

# Evaluating metal–organic frameworks for natural gas storage†

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Metal–organic frameworks have received significant attention as a new class of adsorbents for natural gas storage; however, inconsistencies in reporting high-pressure adsorption data and a lack of comparative studies have made it challenging to evaluate both new and existing materials. Here, we briefly discuss high-pressure adsorption measurements and review efforts to develop metal–organic frameworks with high methane storage capacities. To illustrate the most important properties for evaluating adsorbents for natural gas storage and for designing a next generation of improved materials, six metal–organic frameworks and an activated carbon, with a range of surface areas, pore structures, and surface chemistries representative of the most promising adsorbents for methane storage, are evaluated in detail. High-pressure methane adsorption isotherms are used to compare gravimetric and volumetric capacities, isosteric heats of adsorption, and usable storage capacities. Additionally, the relative importance of increasing volumetric capacity, rather than gravimetric capacity, for extending the driving range of natural gas vehicles is highlighted. Other important systems-level factors, such as thermal management, mechanical properties, and the effects of impurities, are also considered, and potential materials synthesis contributions to improving performance in a complete adsorbed natural gas system are discussed.

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## Natural gas storage

Natural gas has the potential to replace petroleum as the world's primary fuel for transportation. Consisting mainly of methane (CH<sub>4</sub>), natural gas has the highest H to C ratio of any fossil fuel, resulting in less CO and CO<sub>2</sub> released per unit of energy generated.<sup>1</sup> Lower sulfur and nitrogen contents also lead to lower SO<sub>x</sub> and NO<sub>x</sub> emissions, making natural gas a significantly cleaner burning fuel than gasoline.<sup>2</sup> Indeed, initial field tests found up to 86% less CO, 26% less CO<sub>2</sub>, and 77% less NO<sub>x</sub> emissions after converting gasoline cars to run on natural gas.<sup>3</sup> In addition, recent engineering advances in horizontal drilling and hydraulic fracturing have led to a rapid increase in global natural gas reserves, driving the price of natural gas below that of gasoline in many countries.<sup>4</sup>

In spite of this, several challenges have prevented the widespread use of natural gas in vehicles. Most importantly, the volumetric energy density of natural gas at ambient temperature and pressure is only 0.04 MJ L<sup>-1</sup>, compared to 32.4 MJ L<sup>-1</sup> for gasoline.<sup>5</sup> The volumetric energy density can be increased by compression or liquefaction, but both of these solutions are costly and poorly suited for light-duty passenger vehicles. For instance, compressed natural gas (CNG) requires expensive multi-stage compressors that consume energy, as well as heavy, bulky fuel tanks that reduce passenger and cargo space. Even with compression to 250 bar, the energy density of CNG (near 9 MJ L<sup>-1</sup>) is only 26% that of gasoline,<sup>2a</sup> leading to a significant reduction in the driving range of a vehicle. Moreover, CNG refueling stations are not yet common enough for convenient refueling and are costly to build.<sup>6</sup>

As a result of the low critical temperature of CH<sub>4</sub> (190.6 K, Table 1), natural gas cannot be liquefied by compression alone,

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Table 1 Relevant physical properties of pure CH<sub>4</sub>

Critical temperature <sup>8a</sup>	190.6 K
Boiling point <sup>8a</sup>	111.7 K
Kinetic diameter <sup>9</sup>	3.80 Å
Polarizability <sup>9</sup>	2.6 Å <sup>3</sup>
Volumetric density (1 bar, 25 °C) <sup>8</sup>	0.9 v/v
Volumetric density (250 bar, 25 °C) <sup>8</sup>	263 v/v
Volumetric density (1 bar, -162 °C) <sup>8</sup>	591 v/v



and cryogenic cooling is necessary to store liquefied natural gas (LNG). While the volumetric energy density of LNG can reach  $20.8 \text{ MJ L}^{-1}$  (64% of gasoline),<sup>5</sup> the overall system energy density is reduced due to the insulation required to maintain a low temperature and prevent boil-off. Additionally, the high cost of cooling systems and complications of handling a cryogenic fuel make LNG unlikely to find much application in the transportation sector beyond commercial trucking and public transportation.<sup>7</sup>

As an alternative to CNG and LNG, using adsorbents to store natural gas at higher densities at ambient temperature and moderate pressures has been an active area of research since the early 1970s.<sup>10a</sup> Significantly, adsorbents that operate at relatively low pressures should allow the use of inexpensive on-board fuel tanks and single-stage compressors. Lower storage pressures also facilitate at-home refueling,<sup>7</sup> which would reduce the large investment needed to build a new refueling infrastructure since natural gas distribution networks are already connected to many homes throughout the world.<sup>6</sup> Additionally, adsorbed natural gas (ANG) systems would permit the use of lightweight, conformable fuel tanks that can be more optimally integrated into the limited space available within a small car.<sup>11</sup> Note that in addition to natural gas powered cars, which are the focus of this work, ANG systems have also been evaluated for use in mobile natural gas tankers and for large-scale, stationary storage on natural gas distribution pipelines.<sup>12</sup> Although it is important to evaluate and optimize a similar set of adsorbent properties for each of these applications, the relevant storage conditions can differ significantly.

