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# Highly efficient hydrogen evolution from water electrolysis using nanocrystalline transition metal phosphide catalysts†

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Nanocrystalline transition metal phosphides (CoP and Ni<sub>2</sub>P) were successfully synthesized by a simple calcination method by using transition metal hydroxides and NaH<sub>2</sub>PO<sub>2</sub> as raw materials. Their catalytic activities for the hydrogen evolution from water electrolysis were evaluated with silicotungstic acid as an electron-coupled-proton buffer, whereby hydrogen and oxygen could be produced separately. It was found that the CoP sample showed higher catalytic activity (32 mmol min<sup>-1</sup> g<sup>-1</sup>) and good stability (12 h) as compared to the Ni<sub>2</sub>P sample, and its catalytic activity could rival that of the commercial Pt/C catalyst. The electrochemical results revealed that CoP had high cathodic current and small charge transfer resistance, which further suggested it was indeed an efficient noble metal-free catalyst for hydrogen evolution from water electrolysis.

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## 1. Introduction

Hydrogen is considered as an ideal clean green fuel.<sup>1,2</sup> Its large-scale application can solve the energy and environment issues at a global level. Water electrolysis is an important method for hydrogen production on a large scale. Therefore, this technology has received considerable attention in the field of chemistry. Generally, water and energy (in form of electricity) are the only required inputs for the electrolysis of water.<sup>3,4</sup> The separation of hydrogen and oxygen is an important process in this technology, because these gases will diffuse in electrolysis devices and can give rise to hazardous O<sub>2</sub>/H<sub>2</sub> mixtures. The proton exchange membrane electrolysis is the most mature technology used for mitigating the gas crossover, but it still a challenge to prevent such gas crossover.<sup>5,6</sup>

If hydrogen and oxygen are produced separately in the electrolyzer systems, this annoying problem will be rooted out. Cronin group has introduced a concept of the electron-coupled proton buffer (ECPB), which can decouple electrolytic H<sub>2</sub> and O<sub>2</sub> production, producing these gases separately.<sup>7–9</sup> In the reported systems, silicotungstic acid is one attractive material as a candidate of the ECPBs for the electrolysis of water due to its high solubility and reversible redox ability in water.<sup>9</sup>

Silicotungstic acid can accept two electrons to form a 2e<sup>-</sup>-reduced species in water. Furthermore, its 2e<sup>-</sup>-reduced species can reduce H<sup>+</sup> ions, which come from the oxidation of water (2H<sub>2</sub>O = 4H<sup>+</sup> + O<sub>2</sub>), into H<sub>2</sub> gas directly in the present of catalysts (such as Pt/C). This may not only separate H<sub>2</sub> and O<sub>2</sub> gases, but also give the catalysts freedom from the limitation of the low work surfaces of electrodes. However, noble metal Pt is often used as a catalyst for the hydrogen evolution in these studies. For real wide-spread application, catalysts made from elementally abundant and less expensive materials are urgently required.

Earth-abundant transition metal phosphides have received special attention in recent years, because these phosphide nanocrystals can efficiently split water into H<sub>2</sub> by utilizing electricity.<sup>10–21</sup> Nevertheless, very few reports describe the H<sub>2</sub> evolution from water electrolysis using these phosphide nanomaterials in the ECPBs systems. Herein, nanocrystalline transition metal phosphides (CoP and Ni<sub>2</sub>P) were successfully synthesized by a simple calcination method, and their catalytic activities for the hydrogen evolution from water electrolysis were evaluated with silicotungstic acid as an ECPB. The highly efficient catalytic activity of CoP nanocrystal was confirmed *via* various electrochemical techniques. Our results may allow us to highlight the promising application of transition metal phosphides in the highly efficient hydrogen evolution from water electrolysis.

