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# Facile synthesis of potassium copper ferrocyanide composite particles for selective cesium removal from wastewater in the batch and continuous processes

Youli Zong,<sup>b</sup> Yongde Zhang,<sup>a</sup>  Xiaoyan Lin,<sup>ab</sup> Dong Ye,<sup>b</sup> Dan Qiao<sup>b</sup> and Shuangneng Zeng<sup>b</sup>

A composite potassium copper ferrocyanide particle adsorbent (CMC–KCuFC) was fabricated in this study, based on the use of a carboxymethyl cellulose sodium (CMC) biopolymer cross-linked with Cu<sup>2+</sup> via a syringe pump device, serving as an efficient biosorbent for cesium (Cs) ion removal and adsorption from wastewater, and was verified by SEM, EDX, FT-IR, TGA and XRD. Influencing factors in the adsorption of cesium were systematically investigated, including the pH of the solution, contact time, initial concentration, temperature and competing ions. The results demonstrated that use of the CMC–KCuFC adsorbent was feasible under a wide range of pH values (5–10). The cesium adsorption process was described by the Freundlich isotherm model. Meanwhile, the adsorption equilibrium time was reached within 600 min and the kinetic study showed it to be well fitted by the pseudo-second-order kinetic model. Moreover, all materials involved in the CMC–KCuFC adsorbent were biosafe and biodegradable. CMC–KCuFC is expected to be a potential adsorbent for continuous removal of cesium from wastewater.

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## 1. Introduction

In the recent years, there have been growing concerns regarding the contamination caused by radioactive waste. The treatment of radionuclide wastewater is in urgent need, especially after the Fukushima Daiichi nuclear disaster in 2011. Of all the radionuclides, 137-cesium (<sup>137</sup>Cs) has attracted great attention due to its long half-life ( $T_{1/2} = 30.17$  years), high energy gamma ray emission and high solubility in water,<sup>1–3</sup> which can cause adverse effects on the environment and human health. A weak Lewis acid, the Cs<sup>+</sup> ion, exhibits a low tendency to form complexes with ligands. Meanwhile, because of its chemical similarity to potassium, <sup>137</sup>Cs can be easily incorporated into terrestrial and living organisms where it is deposited in the soft tissues, leading to cancer.<sup>4,5</sup> Hence, development of an efficient and economical removal method is principal for the removal of cesium from wastewater in view of the environmental risks.

To date, various methods have been proposed for removal of radiocesium from wastewater, the most main used are solvent extraction,<sup>6,7</sup> chemical precipitation<sup>8</sup> and adsorption method.<sup>9</sup> Among these methods, adsorption has been proved to be an

excellent way to treat wastewater, offering significant advantages, like the low-cost, availability, profitability, easy operation, and efficiency.<sup>10</sup> A variety of <sup>137</sup>Cs adsorbent materials, including clay minerals, metal oxides, zirconium phosphate and silicotitanates are all previously reported for removal of cesium,<sup>11–15</sup> whereas the limitation of the low Cs<sup>+</sup> selectivity or too expensive for large-scale application in environmental cleanup. Accordingly, new adsorption materials are necessary to be researched.

Transition metal (Cu, Fe, Ni, Zn and Co) hexacyanoferrates (MCFs) are considered to be one of the inorganic adsorbents for selective recovery of cesium from wastewater. Among them, potassium copper hexacyanoferrate (KCuFC) is often chosen as the agent in practical application. Due to it is available in powdery and granular form compared to other metal hexacyanoferrates.<sup>16</sup> Moreover, its radiation stability, high selectivity, low cost and excellent ion exchange performance in a broad range of pH make its feasible for large-scale application.<sup>17,18</sup> Nevertheless, direct use of KCuFC as adsorbent has been hampered by its fine powder morphology, and it is unsuitable for continuous column stuffing and difficult to remove from solutions.<sup>19,20</sup> To solve this problem, the immobilization of KCuFC particles into polymers is a key technology to apply these particles for the large-scale applications. An organic polymer, biopolymer carboxymethyl cellulose (CMC) is a desirable candidate for immobilizing agent, due to its unique

<sup>a</sup>Department of Materials Science and Engineering, Southwest University of Science and Technology, Mianyang, Sichuan 621010, China. E-mail: zhangyongde1969@126.com

<sup>b</sup>Engineering Research Center of Biomass Materials, Ministry of Education, Mianyang, Sichuan 621010, China



characteristics such as solubility, non-toxicity and biocompatibility. Furthermore, in the presence of  $\text{Cu}^{2+}$ ,  $\text{Fe}^{3+}$ ,  $\text{La}^{3+}$  and  $\text{Al}^{3+}$  etc.<sup>21</sup> CMC can form stable ionotropic gels. Among them,  $\text{Cu}^{2+}$  can be used as an ecofriendly and nontoxic crosslinking agent for CMC. Additionally, it is one of the raw materials for the synthesis of the KCuFC and does not produce secondary pollution after adsorption. The chemical structure of CMC is shown in Fig. 1.

This work synthesized a novel adsorbent of CMC-KCuFC particles by using copper chloride cross-linked carboxymethyl cellulose sodium (CMC) biopolymer as the immobilized matrix, and built particles within the polymer through a syringe pump for recovering cesium from wastewater. The composite particle was prepared using only eco-friendly materials at room temperature. FT-IR, XRD and SEM were utilized to characterize the extraction mechanism of adsorbent. In addition, to evaluate the adsorption capacity of cesium from aqueous solution in detail under various experimental conditions, isotherm and kinetic models were investigated to understand the adsorption process.

## 2. Materials and methods

### 2.1. Reagents

Sodium carboxymethyl cellulose (CMC, 1000–1400 mPa s, USP grade) was purchased from Aladdin Chemistry Co. Ltd. (Shanghai, China). Copper(II) chloride dihydrate ( $\text{CuCl}_2 \cdot 2\text{H}_2\text{O}$ ), potassium hexacyanoferrate(II) trihydrate ( $\text{K}_4[\text{Fe}(\text{CN})_6] \cdot 3\text{H}_2\text{O}$ ), cesium chloride (CsCl), NaOH and HCl were purchased from Chengdu Kelong Chemicals Company. Stock solution of 20 mg  $\text{L}^{-1}$  cesium ion aqueous solution was prepared by dissolving 0.0253 g CsCl in 1000 mL deionized water. Besides, all reagents in experiment were of analytical reagent grade and used without further purification.

### 2.2. Preparation of CMC-KCuFC particles and CMC-Cu particles

2 g of CMC was dissolved in 100 mL of 2.5% (w/v)  $\text{K}_4[\text{Fe}(\text{CN})_6]$  solution under constant agitating for 4 h at room temperature, then ultrasonicated for several minutes to obtain a homogeneous solution. The mix solution was added drop-wise with continuous stirring to 100 mL of 2% (w/v)  $\text{CuCl}_2$  solution, using a syringe pump (Model: LSP02-1B) at the speed of 1 mL  $\text{min}^{-1}$ , and then the coagulated particles (CMC-KCuFC) were stirred

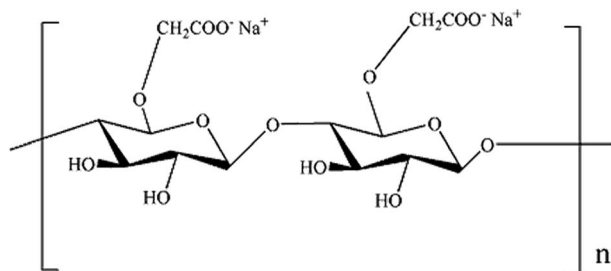


Fig. 1 Chemical structure of CMC.

continuously for 12 h. After that, the CMC-KCuFC particles were collected by rinsing several times with deionized water until removing the residual  $\text{Cu}(\text{II})$  ions. Finally, the CMC-KCuFC particles were dried in oven at 50 °C for use in further studies. The preparation process schematic diagram was displayed in Fig. 2.

The following CMC-Cu particles were prepared by a similar method to that of preparation of CMC-KCuFC particles. Specifically, 2 g of CMC was dissolved in 100 mL of distilled water with vigorous magnetic stirring for 4 h at room temperature, and then ultrasonicated for several minutes to obtain a homogeneous solution. The CMC solution was dropped into 100 mL 2% (w/v)  $\text{CuCl}_2$  solution, using a syringe pump (Model: LSP02-1B) at the speed of 1 mL  $\text{min}^{-1}$ , and then the coagulated particles (CMC-Cu) were stirred continuously for 12 h. After that, the CMC-Cu particles were washed with deionized water to residual  $\text{Cu}(\text{II})$  ions. Finally, the CMC-Cu particles were dried 50 °C in an oven.