While early efforts in ANG storage focused primarily on zeolites, their relatively low surface areas of less than  $1000 \text{ m}^2 \text{ g}^{-1}$  resulted in insufficient  $\text{CH}_4$  capacities.<sup>7,10</sup> With considerably higher surface areas, activated carbons have been the most studied class of materials for ANG over the last several decades.<sup>13</sup> A large portion of research has involved investigating the effects of surface area, pore size, and pore shape on the  $\text{CH}_4$  adsorption properties of different carbons. Indeed, it was demonstrated that slit-shaped pores with a diameter of  $7.6 \text{ \AA}$ , which can accommodate two layers of  $\text{CH}_4$ , are ideal for maximizing the volumetric density of  $\text{CH}_4$  stored at 35 bar and  $25 \text{ }^\circ\text{C}$ .<sup>14,15</sup> Note that 35 bar has been widely used as a standard pressure for evaluating adsorbents for ANG storage, as this has represented the maximum pressure achievable by most inexpensive single-stage compressors.<sup>16</sup> Additionally, strategies for compacting and shaping activated carbons to optimize packing inside a storage tank have been explored in depth,<sup>1</sup> and prototype activated carbon ANG systems have been demonstrated and tested.<sup>17</sup>

In 2012, the US Department of Energy set new  $\text{CH}_4$  storage targets for adsorbents at  $350 \text{ cm}_{\text{STP}}^3 \text{ cm}_{\text{adsorbent}}^{-3} (\text{v/v})$ <sup>18</sup> and  $0.5 \text{ g}_{\text{CH}_4} \text{ g}_{\text{adsorbent}}^{-1} (699 \text{ cm}_{\text{STP}}^3 \text{ g}^{-1})$ .<sup>19</sup> Assuming a 25% loss in volumetric capacity due to packing an adsorbent inside a fuel tank, the target of 350 v/v is required for an ANG system to have a volumetric energy density of 263 v/v, equivalent to that of CNG at 250 bar and  $25 \text{ }^\circ\text{C}$ . The highest reported volumetric  $\text{CH}_4$  capacities for activated carbons are in the range of 100–170 v/v,<sup>20</sup> well below the energy density of CNG, and computational

studies have predicted a theoretical maximum volumetric capacity for carbons of 198 v/v at 34 bar and  $25 \text{ }^\circ\text{C}$ .<sup>14</sup> Accordingly, a next generation of adsorbents is required to meet these storage targets without moving to higher adsorption pressures or lower temperatures, both of which would add significant complexity and cost to an ANG vehicle.

Owing to their high porosity and tunable pore surfaces, metal–organic frameworks have received significant attention as a new class of adsorbents.<sup>21</sup> While early research on these materials for gas storage applications was mostly related to  $\text{H}_2$ ,<sup>22</sup> a growing number of frameworks have been evaluated for  $\text{CH}_4$  storage.<sup>23,24</sup> Significantly, several metal–organic frameworks have reported  $\text{CH}_4$  capacities comparable to or exceeding those of the best activated carbons; however, inconsistencies in reporting adsorption results and a lack of comparative studies have made it challenging to compare the performance of different materials. Here, we discuss the most important material properties for evaluating both new and existing metal–organic frameworks for natural gas storage and briefly review recent work. In this context, six metal–organic frameworks and an activated carbon, with a range of surface chemistries, pore structures, and surface areas representative of the most promising adsorbents for  $\text{CH}_4$  storage, are evaluated in detail.

