alpha$ </sub> successfully converted **3a** and **3b** exclusively to the corresponding mono-hydroxylated products  $\alpha$ -**4a** and  $\alpha$ -**4b**, the latter with >99% conv. (Scheme 2).

As shorter chain dicarboxylic acids like succinic acid **3c** (C4) or adipic acid **3d** (C6) were not converted by P450<sub>Exa</sub> and P450<sub>Spa</sub> (Fig. S21–24<sup>†</sup>), but the longer dicarboxylic acid **3a** (C9)



Scheme 2 Mono-hydroxylation of dicarboxylic acids 3a-b with P450<sub>Exx.</sub> Reactions were performed in 1.5 mL glass crimp vials in a final volume of 1 mL. Conversion [%] (*i.e.*, consumption of substrate) was determined by GC-MS using an int. standard (ISD, lauric acid) after derivatisation (BSTFA, 1% TMCS).

#### Paper

The computational modelling studies revealed that adipic acid (C6) (Fig. 1A) as well as succinic acid (C4) would be completely buried in the hydrophobic access channel. In contrast, the length of the hydrocarbon chains of **3a** (C9) (Fig. 1B) and **3b** (C10) (Fig. 1C) allowed for one of their carboxylic acid moieties to remain on the outside while they were tightly coordinated to the reaction centre like the natural substrate of P450<sub>Exa</sub>, myristic acid (C14) (Fig. 1D). Hence, it was presumed that the second carboxyl group of the longer chain dicarboxylic acids **3a** and **3b** did not lead to unfavourable interactions with



**Fig. 1** Docking of dicarboxylic acids C6 (A), C9 (B), C10 (C) and carboxylic acid C14 (D) into the active site of  $P450_{Exx}$  (PDB: 5YHJ) Docking studies were performed using YASARA and visualized with PyMOL. The docked substrates are visualized in pink in their lowest energy state. The simulation cell was defined at 4 Å around the iron atom of the heme.

the hydrophobic substrate tunnel and therefore to be converted. In contrast, for a transformation of *e.g.* succinic acid 3c (C4) or 3d (C6) also the second carboxylic acid moiety would need to be in the hydrophobic channel causing non-favoured interaction and therefore these substrates were not converted.

#### **Preparative scale reactions**

For the preparative transformations the focus was put first on P450<sub>Spa</sub> and **1b** as high regio- and stereoselectivity was achieved on analytical scale. Running the reactions on a 50 mL scale with 10 and 50 mM 1b substrate concentration, respectively, both experiments resulted in >99% conv. (Table 2, entries 1 and 2) of which the higher substrate concentration (50 mM) reached a TON of 16 667. By increasing the substrate concentration further to 100 mM (100 mL scale), the reaction still went to completion. In this experiment, the wildtype enzyme tolerated a total H<sub>2</sub>O<sub>2</sub> concentration of 100 mM giving 1260 mg of product (S)-α-2b (87%, Table 2, entry 3) corresponding to a TON of 33 333. It was possible to purify the final product and remove any residual substrate by utilizing heptane as a solvent (adapted procedure from literature<sup>69</sup> see ESI "Purification of  $\alpha$ -2b after re-extraction in heptane"<sup>†</sup>). Increasing the substrate concentration even further to 150 mM and thereby also the amount/concentration of H2O2 still allowed to reach 90% conversion, corresponding to a TON of 42 000 (Table 2, entry 4). Interestingly, increasing the substrate concentration for  $P450_{Sp\alpha}$  from 10 mM to 50 mM led to a decrease in ee from >99% to 97%. At 100 and 150 mM the ee was 90-96%.

The hydroxylation of **1c** on 25 mL scale resulted in  $\alpha$ -**2c** as the main product (GC-MS yield of 61%) but also the  $\beta$ - and  $\gamma$ -products were detected *via* GC-MS (Table 2, entry 5).

Finally, dicarboxylic acid **3b** was successfully converted to the mono-hydroxylated product  $\alpha$ -**4b** (Table 2, entry 6) reaching a TON of 3333 under the conditions used. The lower yield (29%) was a result of the higher water solubility of the dicarboxylic acid and using the same work up procedure as for the mono-carboxylic acids.

Table 2 Preparative scale transformations of 1b, 1c and 3b with P450<sub>Spα</sub> and P450<sub>Exα</sub>

Entry	Substrate	Substrate [mM]	Enzyme	Total H <sub>2</sub> O <sub>2</sub> [mM]	GC-MS conv. <sup>a</sup> [%]	Isolated yield [%]/purity <sup>b</sup> [%]	TON <sup>c</sup>
1	1h	10	P450a	20	>00	99 (80 mg)/>99	3333
2	1b 1b	50	P450 <sub>Spα</sub>	100	>99	89 (401 mg)/94 (6% β- <b>2b</b> )	16 667
3	1b	100	$P450_{Sp\alpha}$	150	>99	$87 (1260 \text{ mg}) /> 99^d$	33 333
4	1b	150	$P450_{Sp\alpha}$	150	90	n.d.	42000
5	1c	10	$P450_{Spq}$	20	97 <sup>e</sup>	n.d.	3233
6	3b	10	$P450_{Exa}$	20	>99	29 (26 mg)/>99	3333
7	3b	50	$P450_{Ex\alpha}$	100	25	n.d.	833