### 2.3. Batch adsorption experiment for cesium

Inactive cesium was used to research the adsorption behaviors. In brief, all adsorption experiments were carried out on thermostatic shaker (HZQ-2) with a constant speed of 150 rpm by using batch technique. Initial pH, contact time, initial concentration and temperatures and competing ions on adsorption of cesium were evaluated in 50 mL of test solutions with 0.01 g (dry weight) CMC-KCuFC particles. Besides, 0.05 mol  $\text{L}^{-1}$  HCl and 0.05 mol  $\text{L}^{-1}$  NaOH were used to adjust the pH value of the solution. The concentrations of  $\text{Cs}^+$  remaining in the solution were quantified with a Hitachi Z-2000 Zeeman atomic absorption spectrophotometer with air-acetylene flame (AAS) before and after adsorption. Each sample was designed in triplicate, and the average values were used to evaluate the adsorbent capabilities. The adsorption capacity at equilibrium ( $q_e$ ) and elimination efficiency ( $E\%$ ) of the cesium ions can be evaluated using eqn (1) and (2), respectively.<sup>19,22</sup>

$$q_e = (C_0 - C_e)V/m \quad (1)$$

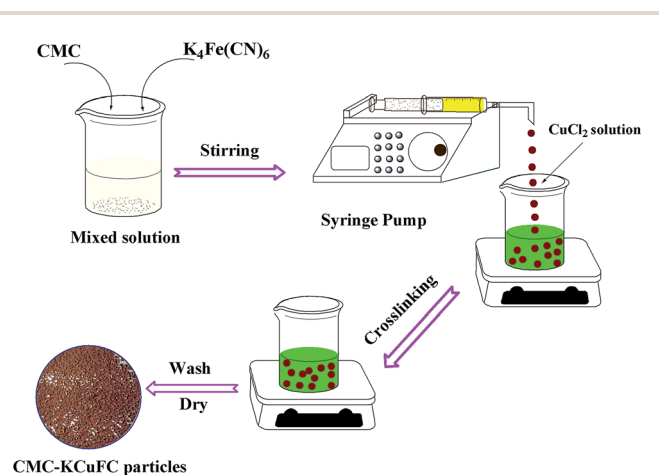


Fig. 2 Schematic presentation of the preparation process of CMC-KCuFC.



$$E(\%) = (C_0 - C_e)/C_0 \times 100 \quad (2)$$

where  $C_0$  ( $\text{mg L}^{-1}$ ) and  $C_e$  ( $\text{mg L}^{-1}$ ) are the initial cesium concentration and cesium concentration at equilibrium in the aqueous solution, respectively.  $V$  ( $\text{mL}$ ) is the volume of cesium solution and  $m$  ( $\text{g}$ ) is the dry weight of the adsorbent.

#### 2.4. Fixed bed column study

In order to study the dynamic behavior of the continuous adsorption of  $\text{Cs}^+$  ions from aqueous solution by CMC-KCuFC particles, fixed bed column adsorption experiments were investigated. The column experiments were carried out in a glass column with an inner diameter (ID = 1.5 cm) and length ( $L = 35$  cm). Column was filled with adsorbent between two supporting layers of glass wool. CMC-KCuFC particles were added from the top of the column. The cesium ions solution is pumped upwards the adsorber from a liquid holding tank, and the inlet flow rate was controlled by using a peristaltic pump. Effluent samples are collected in regular time intervals and stored for analysis, and the influent and effluent cesium concentrations were measured by the AAS. The schematic diagram of the fixed-bed adsorption system was shown in Fig. 3.

#### 2.5. Characterization of the CMC-KCuFC particles

The surface morphology of the adsorbent was characterized by TM3000 scanning electron microscope (SEM). The specific surface area and pore volume of the adsorbent was determined by surface area analyzer (BET, JW-BK112). X-ray spectroscopy (EDX, Ultra 55, Carl Zeiss, Germany) was employed to detect the element composition of the adsorbent surface coated with gold. The surface functional groups of the adsorbent was demonstrated by the Fourier transform infrared spectra (FT-IR, Nicolet-5700, PerkinElmer Instruments Corporation) and adopting the KBr pellet technique, over the spectral range of  $4000\text{--}400$   $\text{cm}^{-1}$ . XRD patterns of adsorbent crystalline structure were analyzed by X'Pert PRO (PANalytical B.V., 40 kV, 40 mA) equipped with a Cu K $\alpha$  source at  $2\theta$  range from  $10^\circ$  to  $80^\circ$ . The thermal stabilities of adsorbent were measured using thermogravimetric analysis (TGA, Q600, USA), the samples were

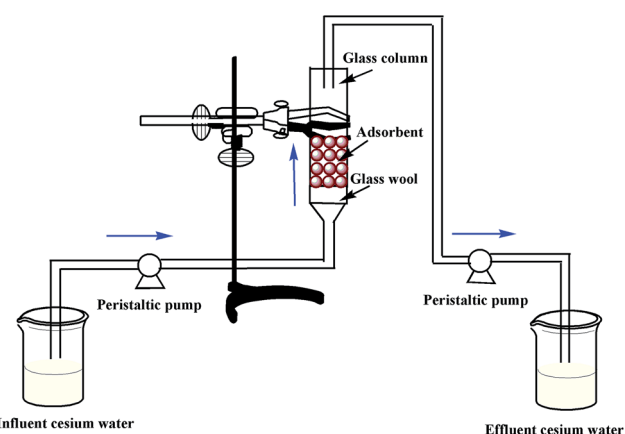


Fig. 3 Schematic diagram of the fixed-bed adsorption experiment.

gradually heated at a rate of  $20$   $^\circ\text{C min}^{-1}$  from  $20$  to  $800$   $^\circ\text{C}$  under the protection of  $\text{N}_2$  with a flow rate of  $20$   $\text{mL min}^{-1}$ .

## 3. Results and discussion

### 3.1. Batch experiments

**3.1.1. Effect of CMC-KCuFC particles size.** In order to investigate the effect of CMC-KCuFC particles size on adsorption of cesium, CMC-KCuFC particles were controlled by different size of syringe needle, the results are shown in Fig. 4, it can be seen that the adsorption capacity decreased slightly with the increase in particles size from 1.5 to 2.0 mm, an effect that might be attributed to the amount of active sites on the adsorbent surface during the adsorption operation process.

**3.1.2. Effect of pH.** The pH of solution played a vital role to affect the chemical reactions and adsorption behavior, especially for ion-exchange process.<sup>23,24</sup> To choose optimal pH for the removal of cesium, the effect of pH on CMC-KCuFC particle was studied in the range of 2–10. The results were shown in Fig. 5. It can be seen that the adsorption capacity increased apparently with increasing pH from 2 to 5, while the adsorption capacity remained steady up when the pH was in the range of 5 to 10. This occurred because that at low pH, ion exchange sites were mainly protonated, making them less available for cation.<sup>25</sup> However, when the pH increased, the sites became available for cation in ion-exchange processes, leading to higher adsorption. Even though, the adsorption capacity of cesium ions was feasible across a wide range of pH values, if the pH was at least 5 or above.<sup>26</sup>

**3.1.3. Effect of contact time and kinetics of cesium adsorption study.** Effect of contact time on the adsorption capacity and elimination efficiency of CMC-Cu and CMC-KCuFC particles were given in Fig. 6, respectively. It was shown that over 61.67% of Cs was removed after 600 min with CMC-KCuFC, while only 5.56% was removed with CMC-Cu and  $q_e$  value was  $7.85$   $\text{mg g}^{-1}$  at relatively low cesium concentration,

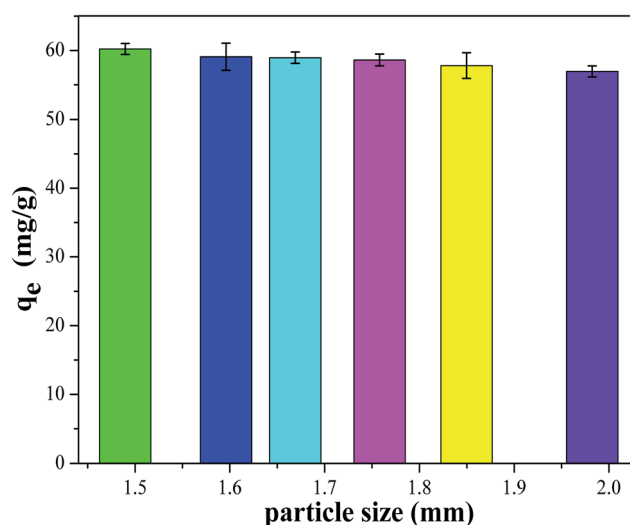


Fig. 4 Effect of particle size of CMC-KCuFC particles on cesium adsorption.