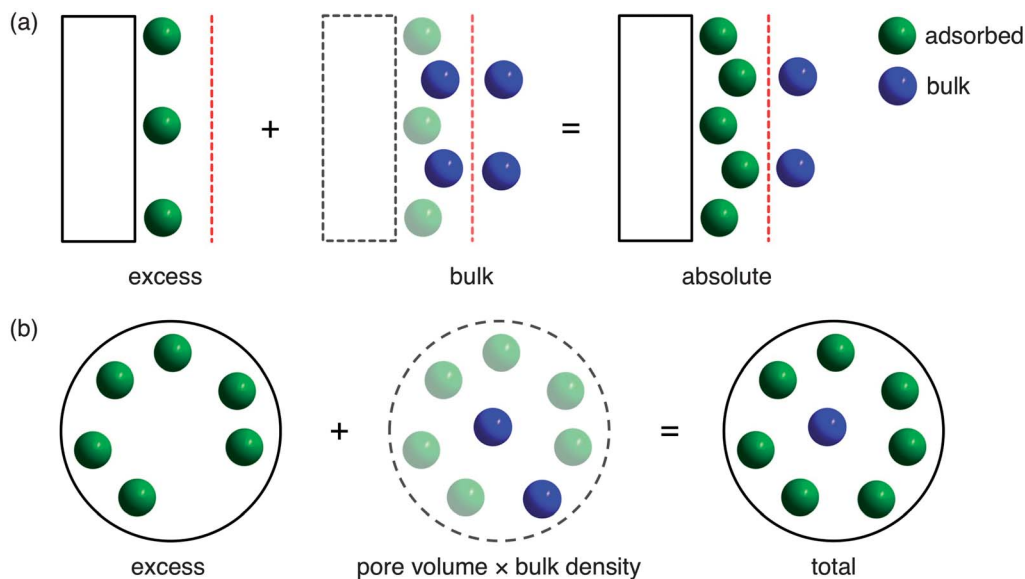
## High-pressure adsorption

All evaluations of adsorbents for natural gas storage rely on the measurement of accurate high-pressure adsorption isotherms. However, high-pressure experiments introduce several complexities, both in terms of collecting isotherm data and interpreting the results, that are not as significant at lower pressures. For instance, there is often inconsistent usage of the terms excess, total, and absolute when describing high-pressure adsorption capacities, which can lead to needless uncertainty when comparing the uptakes of different materials.

### Excess, total, and absolute adsorption

At a fundamental level, a gas is considered to be adsorbed when attractive forces from a surface result in a greater density of gas molecules than would normally be present at the same temperature,  $T$ , and pressure,  $P$ . For adsorption on a two-dimensional surface, the strength of the interaction between the gas and surface will decrease with increasing distance until the attractive forces of the surface become negligible and only bulk or free gas molecules are present. At this distance, an imaginary line, known as the Gibbs dividing surface, can be drawn to divide the total free volume into *adsorbed* and *bulk* regions (Fig. 1a).<sup>25</sup> The *absolute* amount adsorbed,  $n_{\text{abs}}$ , is defined simply as the total number of molecules that are in the adsorbed region. Unfortunately, absolute adsorption cannot be directly measured since it is not possible to determine the location of the Gibbs dividing surface or the size of the adsorbed region experimentally.<sup>26</sup> As a result, all adsorption measurements give *excess* adsorption,  $n_{\text{ex}}$ , which is the difference between the absolute adsorption amount and the amount





**Fig. 1** (a) For adsorption on a two-dimensional surface (rectangle), the Gibbs dividing surface (red) divides the free volume into two regions where gas molecules are either in an adsorbed (green) or bulk (blue) state.<sup>25</sup> *Absolute* adsorption, which includes all gas molecules in the adsorbed state, is the sum of the experimentally measured excess adsorption and the bulk gas molecules that would have been present in the adsorbed region in the absence of a surface. (b) For porous materials, the *total* adsorption includes all gas molecules inside the total pore volume, which corresponds to the sum of the excess adsorption and the bulk gas that would have been present in the pore volume in the absence of adsorption.<sup>28</sup> Note that for microporous materials, the total adsorption is often used as an approximation for absolute adsorption,<sup>29</sup> since it is not possible to determine the location of the Gibbs dividing surface experimentally.<sup>26</sup>

of bulk gas that would have been present in the adsorbed region,  $V_a$ , in the absence of a surface (eqn (1)).<sup>26</sup>

$$n_{\text{ex}} = n_{\text{abs}} - V_a \rho_{\text{bulk}}(P, T) \quad (1)$$

Since it is not possible to determine  $V_a$  experimentally, there is no straightforward method for calculating absolute adsorption from the measured excess adsorption. Instead, the *total* adsorption,<sup>27,28</sup>  $n_{\text{tot}}$ , which includes all gas molecules within the pores of an adsorbent, is often used as an approximation for absolute adsorption (Fig. 1b).<sup>29,30</sup> Total adsorption can be calculated from the excess adsorption using eqn (2) and the experimentally measured total pore volume,  $V_p$ . Note that the total pore volume is typically determined from an  $\text{N}_2$  adsorption isotherm at 77 K by assuming all pores have been completely filled with condensed  $\text{N}_2$  at a sufficiently high  $P/P_0$ , where  $P_0$  is the  $\text{N}_2$  saturation pressure.<sup>31</sup> Based on the Gurvich rule,<sup>32,33</sup> the total pore volume can be calculated by assuming that the molar volume of liquid  $\text{N}_2$  is the same regardless of the size or surface chemistry of the pore it is condensed within. For microporous materials with negligible external surface areas, which have a well-defined plateau in the  $\text{N}_2$  adsorption isotherm at 77 K, the exact  $P/P_0$  used is not particularly important. However, a  $P/P_0$  of 0.9–0.95 is typical and will include any pores less than 200–400 Å in the total volume calculation.<sup>34</sup> Other adsorbates, such as  $\text{CH}_4$ , can be used similarly to determine the total pore volume, but results generally do not vary significantly as long as all pores are equally accessible to the different probe molecules.<sup>35</sup> In most cases, small errors in the total pore volume do not have a significant impact on the calculated total adsorption.<sup>36</sup>

$$n_{\text{tot}} = n_{\text{ex}} + V_p \rho_{\text{bulk}}(P, T) \quad (2)$$

For gas storage applications, the total adsorption is most relevant for comparing the capacities of different adsorbents, as it is an intrinsic property of a material that represents the total amount of gas that can be stored inside a material's pores.<sup>28</sup> Since the density of gas in the bulk phase,  $\rho_{\text{bulk}}$ , is significant at high pressures, there is usually a large difference between the excess and total amount adsorbed at conditions relevant to natural gas storage. As a result, inconsistent usage of the terms excess, absolute, and total makes comparing  $\text{CH}_4$  capacities of different materials challenging, and it is always important to specify clearly the type of adsorption capacity that is being reported.