Reaction conditions: reactions were performed in a 250 mL reaction flask containing reaction buffer (100 mM KPi buffer, pH 7.4), EtOH (5% v/v), fatty acid (10, 50, 100 or 150 mM) and purified enzyme (3  $\mu$ M), in a final volume of 50 mL (100 mL for entry 3 and 25 mL for entry 5). H<sub>2</sub>O<sub>2</sub> was added continuously *via* a syringe pump [entries 1, 5 and 6: 1.6 mM h<sup>-1</sup> over 12 h to a final concentration of 20 mM (stock: 320 mM); entries 2 and 7: 8.3 mM h<sup>-1</sup> over 12 h to a final concentration of 100 mM (stock: 320 mM), entries 3 and 4: 12.5 mM h<sup>-1</sup> over 12 h to a final concentration of 150 mM (stock: 400 mM). N.d. not determined. <sup>*a*</sup> Conversion was determined by GC-MS using lauric acid (5 mM) as ISD by comparison with a sample at *t* = 0. <sup>*b*</sup> Isolated yields [%] were calculated based on the measured mass [mg] of isolated and dried product and the maximum theoretical yields [mg]. Purity [%] was calculated based on GC-MS data. <sup>*c*</sup> TON = turnover number which is defined as mmol substrate converted per mmol catalyst. <sup>*d*</sup> Yield after second purification step. <sup>*e*</sup> α-2c 61% GC-area; β-2c and γ-2c product 26% GC-area and 9% GC-area, respectively.

#### Table 3 Comparison of chemical and biocatalytic methods for the synthesis of $\alpha$ -2b

Entry	Catalyst/reagents	Solvent/workup	Conc. 1b/scale	Yield [%]	Conv. [%] (ee)	TON <sup>e</sup>	Atom economy <sup>f</sup> [%]
1 <sup>16</sup>	LDA TMSOOTMS, H <sup>+</sup>	THF/extraction with ethyl acetate <sup><i>a</i></sup>	250 mM/10 mL	44	rac	n.a.	34.4
$2^{17}$	O <sub>2</sub> /LDA, HMPA	THF/crystallization	200 mM/ 100 mL	63 <sup><i>b</i></sup>	rac	n.a.	35.9
3 <sup>70</sup>	Homogenate of peas/ O <sub>2</sub>	0.2 M phosphate buffer	0.2 mM/ 150 mL	Not isolated	<10 (99% <i>R</i> )	n.a.	n.a.
$4^{38}$	$P450_{CLA}/H_2O_2$ (24 mM)	Kpi (pH 7.5, 100 mM) EtOH (5% v/v)	10 mM <b>1a</b> / 500 μL	Not isolated	78.4 (36% <i>S</i> ) 5 mM α- <b>2a</b> <sup>d</sup>	1568	47.1 <sup>g</sup>
5 <sup>46</sup>	$\begin{array}{c} P450_{CLA}/H_2O_2\\ (20 \text{ mM}) \end{array}$	Tris-HCl (pH 7.5, 100 mM) EtOH (5% v/v)	10 mM/1 mL	Not isolated	>99 (36% <i>S</i> ) >9.9 mM α- <b>2b</b>	3333	89.9
6 <sup>11</sup>	$\frac{P450_{CLA}}{H_2O_2}$ (20 mM)	Kpi (pH 7, 20 mM) EtOH (5% v/v)	10 mM/50 mL	>95	>99 (36% <i>S</i> )	1666	89.9
7 <sup>10</sup>	$P450_{spa}/H_2O_2$ (20 mM)	KPi (pH 7.4, 100 mM) EtOH (10% v/v)	10 mM/1 mL	Not isolated <sup>c</sup>	23 (>99% <i>S</i> ) 2.3 mM α <b>-2b</b>	767	89.9
8 <sup>This</sup> work	$P450_{sp\alpha}/H_2O_2$ (up to 150 mM)	KPi (pH 7, 100 mM) EtOH (5% v/v)/acidification, extraction with ethyl acetate	Up to 150 mM/ 50 mL	Up to >99%	Up to >99 (90- >99% S)	Up to 42 000	89.9

<sup>*a*</sup> Purification by preparative thin-layer chromatography (SiO<sub>2</sub>, 20% ethyl acetate in hexane). <sup>*b*</sup> Hydroxyperoxide product as side product. <sup>*c*</sup> Intermediate in a cascade reaction. <sup>*d*</sup> Over-oxidation to  $\alpha$ -keto acid (2.89 mM). <sup>*e*</sup> TON = turnover number which is defined as mmol substrate converted per mmol catalyst. <sup>*f*</sup> Atom economy =  $\frac{\text{molecular weight of desired product}}{\Sigma \text{ molecular weight of all products}} \times 100\%$ . <sup>*g*</sup> Reduced atom economy due to side product for-

mation ( $\alpha$ -keto acid). n.a. = not applicable.

