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Improvement of fruit juice quality: novel *endo*-polygalacturonase II from *Aspergillus tubingensis* FAT 43 for enhanced liquefaction, clarification, and antioxidant potential

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This study focuses on the isolation, purification, and characterisation of *endo*-polygalacturonase II from *Aspergillus tubingensis* FAT43, particularly emphasising its potential applications in the fruit juice industry. A comprehensive screening test revealed the temporal dynamics of *endo*-polygalacturonase production during a 96-hour fermentation process. The purification process, involving ammonium sulfate and ethanol precipitation followed by ion-exchange chromatography, resulted in a 3.3-fold purification of PG II with a yield of 16% and a specific activity of 6001.67 U mg⁻¹. Molecular analysis confirmed the identity of PG II, its gene (*pgall*), and a high degree of sequence identity with *Aspergillus tubingensis* in the SWISS-PROT database. The optimal pH for PG II activity was 3.5–4.5, with robust stability across a broad pH spectrum (3–7). The enzyme exhibited optimal temperature activity at 45 °C, with a retention of 90% activity at 50 °C. The calculated activation energy for PG II was 62.1 kJ mol⁻¹, indicating good stability. Inactivation kinetics revealed a half-life of 13.7 h at 40 °C, 5.4 h at 50 °C, and 0.85 h at 60 °C, with an activation energy of denaturation of 32.8 kJ mol⁻¹. Compared to literature-reported PGs, PG II from *A. tubingensis* FAT43 demonstrated superior thermal stability. Hydrolysis experiments on different pectins revealed the highest specificity for non-methylated substrates (polygalacturonic acid). In fruit juice processing, PG II significantly increased juice yield and clarity, with the highest impact observed in strawberry juice. Antioxidant activity assays indicated enhanced antioxidant potential in enzyme-treated juices, especially strawberry, quince, and apple juices. The study highlights PG II's potential as an industrially valuable enzyme for fruit juice processing, offering improved thermostability and versatility across various fruit types.

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1. Introduction

Pectic polysaccharides play a pivotal role in inducing cloudiness in fruit juices, posing a significant challenge within the fruit juice industry.¹ These intricate carbohydrates are predominantly located in the middle lamella and cell walls of plant tissues.^{2,3} In a sample of fresh fruit material, pectin comprises between 0.5 and 4% of the total mass.⁴ The elaborate and diverse structures of pectin, characterised by various linkages and modifications, significantly contribute to fruit juices' viscosity and cloudiness.

This cloudiness emerges due to the interaction of pectic polysaccharides with other components present in the juice.⁵ If these polysaccharides are insufficiently broken-down during juice processing, they have the potential to form gels and fibrillar structures, thereby increasing viscosity.⁶ This phenomenon affects the visual clarity of the juice and impedes the efficient separation of liquid and solid phases during processing.⁷

Pectinolytic enzymes, commonly known as pectinases, constitute a vital group of enzymes that hydrolyse pectin by breaking the α -1,4 glycosidic bonds between D-galacturonic acid molecules. Three criteria are used in the literature to classify pectinases: substrate structure (pectin, pectic acid, or oligo-D-galacturonate), catalytic reaction site (random, *endo*-activity, or catalysis from the ends of polymer chains, *exo*-activity), and the type of reaction (hydrolase, lyase, or esterase). These enzymes can be isolated from various sources, including plants, bacteria, fungi, and yeasts.^{4,8}

Filamentous fungi, particularly species of the *Aspergillus* genus, can produce pectinolytic enzymes at elevated concen-

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trations.⁴ Certain *Aspergillus* species, during infection or culturing, produce enzymes such as polygalacturonase (PGs), pectin methylesterase (PMEs), and pectate lyase (PLs). Alkaline pectinases exhibit activity in the retting and degumming of plant material, proving valuable in fruit waste processing. Simultaneously, acidic pectinase finds widespread use in eliminating and clarifying fruit juice.⁹ The diverse applications of these enzymes highlight their significance in industrial and agricultural processes.¹⁰ Commercial pectinase is typically a mixture of enzymes. This is an advantage given the complex nature of plant tissues and the various chemical bonds that need to be hydrolysed. However, a more targeted approach may be essential in certain industrial scenarios, requiring a specific type of pectinase or a carefully selected enzyme mix.

To overcome the challenge of cloudiness, the fruit juice industry employs enzymes known as *endo*-pectinases, with *endo*-polygalacturonases (*endo*-PGs) being a prominent example. The filamentous fungus *Aspergillus tubingensis* FAT 43 was selected from optimised solid-state fermentation as a good *endo*-PG producer. *Endo*-PG targets the internal regions of pectin molecules, breaking them down into smaller, soluble fragments. This enzymatic action effectively reduces the viscosity of the juice by disrupting the complex pectin network, resulting in clearer and more transparent juices.

This study analysed the benefits of endopolygalacturonase II (PG II) from *A. tubingensis* FAT 43. Firstly, PG II enhances the clarity of fruit juices, meeting consumer preferences for visually appealing and transparent beverages. Secondly, these enzymes improve juice yield during pressing by breaking down pectic polysaccharides. This increased yield is valuable in optimising resource utilisation and reducing waste in fruit processing. Moreover, applying PG II positively influences the antioxidative attributes of the juices.¹¹ Cloudiness removal improves product quality and marketability, meeting industry standards and consumer expectations.

2. Materials and methods

2.1 Enzyme production by solid state fermentation

The production of *endo*-PG involved the utilisation of the *A. tubingensis* strain FAT43, following the protocol outlined by Pavlović *et al.* (2023).¹² Initially, the strain was cultivated on Potato Dextrose Agar (PDA) medium, maintaining controlled conditions (temperature 28 °C with a relative humidity of 60%) for five days until sporulation occurred.¹³ Subsequently, spores were harvested using a 0.1% Tween 20 solution, and their concentration was quantified at 2×10^6 spores per mL using a Shimadzu UV-Vis spectrophotometer, measuring optical density (OD) at a wavelength of 605 nm.¹⁴ Under optimised conditions (temperature 28 °C with a relative humidity of 60%), sugar beet pulp and wheat bran substrates were used for solid-state fermentation for 96 h. The fermentation was finished by extracting enzymes from the fermentation media using 25 mM acetate buffer at pH 4.5.

2.2 Diffusion assay for *endo*-PG activity

The *endo*-PG activity was detected by performing a diffusion test on a polyacrylamide gel with 0.2% low methylated pectin solution (in 50 mM acetate buffer pH 4.5). The gel was stained with 0.05% (w/w) Ruthenium Red dye, which enabled the detection of clear zones where the pectin is degraded due to enzymatic activity. The gel was prepared by punching wells after it was polymerised, and then 10 µL enzyme samples were added into the wells. Diffusion was set up in a humid environment at 45 °C for 1 h. After the incubation, the gel was washed with distilled water and stained with Ruthenium Red solution for 20 min. Clear zones around the wells indicated the presence of *endo*-PG activity.

2.3 Purification of *endo*-PG

The primary enzyme extract underwent a series of purification steps to obtain a partially purified enzyme. Initially, the concentration of enzymes was achieved by ultrafiltration, using 10 kDa molecular mass cut-off membranes. The resulting concentrated extract was then subjected to a cold (−20 °C) ethanol precipitation, followed by centrifugation at 13 000g for 10 min. The resulting precipitate was dissolved in 5 mL of 25 mM acetate buffer pH 6, and a subsequent centrifugation step was applied to eliminate insoluble particles, yielding a clarified enzyme solution.