### High-pressure adsorption measurements

Due primarily to the large pressure range that is covered and the increasing nonideal behavior of gases above ambient pressure, adsorption experiments are inherently more difficult to perform accurately at high pressures than at low pressures. This can lead to large errors that make it challenging to compare the properties of different materials. Most commercial high-pressure adsorption instruments operate using either a gravimetric or volumetric measurement technique. At a basic level, gravimetric instruments measure the amount of  $\text{CH}_4$  adsorbed by using a balance to record the change in weight of a sample at different equilibrium pressures of  $\text{CH}_4$ , while volumetric instruments record the change in pressure when dosing  $\text{CH}_4$  from a calibrated volume to a volume containing the sample. In both cases, it is important to be aware of the most common issues that can affect the quality of the experimental data.



For both gravimetric and volumetric adsorption measurements, He is used to determine the precise volume occupied by the adsorbent inside the sample holder, which is needed for buoyancy corrections and free space calculations in gravimetric and volumetric experiments, respectively. Techniques for performing these corrections have been discussed in detail elsewhere,<sup>28,37</sup> but it is worth emphasizing that errors in buoyancy and free space calculations can significantly affect the accuracy of adsorption data (Fig. S17†). Note that for both corrections, He adsorption by the sample is assumed to be negligible, and as such, it is best to perform He measurements at the low pressures and high temperatures where this is most likely to be true.<sup>26,38</sup>

Regardless of the exact method used to perform buoyancy or freespace corrections, there will always be many other potential sources of error in high-pressure experiments, such as volume calibrations, thermocouple readings, pressure transducer readings, sample mass measurements, nonideality corrections and temperature gradients.<sup>37c</sup> Therefore, it is essential to measure background CH<sub>4</sub> adsorption isotherms with empty sample holders, or with a nonadsorbing material similar in volume to a typical sample, at all potential analysis temperatures and pressures.<sup>28</sup> Ensuring that background adsorption is negligible under the exact same conditions as in an actual experiment confirms that all calibrations, corrections, measurements, and calculations are valid, which is critical for verifying the accuracy of the resulting adsorption data. Note that this is equally important for volumetric, gravimetric, commercial, and custom-built high-pressure instruments.

Additionally, for gravimetric adsorption measurements, it is particularly important to ensure that no impurities are present in the CH<sub>4</sub> used, as even small quantities of more strongly adsorbing impurities, such as heavier hydrocarbons or water, can lead to large errors in the measured uptake. Similarly, large errors in volumetric measurements can often result from the fact that high-pressure sample holders, which are typically constructed from stainless steel, are very heavy compared to a typical sample. As a result, it is usually not practical to weigh an activated adsorbent in a fully assembled sample holder, as is common for low-pressure experiments. Thus, it can be difficult to obtain an accurate sample mass, which can lead to significant errors in measured capacities that have a 1 : 1 dependence on the amount of sample present. One potential solution is to measure the surface area of a sample directly prior to a high-pressure measurement in a fully assembled high-pressure sample holder. By confirming that the surface area is as expected, uncertainties associated with sample mass can be mostly eliminated.

## Evaluating metal–organic frameworks

Although high-pressure CH<sub>4</sub> adsorption isotherms have been measured for almost one hundred metal–organic frameworks, their CH<sub>4</sub> uptakes have been reported in a variety of different units and at a range of pressures and temperatures, which makes evaluating the relative performance of a particular compound difficult. To facilitate comparisons between existing materials for which ambient temperature, high-pressure CH<sub>4</sub>

adsorption isotherms have been published, Table 2 lists the total CH<sub>4</sub> uptake of all metal–organic frameworks at conditions as close to 35 bar and 25 °C as possible. To make comparisons between materials more meaningful, all isotherm data that was originally reported in terms of excess adsorption has been converted to total adsorption using each framework's measured pore volume and the bulk gas density from the NIST Refprop database at the appropriate temperature and pressure (eqn (2)).<sup>8</sup> Note, however, that in a number of instances there was no indication of whether reported data were given in terms of excess, total, or absolute adsorption, adding significant uncertainty to comparisons of these uptakes to those of other materials.