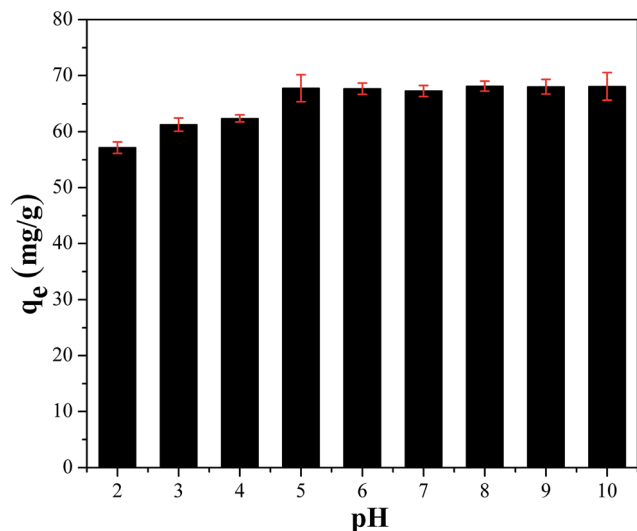


Fig. 5 Effect of pH on adsorption capacity on the remove of 50 mL 20 mg L<sup>-1</sup> Cs<sup>+</sup> for 24 h at 298.15 K.

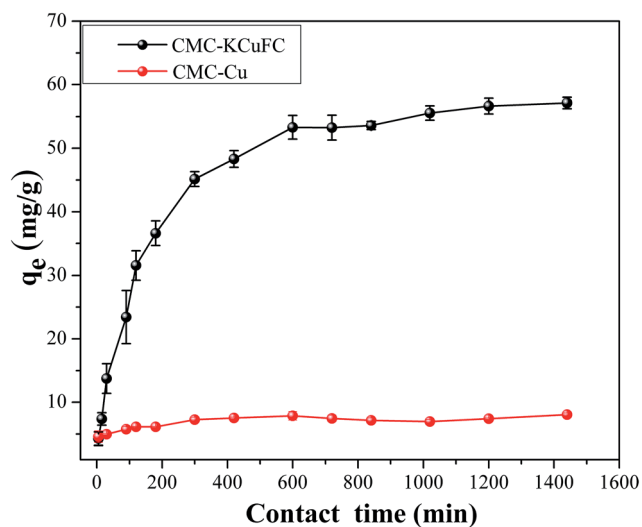


Fig. 6 Effect of contact time on the remove of 50 mL 20 mg L<sup>-1</sup> Cs<sup>+</sup> for 24 h at 298.15 K.

which was specially revealed that the adsorbance of CMC-Cu for cesium in wastewater was insignificant. Therefore, the adsorption of CMC-KCuFC for cesium should be attributed to the existence of KCuFC crystals.

The kinetic studies were used to evaluate the mechanism of interaction between the adsorbent and the adsorbate. For this purpose, the kinetics was analyzed using pseudo-first-order and pseudo-second-order kinetic model. The equations of both linear models can be expressed as follows:<sup>27,28</sup>

$$\log(q_e - q_t) = \log q_e - k_1 t / 2.303 \quad (3)$$

$$t/q_t = t/q_e + 1/k_2 q_e^2 \quad (4)$$

where  $q_e$  (mg g<sup>-1</sup>) and  $q_t$  (mg g<sup>-1</sup>) are the adsorption capacity at equilibrium and at any time  $t$ , respectively.  $t$  (min) is the contact time.  $k_1$  (min<sup>-1</sup>) is the pseudo-first-order rate constant, while  $k_2$  (g (mg<sup>-1</sup> min<sup>-1</sup>)) is the pseudo-second-order rate constant for cesium adsorption process.  $k_1$  and  $k_2$  can be obtained from the plot of experimental data.

The linear fitting of pseudo-first-order and pseudo-second-order model were shown in Fig. 7. The calculated parameters of  $q_e$ ,  $k_1$  and  $k_2$  were tabulated in Table 1, respectively. Compared with the two models, the correlation coefficient ( $R^2 = 0.999$ ) of pseudo-second-order model was higher than pseudo-first-order model. Besides, the calculated equilibrium adsorption capacity  $q_e$  (60.827 mg g<sup>-1</sup>) in pseudo-second-order kinetics model was closer to the experimental data (57.133 mg g<sup>-1</sup>). It was demonstrated that the adsorption of cesium obeyed the pseudo-second-order kinetic model over the whole adsorption process, implying that the main rate limiting step was chemical adsorption involved valence forces through sharing or exchange of electrons between the adsorbent and adsorbate.<sup>23,28</sup> The maximum adsorption capacity was 60.827 mg g<sup>-1</sup>.

**3.1.4. Effect of initial cesium concentration and adsorption isotherm model.** The effect of different initial cesium concentrations varying from 10 to 100 mg L<sup>-1</sup> at different temperatures were showed in Fig. 8. It was found that all the adsorption capacity increased rapidly at the initial concentration of 10–40 mg L<sup>-1</sup> and increased slowly within the concentration of 40–100 mg L<sup>-1</sup> in the range of temperature from 288.15 to 328.15 K. This may be explained that the increasing initial cesium solution concentration of cesium provided a necessary driving force to overcome all the mass transfer resistance to the Cs<sup>+</sup> between the aqueous and solid phases, and then a lower number of coordination sites were available when the adsorption capacity tended to saturate.<sup>29</sup>

Equilibrium isotherms provided information about the adsorption mechanism, surface properties and the affinity of the adsorbent. In this study, Langmuir and Freundlich models were utilized to describe the relationship between adsorbed cesium and its residual in aqueous solution at adsorption equilibrium. The equation of linear Langmuir model can be written as:<sup>30</sup>

$$C_e/q_e = 1/(K_L q_m) + C_e/q_m \quad (5)$$

While Freundlich isotherm explains multilayer adsorption on heterogeneous surfaces in nature.<sup>31</sup> The linear Freundlich model can be expressed as:

$$\ln q_e = \ln K_F + \frac{1}{n} \ln C_e \quad (6)$$

where  $q_e$  (mg g<sup>-1</sup>) is the adsorption capacity of cesium on the adsorbent at equilibrium,  $C_0$  (mg L<sup>-1</sup>) and  $C_e$  (mg L<sup>-1</sup>) are the initial cesium concentration and equilibrium cesium concentration, respectively.  $K_L$  (L mg<sup>-1</sup>) is the calculated Langmuir constant related to the energy of adsorption and  $q_m$  (mg g<sup>-1</sup>) is the monolayer adsorption capacity.  $K_F$  (mg g<sup>-1</sup>) is the



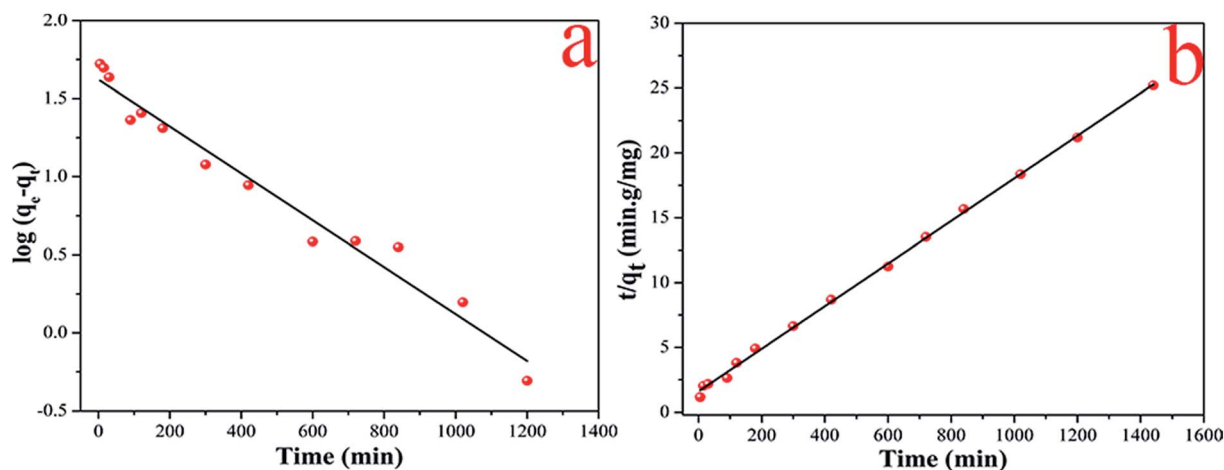


Fig. 7 The linear fitting of pseudo-first-order kinetic models (a) and pseudo-second-order kinetic models (b) of  $\text{Cs}^+$ .