Further purification involved ammonium sulfate (AS) precipitation at various concentrations (30%, 50%, and 70% saturation). The gradual addition of solid AS and continuous mixing with a magnetic stirrer resulted in a protein pellet after precipitation with 70% AS saturation. The pellet was dissolved in 5 mL of 25 mM acetate buffer pH 4.5. The clear, dissolved protein pellet was then subjected to size-exclusion chromatography on a Sephacryl S100HR (column, 530 × 30 mm; bed size, 450 mm; flow rate, 0.8 mL min^{−1}; sample volume 1.5% of the column volume), pre-equilibrated with 25 mM acetate buffer, pH 4.5. The collected fractions were then analysed using the polygalacturonase activity assay and SDS PAGE to determine the size distribution of the proteins sizes in the sample.

Following size-exclusion chromatography, eluted active fractions underwent ion-exchange chromatography on a DEAE Sephadex column, 25 mM acetate pH 4.5. A gradient elution technique was applied after loading the column with samples showing *endo*-PG activity. A linear gradient ranging from 0 to 0.5 M NaCl was applied for enzyme elution. The collected fractions were analysed for *endo*-PG using enzyme activity assay and SDS PAGE.

The partially purified enzyme was subjected to a final polishing step on a Q Sepharose column to achieve final purification. The protein sample underwent buffer exchange, transitioning from acetate to 25 mM Tris-HCl pH 7. Q Sepharose column was pre-equilibrated in the same buffer. A linear gradient ranging from 0 to 0.5 M NaCl was applied for the enzyme elution. All collected fractions were subjected to the *endo*-PG activity assay, and SDS-PAGE was used to determine enzyme purity. The PG II purification scheme is shown in Fig. 1.

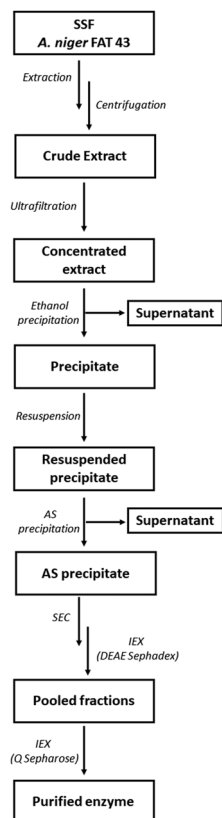


Fig. 1 Flowchart depicting the extraction and purification procedure of *endo*-PG.

After completing the purification steps, the protein concentration of each fraction was determined using the Bradford method, with bovine serum albumin as a standard.¹⁵

2.4 Polygalacturonase activity assay

Polygalacturonase activity was determined using the DNS method described by Bernfeld in 1955.¹⁶ The reaction mixture was composed of 50 μ L of sample and 450 μ L of 0.5% (w/w) polygalacturonate in an acetate buffer with a pH of 4.5. The mixture was incubated for 15 min at 45 $^{\circ}$ C, and then the reaction was stopped by adding the DNS reagent and boiling for 5 min at 100 $^{\circ}$ C. The absorbance at 540 nm was measured using a spectrophotometer, and the enzyme activity was calculated using an enzyme activity standard curve for D-galacturonate. One unit of activity (1 U) was defined as the amount of enzyme capable of releasing 1 μ mol of D-galacturonic acid per min.

2.5 Electrophoresis analysis

To assess the purity and composition of the active chromatographic fraction, SDS-PAGE was performed on a 10% (m/v) gel.¹⁷ The apparent molecular mass was determined using a standard protein mixture Blue Wide Range Protein Ladder (10–245 kDa, Cleaver Scientific).

2.6 Proteomic analysis: mass spectrometry characterisation

A 10 μ L protein sample was reduced and alkylated in one step with 10 mM TCEP and 40 mM CAA in the dark at room temperature for 30 min. The sample was then diluted to 100 μ L with 25 mM NH_4HCO_3 , and 60 ng of trypsin was added for overnight hydrolysis at 37 $^{\circ}$ C. The reaction was terminated by the addition of 1 μ L trifluoroacetic acid. The resulting peptides were analysed using a Bruker Daltonics Compact ESI-qTOF mass spectrometer, coupled to a Waters Acquity UPLC. A 2 μ L hydrolysate was loaded onto a Waters ACQUITY UPLC M-Class Symmetry C18 trap column and washed with 0.1% (v/v) formic acid in water for 10 min. Peptides were separated on a Bruker DaltonicsPepSep C18 analytical column with a 30-minute gradient from 5% to 45% solvent B (0.1% formic acid in ACN), followed by a 1-minute gradient to 90% solvent B at 0.4 μ L min^{-1} . The electrospray ion source operated in positive mode and scanned the precursor MS in the m/z range 150–2200. Spectral data were acquired using the Compass HyStar 6.0 software package and exported as Mascot generic files. They were searched against the SwissProt database using MASCOT software (version 2.8) with the following parameters: 20 ppm peptide and 0.6 Da fragment mass error tolerance, 3 enzyme missed cleavages, 2+ and 3+ peptide charges, carbamidomethyl Cys as a fixed and oxidised Met as a variable modification, and an automatic Decoy database search.

2.7 Gene amplification

To confirm the presence of the *A. tubingensis* pgaII gene for polygalacturonase (PG II) two sets of primers were designed: one for first exon (PecAt_ex1_Fw1 ATCCCCCATCGAAGCCCGG and one PecAt_ex1_Rev1 CGCCAGAGTTGATCGCAAGACAG resulting in 570 bp PCR DNA fragment) and second pair of primers for exon II (PecAt_ex2_Fw2 CATCTGGTTTACCAGCGGC and PecAt_ex2_Rev2 CAAAAGCTTGTTAGCAAGTGCTACAACCG resulting in 502 bp PCR fragment) based on GenBank sequence X58894.

The total DNA of *A. tubingensis* strain FAT43 was extracted from the white mycelium of isolate grown on PDA (3 days at 28 $^{\circ}$ C) using the protocol Day and Shattock (1997) described.¹⁸ Polymerase chain reaction (PCR) was performed using Phusion High Fidelity DNA Polymerase (0.5 U per 50 μ L reaction) with isolated total DNA of strain FAT43 and designed primers under the following conditions: initial denaturation 2 min at 98 $^{\circ}$ C, 30 cycles composed of the following steps: denaturation for 20 seconds at 98 $^{\circ}$ C, annealing for 30 s at 55 $^{\circ}$ C, polymerisation at 72 $^{\circ}$ C and final polymerisation for 5 min at 72 $^{\circ}$ C. The amplification success of according DNA fragments was analysed on a 1% agarose gel. The size of the fragments was determined based on the standard GeneRuler DNA Ladder Mix (Thermo Scientific).

2.8 PG characterisation

Purified PG II was biochemically characterised to optimise its efficiency and investigate its possible application in biotechnology.

2.8.1 Isoelectric focusing electrophoresis and zymography.

The pI value of PG II was determined using isoelectric focusing electrophoresis (IEF). The method was performed on a 6% polyacrylamide gel (PA) in accordance with the manufacturer's instructions (LKB Pharmacia, Sweden), at 1000 V, 4.8 Ma, and 5 W for 1.5 h. Calibration was done using ampholytes (3.5–9.5 pH). After IEF, the PA gel was washed with distilled water and 50 mM acetate buffer pH 4, and then incubated in 0.5% LM pectin solution (in 50 mM acetate buffer pH 4) for 1 h. The visualisation of PGII was achieved by using a 0.05% RR solution for 20 min.

