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1. Introduction

The importance of researching green and renewable energy has grown due to the rising concerns about energy and the environment. Consumer electronics have increasingly adopted lithium-ion batteries because of their exceptional energy density, portability, and outstanding capacity. However, the limited availability of lithium resources and safety concerns associated with flammable organic electrolytes have hindered their further development. The need for more sustainable and affordable battery options has led to the creation of postlithium-ion batteries that utilize elements found abundantly in the earth's crust, such as Na, K, Zn, Mg, and Al^{1-6} A new and innovative water battery technology called aqueous zinc-ion batteries (AZIBs) uses a slightly acidic or near-neutral aqueous solution as an electrolyte and Zn metal as an anode. AZIBs are known for their safety, eco-friendliness, affordability, and high power capability. They have a low redox potential of -0.763 V (vs. H^{\dagger}/H_2) and a high theoretical capacity of 820 mA h $\rm{g^{-1}}$, making them a promising option for large-scale energy storage and smart grids.^{7–9}

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Synergistic carbon and oxygen vacancy engineering on vanadium dioxide nanobelts for efficient aqueous zinc-ion batteries†

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Vanadium-based compounds with stable crystal structures and high capacities are promising cathode materials in aqueous zinc-ion batteries (AZIBs); nevertheless, the sluggish solid-phase diffusion kinetics of zinc ions and poor electronic conductivity have obstructed their application. Herein, this study proposes a synergistic engineering approach involving carbon and oxygen vacancies to improve the performance of VO₂. Compared to VO₂, VO₂@C shows improved electron/ion transport kinetics due to carbon coating, oxygen vacancy, expanded lattice, and reduced grain size. This composite also offers improved structural stability and extra active sites, enhancing zinc-ion storage performance. The optimized VO₂@C-350 composite electrode displays a remarkable discharge capacity of 391 mA h g⁻¹ at 0.1 A g⁻¹ over 100 cycles and maintains good cycle stability performance at 2 A g⁻¹ for over 2000 cycles. Further analysis has identified that its reaction mechanism involves a co-intercalation/ de-intercalation process of the proton $(H⁺)$ and $Zn²⁺$. This innovative synergistic engineering approach can be implemented in other zinc storage materials to achieve efficient AZIBs. **PAPER**
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The cathode is an essential component in determining the energy density and cycle life of AZIBs. Various cathode hosts have been developed by researchers, including Prussian blue analogs $(PBAs),¹⁰$ Mn-based,¹¹ V-based,¹² and organic compounds.¹³ Cathode materials containing vanadium have gained significant attention due to their diverse crystal structures and valence states. $14-16$ These materials possess remarkable specific capacity, exceptional rate capability, and longlasting cycle life. Among these, B-phase vanadium dioxide $(VO₂)$ is noteworthy for its one-dimensional tunnel structure formed by corners and edges shared by $VO₆$ octahedra, which supports the intercalation and delamination of $\text{Zn}^{2+17,18}$ However, VO₂ frequently faces issues such as sluggish solid-phase diffusion kinetics of zinc ions, poor electronic conductivity, and structural deterioration upon repeated ion (de)intercalation, leading to poor rate performance and a rapid decrease in capacity.^{19,20} To date, numerous high-efficiency strategies have been suggested to tackle these issues. To improve the electronic conductivity and structural durability of $VO₂$, highly conductive carbon substrates such as graphene, $21-24$ carbon cloth, 25 carbon fiber,²⁶ and carbon coating layer²⁷⁻³⁰ have been utilized. Oxygen vacancy engineering has been implemented to quicken the Zn^{2+} diffusion in the solid phase and modulate the VO₂ band gap.³¹⁻³³ Nevertheless, there are only limited attempts to employ dual engineering of carbon and oxygen vacancy to enhance the electrochemical properties of $VO₂$. Additionally,

a straightforward and efficient method to simultaneously implement carbon and oxygen vacancy is urgently required.