Table 1 Parameters of linear pseudo-first-order kinetics and pseudo-second-order kinetics

Type	Pseudo-first-order model				Pseudo-second-order model		
	$q_{e(\text{exp})}$ ( $\text{mg g}^{-1}$ )	$q_e$ ( $\text{mg g}^{-1}$ )	$k_1$ ( $\text{min}^{-1}$ )	$R^2$	$q_e$ ( $\text{mg g}^{-1}$ )	$k_2$ ( $\text{g} (\text{mg}^{-1} \text{min}^{-1})$ )	$R^2$
Linear	57.133	41.941	$3.45 \times 10^{-3}$	0.970	60.827	$1.68 \times 10^{-4}$	0.999

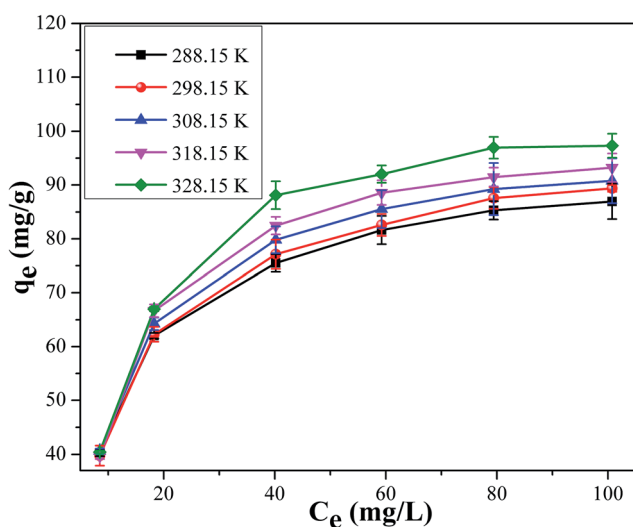


Fig. 8 Effect of initial concentration on adsorption capacity of 50 mL  $\text{Cs}^+$  for 24 h at 288.15–328.15 K.

Freundlich constant indicates the multilayer adsorption capacity and  $n$  is the intensity of adsorption.

The Langmuir and Freundlich values of  $q_m$ ,  $K_L$ ,  $n$  and  $K_F$  can be obtained from the slope and intercept of the plots (Fig. 9), and the results were listed in Table 2. As evidenced by the correction coefficient  $R^2$ , the Freundlich model presented more suitable than Langmuir model, indicating that the adsorption process belongs to multilayer adsorption with non-uniform

distribution of adsorption heat and affinities over the heterogeneous surface. Additionally, the obtained  $1/n$  values were between 0 and 1, indicating a highly favorable interaction in the whole adsorption process.

**3.1.5. Effect of temperatures and the evaluation of adsorption thermodynamics.** Effect of various temperatures on the adsorption of cesium onto CMC-KCuFC particle was investigated at different initial concentrations range from 10 to 100  $\text{mg L}^{-1}$ . As shown in Fig. 10, while increasing the temperature from 288.15 to 328.15 K the influence of temperature was not obvious at all the initial concentrations ranging from 10–100  $\text{mg L}^{-1}$ . Therefore, from the aspect of energy saving, the following experiments were all conducted at 298.15 K.

In order to evaluate the thermodynamic feasibility and under the nature of the adsorption process, three basic thermodynamic parameters ( $\Delta H^\circ$ ,  $\Delta S^\circ$  and  $\Delta G^\circ$ ) were calculated by the following.<sup>31,32</sup>

$$K_d = q_e / C_e \quad (7)$$

$$\ln K_d = \Delta S^\circ / R - \Delta H^\circ / RT \quad (8)$$

$$\Delta G^\circ = \Delta H^\circ - T\Delta S^\circ \quad (9)$$

where  $T$  (K) is the temperature.  $R$  ( $8.314 \text{ J} (\text{mol}^{-1} \text{K}^{-1})$ ) is the universal gas constant.  $K_d$  ( $\text{mL g}^{-1}$ ) is the distribution coefficient.  $\Delta H^\circ$  ( $\text{kJ mol}^{-1}$ ),  $\Delta S^\circ$  ( $\text{J} (\text{mol}^{-1} \text{K}^{-1})$ ),  $\Delta G^\circ$  ( $\text{kJ mol}^{-1}$ ) are in the enthalpy change, entropy change and Gibbs free energy for the adsorption process, respectively. The values of  $\Delta H^\circ$  and  $\Delta S^\circ$





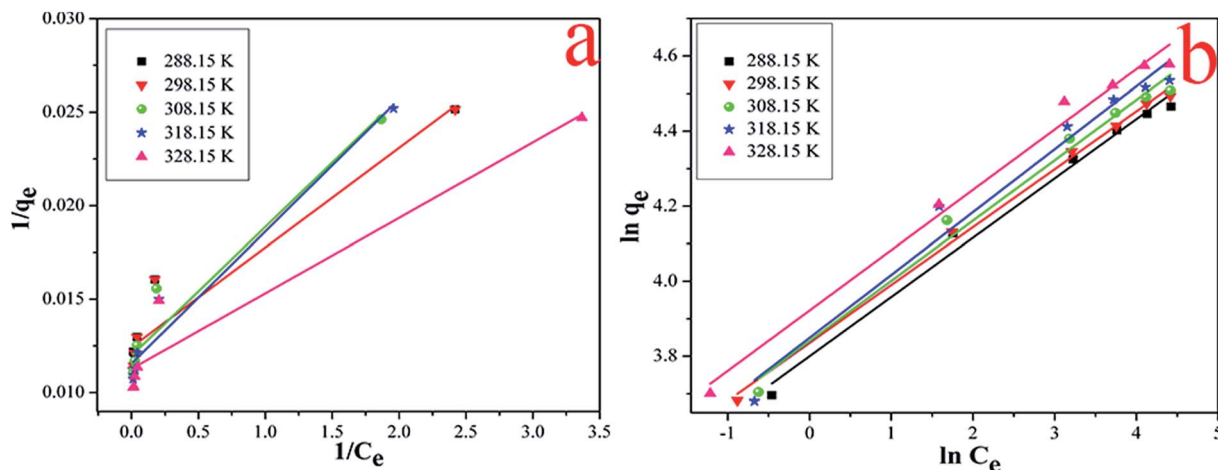


Fig. 9 The linear of Langmuir models (a) and Freundlich models (b) of  $\text{Cs}^+$ .

Table 2 The linear of Langmuir and Freundlich models

Type	$T$ (K)	Langmuir			Freundlich		
		$q_m$ ( $\text{mg g}^{-1}$ )	$K_L$ ( $\text{L mg}^{-1}$ )	$R^2$	$K_F$ ( $\text{mg g}^{-1}$ ) ( $\text{L mg}^{-1}$ ) $^{1/n}$	$n$	$R^2$
Linear	288.15	80.451	2.328	0.909	1.335	6.327	0.986
	298.15	80.451	2.328	0.909	1.344	6.483	0.995
	308.15	83.542	1.737	0.932	1.345	6.220	0.983
	318.15	86.580	1.634	0.955	1.348	5.965	0.966
	328.15	88.731	2.790	0.918	1.367	6.216	0.985

can be obtained from the slope and intercept of the Van't Hoff linear plots of  $\ln K_d$  versus  $1/T$ . The results were shown in Fig. 11. Meanwhile, the values of thermodynamic parameters for the adsorption of cesium at different temperatures were given in Table 3.