2.8.2 Determination of temperature optimum, thermal stability and thermal inactivation kinetics. The optimal temperature range (30 to 60 °C) for PG II was determined by assessing activity in 50 mM acetate buffer, pH 4. The activation energy was calculated using the Arrhenius equation after measuring enzyme activities at different temperatures by plotting $\ln k$ versus $1/T$, where k is a rate constant at temperature T (absolute temperature) according to the linear modification of Arrhenius equation:

$$\ln k = \ln A - \frac{E_a}{RT}$$

Thermal stability and the kinetics of irreversible loss of enzyme activity were investigated: the purified enzyme was distributed into test tubes and subjected to incubation at temperatures of 40, 50, and 60 °C for varying time intervals (t). At specific time points, samples were collected, and the remaining activity was measured using the enzyme assay conditions. The inactivation rate constants, k_d , were calculated using the following equation:

$$\ln(A_t/A_0) = -k_d t$$

A_t/A_0 is the residual PG II activity value after time t (A_t is the activity of heated PG II, and A_0 is the initial activity of unheated PG II). The enzyme's half-life values were determined from the equation:

$$t_{1/2} = \ln 2/k_d$$

The enzyme inactivation energy (E_d) was obtained from linear modification of the Arrhenius equation by plotting $\ln k_d$ against the inverse of absolute temperature (R is the universal gas constant and T is the absolute temperature).

$$t_{1/2} = \ln 2/k_d$$

The thermodynamic properties of PG II can be approximated using the Eyring equation, which involves constants: R is the universal gas constant, $8.314 \text{ J mol}^{-1} \text{ K}^{-1}$, k_B (Boltzmann constant, $1.38 \times 10^{-23} \text{ J K}^{-1}$), T (absolute temperature), h (Planck constant, $6.63 \times 10^{-34} \text{ Js}$), ΔH (enthalpy of activation in kJ mol^{-1}), and ΔS (entropy of activation in $\text{J mol}^{-1} \text{ K}^{-1}$). The enthalpy of activation (ΔH), specified in the given equation, is

determined by calculating the energies of enzyme denaturation, as detailed in the following equations.

$$k_d = \frac{k_B T}{h} e^{-\frac{\Delta H}{RT}} e^{\frac{\Delta S}{R}}$$

$$\Delta H = E_d - RT$$

$$\Delta G = -RT \ln \left[\frac{k_d h}{k_B T} \right]$$

$$\Delta S = \frac{\Delta H - \Delta G}{T}$$

The free energy of activation (ΔG) can also be derived from the given equation. Finally, as described, the entropy of activation (ΔS) is calculated using the enthalpy and free energies of activation, as presented in the given equation.

D -value, the decimal reduction time is the time needed for reduction of the initial activity to 10% residual at a given temperature and was calculated using the following equation:

$$D = \frac{\ln 10}{k_d}$$

The Z -value, sensitivity factor, represents the temperature increment required to reduce the D -value tenfold. It serves as the slope when the log of the D -value is plotted against the temperature.¹⁹

2.8.3 Determination of optimal pH activity and stability.

Enzyme activity in a 50 mM Britton–Robinson buffer series was examined under precise enzyme assay conditions to determine the optimal pH range for PG II. To evaluate pH stability, the enzyme was subjected to controlled incubation at specified pH values between 3.0 and 8.0 at constant temperature (25 °C) for a period of 1, 2 and 7 days. Samples were taken at the indicated time intervals and the residual activity was quantified using established enzyme assay conditions.

2.8.4 Thin layer chromatography.

Thin Layer Chromatography (TLC) was employed to analyse the hydrolysis products of different substrates. For this purpose, various substrates in the concentration of 1% (w/w), including high methylated pectin (HMP), low methylated pectin (LMP), and polygalacturonic acid (PGA), were incubated with a purified enzyme. The hydrolysis process was conducted for 1 and 3 h. Subsequently, the resulting products were analysed on TLC plates (Silica Gel 60 F254, Sigma-Aldrich) using a solvent system comprising n-butanol, ethanol, water, and acetic acid in a 5 : 3 : 2 : 0.5 (v/v/v) ratio. Standards such as monogalacturonate and digalacturonate were utilised. The products were visualised through the application of α -naphthol reagent and heating.

2.9 Fruit juice processing

The preparation of fresh fruit pulp, such as apples, quinces, strawberries, oranges, and bananas, as well as the enzymatic treatment of fruit juices, was carried out following the method described by Pavlović *et al.* (2023).¹² Enzymatic processing of fruit juices aimed at enhancing liquefaction and clarification.

The liquefaction assay utilised the optimal temperature (40 °C) for the PG II from *A. tubingensis* FAT43. Juice yield was calculated using the equation:

$$\text{Juice yield (\%)} = \frac{\text{Mass of clear juice (g)}}{\text{Mass of pulp (g)}} \times 100$$

Fresh pulps were homogenised, and enzyme treatment (2 IU per gram of pulp) was conducted at 40 °C for 60 min. Control samples, replacing the enzyme with an acetate buffer, were also prepared. After centrifugation, liquefaction was quantified by measuring the increase in juice volume compared to the control sample. Experiments were triplicated, and mean values with standard deviations were determined for each juice.

After liquefaction of the fruit pulps prepared with the above-described method, a clarification test was performed after filtering the supernatant through filter paper to remove all suspended particles. The transmittance was measured at 660 nm (UV-1800 UV/Vis spectrophotometer; Shimadzu, Kyoto, Japan) in the obtained juices. The percentage of clarification is expressed as the degree of reduction in transmittance compared to juices not treated with a PG II. Experiments were conducted in triplicate, and mean values with standard deviations were calculated for each juice.

2.9.1 Determination of total phenolic content. The total phenolic content (TPC) of enzymatically treated and untreated juices was measured in accordance with Singleton and Rossi's (1965) method.²⁰ Gallic acid equivalents (GAE) were used to express the TPC as mg per 100 mL juices. The polyphenol concentration in the samples was calculated using a standard curve. The obtained results before and after enzyme treatment were compared using a *t*-test.

2.9.2 Antioxidant activity of treated and untreated juices. To investigate changes in the antioxidant properties of juices, FRAP (Ferric Reducing Antioxidant Power) and DPPH (2,2-diphenyl-1-picrylhydrazyl) assays were conducted before and after treatment with polygalacturonase.

To initiate the FRAP test, 100 µL of the sample is mixed with 900 µL of the FRAP reagent, composed of 50 mL of pH 3.6 acetate buffer, 5 mL of tripyridyltriazine (TPTZ), and 5 mL of FeCl₃·6H₂O. The resulting mixture is left in complete darkness for 5 min to allow the reaction to occur. After 5 min, the absorbance of the mixture is measured at 593 nm. The obtained value is inserted into the standard line to calculate the FRAP value, equivalent to ascorbic acid.

The DPPH test is initiated by combining 10 µL of the sample with 900 µL of the DPPH reagent (1 mM 2,2-diphenyl-1-picrylhydrazyl dissolved in methanol). The reaction is carried out in complete darkness for 15 min. The result of the reaction can be presented in two ways: as a percentage of discoloration or as an equivalent to a standard, such as ascorbic acid. The obtained results before and after enzyme treatment were compared using a *t*-test.