In almost all standard adsorption measurements, the amount adsorbed is determined per unit mass, not volume, of adsorbent. However, the amount of CH<sub>4</sub> adsorbed per volume, which ultimately determines the amount of natural gas that can be stored in a given fuel tank, has to be calculated using the density of a material. For metal–organic frameworks, the ideal crystallographic density has commonly been used to convert gravimetric adsorption capacities to a volumetric capacity that represents the maximum possible volumetric uptake in the absence of any loss in density from packing actual particles together inside a fuel tank. This method of calculating volumetric capacities certainly over-estimates what is realistically achievable, but it is still useful for initial comparisons between adsorbents, provided the crystallographic densities used are appropriate. Here, a substantial effort was made to ensure that all crystallographic densities were as representative as possible of the framework during CH<sub>4</sub> adsorption, which mainly involved confirming that both metal-bound and free solvent molecules from solvated crystal structures were not included in density calculations. Based upon these and other observations made while surveying published CH<sub>4</sub> adsorption data for metal–organic frameworks, we make the following recommendations for future evaluations of new frameworks for ANG storage:

(1) Report background high-pressure CH<sub>4</sub> adsorption isotherms for an empty sample holder (or sample holder with a nonadsorbing solid) at all measured temperatures and pressures as supplementary information.<sup>28,39</sup>

(2) Specify whether all isotherms are reported in terms of excess, total, or absolute adsorption. Methods used to convert experimental excess adsorption data to total or absolute adsorption should be detailed, including any assumptions made about the size of the adsorbed volume.<sup>28</sup> If a pore volume was used to calculate total adsorption, it should be reported along with the isotherm used to calculate it.

(3) When volumetric uptakes are reported, the density used should be given and the type of density (*e.g.* crystallographic, bulk, tap, pellet) specified.<sup>40</sup> When crystallographic densities are used, details of their calculation should be provided, including at a minimum: unit cell volume, unit cell content, and any potential differences between the state of the framework when the unit cell was determined and when adsorption isotherms were measured, which may involve desolvation, removal of excess ligand, framework flexibility, and/or different measurement temperatures.





(4) If the unit  $\text{cm}^3_{\text{STP}}$  is used to report adsorption data, the standard temperature and pressure should be defined.

(5) When isosteric heats of adsorption are reported, the method used to calculate them should be specified. Note that stating that the Clausius–Clapeyron relation was used is not sufficient, as this does not give any indication about how interpolations between measured data points were made.

(6) When mathematical models are used to fit experimental adsorption isotherms, all fitted parameters should be given, and the quality of the isotherm fits should be illustrated.

### CH<sub>4</sub> adsorption isotherms

In examining Table 2, there are many cases, particularly for the highest capacity frameworks, where CH<sub>4</sub> adsorption isotherms have been reported for the same material in multiple publications with inconsistent results. This makes it challenging to compare different frameworks and to understand the effects of different characteristics of the materials on CH<sub>4</sub> uptake. For example, HKUST-1 has been reported to have total CH<sub>4</sub> uptakes at 35 bar ranging between 184 and 220 v/v. By synthesizing and activating a selection of the most promising compounds in the same laboratory and measuring high-pressure isotherms on the same instrument, evaluating and comparing their CH<sub>4</sub> adsorption properties becomes more straightforward. To this end, the six metal–organic frameworks depicted in Fig. 2, along with an activated carbon for comparison, were chosen for a detailed evaluation. The seven materials have features that are common to many of the adsorbents that have shown the highest gravimetric and volumetric CH<sub>4</sub> uptakes at 35 bar, including strong adsorption sites, pores shaped by Cu<sub>2</sub>-paddlewheel units, and high surface areas.

With modest gravimetric surface areas of 1500–2000  $\text{m}^2 \text{g}^{-1}$ , the M<sub>2</sub>(dobdc) (M = Ni, Co, Mg; dobdc<sup>4-</sup> = 2,5-dioxido-1,4-

benzenedicarboxylate; M-MOF-74, CPO-27-M) compounds have one-dimensional hexagonal channels featuring square pyramidal metal cations that have been shown to act as strong adsorption sites for many small gas molecules.<sup>41,42</sup> The compounds Cu<sub>3</sub>(btc)<sub>2</sub> (btc<sup>3-</sup> = 1,3,5-benzenetricarboxylate; HKUST-1)<sup>43,44</sup> and Cu<sub>2</sub>(adip) (adip<sup>4-</sup> = 5,5'-(9,10-anthracenediyl)di-isophthalate; PCN-14)<sup>44c,45</sup> are built from Cu<sub>2</sub>-paddlewheels that also contain exposed metal cations upon desolvation; however, their pore structures are significantly more complicated than M<sub>2</sub>(dobdc), with several differently sized pores and pore windows. Significantly, PCN-14 has been widely cited as one of the best existing metal–organic frameworks for CH<sub>4</sub> storage, based upon its reported total volumetric uptake of 230 v/v at 17 °C and 35 bar.<sup>45a</sup> The compound Zn<sub>4</sub>O(bdc)<sub>3</sub> (bdc<sup>2-</sup> = 1,4-benzenedicarboxylate; MOF-5, IRMOF-1) has a high Langmuir surface area of 3995  $\text{m}^2 \text{g}^{-1}$ , but does not contain any inherently strong adsorption sites for CH<sub>4</sub>.<sup>21a,24a,46</sup> Indeed, its pore surface is more similar to that of an activated carbon. For comparison, the activated carbon AX-21, which has an exceptionally high Langmuir surface area of 4880  $\text{m}^2 \text{g}^{-1}$  and is one of many activated carbons that have been studied in detail for ANG storage, was also evaluated.<sup>47</sup>