Our study showcases a versatile and straightforward technique for producing carbon-coated VO₂ nanobelts (VO₂@C) with oxygen vacancies through C_2H_2 chemical vapor deposition. Structural and electrochemical analyses demonstrate that $C₂H₂$ heat treatment results in a carbon coating, oxygen vacancy, expanded lattice, and reduced grain size in $VO₂$, thus enabling extra active sites, accelerating electron/ion transport, and preventing structural degradation. This leads to enhanced electrochemical performance compared to pure $VO₂$ in AZIBs. The optimized $VO₂(Q)C-350$ composite electrode displays an impressive specific capacity of 391 mA h $\rm g^{-1}$ at 0.1 A $\rm g^{-1}$ over 100 cycles. It also maintains stability at 1 and 2 A $\rm g^{-1}$ throughout 2000 cycles and exhibits a reliable rate performance of 174 mA h g^{-1} at 5 A g^{-1} . Our research proposes an innovative method for introducing carbon and oxygen vacancy to develop advanced cathode materials for AZIBs.

2. Experimental section

2.1 Materials synthesis

For the experiment, only analytically pure reagents were used without further purification. In order to produce vanadium dioxide, we combined 14 mmol of oxalic acid with 7 mmol of vanadium pentoxide in 40 mL of deionized water. The mixture was stirred for an hour at 75 \degree C before being transferred to a 50 mL Teflon autoclave and reacted at 180 $^{\circ}$ C for three hours. After producing the $VO₂$ nanobelts were gathered and cleaned using distilled water and ethanol before drying in a vacuum. Finally, we ensured good crystallinity by calcining them at 300 °C in the air. To produce $VO_2@C-300$, $VO_2@C-350$, and VO₂@C-400 nanobelts, the VO₂ nanobelts were subjected to calcination with a C_2H_2/Ar gas mixture (volume ratio of 1:9) at temperatures of 300 $^{\circ}$ C, 350 $^{\circ}$ C, and 400 $^{\circ}$ C for one hour each.

2.2 Materials characterizations

We obtained X-ray diffraction (XRD) patterns from a Panalytical X'Pert Pro MPD and X-ray photoelectron spectroscopy (XPS) results from a Thermo Scientific ESCALAB 250Xi instrument. To carry out XRD and XPS tests ex situ, we dismantled cells at specific voltages and thoroughly rinsed them with distilled water multiple times. Afterward, we dried them in a vacuum to prepare the electrodes. We captured visuals of the specimens with field-emission transmission electron microscopy (TEM, JEOL-2100F), energy dispersion X-ray spectroscopy (EDS), and field-emission scanning electron microscopy (SEM, JEOL JSM-7500F). We used a NEXUS 670 Raman spectrometer with a 532 nm excitation source to acquire Raman spectra. We used a TG-DTA STA409PC thermogravimetric analyzer to perform thermogravimetric analysis (TGA) on the samples. Additionally, we adopted an EPR spectrometer (A300-10-12, Bruker) to conduct room temperature electron paramagnetic resonance (EPR) tests on the samples, using a 9.45 GHz x-band with an

amplitude of 5.00 g modulation and 100 kHz magnetic field modulation.

2.3 Electrochemical measurements

A consistent blend of VO₂@C, acetylene black, and polyvinylidene difluoride (PVDF) in a 7 : 2 : 1 weight ratio was utilized to make a cathode slurry. We applied the slurry onto a Ti foil and dried it under a vacuum at 120 \degree C. We cut the dried foil into disks that were 12 mm in diameter, which gave an active material mass loading of around 1 mg cm^{-2} . We used zinc foil for the anodes, 3 M $Zn(CF_3SO_3)_2$ aqueous solution for the electrolytes, and Whatman glass microfiber (GF/D) for the separators. We assembled CR2032 coin cells under an air atmosphere with an electrolyte drop volume of 120 µL to evaluate the electrochemical performance. To perform cyclic voltammetry (CV) tests, we utilized a CHI760E electrochemical workstation (Shanghai Chenhua). Additionally, we conducted galvanostatic charge/discharge measurements on a LAND-CT2001A battery cycler at different current densities. We used The voltage window between 0.25 and 1.4 V compared to Zn^{2+}/Zn . For the electrochemical impedance spectroscopy (EIS) measurements, we utilized a Gamry-Reference 3000 electrochemical workstation. The measurements were conducted across a 100 kHz to 0.01 Hz frequency range. Before completing the EIS measurements, we cycled the electrodes for 10 cycles at 0.1 A g^{-1} . To calculate zinc-ion diffusion coefficients $(D_{\text{Zn}^{2+}})$, we employed eqn (1). **Paper**
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$$
D_{\text{Zn}^{2+}} = \frac{R^2 T^2}{2A^2 n^4 F^4 C^2 \sigma^2}
$$
 (1)