## 2. Results and discussion

### 2.1. Preparation and characterization

The crystal structures and morphologies of the as-prepared transition metal phosphides have been characterized by X-ray

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† Electronic supplementary information (ESI) available: Electrochemical reduction of H<sub>4</sub>SiW<sub>12</sub>O<sub>40</sub> by a two-compartment home-made H-cell by using a classical two-electrode configuration; production of hydrogen and oxygen during the durability experiment for the CoP sample; XRD patterns for the CoP sample before and after the catalytic test. See DOI: 10.1039/c8ra07195k



diffraction (XRD) and transmission electron microscope (TEM) techniques, respectively. Fig. 1a shows the XRD pattern of the CoP sample. All diffraction peaks of the pattern are well indexed to orthorhombic cobalt phosphide (CoP, JCPDS card no. 29-0497). The main peaks at  $2\theta$  values about 31.6, 32.0, 35.3, 36.3, 36.7, 45.1, 46.2, 48.1, 48.4, 52.3, 56.0, 56.4 and 56.8° can be assigned to the diffraction peaks of the (011), (002), (200), (111), (102), (210), (112), (211), (202), (103), (020), (212) and (301) planes, respectively. Furthermore, as shown in Fig. 1d, the nickel phosphide sample is mainly composed of hexagonal Ni<sub>2</sub>P (JCPDS card no. 03-0953), and contains a small amount of hexagonal Ni<sub>5</sub>P<sub>4</sub> (JCPDS card no. 18-0883). The TEM images of the as-prepared samples are showed in Fig. 1b and e, respectively. It is found that the cobalt phosphide sample consists of CoP nanoparticles with a diameter of 10–20 nm, while the particle size of the Ni<sub>2</sub>P sample ranges from 20 to 30 nm. Moreover, HRTEM images show clear lattice fringes for the as-prepared samples. Note that the  $d = 0.189$  and  $0.283$  nm of lattice fringes in Fig. 1c match those of the (211) and (011) crystallographic planes of CoP, respectively. And the lattice spacing of  $d = 0.221$  nm in Fig. 1f corresponds to the (111) plane of Ni<sub>2</sub>P. In addition, the morphology of the CoP sample has been confirmed by scanning electron microscope (SEM) (see Fig. S1†). Surface chemical compositions of the as-prepared sample have also been studied by X-ray photoelectron spectroscopy (XPS). Fig. S2† shows the high-resolution XPS spectra of Co 2p and P 2p for the CoP sample. The peaks at 778.6, 793.6, 129.3 and 130.1 eV can be attributed to the Co 2p<sub>3/2</sub>, Co 2p<sub>1/2</sub>, P 2p<sub>3/2</sub> and P 2p<sub>1/2</sub> in CoP, respectively.<sup>12,22</sup> Two satellite peaks at

786.1 and 802.9 eV are observed for the Co 2p in the CoP sample.<sup>22</sup> The additional peaks at 781.6 and 797.7 eV in the high-resolution XPS spectrum of Co 2p and the broad peak at 133.5 eV in the high-resolution XPS spectrum of P 2p may come from the cobalt phosphate formed on the surface of CoP due to the exposure of the sample to air.<sup>12,22,23</sup> These results suggest that nanocrystalline transition metal phosphides can be obtained in this work by a simple calcination method *via* using transition metal hydroxides and NaH<sub>2</sub>PO<sub>2</sub> as raw materials.

## 2.2. Catalytic performance for H<sub>2</sub> evolution from water electrolysis

The catalytic activities of the as-prepared transition metal phosphides for the hydrogen evolution from water electrolysis have been evaluated with silicotungstic acid as an ECPB, whereby hydrogen and oxygen can be produced separately. In the present system, H<sub>4</sub>SiW<sub>12</sub>O<sub>40</sub> is firstly reduced to H<sub>6</sub>SiW<sub>12</sub>O<sub>40</sub> in a two-compartment home-made H-cell by using a classical two-electrode configuration (see Fig. S3†), and water are oxidized to molecular oxygen at the same time. Then, the 2e-reduced silicotungstic acid will reduce H<sup>+</sup> ions to molecular hydrogen in water with the obtained samples as the catalysts. Fig. 2 shows the hydrogen yield as a function of reaction time in the presence of the as-prepared catalysts. It is found that the as-prepared samples show excellent activities for the H<sub>2</sub> evolution from water electrolysis, and the catalytic activity of the CoP sample is much higher than that of the Ni<sub>2</sub>P sample. For the CoP sample, the initial rate of the H<sub>2</sub> evolution is 32 mmol min<sup>-1</sup> g<sup>-1</sup>, corresponding to a turnover frequency of 2.9 min<sup>-1</sup>. In theory, 74.6 mL (3.3 mmol) of H<sub>2</sub> can be obtained, because the 2e-reduced silicotungstic acid can provide 6.7 mmol of electrons to take part in the hydrogen evolution. However, only a half of the hydrogen yield (~37 mL) is collected in the present system. This can be ascribed to the low reducing ability of the 1e-reduced silicotungstic acid ( $E$  (H<sub>5</sub>SiW<sub>12</sub>O<sub>40</sub>/H<sub>4</sub>SiW<sub>12</sub>O<sub>40</sub>) = 0.01 V *vs.* RHE).<sup>9</sup> As a part of this work, the catalytic activity of the commercial Pt/C (5 wt%, Aladdin Co.) has been investigated under same conditions (see Fig. 2). Note