It can be found that all the  $\Delta G^0$  values were negative at the temperature range of 288.15 to 328.15 K, conforming that the

adsorption of cesium onto CMC-KCuFC particle was thermodynamically feasible and spontaneous in nature. For the adsorption of cesium the positive values of  $\Delta H^0$  indicated that the adsorption was endothermic. Moreover, the positive value of  $\Delta S^0$  was interpreted as the result of an increase in the randomness at the solid/liquid interface during the adsorption of cesium on the adsorbent.<sup>33</sup>

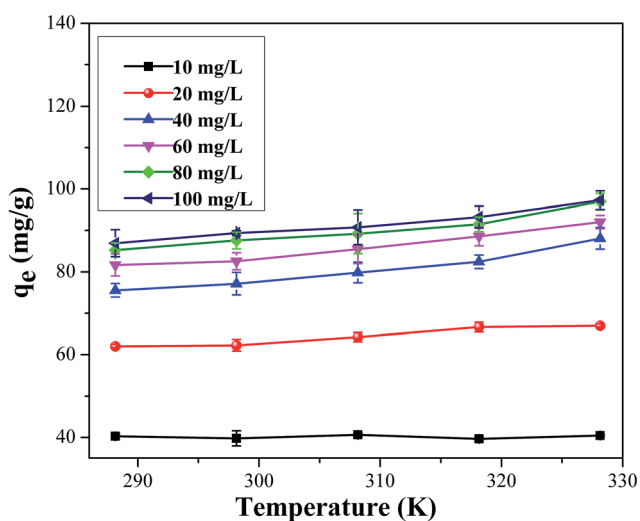


Fig. 10 Effect of temperature on the remove of 50 mL  $\text{Cs}^+$  for 24 h at 288.15–328.15 K.

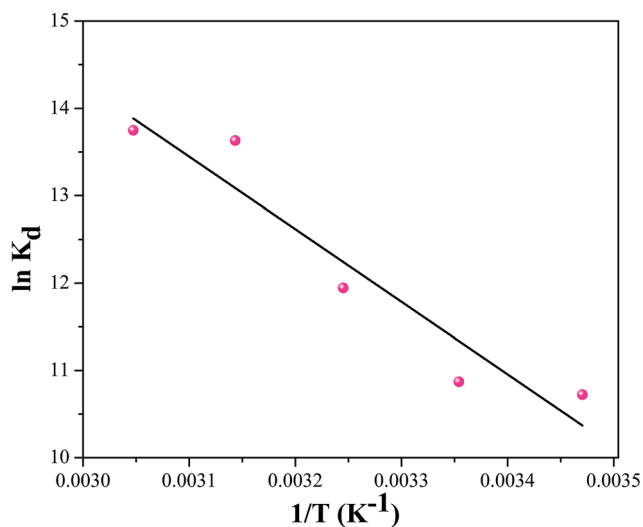


Fig. 11 The relationship between  $\ln K_d$  and  $1/T$  for  $\text{Cs}^+$  adsorption of CMC-KCuFC particles.



**Table 3** Thermodynamic parameters for the adsorption process of cesium on CMC–KCuFC

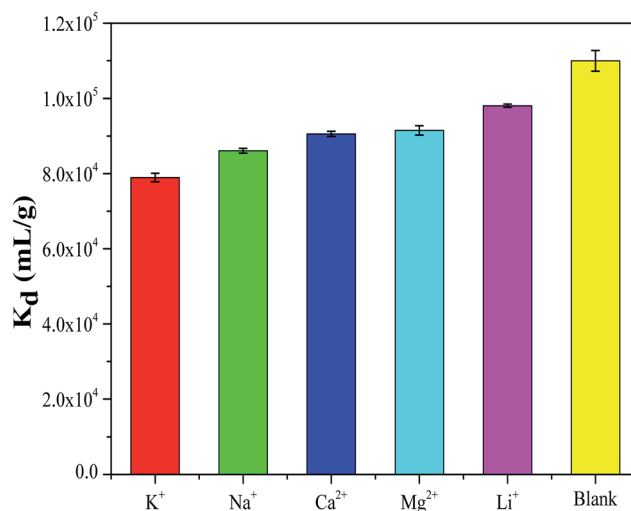
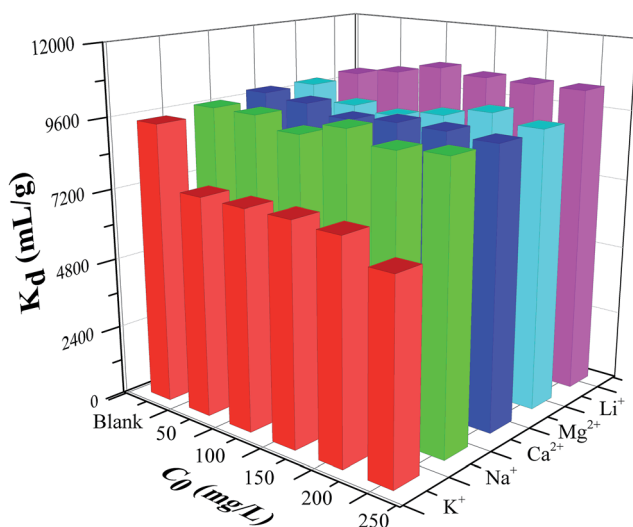
T (K)	ln $K_d$	$\Delta G^\circ$ (kJ mol <sup>-1</sup> )	$\Delta H^\circ$ (kJ mol <sup>-1</sup> )	$\Delta S^\circ$ (J (mol <sup>-1</sup> K <sup>-1</sup> ))
288.15	10.723	-24.843	69.087	325.974
298.15	10.871	-28.102		
308.15	11.945	-31.362		
318.15	13.633	-34.622		
328.15	13.750	-37.882		

**3.1.6. Effect of competing ions on the adsorption of cesium.** The influence of competing cations (*e.g.* Na<sup>+</sup>, K<sup>+</sup>, Li<sup>+</sup>, Ca<sup>2+</sup> and Mg<sup>2+</sup>) on the  $K_d$  value of cesium ion onto the CMC–KCuFC particle was investigated. These five cations were selected due to their natural abundance in wastewater. The effect was studied by keeping the concentration of Cs<sup>+</sup> constant (20 mg L<sup>-1</sup>), and varying the concentrations of Na<sup>+</sup>, K<sup>+</sup>, Li<sup>+</sup>, Ca<sup>2+</sup> and Mg<sup>2+</sup> under pH (5 ± 0.02) at 298.15 K. In the absence of added cations, the value of  $K_d$  was 9493.094 mL g<sup>-1</sup>. The results under competition with added cations were presented in Fig. 12. As the concentration added cations increase from 50 to 250 mg L<sup>-1</sup>, the  $K_d$  value was substantially increased in the following sequence: K<sup>+</sup> < Na<sup>+</sup> < Ca<sup>2+</sup> < Mg<sup>2+</sup> < Li<sup>+</sup>. The  $K_d$  value was lowest in the presence of K<sup>+</sup>, which could be attributed to the closer similarity in hydration radius between K<sup>+</sup> (3.30 Å) and Cs<sup>+</sup> (3.25 Å) than that of the other cations.<sup>34</sup> Meanwhile, the influences of Ca<sup>2+</sup> and Mg<sup>2+</sup> cations on the adsorption might be involved in other process or steps except ion exchange, such as nonspecific surface adsorption.<sup>35</sup>

In order to investigate effect of adsorbent dose on the  $K_d$  value, the results were shown in Table 4 and Fig. 13. It was obvious that the  $K_d$  value of cesium increased rapidly with increasing dose of CMC–KCuFC particles, which might be due to the reason that the adsorbent provided greater surface area and available active adsorption sites with increasing dose of CMC–

**Table 4** Effect of adsorbent dose on the  $K_d$  value of cesium ion by the CMC–KCuFC particles [cesium concentration: 20 mg L<sup>-1</sup>, temperature: 298.15 K]

Adsorbent dose (g)	Waste volume (mL)	Adsorption capacity (mg g <sup>-1</sup> )	$K_d$ (mL g <sup>-1</sup> )
0.006	50	63.177	6030.873
0.007	50	63.280	7043.821
0.008	50	61.994	7779.583
0.009	50	60.727	8627.267
0.010	50	59.372	9493.094
0.020	50	43.927	1.099 × 10 <sup>5</sup>
0.030	50	29.862	4.117 × 10 <sup>5</sup>
0.040	50	22.438	4.533 × 10 <sup>5</sup>

**Fig. 13** Effect of competing ions on  $K_d$  by CMC–KCuFC particles (pH: 5, initial cesium concentration: 20 mg L<sup>-1</sup>, adsorbent dose: 0.02 g, temperature: 298.15 K).**Fig. 12** Effect of competing ions on the remove of 50 mL 20 mg L<sup>-1</sup> Cs<sup>+</sup> for 24 h at 298.15 K.