After synthesis, surface areas and pore volumes were measured for all seven materials to ensure samples were fully activated and of high quality (Fig. S7–S15†). High-pressure CH<sub>4</sub> adsorption isotherms from 0 to 100 bar were then measured for each material at –25, 25, 38, and 50 °C. Experimentally measured excess adsorption isotherms were converted to total adsorption using total pore volumes, as determined from N<sub>2</sub> isotherms at 77 K ( $P/P_0 = 0.9$ ), and the bulk gas density at each temperature and pressure from the NIST Refprop database (eqn (2)).<sup>8</sup> Volumetric adsorption was calculated using the crystallographic densities of desolvated structures at as near ambient temperature as possible (Table S2†).

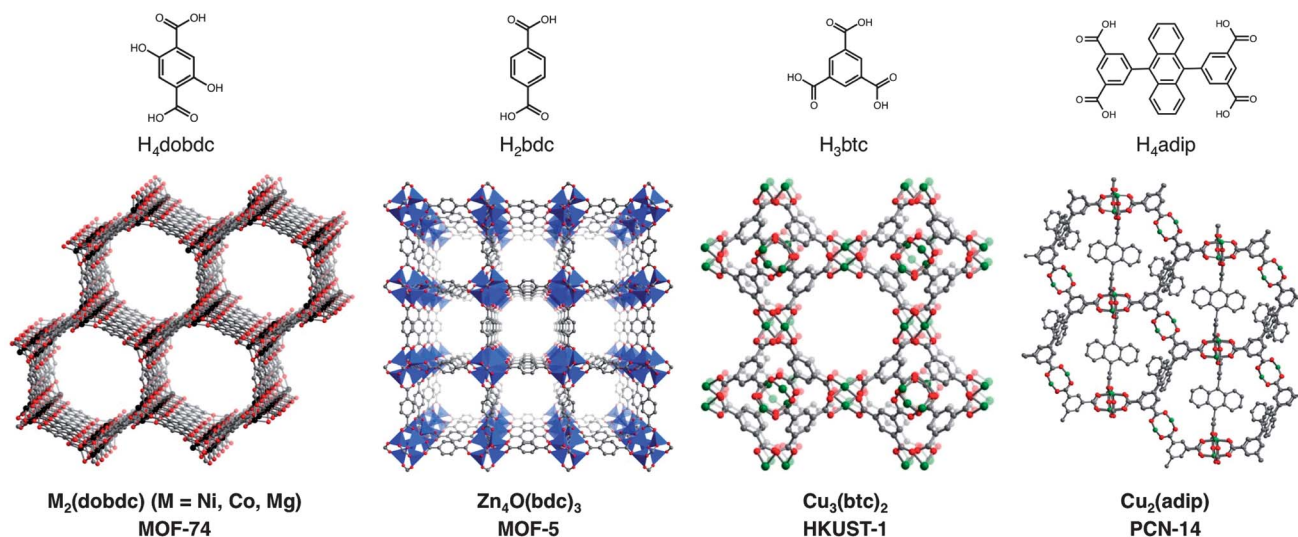


Fig. 2 Crystal structures and organic bridging ligands for the six metal–organic frameworks evaluated in this work: M<sub>2</sub>(dobdc) (M = Ni, Co, Mg; dobdc<sup>4-</sup> = 2,5-dioxido-1,4-benzenedicarboxylate; M-MOF-74, CPO-27-M), Zn<sub>4</sub>O(bdc)<sub>3</sub> (bdc<sup>2-</sup> = 1,4-benzenedicarboxylate; MOF-5, IRMOF-1), Cu<sub>3</sub>(btc)<sub>2</sub> (btc<sup>3-</sup> = 1,3,5-benzenetricarboxylate; HKUST-1), and Cu<sub>2</sub>(adip) (adip<sup>4-</sup> = 5,5'-(9,10-anthracenediyl)di-isophthalate; PCN-14). Green, gray, and red spheres represent Cu, C, and O atoms, respectively; H atoms have been omitted for clarity. Black spheres represent Ni, Co, or Mg atoms, and blue tetrahedra represent Zn atoms.