3. Results and discussion

Although *endo*-PGs have been extensively studied as enzymes in the commercial pectinolytic complex, there is still a global interest in discovering new and improved enzyme variants for industrial and biotechnological applications. These enzymes are primarily found in fungi, particularly in species of *Aspergillus*. For instance, various *Aspergillus* species, including *A. niger*, *A. awamori*, *A. carbonarius*, *A. aculeatus*, and *A. flavus*, have been isolated for their *endo*-PGs properties.²¹ There is still great demand for highly effective enzymes with a wide pH and temperature range in different industrial processes, such as the fruit juice industry. This study found that *A. tubingensis* FAT43 isolated from quince fruit surface secretes *endo*-PGs after four days of growth at 28 °C. Subsequently, these enzymes were detected using the diffusion assay method, which confirmed the presence of *endo*-PG activity at various time points during the 24, 48, 72, and 96 h of fermentation. The visual representation in the accompanying image illustrates the pectin in the gel stained with RR colour, revealing the hydrolysis of pectin in the illuminated areas (clear zones) due to *endo*-PG activity. Notably, the diameter of the enlightened (clear) zones indicates an increase in *endo*-PG activity with prolonged fermentation. The sample subjected to a 96-hour fermentation period exhibited the largest diameter of enlightenment, while the 24-hour sample presented the smallest clear zone diameter (Fig. 2). This comprehensive screening test provides a clear understanding of the temporal dynamics of *endo*-PG production during the fermentation process.

3.1 Purification and characterisation of PG II

Polygalacturonase is usually purified from fermentation media in several steps, with standard fractionation methods such as ammonium sulfate (AS) and ethanol precipitation, followed by various column chromatography techniques. Standard methods were also utilised in our purification procedure, including ion-exchange chromatography on a DEAE Sephadex and Q-Sepharose column, to successfully purify the predominant isoform of *endo*-PG from the fermentation extract (Fig. 3 and Table 1). The two ion-exchange chromatography steps resulted in a purification fold of 3.3 for polygalacturonase with a yield of 16% and specific activity of 6001.67 U mg⁻¹. Different methods were used to purify polygalacturonase from fungi compared to previous studies. For example, PG II was purified from *A. tubingensis* using DEAE Sephadex chromatography, which resulted in a remarkable 16.8-fold purification,

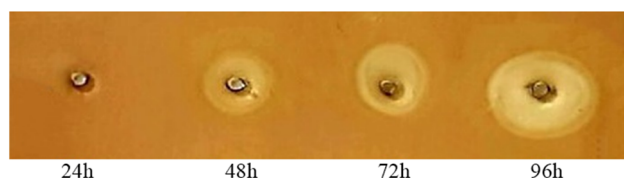


Fig. 2 Diffusion assay for *endo*-PG activity.

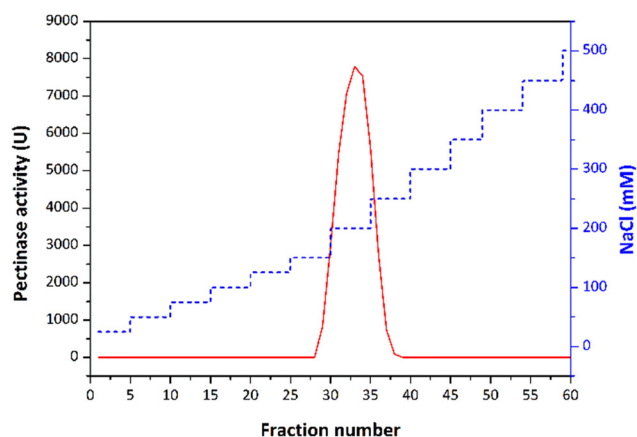


Fig. 3 The elution curve in ion exchange chromatography on Q Sepharose.

albeit with a lower yield of 13%.²² Similarly, a semi-purification process applied to polygalacturonase from *A. japonicas*²³ resulted in a 2.8-fold purification after two chromatography steps, which is similar to the semi-purified polygalacturonase from *A. terreus* with yields of 2.5% and 6.2%, respectively.²⁴ These comparative results emphasise the effectiveness of the applied purification strategy in achieving a considerable purification fold for the polygalacturonase of interest, with a competitive yield and specific activity.

The crude enzyme preparation with high *endo*-PG activity was purified to electrophoretic semi-homogeneity, as shown in Fig. 4. The protein fraction with high *endo*-PG activity was reduced, alkylated, and digested with trypsin. ESI-qTOF-MS analysis identified two peptides of *endo*-PG II: DITVTGASGHLINCDGAR and LESVTGTVDSK, accounting for 8% of the sequence coverage. These results confirm that the predominant isoform of *endo*-PG is PG II, which is most abundantly produced in *A. tubingensis* FAT43. The apparent molecular mass of the protein of ~38 kDa determined by SDS-gel electrophoresis (Fig. 4) was higher than the theoretically calculated 34.82 kDa, suggesting that it is significantly increased by N-glycosylation.

An analysis of all available genome sequences of *A. tubingensis* from the SWISS-PROT protein sequence database was performed to find the gene coding for PG II (Fig. 5). The search revealed a gene *pgII* that is 1086 bp long and codes for a PG II consisting of 362 amino acids. Using genomic DNA samples of *A. tubingensis* FAT43 and specific primers, two frag-

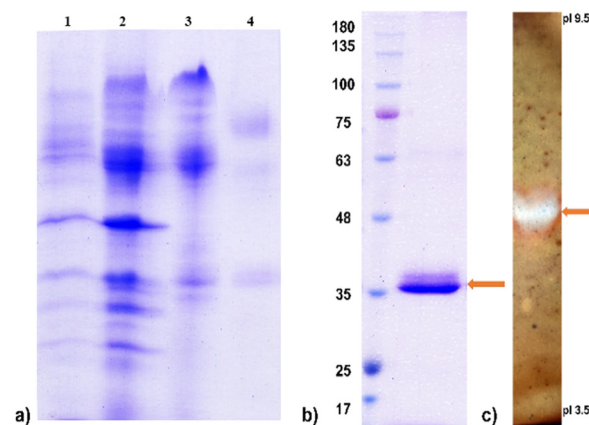


Fig. 4 Protein profiles after electrophoresis separation. (a) Crude enzyme extract (1), resuspended precipitate after precipitation with 70% AS (2), after GF on Sephacryl S100 HR (3), semi-purified PG II by IEX on DEAE Sephadex (4) (b) SDS-PAGE: protein molecular weight markers and purified PG II (~38 kDa) by IEX on Q Sepharose (c) Zymography analysis after isoelectric focusing.

ments were obtained by PCR. The fragments contained an open reading frame (ORF) that encodes 189 and 153 amino acids, respectively. It is worth noting that the mature protein contains 342 amino acids. Comparative analysis of the PG II sequence is a recurring characteristic observed in different strains of *Aspergillus* species. However, a comprehensive characterisation of only a limited number of PG II enzymes from the genus *Aspergillus* can be found in the literature.²⁵

Since the two peptides identified by MS analysis show 100% identity with the corresponding part of the sequence of the known PG II from *A. tubingensis* (GenBank accession number X58894), we investigated whether the FAT43 strain has an identical gene in its genome. Appropriate primers based on the known sequence (for the first and the second exon) were designed and PCR amplification was performed under stringent conditions. The successful amplification of DNA fragments of the expected size (570 and 500 bp) indicates with high confidence that strain FAT 43 possesses a *pgII* gene that is highly identical to that of *A. tubingensis* (GenBank accession number X58894).