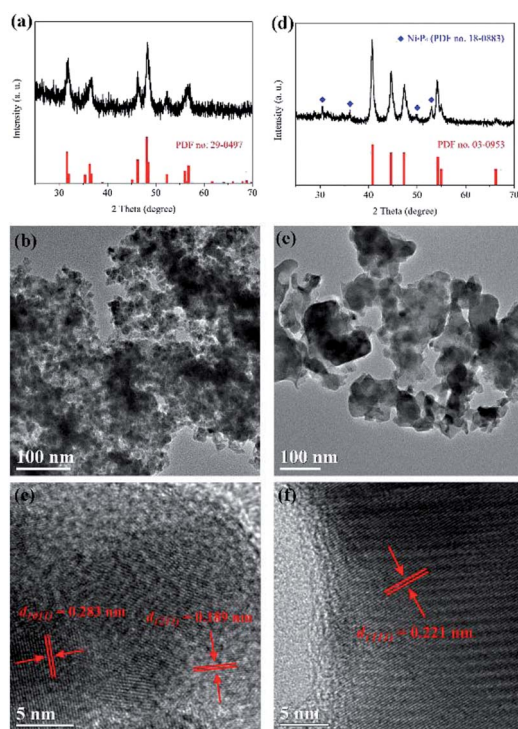


Fig. 1 XRD patterns, TEM images and high-resolution TEM images of the as-prepared samples. (a)–(c) for the CoP sample and (d)–(f) for the Ni<sub>2</sub>P sample.

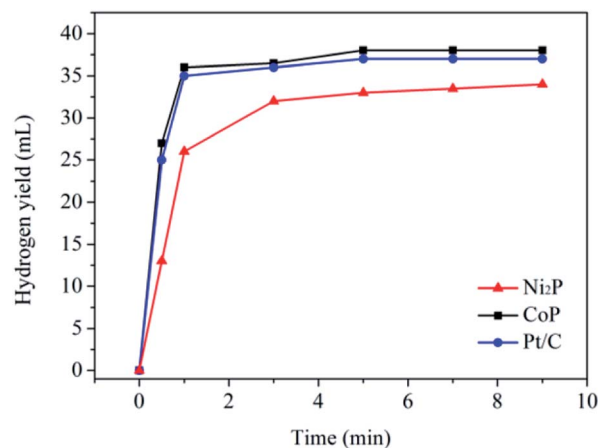


Fig. 2 Hydrogen yield as a function of reaction time in the presence of the as-prepared catalysts.



that the catalytic activity the CoP sample can rival that of the commercial Pt/C catalyst. These results may highlight the promising application of earth-abundant transition metal phosphides in the highly efficient hydrogen evolution from water electrolysis.