KCuFC particles.<sup>36</sup> Besides, it can be found that the adsorption properties of competing ions for Cs in the high adsorbent dose were consistent with the results obtained in the low adsorbent dose of Cs, and in the condition of high concentration of five cations, the  $K_d$  value of cesium ion still remain at a very high level (>8 × 10<sup>4</sup> mL g<sup>-1</sup>), the results indicated that the CMC–KCuFC particles has good selectivity for cesium ion.

**3.1.7. Comparison with other adsorbents.** Comparing the adsorption capacity of other cesium adsorbents with that of the CMC–KCuFC adsorbent,<sup>9,33,37–39</sup> the result was listed in Table 5. It clearly revealed that the adsorption capacity of prepared adsorbent was much higher than most of cesium adsorbents. More important, this adsorbent was prepared only using environmental friendly and inexpensive materials at room temperature. Therefore, CMC–KCuFC adsorbent was a cost-effective adsorbent for cesium removal.

## 3.2. Adsorption experiments in a fixed bed column

**3.2.1. Effect of bed height.** Effect of bed height (2, 3 and 4 cm) on the breakthrough curve at a constant initial cesium



Table 5 Comparison of maximum adsorption capacity of adsorbents reported in literature for Cs<sup>+</sup> adsorption<sup>a</sup>

Adsorbent	pH	T (K)	q <sub>max</sub> (mg g <sup>-1</sup> )	References
Whisker-supported composite	6	298.15	32.90	38
Pre-treated arca shell biomass	5.5	—	3.93 ± 0.11	33
Prussian-blue-modified magnetite	—	—	16.20	39
Nickel hexacyanoferrate-walnut shell	—	298.15	4.94 ± 0.5	9
Nanocrystalline mordenite	—	298.15	37.30	40
CMC-KCuFC particles	4–10	298.15	60.827	This study
CMC-Cu	4–10	298.15	7.85	This study

<sup>a</sup> Note: '—' represented the information was not given in the references.

concentration (10 mg L<sup>-1</sup>) and flow rate (2.4 mL min<sup>-1</sup>) was shown in Fig. 14. With an increase of the bed height, the breakthrough curve moves from left to right and both breakthrough point and the saturation point were obviously increased. The explanation was that more available adsorption binding sites at higher bed height, which meant that consequently the total adsorbed cesium ions increased. Moreover, an increase in the bed height resulted in a wide mass transfer zone,<sup>40</sup> which made the breakthrough curves moderately steeper. In fact when the bed height increased, a longer time was required to reach the breakthrough point and saturation point. Therefore, for better performance of a fixed-bed column, a desirable bed height would be important for removal of the metal ions by CMC-KCuFC particles in the practical application.

**3.2.2. Effect of influent cesium concentration.** Effect of influent cesium concentration (5, 10 and 20 mg L<sup>-1</sup>) on the breakthrough curve at a constant bed height (3 cm) and flow rate (2.4 mL min<sup>-1</sup>) was shown in Fig. 15. An increase in the influent cesium concentration can lead to the faster breakthrough point and saturation point and as a consequence the sharper breakthrough curves shifted to the left. The adsorption

process reached saturation faster and the breakthrough time appeared earlier with increasing influent concentration. It might be for the reason that the more feeding of adsorbent on per unit surface area of the adsorbent caused the faster saturation of the column bed.<sup>41</sup> On the other hand, it can be explained that a higher concentration gradient caused a faster transport due to an increase in the diffusion coefficient or mass transfer coefficient.<sup>42,43</sup>

### 3.3. Characterization of the materials

**3.3.1. SEM and BET analysis.** SEM analysis of CMC-KCuFC adsorbent before and after adsorption were presented in Fig. 16. As shown in Fig. 16a, all the particles were of spherical shape, with a remarkably similar size of 2–3 μm after drying. It was observed that the outer surface of the dried CMC-KCuFC particles contained large porous channels, and large pores were visible in the SEM image (Fig. 16b). From highly magnified images of Fig. 16c, it was clearly showed that they were highly cross-linked. Lots of KCuFC particles were encapsulated in the network of CMC. Comparing with CMC-KCuFC particles before and after adsorption (Fig. 16c and d), it was obvious that there is no significant shape change. It can be demonstrated that CMC-

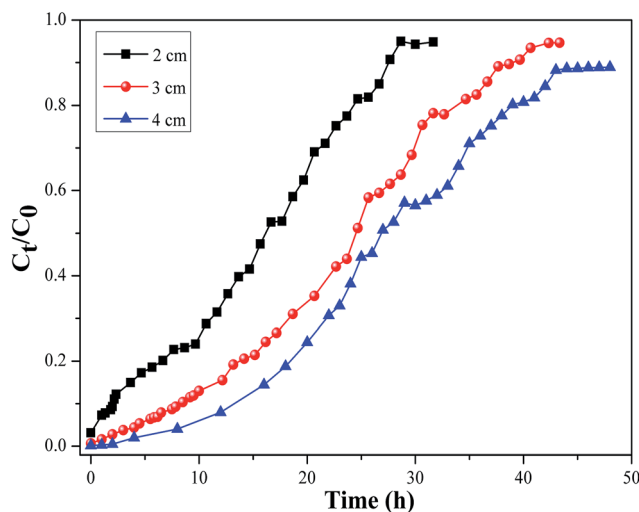


Fig. 14 Effect of bed height on the breakthrough curve of Cs adsorption onto CMC-KCuFC particles (pH 5 ± 0.02, influent concentration = 10 mg L<sup>-1</sup>, influent flow rate = 2.4 mL min<sup>-1</sup>, T = 298.15 K).

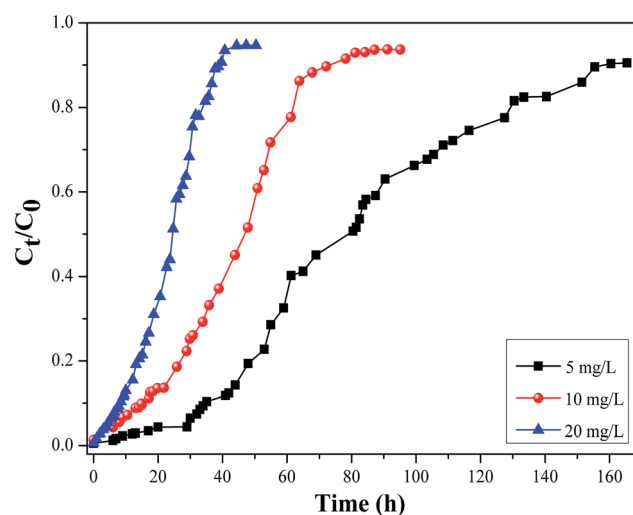


Fig. 15 Effect of influent cesium concentration on the breakthrough curve of Cs adsorption onto CMC-KCuFC particles (pH 5 ± 0.02, bed height = 3 cm, influent flow rate = 2.4 mL min<sup>-1</sup>, T = 298.15 K).





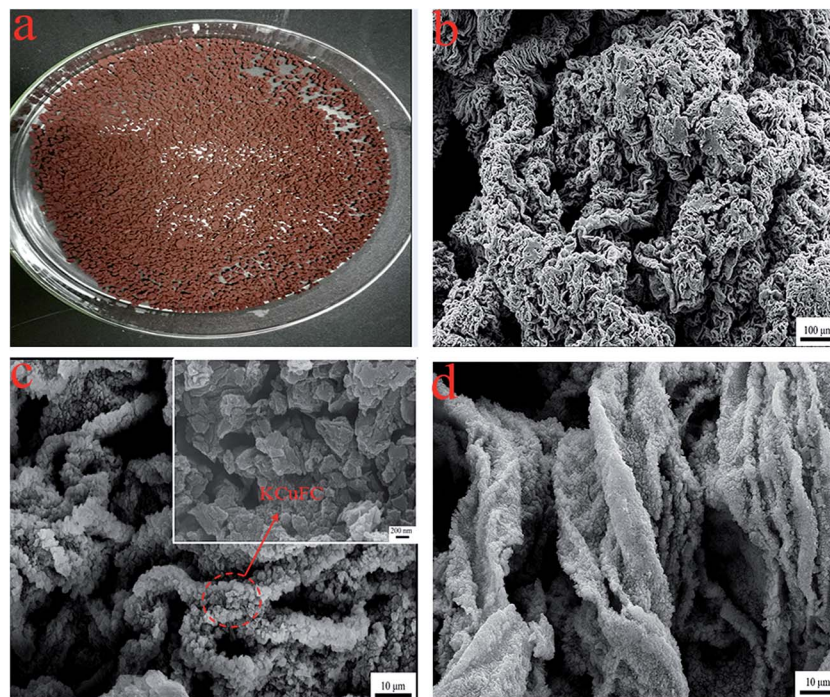


Fig. 16 SEM analyses of the samples: the digital photos of (a) CMC-KCuFC after drying (b) SEM of CMC-KCuFC before adsorption, (c) and inset are SEM of CMC-KCuFC particles after adsorption (higher magnification), (d) is SEM of CMC-KCuFC particles after adsorption.