The expression of the *pgII* gene is strongly regulated by the carbon source. In a minimal medium containing simple sugars such as sucrose, glucose, xylose, or galacturonic acid, both *A. niger* N400 and *A. tubingensis* NW756 showed minimal or negligible PG activity. Interestingly, a substantial induction

Table 1 Purification steps PG II

Purification steps	Total activity (U)	Total protein (mg)	Specific activity (U mg ⁻¹)	Purification fold	Yield (%)
Crude extract	255 000	140	1821.42	1	100
Ethanol precipitation	182 362.5	109.5	1665.41	0.91	71.51
AS precipitation	167 025	95.7	1709.57	0.94	65.50
SEC (Sephacryl S100 HR)	92 182.5	22.04	4182.99	2.3	36.15
IEX (DEAE Sephadex)	51 127.5	10.04	5092.33	2.8	20.50
IEX (Q Sepharose)	40 800	6.80	6001.67	3.3	16

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ATGCACTCCTTTGCTTCTCTTCTGGCCTACGGCCTAGCCGCCAGCGCCACCCTCGCTTCT 60
M H S F A S L L A Y G L A A S A T L A S

GCC TCCCCCATCGAAGCCCGGGGAAGCTGCACCTTCAAAACGGCTGCTGCTGCCAAAGCG 120
A S P I E A R G S C T F K T A A A A K A

GGCAAGGCAGGGTGCTCTACCATCACCCTTGACAACATCGAAGTCCCGCTGGAACCACC 180
G K A G C S T I T L D N I E V P A G T T

CTCGACCTGACCGGTCTCACCAGCGGTACGAAGGTCATCTTCGAGGGCACCACGACCTTC 240
L D L T G L T S G T K V I F E G T T T F

GATTATGAAGAATGGGCAGGCCCTTGATCTCCATGAGTGGCAAAGATATCACCCTCACT 300
D Y E E W A G P L I S M S G K D I T V T

GGTGCCTCAGGCCATCTCATCAACTGCGACGGTGCGCGGTGGTGGGACGGCAAGGGGACC 360
G A S G H L I N C D G A R W W D G K G T

AGCGGAAAGAAGAAGCCCAAGTTCTTCTACGCTCATGGCCTTGACTCCTCGTCCATTACT 420
S G K K K P K F F Y A H G L D S S S I T

GGATTGAATATCAAGAACTCCCTTATGGCGTTTAGTGTTCAGGCGGATGACATCACT 480
G L N I K N T P L M A F S V Q A D D I T

CTGACTGACATTACCATCAACAACGCGGACGGTGATACCTGGGTGGACACAACACTGAT 540
L T D I T I N N A D G D T L G G H N T D

GCGTTTGTATGTTGGTAACTCTGTGCGGTGTGAATATCATCAAACCGTGGGTCCATAACCAG 600
A F D V G N S V G V N I I K P W V H N Q

GATGACTGTCTTGCGATCAACTCTGGCGAGGTAAGCAGCTTTGAACATAGATTGATTG 660
D D C L A I N S G E INTRON

CATGTATGTTGATATTCTATAGAACATCTGGTTTACCAGCGGCACCTGCATTGGCGGCCA 720
INTRON N I W F T S G T C I G G H

CGGTCTCTCCATCGGTTCTGTGCGCGCCGCTCCAACAACGTTGTCAAGAACGTCACTAT 780
G L S I G S V G G R S N N V V K N V T I

CGAACACTCCACCGTGAGCAATTCGAGAACGCCGTCCGGATTAAGACCGTCTCTGGTGC 840
E H S T V S N S E N A V R I K T V S G A

CACTGGTTCCGTTGTCTGAGATCACATACTCCAACATTGTCTGTCGCGCATCTCCGATTA 900
T G S V S E I T Y S N I V M S G I S D Y

CGGCGTCGTTATCCAGCAGGATTACGAGGATGGCAAGCCTACGGGTAAGCCACGAACGG 960
G V V I Q Q D Y E D G K P T G K P T N G

TGTCACATATTACGGATGTCAAGCTGGAGAGCGTGACTGGTACTGTGGATAGTAAGGCTAC 1020
V T I T D V K L E S V T G T V D S K A T

TGATATCTATCTCCTTTGCGGATCTGGTAGCTGCTCGGACTGGACTTGGGACGATGTGAA 1080
D I Y L L C G S G S C S D W T W D D V K

GGTCACTGGAGGAAAGAAGTCTACTGCTTGCAAAAACCTACCCTTCGGTGGCTTCTTGCTAG 1141
V T G G K K S T A C K N Y P S V A S C *

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Fig. 5 Gene sequence of PG II (342 amino acids) with ORF fragments encoding 189 and 153 amino acids. The black lined sequence denotes the intronic region, and red marks indicate the leader peptide. Peptide fragments from MS analysis are highlighted in blue and green.

of *endo*-PG production was observed in *A. tubingensis* FAT 43 when pectin-containing substances such as sugar beet pulp were used as a carbon source, similar to the trend observed in *A. niger* N400 and *A. tubingensis* NW756.²⁵

Five different *endo*-PGs from *A. niger* and *A. tubingensis* have been described in the literature, with PG I and PG II proving to be the predominant enzymatic activities with isoelectric points around 5–6 and 3.5, respectively.²⁵ The lower isoelectric point probably corresponds to PG I. PGs with higher isoelectric points from *A. tubingensis* FAT 43 are very similar to *A. tubingensis* NW756 and *A. niger* N400 PGs and have an apparent molecular mass identical to that of PG II from

A. tubingensis FAT 43 (~38 kDa). However, these enzymes differ, as shown by the slightly higher isoelectric point of both *A. tubingensis* FAT43 and *A. tubingensis* NW756 PG II (~6.0) compared to *A. niger* N400 PG II (5.2).²⁵

3.2 Optimal pH and temperature for the PG II activity and stability

The optimal temperature for fungal PG varies depending on the source and environmental conditions. However, these enzymes generally are active within a wide temperature range. The catalytic activity of PG II was systematically investigated at temperatures between 30 and 60 °C, with the highest enzyme

activity observed at 45 °C and 90% of the maximum activity maintained at 50 °C (Fig. 6a). It is noteworthy that for PGs of *F. oxysporum* and *A. tubingensis* isolated from banana and peach, respectively, a congruent temperature optimum in the range of 40–50 °C was observed.²² The activation energy calculated from the Arrhenius equation is an important parameter and indicates the stability of the enzyme to temperature change. The calculated E_a of isolated PG II from the Arrhenius plot was 62.1 kJ mol⁻¹.

Fig. 6b shows the inactivation kinetics of PG II at different incubation temperatures of 40 °C, 50 °C, and 60 °C. The logarithmic transformation of the data shows a linear relationship, indicating that the thermal inactivation of PG II is a first-order kinetic process. The enzyme's half-life at 40 °C and 50 °C was 13.7 h and 5.4 h, respectively. However, at a higher temperature of 60 °C, the enzyme's half-life was significantly decreased to 0.85 h. The obtained values for the half-life at 40 °C are higher than those previously published in the literature, as well as at temperatures of 50 °C and 60 °C, except in the case of Pectinase from *A. niger* NRC1ami, which exhibits better thermostability at 50 °C and the same as PG II at 60 °C (Table 2). The thermal denaturation process requires a minimum energy, referred to as the activation energy of denaturation (E_d). When the initial energy input is below E_d , the unstable intermediate, which begins to desaturate, has the capability to fold to the native enzyme structure upon cooling. However, once this E_d barrier is surpassed, the enzyme undergoes denaturation and loses its ability to fold back to its native form. The calculated energy of denaturation PG II was 32.8 kJ mol⁻¹ which is a much higher value compared to E_d of pectinase isolated from *A. niger* NRC1ami.²⁶ Because E_d is directly related to the activation enthalpy of denaturation (ΔH), which expresses the total amount of energy required to denature the enzyme, large and positive values of E_d and ΔH should be associated with high enzyme thermostability.²⁷ Table 2 shows the results

of ΔH and other thermodynamic parameters of thermal denaturation of PG II at temperatures ranging from 40 to 60 °C. Negative ΔS and ΔH positive values suggested that the denaturation process is not spontaneous at a given temperature and, the enzyme inactivation can be reversible.²⁸ The same relation between calculated ΔS and ΔH was reported previously for pectinase derived from *A. niger* isolated from orange, but the stability of this enzyme was low even after a chemical modification that resulted in a minimal increase in enzyme stability.²⁶ The thermal stability of the enzyme isolated in this research was higher than previously reported based on the D -values comparison, which is higher than other research groups reported.^{19,26}