Eqn (1) includes different variables such as σ , representing the Warburg factor, F for the Faraday constant, C for the zincion concentration, A for the electrode surface area, T for the absolute temperature, n for the number of electrons per molecule, and R for the gas constant. To determine the value of σ , one can calculate the line slope using eqn (2).

$$
Z' = RD + RL + \sigma \omega^{-1/2}
$$
 (2)

We conducted galvanostatic intermittent titration technique (GITT) tests to determine the diffusion coefficient of Zn^{2+} in the electrode. As part of the GITT tests, participants were instructed to cycle for 20 minutes at 50 mA g^{-1} and rest for 2 hours after completing 10 activation cycles. During each relaxation period, the potential change indicated the overpotential of the corresponding discharge/charge state. To determine $D_{Zn^{2+}}$, we employed Fick's second law and used a simplified equation.

$$
D_{\text{Zn}^{2+}} = \frac{4}{\pi \tau} \left(\frac{m_{\text{B}} V_{\text{M}}}{M_{\text{B}} S} \right)^2 \left(\frac{\Delta E_{\text{S}}}{\Delta E_{\tau}} \right)^2 (\tau \ll L^2 / D_{\text{Zn}^{2+}})
$$
(3)

Eqn (3) includes various factors such as the mass of the electrode material (m_B) , its molar mass (M_B) , molar volume (V_M) , geometric area (S), potential equilibrium difference (ΔE_s), change in cell voltage due to impulse current (ΔE_{τ}) , and average thickness of the electrode (L) .

3. Results and discussion

The process of creating VO₂@C nanobelts is shown in Fig. 1(a). The initial step involves producing pure $VO₂$ nanobelts through a hydrothermal reaction using vanadium pentoxide and oxalic acid as reagents. Subsequently, these nanobelts undergo calcination in the air. The next step involves the calcination of $VO₂$ nanobelts with mixed C_2H_2/Ar under varying temperatures to create $VO_2@C$ nanobelts with different microstructures. SEM and TEM measurements were carried out to examine the microstructures and morphologies of $VO₂$ -based samples. Fig. 1(b) displays the nanobelt structure of pure $VO₂$, with the belt width ranging from 50–150 nm. The nanobelt architecture shows no changes after undergoing C_2H_2 heat treatment for VO₂@C-300, VO₂@C-350, and VO₂@C-400 (Fig. 1(c)-(e)). Upon analysis of the high-resolution TEM (HRTEM) images of VO₂@C-350 (Fig. 1(f) and (g)), it can be confirmed that the coreshell nanobelt structure has indeed been formed after the C_2H_2 heat treatment, and the carbon coating thickness on the sample after calcination at 350 $^{\circ}$ C is approximately 2 nm. A lattice stripe, with an interplanar spacing of 0.616 nm, is also visible, aligning with the (001) VO₂(B) plane (Fig. 1(g)). In addition, the EDS pattern of $VO₂@C-350$ displays an even dispersion of V, O, and C components throughout its composition, as depicted in Fig. 1(h). The $VO₂(Q)CO₂300$ and $VO₂(Q)CO₂400$ samples were also subjected to HRTEM and EDS characterizations. Despite the relatively low calcination temperature, EDS maps confirm the existence of a carbon coating layer on $VO₂(Q)CO₃(Q)CO₄$ albeit barely visible, as shown in Fig. S1 (ESI†). In contrast, the carbon layer on $VO₂(Q)CO₂(1)$ grows considerably, measuring around 4 to 20 nm, as observed in Fig. S2 (ESI†).

Fig. 1 (a) Scheme of the synthesis process for VO₂@C nanobelts. SEM images for (b) VO₂, (c) VO₂@C-300, (d) VO₂@C-350, and (e) VO₂@C-400. (f) and (g) HRTEM images, and (h) EDS maps of $VO₂@C-350$.