### 2.3. Stability test

It is widely regarded that the stability of a catalyst is a very important factor for its practical applications. Therefore, the stability of the CoP sample for the hydrogen evolution from water electrolysis has been carried out. For the sake of simplicity, the CoP sample is directly added into the one compartment of the two-compartment H-cell containing 1e-reduced silicotungstic acid ( $\text{H}_5\text{SiW}_{12}\text{O}_{40}$ ). After a potential of 8.3 V is set between the working electrodes, the evolving  $\text{H}_2$  and  $\text{O}_2$  gas are captured in two 100 mL measuring cylinder filled with water, respectively. As shown in Fig. 3 and S4,<sup>†</sup>  $\text{H}_2$  and  $\text{O}_2$  evolutions proceed continuously in a molar ratio of  $\text{H}_2/\text{O}_2$  of 2.1 ( $\sim 49 \text{ mL h}^{-1}$  for  $\text{H}_2$  and  $\sim 23 \text{ mL h}^{-1}$  for  $\text{O}_2$ ), almost equal to the theoretical value of 2 for overall water splitting. Moreover, it can be seen that the production rates of hydrogen and oxygen do not obviously decrease after 12 h with a faradaic efficiency of nearly 100%. The low rate of the  $\text{H}_2$  evolution for the initial phase can be attributed to the introduction of air during the addition of the CoP sample. The crystal structure, morphology and surface chemical compositions of the as-prepared sample before and

after the reaction have also been studied by XRD, TEM and XPS (see Fig. S5–S7<sup>†</sup>). There are no obvious changes in the crystal structure, morphology and surface chemical compositions after the reaction for the CoP sample. Furthermore, the  $\text{Co}^{2+}$  concentration measured by inductively coupled plasma-atomic emission spectrometry (ICP-AES) is only 40 ppm after the reaction. The  $\text{Co}^{2+}$  ions in the present system may come from the cobalt phosphate formed on the surface of the CoP particles due to the exposure of the sample to air.<sup>10,12,13,17,22,23</sup> These results suggest that the CoP catalyst exhibits good stability in the present system.

### 2.4. Roles of ECPB and catalyst

Production rate of  $\text{H}_2$  in the two-electrode system have been investigated under different conditions (see Table 1). It is found that the production of  $\text{H}_2$  is negligible in the present of  $\text{H}_4\text{SiW}_{12}\text{O}_{40}$ . However, after reducing  $\text{H}_4\text{SiW}_{12}\text{O}_{40}$  to  $\text{H}_5\text{SiW}_{12}\text{O}_{40}$  and adding the CoP sample,  $\text{H}_2$  can be detected with a rate of  $48 \text{ mL h}^{-1}$ . Control experiments exhibit only a half of  $\text{H}_2$  is obtained without the ECPB, and the adding of the catalyst can't improve the production of  $\text{H}_2$  (see entry 3 and 4 in Table 1). These results confirm  $\text{H}_4\text{SiW}_{12}\text{O}_{40}$  and CoP are the efficient ECPB and catalyst, respectively. Furthermore,  $\text{H}_2$  evolution from such a system is no longer directly coupled to the rate of water oxidation, and the activity of the catalyst don't limit by the electrode's work surface.

### 2.5. Electrochemical properties of transition metal phosphides

Electrochemical measurements have been conducted in a typical three-electrode cell to get further insight into the hydrogen evolution reaction process of transition metal phosphides. Fig. 4a shows the polarization curves of the as-prepared samples loaded on glassy carbon electrodes, which are measured in the  $\text{N}_2$ -saturated 0.5 M  $\text{H}_2\text{SO}_4$  with a scan rate of  $100 \text{ mV s}^{-1}$ . The Pt/C electrode prepared with a similar content has also been examined for comparison. The overpotential required for different electrocatalysts to produce a cathodic current density of  $10 \text{ mA cm}^{-2}$  ( $\eta_{10}$ ) is usually compared in the literature to assess their catalytic activities, and the lower overpotentials are helpful for the hydrogen evolution from water electrolysis.<sup>11–14</sup> The  $\eta_{10}$  of the CoP and  $\text{Ni}_2\text{P}$  sample shown in Fig. 4a are 65 and 150 mV, respectively. Although the  $\eta_{10}$  of the CoP sample is higher than that of the Pt/C sample ( $\eta_{10}$