The prevailing characterisation of PGs currently describes a predominant pattern of significantly low thermal stability. A study by da Câmara Rocha *et al.* (2020) showed that *A. niger* exhibits sustained PG activity over 2 h at 30 °C and 40 °C within the pH range of 4.0–6.0.³² Similarly, Vaz *et al.* (2021) reported that the PG of *A. terreus* reaches its half-life after 2 h of incubation at 40 °C,²⁴ mirroring the behaviour observed in the PG from *A. japonicus* at 50 °C.²³ However, the mandatory transition to PG variants for industrial applications requires an improvement in thermostability. Conventional acidic mesothermal PGs are susceptible to thermal inactivation from 50 °C to 65 °C, with enzymatic activity decreasing within 10 to 60 min. This emphasises the need for enzymes with increased thermal resistance in industrial contexts. In particular, PG II isolated from *A. tubingensis* FAT 43 proves to be a promising candidate as it exhibits better thermostability compared to a broader range of characterised PG enzymes. These properties make PG II a potential asset for applications in industries where PGs with high thermostability requirements are essential.

The pH activity profile of PG varies greatly depending on the producing organism. The low pH optimum for *Aspergillus*

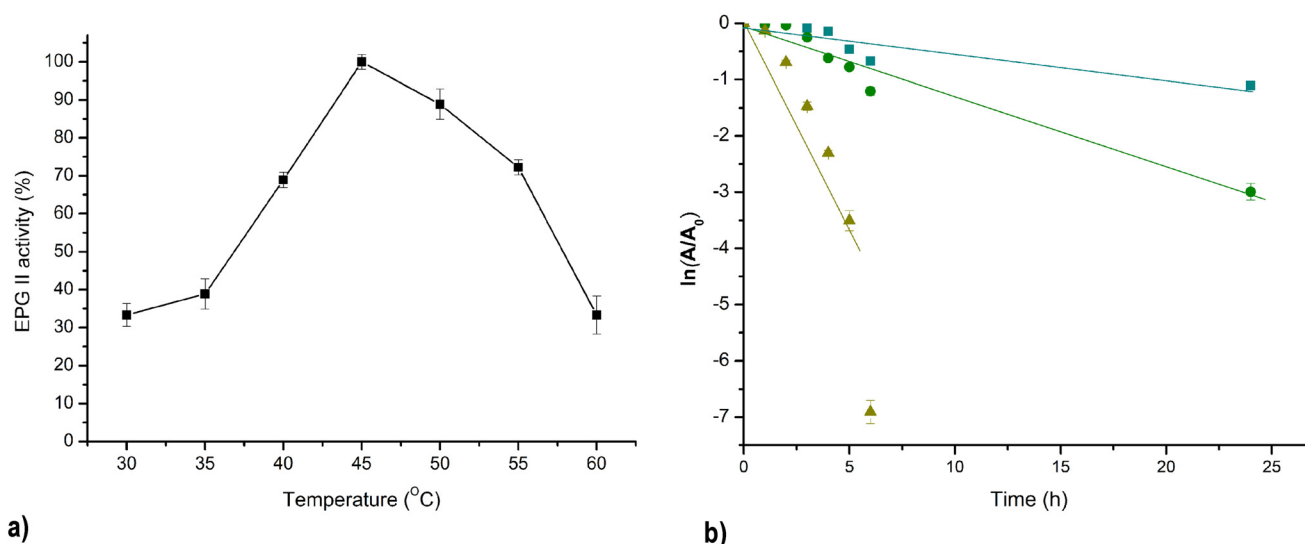


Fig. 6 Effect of temperature on PG II activity: T optimum (a) and thermal deactivation; ■ – 40 °C, ● – 50 °C, ▲ – 60 °C (b).

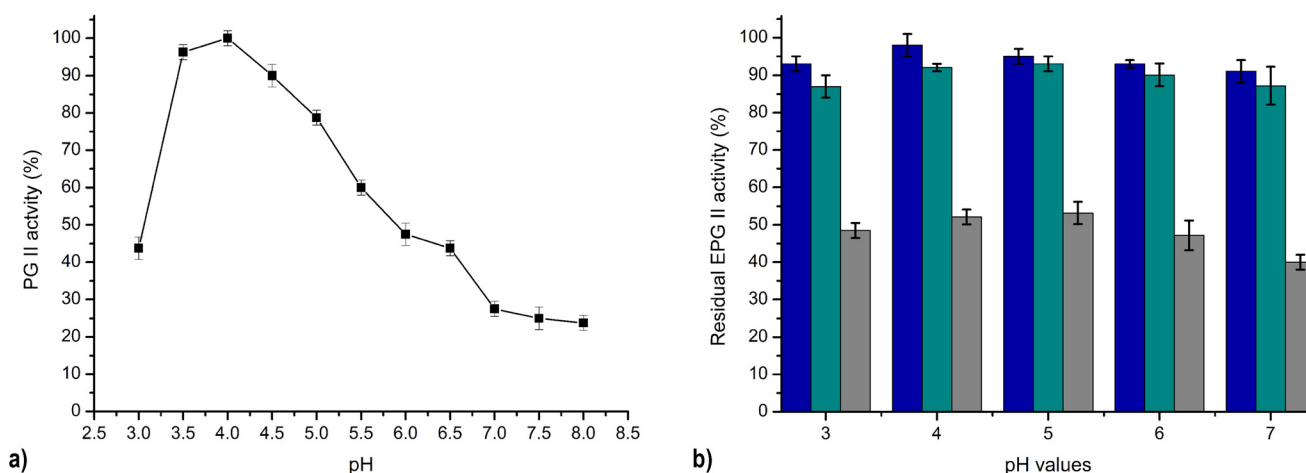
Table 2 Thermodynamic and kinetic parameters for thermal deactivation of PG II