Fig. 2 Structural characterizations of VO₂-based samples. (a) and (b) XRD patterns, (c)–(e) high-resolution C 1s, V 2p, and O 1s XPS spectra, and (f) EPR spectra

The VO₂-based samples' crystal structures were analyzed using XRD. In Fig. 2(a), the XRD patterns of these samples are shown. It can be observed that all diffraction peaks correspond to $VO₂(B)$ (JCPDS no. 81-2392) having the space group of $C2/m$. Moreover, no noticeable impurities have been observed either before or after the C_2H_2 heat treatment. By analyzing the zoomed-in view of XRD patterns shown in Fig. 2(b), the diffraction peaks' intensity decreases as the calcination temperature increases. This decrease in intensity suggests a reduction in crystallinity. Additionally, the characteristic peak (110) is observed to broaden and shift to a lower angle, indicating a decrease in grain size and an increase in interlayer spacing. These changes favor embedding and exfoliating zinc ions during discharging/charging. In Fig. S3 (ESI†), we can observe the Raman spectra of $VO₂$ -based samples. The peaks detected at 148, 288, 414, 530, and 997 cm^{-1} in VO₂ indicate stretching and bending vibrations between the V–O within the layers. 30,34 Additionally, the peak at 697 $\rm cm^{-1}$ shows the coordination of the vanadium atom with three oxygen atoms. 22 Interestingly, the vibration patterns of $VO₂@C$ samples are comparable to those of the original $VO₂$, suggesting that VO₂'s crystal structure remains intact after the C_2H_2 heat treatment. In addition, the presence of D and G bands in VO2@C samples confirms the formation of carbon.

An XPS analysis examined the samples' electronic structure and surface composition. Based on the XPS survey spectra (shown in Fig. S4, ESI†), it can be determined that all $VO₂(Q)CO$ samples contain V, O, and C elements. The spectra of the $VO₂(Q)$ C samples in Fig. 2(c) show three distinct peaks at 284.8, 286.2, and 288.4 eV in the C 1s region. These peaks indicate the presence of C–C, C–O, and C $=$ O bonds, respectively. These findings suggest that carbon has been successfully introduced.^{35,36} Pure VO₂ exhibits two peaks at 515.8 and

522.8 eV in the V 2p spectrum, indicating the presence of V^{4+} in VO₂, as depicted in Fig. 2(d).²³ Following the C₂H₂ heat treatment, it was observed that the $VO₂(a)$ C samples displayed two additional peaks at 513.6 and 521.1 eV, which corresponded to V^{3+} , indicating the formation of oxygen vacancies in VO₂.³² The area ratios of V^{3+}/V^{4+} calculated for VO₂@C-300, VO_2 (a)C-350, and VO_2 (a)C-400 are 0.24, 0.27, and 0.29, respectively. These results indicate that the proportion of V^{3+} increases gradually with increasing calcination temperature, leading to an increase in the content of oxygen vacancies in the samples. The presence of these vacancies facilitates the rapid migration of ions and provides more channels for ion migration. From the O 1s spectra illustrated in Fig. 2(e), it can be inferred that the VO₂@C samples contain oxygen vacancies. The peaks at 529.6, 531.1, 531.8, and 532.4 eV signify V–O, oxygen vacancy (O_v) , C–O, and C=O, respectively.³² Further evidence of the presence of oxygen vacancies was obtained through EPR spectroscopy, as shown in Fig. 2(f). The signal of VO2@C-350 exhibits a more pronounced symmetry peak at $g = 2.0$ compared to VO₂. This is generally attributed to the presence of oxygen vacancy. TGA was utilized to determine the carbon mass fraction in the $VO₂@C$ composites produced at various temperatures, and the results are shown in Fig. S5 (ESI†). During heating in the air at a ramp rate of 10 $^{\circ}$ C per minute to 700 \degree C, there was a weight loss observed up to 200 \degree C. This was attributed to the loss of adsorbed water. C was converted to $CO₂$ as the temperature increased, and $VO₂$ was oxidized to V_2O_5 .^{21,22} As a result, VO₂@C-300, VO₂@C-350, and $VO₂(Q)CO₂(Q)$ and 16.5 wt%, respectively. These findings align with the carbon layer thickness observed on HRTEM.