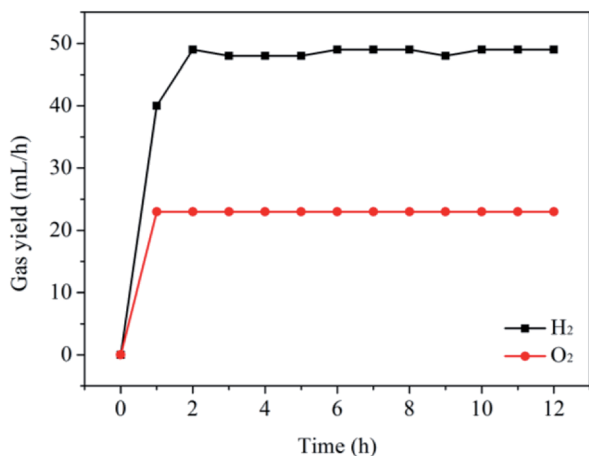


Fig. 3 Production rates of hydrogen and oxygen during the durability experiment for the CoP sample.

Table 1 Production rate of  $\text{H}_2$  in the two-electrode system under different conditions<sup>a</sup>

Entry	Components <sup>b</sup>	Current (mA)	Production rate of $\text{H}_2$ ( $\text{mL h}^{-1}$ )
1	$\text{H}_4\text{SiW}_{12}\text{O}_{40}$	100	No detected
2	$\text{H}_4\text{SiW}_{12}\text{O}_{40}$ + CoP	100	48
3	$\text{H}_3\text{PO}_4$	50	26
4	$\text{H}_3\text{PO}_4$ + CoP	50	28

<sup>a</sup> Conditions: a two-compartment H-cell separated by a piece of 0.18 mm-thick Nafion N-117 membrane; platinum mesh working electrode ( $1 \times 1 \text{ cm}^2$ ), 0.9 mL of  $\text{H}_3\text{PO}_4$  and 60 mL of  $\text{H}_2\text{O}$  in the left compartment; carbon felt working electrode ( $3 \times 2 \text{ cm}^2$ ) and various components in the right compartment; Ar atmosphere; reaction time, 4 h. <sup>b</sup> Dosages:  $\text{H}_4\text{SiW}_{12}\text{O}_{40}$ , 10 mmol;  $\text{H}_3\text{PO}_4$ , 0.9 mL (13.3 mmol); CoP, 50 mg.



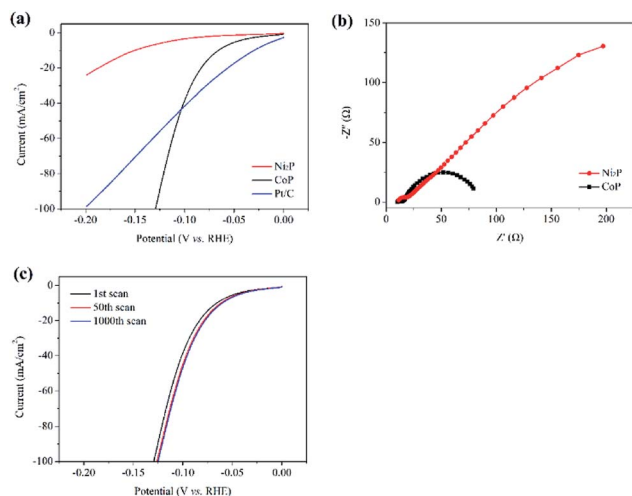


Fig. 4 (a) Polarization curves, (b) Nyquist plots for different samples and (c) polarization curves for the CoP sample before and after 1000 cycles.

= 28 mV), the CoP sample shows a high cathodic current in the range of  $-0.1$  to  $-0.2$  V vs. RHE. It only needs  $\sim 130$  mV to afford a current density of  $100 \text{ mA cm}^{-2}$ , which is lower than that of the Pt/C sample ( $\eta_{100} > 200$  mV). This may explain the efficient catalytic activity of the CoP sample at a low redox potential ( $E(\text{H}_6\text{SiW}_{12}\text{O}_{40}/\text{H}_5\text{SiW}_{12}\text{O}_{40}) = -0.49$  V vs. RHE), which can rival that of the commercial Pt/C catalyst.