	Temperature	Inactivation rate constants, k_d (h^{-1})	$t_{1/2}$ (h)	ΔH (kJ mol^{-1})	ΔG (kJ mol^{-1})	ΔS ($\text{J mol}^{-1} \text{K}^{-1}$)	D value (h)	Z value ($^{\circ}\text{C}$)	Ref.
PG II, <i>Aspergillus tubingensis</i> FAT43	40 $^{\circ}\text{C}$	0.05062	13.7	30.20	63.24	−105.6	45.5	16.58	This paper
	50 $^{\circ}\text{C}$	0.1294	5.36	30.11	62.82	−101.3	17.8		
	60 $^{\circ}\text{C}$	0.8144	0.85	30.03	59.76	−89.27	2.83		
Rapidase C80 (Gist–Brocades)	40 $^{\circ}\text{C}$	0.1980	3.50	143	102–98.5	130			29
	50 $^{\circ}\text{C}$	1.2378	0.56						
	60 $^{\circ}\text{C}$	5.3319	0.13						
Pectinase CCM (Biocon)	40 $^{\circ}\text{C}$	0.0990	7.00	73.9	104–105	−95.5			
	50 $^{\circ}\text{C}$	0.1873	3.70						
	60 $^{\circ}\text{C}$	0.6730	1.03						
Pectinex 3XL (Novozyme)	40 $^{\circ}\text{C}$	0.1540	4.50	157	103–99.8	176			
	50 $^{\circ}\text{C}$	1.4440	0.48						
	60 $^{\circ}\text{C}$								
Pectinase, <i>Aspergillus niger</i> NRC1ami	50 $^{\circ}\text{C}$	0.3466	2.00	11.89	85.6	−4.22	6.60		26
	60 $^{\circ}\text{C}$	0.8155	0.85	11.81	85.97	−3.70	2.45		
Endo-PG (PG8fn),	50 $^{\circ}\text{C}$	0.4332	1.6						30
<i>Achaetomium</i> sp. strain Xz8	55 $^{\circ}\text{C}$	1.2603	0.55						
PG, <i>E. carotovora</i> subsp. <i>carotovora</i> (Ecc) BR1	40 $^{\circ}\text{C}$	0.3332	2.08	42.60	84.23	−133.04			31
	50 $^{\circ}\text{C}$	0.3707	1.87		85.56				
	60 $^{\circ}\text{C}$	0.9002	0.77		86.10				

PG activity was obtained in our findings. The maximum PG II *A. tubingensis* FAT43 activity towards polygalacturonic acid was noticed over a pH range of 3.5 to 4.5, as shown in Fig. 7a. A similarly broad pH optimum was found for PG from *A. niger*, which showed a pH optimum in the range of 4.3 to 4.9.³³ This range is consistent with the pH conditions found in many plant tissues.

The pH stability of PG II was measured over a broad pH range from 3 to 7, as shown in Fig. 7b. The results elucidate that PG II retains its full enzymatic activity at a pH of 4, and has 91–95% of its original activity at the other pH values after one day. Remarkably, the residual activity of PG II remained consistently high under the same conditions for all pH values tested, ranging between 87–93% and 40–53% of the original activity after 2 and 7 days, respectively (Fig. 7b). The significant

lower pH stability of purified PG from *A. niger* NRC1ami was reported in the literature in the same pH range after 2 h of incubation,²⁶ while polygalacturonase from *A. japonicus* showed high stability in pH range 3–6 during 24 h incubation at 4 $^{\circ}\text{C}$.²³ The sustained enzymatic activity across different pH values, coupled with robust stability, is of utmost importance for potential industrial applications. In juice processing, the intrinsic acidities of different fruit types lead to different initial pH values. The liquefaction step in this industrial process is usually limited to acidic pH conditions. Consequently, the subsequent processing steps, such as liquefaction and clarification of the juices, require pH adjustment, often to pH 5. Eliminating the pH adjustment step would greatly simplify the process and contribute significantly to economic efficiency, which represents a significant challenge

**Fig. 7** Effect of pH on PG II activity: pH optimum (a) and pH stability; blue – 24h, green – 48h, grey – 7 days (b).

for ongoing research. In this context, the pectinolytic enzyme PG II, characterised by its stability and activity at low pH values, appears promising for integration into industrial processes. Its compatibility with low pH conditions makes it possible to carry out all processing phases simultaneously and avoid additional pH adjustment steps. This emphasises the practical applicability of PG II and represents a potential opportunity to improve the efficiency and cost-effectiveness of industrial juice processing.

3.3 Hydrolysis of different pectins

The composition of pectin in fruit juices is influenced by various factors, such as the type of fruit, its degree of ripeness, and the method used for juice extraction. Pectin is a complex polysaccharide found in plant cell walls. There are different types of pectins, including homogalacturonans, rhamnogalacturonans and xylogalacturonans, each of which contributes to the unique character of fruit pectins. Homogalacturonans are the most abundant type. Polygalacturonate is a special form of pectin produced by the breakdown of homogalacturonan. The addition of methyl and acetyl groups to the galacturonic acid units in the pectin structure has a significant impact on the physicochemical properties of pectin, including solubility and gelation. These modifications lead to the intricate details of pectin in fruit juices. The hydrolysis products of these complex

substrates can be analysed using TLC, a useful tool for studying the dynamic changes that occur during enzymatic hydrolysis processes. Purified PG II was used to perform enzymatic hydrolysis experiments with polygalacturonate, low-methylated pectin and high-methylated pectin. The resulting hydrolysis products are found to consist exclusively of mono- and digalacturonates (Fig. 8). It is worth noting that the highest hydrolysis specificity was observed with the non-methylated substrate, polygalacturonic acid. Accordingly, the specificity of hydrolysis decreased with increasing degree of methylation, which was reflected in significantly lower yields of hydrolysis products for both low- and high-methylated pectin. These results are consistent with previous studies indicating that an increase in the degree of methylation is associated with a decrease in the efficiency of substrate hydrolysis.³⁴

3.4 Fruit processing with PG II

This study investigates the potential of the focus on optimising juice yield, improving clarity and investigating possible changes in antioxidant capacity. Experimental analyses were conducted on quince, apple, banana, strawberry, and orange to investigate the effects of enzyme on key aspects of fruit juice production. The pectin content of the individual fruits varies. Reported inconsistencies in measuring the pectin content of these fruits render categorization based solely on pectin content unreliable. These inconsistencies stem from variations in measurement methodologies; for instance, some studies measure peel pectin content, while others assess dry weight values or soluble pectins instead of total pectins. Moreover, pectin levels may fluctuate depending on the fruit's ripeness. Consequently, relying solely on pectin content for fruit categorization may not accurately depict their true composition.^{35–37}

The liquefaction and clarification of fruit juices utilising pectinases depends on the fruit's various pectins and other polysaccharides that serve as substrates for the enzyme

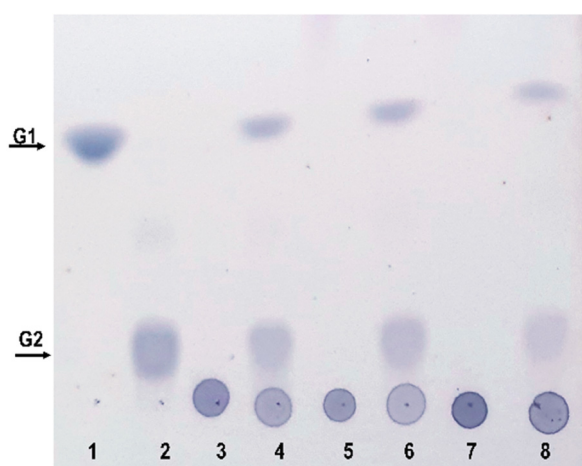


Fig. 8 TLC analysis of hydrolytic products of PGII. Standard markers: G1-galacturonic acid (1) and G2-digalacturonic acid (2). Unhydrolysed and hydrolysed substrates: PGA, (3 and 4) LMP (5 and 6), and HMP (7 and 8).

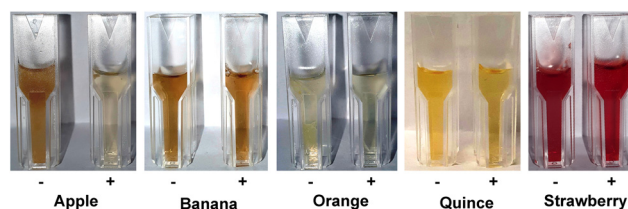


Fig. 9 The appearance of fruit juices after enzyme treatment, (–) untreated and (+) treated (b).