**Table 2** Crystallographic density, pore volume, surface area and total CH<sub>4</sub> adsorption near 35 bar and ambient temperature for metal–organic frameworks (sorted by decreasing volumetric uptake)

Chemical formula <sup>a</sup>	Common name	$\rho_{\text{cyst}}$ (g cm <sup>-3</sup> )	$V_p$ (cm <sup>3</sup> g <sup>-1</sup> )	Surface area (m <sup>2</sup> g <sup>-1</sup> )		Total CH <sub>4</sub> adsorption <sup>b</sup>		$T$ (°C)	Ref.
				BET	Langmuir	cm <sup>3</sup> STP cm <sup>-3</sup>	cm <sup>3</sup> STP g <sup>-1</sup>		
Ni <sub>2</sub> (dobdc)	Ni-MOF-74, CPO-27-Ni	1.195	0.56	1593	230	193	35	25	This work 41h
Cu <sub>3</sub> (btc) <sub>2</sub>	HKUST-1	0.881	0.47	1218	214	179	35	25	42
			0.44	1027	206	172	35	25	43b
			0.77	2203	225	255	35	25	This work 43d
Co <sub>2</sub> (dobdc)	HKUST-1 tablet (3 × 3 mm) Co-MOF-74, CPO-27-Co	0.582 <sup>c</sup>	0.75	1663	220	250	35	22	43e
			0.67	1850	217	246	35	30	43g
			0.76	1502	2216	198	225	35	30
Cu <sub>2</sub> (adip)	PCN-14	0.829	0.71	1555	194	221	35	30	43d
			0.72	94 <sup>d</sup>	184	209	35	30	44b
Mg <sub>2</sub> (dobdc)	Mg-MOF-74, CPO-27-Mg	0.909	0.51	1433	221	188	35	25	This work 42
			0.48	1056	194	165	35	25	45a
Cu <sub>2</sub> (bdpp)	NJU-Bai10	0.668	0.83	1984	202	244	35	25	This work 41h
			0.87	1753	235	283	35	17	45a
Cu <sub>2</sub> (1,4-nddi)	NOTT-109	0.790	0.69	2360	200	220	35	25	This work 42
			0.63	1542	188	207	35	25	41h
Zn(bdc)(ted) <sub>0.5</sub>	NOTT-109	0.893	0.61	3108	197	296	35	25	42
			0.85	2110	197	250	35	17	80
Cu <sub>3</sub> (bdb)	UTSA-20	0.91	0.65	2015	197 <sup>d</sup>	221 <sup>d</sup>	35	27	61
			0.63	1156	197	217	35	25	81
Cu <sub>2</sub> (tpic)	NOTT-101	0.684	0.63	2805	196	286	35	27	82
			0.91	1931	194	259	35	27	61
Cu <sub>2</sub> (sbtc)	PCN-11	0.749	0.91	2442	194	259	35	25	83
			0.677	1661	194	209	35	27	61
Cu <sub>2</sub> (bptc)	NOTT-100, MOF-505	0.927	0.677	1661	194	209	35	27	61
			0.643	2958	194	301	35	27	61
Cu <sub>2</sub> (2,6-nddi)	NOTT-103	0.685	1.157	3120	194	283	35	25	84
			1.14	2718	194	283	35	25	84
[Zn <sub>3</sub> (OH) <sub>4</sub> (tbcppm)- (H <sub>2</sub> tbcppm) <sub>2</sub> ]	PCN-16	0.724	1.06	2800	192	265	35	27	85
			0.767	1770	191	252	35	25	2-4h and 86
Cu <sub>2</sub> (C <sub>20</sub> H <sub>20</sub> O <sub>8</sub> )	NOTT-107	0.756	1.074	2823	190	280	35	27	87
			0.679	885	188	153	35	25	87
Cu <sub>2</sub> (pddi)	ZJU-5	1.231	0.41	1235	186 <sup>d</sup>	190 <sup>d</sup>	35	30	88
			0.978	1627	186 <sup>d</sup>	190 <sup>d</sup>	35	30	88
Zn <sub>2</sub> (dobdc)	Zn-MOF-74	0.978	0.54	1627	186 <sup>d</sup>	190 <sup>d</sup>	35	30	88
Al(OH)(bdc)	MIL-53 (Al)	0.978	0.54	1627	186 <sup>d</sup>	190 <sup>d</sup>	35	30	88



Table 2 (Contd.)