We conducted a study to evaluate the Zn storage performance of VO_2 -based samples using a coin cell model (Fig. 3) to

Fig. 3 Zn storage performance of VO₂-based samples. (a) CV curves of VO₂@C-350 at 0.2 mV s⁻¹. (b) Charge/discharge curves of VO₂@C-350 at 0.1 A g $^{-1}$. (c) Cycle performance and CEs of VO₂-based samples at 0.1 A g $^{-1}$. (d) Rate performance of VO₂-based samples. (e) Charge/discharge profiles of VO₂@C-350 at 0.1 to 5 A g⁻¹. (f) Comparison of VO₂@C-350 with other VO₂-based cathode materials for AZIBs. (g) Long cycle performance of VO2@C-350.

assess how oxygen vacancy and carbon coating affect the properties. In Fig. 3(a), the CV curves of $VO₂(Q)C-350$ are displayed at a scan rate of 0.2 mV s^{-1} , ranging from 0.25 to 1.4 V. Based on our research, it appears that there is a notable redox coupling occurring at 0.37/0.56 and 0.92/1.05 V. This finding indicates a potential two-step zinc-ion (de)intercalation mechanism.²⁰ Upon conducting the initial two scans, we observe stable redox couples, showing a remarkably reversible (de)intercalation reaction of Zn^{2+} . The voltage curve for VO₂@ C-350's Zn storage process at 0.1 A g^{-1} is depicted in Fig. 3(b). In the initial cycle; the cell experiences an activation reaction that cannot be reversed. During the subsequent processes, two significant cathodic/anodic platforms occur at around 0.6/0.7 and 0.9/1.0 V, corresponding to the zinc ions' (de)intercalation process. This is consistent with the findings derived from the analysis of the CV. In Fig. 3(c), the performance of VO_2 , VO_2 @ C-300, VO₂@C-350, and VO₂@C-400 in terms of cycle performance and Coulombic efficiency (CE) at 0.1 A g^{-1} is demonstrated. Unfortunately, pure $VO₂$ does not display good electrochemical activity, with an initial discharge capacity of only 319 mA h $\rm g^{-1}$. However, VO₂@C-300 and VO₂@C-350 show improved electrochemical activity with initial discharge capacities of 330 and 335 mA h g^{-1} after carbon cladding. Interestingly, VO₂@C-400, with substantial carbon cladding, only

delivers 260 mA h g^{-1} discharge capacity. Based on the $VO₂(Q)$ C samples, there appears to be a gradual increase in the first few cycles, possibly attributed to the activation process of the electrodes. After 100 cycles, it has been observed that VO2@C-350 shows the highest electrochemical stability among the samples. It has a discharge capacity of around 391 mA h g^{-1} and no capacity decay. At the same time, the CE of $C@VO_2$ -350 is maintained at 99.5% throughout the cycles. After 100 cycles, pure $VO₂$ has a capacity retention rate of 83.4%, with its capacity dropping to only 266 mA h g^{-1} . In Fig. 3(d), we can see the rate performance of different samples at varying currents of 0.1 to 5 A g^{-1} . Out of all the samples, VO₂@C-350 has the most impressive rate performance. It can deliver discharge capacities of 331, 413, 406, 381, 350, and 174 mA h g^{-1} at 0.1, 0.2, 0.5, 1.0, 2.0, and 5.0 A g^{-1} . It's important to note that the $VO₂(a)$ $C₃50$'s capacity remains consistent even when the rate drops abruptly to 0.1 A g^{-1} . Fig. 3(e) displays the voltage curves for the discharge and charge of $VO₂(Q)CO₃350$. Furthermore, according to the data presented in Fig. $3(f)$, VO₂@C-350 exhibits a higher rate performance compared to other cathodes that are based on VO₂ for AZIBs, such as VO_{2-x}(B),³⁷ coin-shaped VO₂,³⁸ VO₂ nanorods,³⁹ β -VO₂/CNTs,⁴⁰ and VO₂/Mxene.⁴¹ In Fig. 3(g), the performance of VO₂@C-350 is observed throughout a lengthy cycling period, with its corresponding CE at 1 and 2 A g^{-1} .

Before the high-current test, the electrodes are activated with a slight current density of 0.1 A g^{-1} . At a rate of 1 A g^{-1} , the initial capacity is 438 mA h g^{-1} , while at 2 A g^{-1} , it is 342 mA h $\rm g^{-1}$. After undergoing 2000 cycles, the VO₂@C-350 exhibits a discharge capacity of 350 and 254 mA h $\rm g^{-1}$ while maintaining 98.7% and 99.2% CE, respectively. These findings demonstrate the impressive cycling stability of $VO₂(Q)C-350$, indicating that the carbon cladding layer and oxygen vacancy can enhance conductivity and preserve the electrode material's structure.