KCuFC particles had excellent mechanical stability. Meanwhile, the results of multipoint BET analysis were shown in Table 6. It can be seen easily that the BET surface area of CMC-KCuFC particles was  $55.275 \text{ m}^2 \text{ g}^{-1}$ , which was more than twice of CMC-Cu, and the total pore volumes of CMC-KCuFC particles was  $0.024 \text{ cm}^3 \text{ g}^{-1}$ , while that of CMC-Cu was  $0.0036 \text{ cm}^3 \text{ g}^{-1}$ . Therefore an increase in the total surface and pore volume in the CMC-KCuFC particles would have increased the possibility of internal diffusion.

**3.3.2. FT-IR analysis.** Shown in Fig. 17a-c were the FT-IR spectra of CMC, CMC-KCuFC particles and CMC-KCuFC particles after adsorption, respectively. A broad absorption band at  $3429\text{--}3432 \text{ cm}^{-1}$  was relative to the -OH stretching vibration, while the bands around  $2919\text{--}2923 \text{ cm}^{-1}$  attributed to the C-H stretching vibration from -CH<sub>2</sub> group. And the absorption band around  $1611 \text{ cm}^{-1}$ ,  $1422 \text{ cm}^{-1}$  and  $1060 \text{ cm}^{-1}$  were referred to the stretching vibration of COO<sup>-</sup> (asymmetric), COO<sup>-</sup> (symmetric) and C-O group, respectively.<sup>43</sup> Comparing the spectrum of the CMC-KCuFC with that of the CMC, a sharp absorption band located at  $2096 \text{ cm}^{-1}$  appeared which was attributed to the C≡N stretching vibration.<sup>1</sup> Compared Fig. 17a

with 17b, two smaller peaks at  $494.8$  and  $600.5 \text{ cm}^{-1}$  were assigned to Fe<sup>2+</sup>-C≡N- and -C≡N-Cu<sup>2+</sup> in-plane deformation vibration.<sup>16,19</sup> All these characteristic peaks clearly suggested that the expected KCuFC particles in the CMC-KCuFC particles were successfully prepared.

**3.3.3. EDX analysis.** EDX analysis spectra of adsorbents were shown in Fig. 18. Comparing Fig. 18a and b, the element peaks of N, Fe, C, Cu and K were recorded in the EDX spectra of CMC-KCuFC particles (Fig. 18b). After the Cs<sup>+</sup> adsorption, new peaks corresponding to cesium ion appeared (Fig. 18c), which

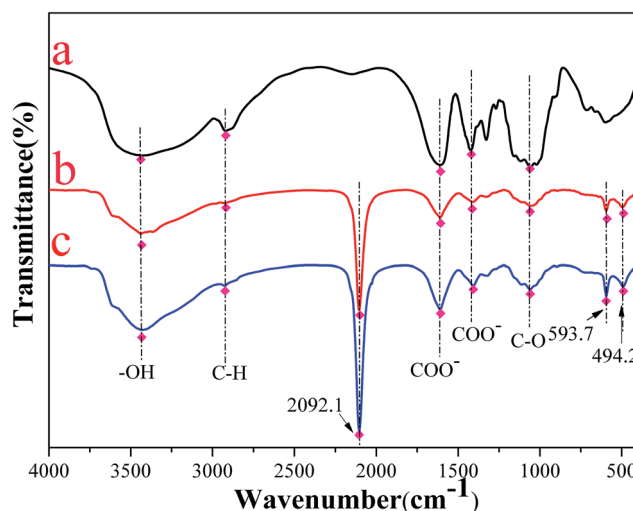


Fig. 17 FT-IR spectra of the samples: (a) CMC, (b) CMC-KCuFC particles, (c) CMC-KCuFC particles after adsorption.

Table 6 Pore structure parameters of CMC-Cu and CMC-KCuFC particles

Sample	Surface area ( $\text{m}^2 \text{ g}^{-1}$ )	Total pore volume ( $\text{cm}^3 \text{ g}^{-1}$ )
CMC-Cu	37.181	0.0086
CMC-KCuFC	55.275	0.0240



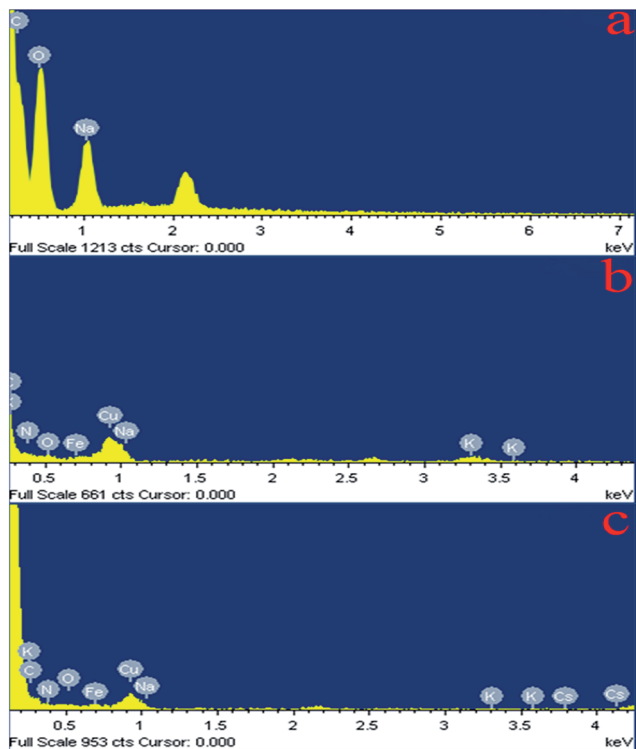


Fig. 18 EDX micrographs of (a) CMC, (b) CMC-KCuFC, (c) CMC-KCuFC-Cs.

elucidated that  $\text{Cs}^+$  was effectively adsorbed onto CMC-KCuFC adsorbent.

The percentage of surface atomic concentration determined by EDX spectra is listed in Table 7. Element content of Na and Cu before and after reaction are changed from 7.53% and 0 to 0.26% and 6.09%, respectively. Which shows that  $\text{Na}^+$  along with  $\text{Cu}^{2+}$  participated in the ion exchange. Moreover, element content of K change from 2.30% to 0.06% before and after Cs adsorption, indicating that the  $\text{K}^+$  is exchanged with  $\text{Cs}^+$ .

**3.3.4. XRD analysis.** XRD analysis of CMC, CMC-Cu and CMC-KCuFC were given in Fig. 19. The characteristic peaks for CMC-Cu were not observed, which was considered to be the amorphous structure of CMC-Cu. Similar result was obtained for the XRD profile for FPPB nanocomposite.<sup>44</sup> After the growth of KCuFC, a few new diffraction peaks appeared at  $44.8^\circ$ ,  $40.0^\circ$ ,  $35.7^\circ$ ,  $24.9^\circ$  and  $17.6^\circ$  were assigned to the (4 2 2), (4 2 0), (4 0 0), (2 2 0) and (2 0 0) plane, which agreed with KCuFC crystal (JCPDS card no. 53-0084). Taken together with the IR analysis, it can be inferred that presence of KCuFC was dispersed in the polymer matrix.