Furthermore, the charge transfer rate has been studied by electrochemical impedance spectroscopy (EIS) and the expected semicircular Nyquist plots for the transition metal phosphides (Fig. 4b), with a significantly decreased diameter for the CoP sample, have been obtained. It is generally accepted that a small diameter means a low impedance and gives rise to fast charge transfer kinetics.<sup>18,24</sup> These results imply that the CoP sample indeed is an efficient catalyst for the  $\text{H}_2$  evolution from water electrolysis in this work. The polarization curves that are measured for the CoP sample before and after 50 cyclic voltammetry cycles at a scan rate of  $100 \text{ mV s}^{-1}$  are shown in Fig. 4c. At the end of the cycling experiment, a significant improvement of current density has occurred, which can be attributed to the elimination of the oxidation layer on the CoP sample. While increasing the cycling times to 1000, the curve exhibits negligible loss in current density compared to that of the 50th scan. This further suggests the excellent stability of the CoP sample for the  $\text{H}_2$  evolution from water electrolysis in acid condition.

### 3. Conclusions

Nanocrystalline transition metal phosphides (CoP and  $\text{Ni}_2\text{P}$ ) with a diameter of 10–30 nm were successfully synthesized by a simple calcination method *via* using transition metal hydroxides and  $\text{NaH}_2\text{PO}_2$  as raw materials. They were used as the catalysts for the hydrogen evolution from water electrolysis with silicotungstic acid as an ECPB, whereby hydrogen and oxygen could be produced separately. It was found that the CoP sample showed higher catalytic activity ( $32 \text{ mmol min}^{-1} \text{ g}^{-1}$ ) as

compared to the  $\text{Ni}_2\text{P}$  sample, and its catalytic activity could rival that of the commercial Pt/C catalyst. The stability tests demonstrated that the production rate of hydrogen did not obviously decrease after 12 h. And the analysis results of the XRD, TEM, XPS and ICP showed that the crystal structure, morphology and surface chemical compositions of the as-prepared CoP sample had no obvious change. These results revealed that it exhibited good stability in the present system. The electrochemical results indicated that CoP had high cathodic current and small charge transfer resistance, which further suggested it was indeed a noble metal-free catalyst for efficient hydrogen evolution. Our results may allow us to highlight the promising application of transition metal phosphides in the highly efficient hydrogen evolution from water electrolysis.

## 4. Experimental section

### 4.1. Preparation

5 mmol of transition metal chlorides ( $\text{NiCl}_2 \cdot 6\text{H}_2\text{O}$  or  $\text{CoCl}_2 \cdot 6\text{H}_2\text{O}$ , Sinopharm Chemical Reagent Co. (SCRC)) was dissolved in 40 mL of deionized water. Then, 20 mL of 1 M NaOH aqueous solution (SCRC) was dropped under stirring (200 rpm). Transition metal hydroxides were collected and were washed with deionized water two times after 30 min of stirring, and then were dried in air at  $60^\circ \text{C}$  overnight.

50 mg of the obtained hydroxides and 250 mg of  $\text{NaH}_2\text{PO}_2$  (Aladdin Co.) were mixed well in an agate mortar. These mixtures were heated to  $300^\circ \text{C}$  with a ramping rate of  $2^\circ \text{C min}^{-1}$ , and kept at  $300^\circ \text{C}$  for 60 min. This process was carried out in Ar flow ( $50 \text{ mL min}^{-1}$ ) all through. After naturally cooled to room temperature under Ar atmosphere, the as-prepared phosphides were soaked in 1 M HCl aqueous solution (SCRC) for 36 h to remove any unstable species. Then, the transition metal phosphides were washed with deionized water and absolute ethyl alcohol three times, and dried in vacuum at  $60^\circ \text{C}$  for 1 h.