Using EIS testing, it was discovered that $VO₂(Q)C-350$ had better reaction kinetics than the other materials. The Nyquist plots for these VO_2 -based samples exhibit comparable features (Fig. 4(a)). They all show a semi-circle that represents the charge transfer resistance $(R_{\rm ct})$ of the electrode/electrolyte interface, along with a straight line that denotes the Warburg impedance (Z_w) . According to Table S1 (ESI†), VO₂@C-350 has a charge transfer resistance of only 92.2 Ω , which is lower than VO₂ (119.1 Ω), VO₂@C-300 (100.4 Ω), and VO₂@C-400 (127.3 Ω). This suggests that $VO₂(Q)C-350$ has superior charge transfer kinetics. Fig. 4(b) illustrates a correlation between Z' and $\omega^{-1/2}$ in the low-frequency range. The Warburg factor (σ) , which represents the slope of the line, shows a direct correlation with $D_{\text{Zn}^{2+}}$. After evaluating the Warburg factor, we were able to determine the diffusion coefficient of Zn^{2+} to be 9.7 \times 10^{-11} cm² s⁻¹ for VO₂, 1.7 × 10⁻¹⁰ cm² s⁻¹ for VO₂@C-300, 2.7×10^{-9} ${\rm cm^2~s^{-1}}$ for VO₂@C-350, and 1.3 \times 10^{-10} ${\rm cm^2~s^{-1}}$ for VO2@C-400 (refer to Table S1, ESI†). We performed GITT measurements to evaluate $D_{\text{Zn}^{2+}}$ in electrodes made from VO₂. Fig. S6 (ESI†) displays the curves for voltage response and $D_{Zn^{2+}}$ for VO_2 , VO_2 @C-300, VO_2 @C-350, and VO_2 @C-400, as well as their associated discharge/charge states. Based on the EIS

analysis and GITT measurements, the order of $D_{\text{Zn}^{2+}}$ in the electrodes appears as follows: $VO₂@C-350 > VO₂@C-300 >$ $VO₂(Q)C-400 > VO₂$. From the results, we can conclude that $VO₂(Q)CO₂(Q)CO₃CO₂$ exhibits outstanding charge transfer and zinc-ion diffusion kinetics due to its optimized structure. Compared to the other samples, this contributes to its ability to achieve the highest storage capacity for Zn ions, cycling durability, and rate capability. We conducted CV tests on $VO_2@C_350$ to determine the extent of diffusion-controlled and capacitance-controlled Zn ion storage. The results, displayed in Fig. 4(c), show that the CV curves of VO₂@C-350 have similar shapes at 0.1–0.5 mV s⁻¹. When the scan rate increases, the oxidation peak moves towards higher voltages, and the reduction peak moves towards lower voltages. The equation $i = av^b$ determines the peak current (i) based on the sweep frequency (v) , with parameters a and b. When the value of b approaches 0.5, it suggests that ion diffusion processes are the primary factor influencing capacity. On the other hand, when b approaches 1, capacitive processes play a more significant role in determining capacity. By applying a logarithmic transformation to the current–sweep relationship shown in Fig. 4(d), the values of b for peaks 1, 2, 3, and 4 can be computed as 0.99, 0.86, 0.94, and 1.14, respectively. These values suggest that the pseudocapacitance contribution of VO₂@C-350 is present throughout the redox process. An equation is used to determine the capacitance contribution: $i = k_1 v + k_2 v^{1/2}$. The equation includes k_1 and k_2 , which serve as percentage coefficients for the capacitance and diffusion factors in the overall capacity calculation. According to Fig. 4(e), the level of capacitance contribution rises considerably as the scan rate increases, resulting in advantageous outcomes for quick Zn^{2+} storage and cycle durability. According to the data shown in Fig. 4(f), when the scan rate is set at 0.5 mV s^{-1} , Puper

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Fig. 4 (a) Nyquist plots and equivalent circuit of VO₂-based samples. (b) Correlation between Z' and $\omega^{-1/2}$. (c) CV curves for VO₂@C-350 at 0.1–0.5 mV s⁻¹. (d) Log(i) versus log(v) plots of VO₂@C-350. (e) Contribution of capacitive ion storage of VO₂@C-350 at 0.1–0.5 mV s⁻¹. (f) Contribution of capacitive ion storage of VO₂@C-350 at 0.5 mV s⁻¹.