Table 3 The improvement of juice clarification after their treatment with PG II

Pectinase, source	Apple (%)	Banana (%)	Orange (%)	Quince (%)	Strawberry (%)	Ref
PGII, <i>A. tubingensis</i> FAT 43	90.0	19.0	5.8	11.2	51.4	This paper
PGAj, <i>A. japonicus</i>	9.4	10.8				23
exo-PG, <i>A. niger</i> MTCC 478			27.0			43
PG, <i>A. awamori</i> Nakazawa MTCC 6652	66.4					44
PGP2, <i>A. niger</i>			42			45
Pectinase, <i>A. niger</i> LB-02-SF					60	46

Table 4 Antioxidant activities of untreated and PG II treated fruit juices

Fruit juice	DPPH (mmol AAE)			FRAP (mmol AAE)			TPC (μ mol GAE)		
	Untreated	Treated	<i>p</i> -value	Untreated	Treated	<i>p</i> -value	Untreated	Treated	<i>p</i> -value
Apple	0.74 $\pm$ 0.02	0.89 $\pm$ 0.03	0.002	0.13 $\pm$ 0.01	0.16 $\pm$ 0.01	0.127	56 $\pm$ 2	65 $\pm$ 2	0.005
Banana	1.16 $\pm$ 0.04	1.20 $\pm$ 0.05	0.340	1.00 $\pm$ 0.02	0.96 $\pm$ 0.03	0.178	958 $\pm$ 32	1002 $\pm$ 41	0.217
Orange	2.75 $\pm$ 0.09	2.89 $\pm$ 0.10	0.146	6.32 $\pm$ 0.24	6.64 $\pm$ 0.24	0.148	885 $\pm$ 31	885 $\pm$ 24	1.000
Strawberry	3.51 $\pm$ 0.12	3.69 $\pm$ 0.13	0.153	1.70 $\pm$ 0.28	1.51 $\pm$ 0.32	0.017	1500 $\pm$ 51	2027 $\pm$ 45	0.0002
Quince	1.11 $\pm$ 0.04	1.63 $\pm$ 0.04	0.0001	1.99 $\pm$ 0.07	2.23 $\pm$ 0.08	0.127	479 $\pm$ 18	498 $\pm$ 15	0.233

activity.³⁸ Pectins are initially present in the cell wall of strawberries in a highly methylated form. They are then de-esterified by the activity of pectin methyl esterase, an enzyme found in strawberries, which increases the number of acidic pectins that are a suitable substrate for the activity PG II. The highest juice yield was achieved with strawberries. The yield of the treated juice increased by 25% compared to the untreated juice. Apples, oranges and bananas have highly methylated pectin (degree of methylation above 50%).^{39–41} The results of clarification of these juices are presented in Table 3 and Fig. 9.

The treatment of orange juice resulted in a percentage clarification of 87.1% clarity and a yield increase of 12.5%. The yield of the treated apple juice increased by 15.83%, and the clarity of the juice was an excellent 95%. The yield of banana juice increased by 21%, and 76.1% was clarified. Quince has a significantly methylated pectin (degree of methylation >85%),⁴² which could be a sign of a lower efficiency of PG II in liquefying this juice (10% higher juice yield).

Antioxidants are crucial in slowing down, controlling, or preventing oxidation processes that can lead to the deterioration of food quality or trigger and spread inflammatory diseases.⁴⁷ Various assays with different mechanisms can assess antioxidant activity. This study evaluated the antioxidant activities of untreated and enzyme-treated fruit juice by determining their DPPH radical scavenging activities and FRAP (Table 4). The statistically significant results for TPC, DPPH and FRAP before and after enzyme treatment were compared using the Student's *t*-test. Based on the obtained *p*-values, they were classified into two groups.

A statistically significant difference, or an increase in the content of total phenols and/or antioxidative activity after enzyme treatment, was observed when the *p*-value < 0.05. In cases where the *p*-value > 0.05, there was no statistically significant increase in these values. The content of total phenols differs in the PG II-treated juices compared to the untreated juices, with the exception of orange juice, where there is no change in the phenolic composition of the juice. After enzymatic treatment, strawberry juice showed the greatest increase in phenolic components, consistent with the juice's strongest antioxidant potential, as demonstrated by DPPH and FRAP tests. The antioxidant activity directly depends on the concentration of POS and its composition.^{48,49} This result is in contrast with the findings of a study by Sandri and da Salveira 2018⁴⁶ according to which the addition of pectinases from *A. niger* to strawberry juice did not increase the antioxidant

capacity of the juice. However, the most significant increase in antioxidant capacity was obtained in the treatment of quince (47%) and apple (20%) juice. Treatment of the other juices (orange and banana) also increased antioxidant activity. The increase in antioxidant activity of fruit juice could be due to improved extraction of antioxidants such as phenols and carotenoids from the cell cytoplasm.⁵⁰ Pectinase plays a crucial role in the breakdown of the middle lamella of the cell and primary wall and facilitates the release of polyphenolic compounds and carotenoids from the cells. An improvement in the antioxidant potential of fruit juice after enzyme treatment has already been observed in apricot and raspberry juices.^{50,51} The increase in the antioxidant potential of pectin after pectinase treatment or the antioxidant activity of the field compared to the original pectin has been previously demonstrated in the literature.⁵² In addition, previous studies have shown that electron-donating groups such as carboxyl, hydroxyl, and methoxy groups can enhance the antioxidant properties of a sample.⁵³ While the free radical scavenging activity of hydroxyl groups in polysaccharides is relatively low due to the lack of a phenolic structure, numerous other factors, including the presence of galacturonic acid and other chemical components in polysaccharides, are thought to play an important role in their antioxidant activities.⁵⁴

4. Conclusion

The optimal temperature range (30–60 °C) for the activity of PG II, with a peak at 45 °C and remarkable thermal stability, makes it a versatile enzyme for industrial applications. The enzyme's pH activity profile, which shows a low optimum pH (3.5–4.5) and robust stability over a broad pH spectrum (3–7), emphasises its adaptability to different processing conditions. The high specificity of PG II for the hydrolysis of non-methylated substrates indicates its effectiveness in various enzymatic processes. In the processing of fruit juices, experiments with different fruit juices showed the effectiveness of PG II in liquefaction and clarification, resulting in increased yield and clarity. Strawberry juice, in particular, showed the greatest influence on the increase in yield. In addition, the application of PG II increased antioxidant activity in the treated juices, with significant improvements observed in strawberry, quince, and apple juices, suggesting potential health-promoting benefits. PG II derived from *A. tubingensis* FAT43-derived is a

promising enzyme with favourable properties for industrial processes, especially fruit juice processing. Its versatility, improved thermal stability and adaptability to different pH conditions make PG II a valuable asset for potential applications in biotechnology. Further studies could explore its synergies with other enzymes and broader industrial applications.

Author contributions

Conceptualization: M. P. and M. Š. S.; formal analysis: M. P. and A. M.; funding acquisition: Z. V. and I. K.; investigation: M. P., M. Š. S. and A. L.; methodology: A. M., M. Š. S. and M. K.; supervision: Z. V. and I. K.; validation: A. M.; writing – original draft: M. P., M. Š. S. and A. M.; writing – review & editing: M. K. and A. L.

Conflicts of interest

There are no conflicts to declare.

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