### 4.2. Characterization

XRD patterns were collected on a Miniflex II X-ray diffractometer (Rigaku Co.) with Cu  $K\alpha$  radiation. The data were recorded in a  $2\theta$  range of  $25\text{--}70^\circ$ . TEM images were obtained using a FEI Tecnai 20 transmission electron microscope at an accelerating voltage of 200 kV. Samples for TEM imaging were prepared by placing a drop of the sample ethanol suspension on a copper grid coated with carbon film and dried in the atmosphere. SEM image was obtained on a JEOL JSM-7500F field emission scanning electron microscope at an accelerating voltage of 5 kV. XPS measurement was carried out by using a Escalab 250Xi X-ray photoelectron spectrometer (Thermo Fisher scientific Co.) equipped with Al  $K\alpha$  X-ray source. The binding energy calibration of the spectra was referred to C 1s peak located at 284.6 eV for the analysis. Electrochemical experiments were taken on a CHI660e workstation (CH Instruments, Inc.). The electrochemical measurements were performed in a typical three electrode cell, using Pt wire and saturated Ag/AgCl electrode as counter electrode and reference



electrode, respectively. Glassy carbon electrode (3 mm in diameter) coated with the as-prepared samples were used as the working electrodes. In the fabrication of the working electrode, the catalyst ink was prepared by dispersing 5.0 mg of the catalyst into a mixed solvent containing 0.98 mL of deionized water and 20  $\mu\text{L}$  of 5 wt% Nafion solution (D521, Alfa Aesar Co.), and then the mixture was sonicated for 30 min to form a homogeneous ink. After that, 5  $\mu\text{L}$  of the catalyst ink was loaded onto glassy carbon electrode and dried at room temperature. The electrolyte was a 0.5 M  $\text{H}_2\text{SO}_4$  aqueous solution (SCRC) and was purged with nitrogen gas for 30 min prior to the measurements. In all measurements, the saturated Ag/AgCl reference electrode was calibrated with respect to reversible hydrogen electrode (RHE). In 0.5 M  $\text{H}_2\text{SO}_4$ ,  $E(\text{RHE}) = E(\text{Ag}/\text{AgCl}) + 0.198 \text{ V}$ .

### 4.3. $\text{H}_2$ evolution from water electrolysis

The electrochemical reduction of silicotungstic acid ( $\text{H}_4\text{SiW}_{12}\text{O}_{40}$ ) was carried out by a modified method:<sup>8,9</sup> 10 mmol of  $\text{H}_4\text{SiW}_{12}\text{O}_{40}$  (SCRC) and 60 mL of deionized water were added into one compartment of a two-compartment H-cell, and 0.9 mL  $\text{H}_3\text{PO}_4$  (13.3 mmol, SCRC) and 60 mL of deionized water were placed into the other compartment. The compartments of the H-cells were separated by a piece of 0.18 mm-thick Nafion N-117 membrane (Alfa Aesar Co.). All electrochemical experiments were performed by using a classical two-electrode configuration (TPR6010S regulated power supply, ATTEN instruments Co.). The  $\text{H}_4\text{SiW}_{12}\text{O}_{40}$  compartment was equipped with a large area carbon felt working electrode ( $3 \times 2 \text{ cm}^2$ ), and the other compartment of the cell was equipped with a large area platinum mesh working electrode ( $1 \times 1 \text{ cm}^2$ ). To fully reduce  $\text{H}_4\text{SiW}_{12}\text{O}_{40}$  to  $\text{H}_6\text{SiW}_{12}\text{O}_{40}$  by two electrons, a potential of 8.3 V was set between the working electrodes and 1931 C of charge was passed at this potential (working current: 0.1 A, working time: 5.4 h). Prior to the experiment, the  $\text{H}_4\text{SiW}_{12}\text{O}_{40}$  solution was bubbled with argon (60 mL  $\text{min}^{-1}$ ) for 60 min, stirred vigorously and kept under an argon atmosphere throughout the experiment.

50 mg of the as-prepared sample was dispersed in 5 mL of deionized water in a 50 mL three-necked round-bottomed flask. After thoroughly flushed with argon, the freshly produced  $\text{H}_6\text{SiW}_{12}\text{O}_{40}$  (20 mL) was added to the sample aqueous dispersion under Ar atmosphere and stirred vigorously *via* a pressure-equalizing dropping funnel. The evolving  $\text{H}_2$  gas was captured in a 100 mL measuring cylinder filled with water. Furthermore, the evolving  $\text{H}_2$  gas was identified by gas chromatography (GC2014C, Shimadzu Co., TCD, molecular sieve 5A column, argon carrier).

## Conflicts of interest

There are no conflicts to declare.

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