Fig. 5 Ex situ structural characterizations of VO₂@C-350 electrode in the 1st cycle. (a) XRD patterns, (b) V 2p XPS spectra, and (c) Zn 2p XPS spectra.

the capacitance contribution reaches its peak at 66%. Moreover, we analyzed the Zn storage in the electrodes of $VO₂$, $VO₂(Q)CO₂(Q)$ method. The results in Fig. S7–S9 (ESI†) indicate that the VO2@C-350 electrode exhibits a much higher capacitance contribution than the $VO₂$ and $VO₂(Q)C-300$ electrodes. This highlights the superior performance of the $VO₂(QC-350$ electrode. Our research shows that the samples demonstrate a blend of ion storage mechanisms controlled by both capacitive and diffusion processes. Additionally, we observed that introducing oxygen vacancy and carbon coating into $VO₂$ facilitated zinc-ion adsorption/desorption behavior.

We carried out ex situ XRD and XPS investigations to gain insights into the process of zinc-ion storage in $VO₂(QC-350)$ (Fig. 5). In the first cycle, Fig. 5(a) displays ex situ XRD patterns of the VO₂@C-350 electrode. The pristine electrode displays distinct diffraction peaks, including 25.3, 30.0, and 44.9° , which correspond to the crystal planes $(110),$ $(-401),$ and (-601) of VO₂(B). Notably, the peaks observed during charging/discharging are consistently present, which suggests that the zinc-ion storage of $VO₂(Q)C-350$ is highly reversible and that the structural stability of the material is excellent. Moreover, new heights appear at 12.4 and 36.1° during discharge, which can be attributed to the $\text{Zn}_x(\text{OH})_2\text{V}_2\text{O}_7\cdot 2\text{H}_2\text{O}$ species. ^{24,42} It seems that introducing zinc ions triggers a new phase, while their removal causes it to disappear. This implies that zinc storage relies on a co-intercalation/de-intercalation process of

the Zn^{2+} and proton (H⁺). Fig. 5(b) displays the V 2p spectra of the VO₂@C-350 electrode at different states. The ratio of V^{3+}/V^{4+} in the pristine electrode is 0.24, which increases to 1.32 following discharge to 0.25 V due to H^{\dagger}/Zn^{2+} intercalation. Once charged to 1.4 V, the ratio of V^{3+}/V^{4+} almost returns to its initial state. This indicates a reversible extraction of $H^{\dagger}/\mathrm{Zn}^{2+}$ from the VO₂@C-350 structure. The Zn 2p spectrum (Fig. 5(c)) also supports this conclusion, as no Zn elemental is observed in the pristine electrode before charging and discharging. The Zn signal is significantly reduced during charging compared to the peaks during discharge, indicating that Zn^{2+} is extracted from $VO₂(Q₀C-350)$. However, trace Zn peak signals may be attributed to residual electrolytes on the electrode surface and irreversible Zn^{2+} intercalation in the VO₂@C-350 electrode even after charging. Based on ex situ XRD and XPS analysis, it has been determined that VO₂@C-350 exhibits an $H^{\dagger}/\text{Zn}^{2+}$ storage process that follows a (de)intercalation reaction mechanism.

4. Conclusions

We synthesized $VO₂(Q)$ C composites with oxygen vacancies using $C₂H₂$ heat treatment. The composites underwent evaluation as possible AZIB cathodes. The $VO₂(Q)C-350$ electrode, which was optimized, displayed remarkable ion storage capacity, boasting a specific capacity of 391 mA h g^{-1} at 0.1 A g^{-1} over 100 cycles and stable cycle performance at 1 and 2 A g^{-1} throughout 2000 cycles.

Based on experimental findings, the remarkable electrochemical capabilities of $VO₂(Q)C-350$ can be traced back to its improved charge transfer, heightened ion transportation, and better pseudocapacitive properties. Furthermore, ex situ XRD and XPS analyses discovered that $H^{\dagger}/\mathrm{Zn}^{2+}$ storage in VO₂@C-350 follows a (de)intercalation reaction mechanism.

Conflicts of interest

There are no conflicts to declare.

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