Increasing the substrate concentration to 50 mM and using 100 mM of  $H_2O_2$  indicated the limits of the used enzyme reaching 25% conv. (Table 2, entry 7).

#### Comparison of chemical and biocatalytic methods

Comparing this study with established chemical and other biocatalytic strategies from literature (Table 3), two chemical options for the synthesis of  $\alpha$ -**2b** have been reported using lithium diisopropylamide (LDA), hexamethyl-phosphoramide (HMPA) and either bis(trimethylsilyl)-peroxide (TMSOOTMS) or molecular oxygen (O<sub>2</sub>) as oxygen source (Table 3, route 1 and 2).<sup>16,17</sup> Although the substrate concentration was high (200–250 mM), these routes have the lowest atom economy and use toxic and carcinogenic (HMPA) reagents. Additionally, the products were obtained in low yields and in the racemic form only.

On the other hand, all biocatalytic approaches are performed in aqueous media requiring  $H_2O_2$  as oxidation reagent, except for entry 3 (Table 3) where molecular oxygen was used with a homogenate of peas, representing a less well-defined reagent.

The CYP152 family offers high potential for regio- and stereoselective hydroxylation on medium chain fatty acids on preparative scale.

When comparing the two biocatalysts from the CYP152 family used for the  $\alpha$ -hydroxylation of **1b** (P450<sub>CLA</sub> and P450<sub>Spa</sub>) concerning stereoselectivity, P450<sub>Spa</sub> is superior as highly optically enriched product  $\alpha$ -**2b** was obtained (96–99% ee), while P450<sub>CLA</sub> gave the  $\alpha$ -hydroxy acid with an ee of 36% only (Table 3, entries 6, 7 *versus* 4–6).

Comparing the approach of this study  $P450_{Sp\alpha}$  (Table 3, route 8) with all previous studies involving peroxygenases, it becomes clear that  $P450_{Sp\alpha}$  can be used also at elevated substrate concentration (up to 150 mM), while previous studies

used **2a** at a maximum substrate concentration of 10 mM only. In comparison to route 7 where the hydroxy acid was not the main target, in our study  $\alpha$ -**2b** was obtained with up to >99% conversion allowing to reach an outstanding TON and the product was isolated from a preparative scale experiment. An important key to success was the method of applying stoichiometric amounts of H<sub>2</sub>O<sub>2</sub> continuously *via* a syringe pump. This turned out to be clearly superior to the previous approaches, where H<sub>2</sub>O<sub>2</sub> was added at the beginning or was produced during the reaction.

Consequently, high conversions of **1b** with  $P450_{Sp\alpha}$  on 50 mL scale were achieved reaching TONs of up to 42 000. So far, the highest turnover number (TON) for CYP152s in literature did not exceed a value of  $3333.^{46}$  On small scale a TON of 3333 was reached for the conversion of **1b** (10 mM) by  $P450_{CLA}$  (3  $\mu$ M). For pelargonic acid (C9:0) the reaction was conducted in 20 mM KPi buffer and yielded in 0.49 g product (>99% conv., 95%  $\alpha$ -hydroxylated nonanoic acid, TON 3330) on 150 mL scale.<sup>11</sup> Thus, the TON achieved here are one order of magnitude higher than reported before and are therefore the highest reported for a peroxygenase from the CYP152 family.

### Conclusions

In this study an atom economical process for the stereoselective biocatalytic  $\alpha$ -hydroxylation of medium chain fatty acids was developed, requiring hydrogen peroxide as the only stoichiometric reagent. The enzyme P450<sub>Ex $\alpha$ </sub> showed high conversions, regio- and stereoselectivity for the substrates **1a** [conv. 95%; 70%  $\alpha$ -**2a**; ee 81% (*S*)] and was active towards longer chain dicarboxylic acids **3a** (conv. 68%) and **3b** (conv.

99%) with a remarkable chemoselectivity for mono-hydroxylation.  $P450_{Sp\alpha}$  allowed to achieve excellent conversion for the fatty acids C8:0 (1b) and C10:0 (1c) (>99%) with up to >99% (S) ee. These results allowed an efficient and scalable process to produce  $\alpha$ -hydroxylated fatty acids where the amount of required chemicals and waste produced were kept at a minimum. In summary, TONs of up to 42 000 were achieved for the conversion of **1b** on preparative scale using P450<sub>Spg</sub> as catalyst at substrate concentrations up to 150 mM giving the desired product in gram quantities.

## Author contributions

K. B., A. S., S. V., H. R., M. L. and S. P. performed the experiments. K. B., S. W. and W. K. planned experiments. All authors analysed data. M. L., S. P., S. W., W. K., C. S. provided scientific feedback. K. B. and W. K. wrote the manuscript. W. K. and S. W. conceived the study. W. K. raised funding and supervised the study. All authors have given approval to the final version of the manuscript.

## Conflicts of interest

There are no conflicts to declare.

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