**3.3.5. TGA analysis.** Thermogravimetric analysis (TGA) curves in the oxygen atmosphere of CMC, CMC-Cu and CMC-KCuFC were shown in Fig. 20. These composites showed the initial weight loss at 33–170 °C, was related to the evaporation water molecules. The major mass loss of CMC begun at 260 °C (11%), whereas the major mass loss of the composite CMC-Cu started at 160 °C (14%), and the composite CMC-KCuFC exhibited its major weight loss at 165 °C (22%). Between 339 °C and 441 °C, CMC-KCuFC particles showed a more obvious

Table 7 Atomic concentrations on the absorbent surfaces obtained using EDX (data precision is  $\pm 5\%$ )

Sample	Atomic concentration (%)				
	Na	Cu	Fe	K	Cs
CMC	7.53	0	0	0	0
CMC-KCuFC	0.26	6.09	7.36	2.30	0
CMC-KCuFC-Cs	0.23	5.65	6.47	0.06	1.36

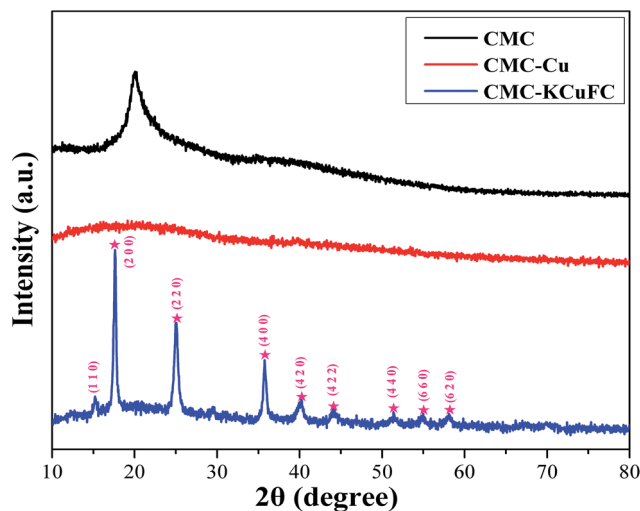


Fig. 19 XRD spectra of the samples: CMC, CMC-Cu and CMC-KCuFC particles.

weight loss compared with CMC and CMC-Cu, corresponding to the decomposition of the cyanide group.<sup>45</sup> The rapid weight loss in the range of 220–370 °C both in the CMC and CMC-KCuFC was attributed to polymer degradation. After heating up to 750 °C, about 27% residue was left as charred mass. As it can

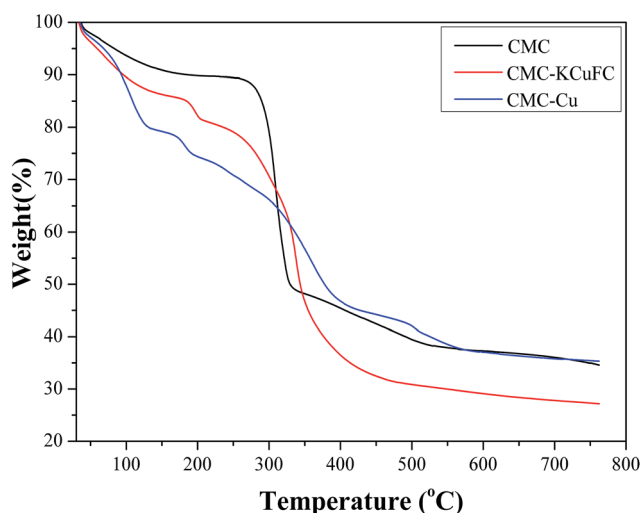


Fig. 20 TGA curves of the samples: CMC, CMC-Cu and CMC-KCuFC particles.



be observed from these results, the prepared composite was stable up to 180 °C.

**3.3.6. Mechanism of Cs adsorption.** To understand the  $\text{Cs}^+$  adsorption mechanism of CMC–KCuFC particles, based on the adsorption models with the analysis of SEM, FT-IR, EDX discussed in the above sections, the mechanism of CMC–KCuFC particles formation and cesium adsorption by CMC–KCuFC particles can be proposed in Fig. 21. It could be concluded that ion-exchange reactions between  $\text{Na}^+$  and  $\text{Cu}^{2+}$ . The process was shown in Fig. 21A.

KCuFC was a cubic, lattice-based, crystal with  $\text{Cu}^{2+}$  and  $\text{Fe}^{2+}$  atoms occupying alternate corners of the cubic lattice, and cyanide groups on the edges, the  $\text{Cu}^{2+}$  ions were octahedrally coordinated to the nitrogen from the cyanide bridge, and the  $\text{Fe}^{2+}$  linked to their carbon ends.  $\text{Fe}^{2+}$  was six fold carbon-coordinated, while  $\text{Cu}^{2+}$  was six fold nitrogen coordinated. In the adsorption process of  $\text{Cs}^+$  uptake by CMC–KCuFC, adsorption kinetic study showed that Cs adsorption on the CMC–KCuFC was controlled by chemisorption. That was to say, the adsorption process was dependent on the number of available adsorption sites on the adsorbent surface, and was eventually controlled by the binding of  $\text{Cs}^+$  to the surface or internal of the adsorbent. In addition, we investigated the changed values of the concentrations of  $\text{Cs}^+$  and  $\text{K}^+$  before and after adsorption, the results were shown in Table 8. It was observed that the amount of  $\text{K}^+$  in the solution increased from 0 to 0.031 mmol while the amount of  $\text{Cs}^+$  decreased from 0.038 to 0.025 mmol. Thus, as predicted, the exchange mechanism being the insertion of Cs ions into KCuFC crystal lattice, and concurrently displaced K ions from the lattice. The process was shown in

**Table 8** The changed values before and after adsorption [initial concentration of  $\text{Cs}^+$ : 100 mg  $\text{L}^{-1}$ , dose: 0.05 g,  $T$ : 298.15 K]

Material	$\text{Cs}^+$ (mmol)	$\text{K}^+$ (mmol)
CMC–KCuFC before adsorption	0.038	0
CMC–KCuFC after adsorption	0.025	0.012

Fig. 21B, and this is similar to the mechanism of cesium removal using  $\text{K}_2\text{CuFe}(\text{CN})_6$  adsorbent as ref. 46.

## 4. Conclusions

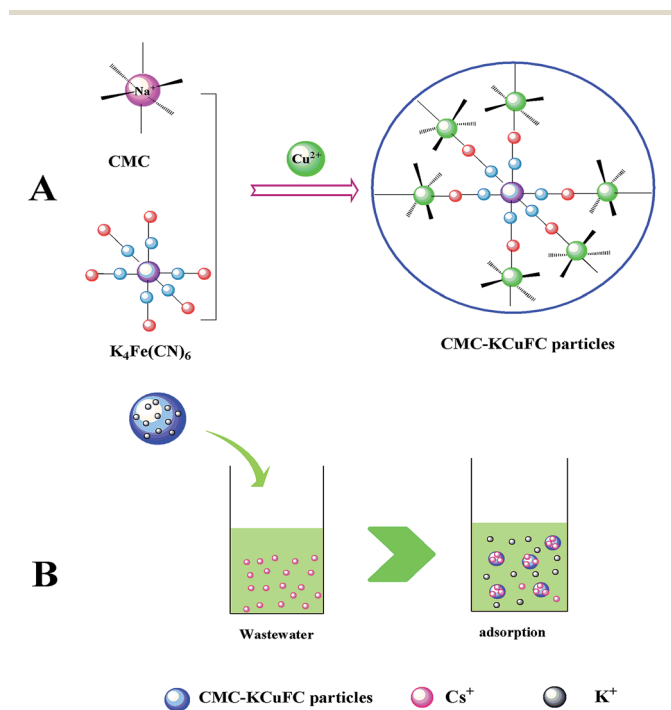
The CMC–KCuFC adsorbent was successfully synthesized *via* an syringe pump device and used for removal of cesium from water. Batch experiments were investigated for the adsorption property of CMC–KCuFC adsorbent, and the results showed a high adsorption capacity was 60.827 mg  $\text{g}^{-1}$  for  $\text{Cs}^+$ . The adsorption behavior of CMC–KCuFC fitted well with Freundlich isotherm models and the pseudo-second-order kinetic model. In addition, studies with the effect of pH confirmed that these particles can be used effectively over the pH range of 5–10. Moreover, the CMC–KCuFC with adsorbed  $\text{Cs}^+$  was easily separated from water with filtration. Thus, the simple preparation method and excellent adsorption capacity enabled CMC–KCuFC adsorbent to be one of the promising candidates for efficient and sensitive removal of cesium in continuous operation.

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**Fig. 21** (A) Schematic diagram of the fabrication process of CMC–KCuFC particles, (B) supposed mechanism of the adsorption of cesium.





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