Chemical formula <sup>a</sup>	Common name	$\rho_{\text{cyst}}$ (g cm <sup>-3</sup> )	$V_p$ (cm <sup>3</sup> g <sup>-1</sup> )	Surface area (m <sup>2</sup> g <sup>-1</sup> )		Total CH <sub>4</sub> adsorption <sup>b</sup>		$T$ (°C)	Ref.
				BET	Langmuir	cm <sup>3</sup> STP cm <sup>-3</sup>	cm <sup>3</sup> STP g <sup>-1</sup>		
Cu <sub>3</sub> (tdpat)			0.54	1140	1590	155	159	31	89 and 90
Cu <sub>2</sub> (qptc)		0.782	0.56	1938	2608	121	124	30	91
Cu <sub>2</sub> (fddi)	NOTT-102	0.587	0.93	3342		182	232	25	50
Cu <sub>2</sub> (fddi)	ZJU-25	0.622	1.268	2125	3304	180	289	27	61
Cu <sub>3</sub> [(C <sub>6</sub> H <sub>3</sub> )(C <sub>2</sub> N <sub>3</sub> H) <sub>3</sub> ] <sup>-</sup> (C <sub>6</sub> H <sub>3</sub> )(COO) <sub>6</sub> ]	NU-125	0.578	1.29	3120		179	310	25	93
Zn <sub>4</sub> O(C <sub>2</sub> H <sub>4</sub> -bdc) <sub>3</sub>	IRMOF-6	0.65	0.92	1102	2630	177	272	25	94
Mn <sub>2</sub> (dobdc)	Mn-MOF-74	1.084	0.5	1448	2104	164	199	25	42
Zn <sub>2</sub> (bdc) <sub>2</sub> (dabco)		0.822	0.75	1450		159	194	30	43b
Cu <sub>3</sub> (OH-stpdc)	SDU-6	0.611	1.17	2826		172	281	23	95
Cu <sub>3</sub> (bte)	PCN-61	0.56	1.36	3000	3500	171	306	25	96
Cu <sub>2</sub> (bdi)	PCN-46	0.619	1.012	2500	2800	171	277	25	97
Zn <sub>4</sub> O(bdc) <sub>3</sub>	IRMOF-1, MOF-5	0.621	1.4 <sup>e</sup>			168	271	25	98
			1.4	3995		150	241	25	23a
									This work
Zr <sub>6</sub> O <sub>4</sub> (OH) <sub>4</sub> (NH <sub>2</sub> -bdc) <sub>6</sub>	UiO-66-NH <sub>2</sub>	1.36	1.2	3800	4400	143	230	27	39
Cr(OH)(bdc)	MIL-53 (Cr)	1.04	1.55	1080		138	223	25	46d
Co <sub>2</sub> (bdc) <sub>2</sub> (dabco)		0.815	0.4	1500		167	123	30	43g
Cu <sub>3</sub> (Me-stpdc)	SDU-7	0.605	0.82	1600	2300	161	197	31	89
Cu <sub>3</sub> (tipb)	UTSA-34	0.84	1.1	2713		159	263	30	99
Cu <sub>3</sub> (dceni)	UTSA-40	0.827	0.542	991	1661	159	189	17	100
Cu <sub>2</sub> (ndc) <sub>2</sub> (dabco)	DUT-8 (Cu)	0.681	0.65	1630		152	184	27	101
Cu <sub>2</sub> (btcc)	PCN-80	0.575	1.04	2535	4150	148	217	25	102
Zn <sub>4</sub> O(tcppa) <sub>2</sub>	SNU-77	0.586	1.47	3850	4180	147	255	23	103
Cu <sub>3</sub> (iBu-stpdc)	SDU-8	0.613	1.52	3670		147	250	25	104
Zr <sub>6</sub> O <sub>4</sub> (OH) <sub>4</sub> (bdc) <sub>6</sub>	UiO-66	1.32	1.02	2516		146	238	25	105
Zn <sub>4</sub> O(NH <sub>2</sub> -bdc) <sub>3</sub>	IRMOF-3	0.63	0.36	970		146	110	30	43g
			1.07			144	228	25	23a
									and 106
Ti <sub>8</sub> O <sub>8</sub> (OH) <sub>4</sub> (bdc) <sub>6</sub>	MIL-125	0.81	0.67	1820		141	174	30	43g
Yb <sub>2</sub> O <sub>3</sub> [(C <sub>6</sub> H <sub>3</sub> ) <sub>4</sub> (C <sub>6</sub> H <sub>4</sub> ) <sub>6</sub> ] (COO) <sub>6</sub> ](NO <sub>3</sub> )	UTSA-62	0.59	0.91	2190		139	236	25	107
Cu <sub>3</sub> (tcepb)	NU-111	0.409	2.09	4930		136	333	25	49
Cu <sub>3</sub> (ntei)	PCN-66	0.44	1.63	4000	4600	134	304	25	108
Co <sub>2</sub> (bipy) <sub>3</sub> (btb) <sub>4</sub>	DUT-23 (Co)	0.401	2.03	4850		133	331	25	109
Zn(MeIM) <sub>2</sub>	ZIF-8	1.141	0.49			131	115	27	39
			0.59	1445		124	109	30	110
Zn <sub>4</sub> O(ceb) <sub>3</sub>	SNU-71	0.835	0.709	1770	1923	130	155	25	111
Ni(ndc)(ted) <sub>0.5</sub>		0.789	0.84	2307	2647	128 <sup>d</sup>	162 <sup>d</sup>	25	81
Cu <sub>3</sub> (pre)	PCN-68	0.38	2.13	5109	6033	126	332	25	97



Table 2 (Contd.)

Chemical formula <sup>a</sup>	Common name	$\rho_{\text{cyst}}$ (g cm <sup>-3</sup> )	$V_p$ (cm <sup>3</sup> g <sup>-1</sup> )	Surface area (m <sup>2</sup> g <sup>-1</sup> )		Total CH <sub>4</sub> adsorption <sup>b</sup>		$T$ (°C)	Ref.
				BET	Langmuir	cm <sup>3</sup> STP cm <sup>-3</sup>	cm <sup>3</sup> STP g <sup>-1</sup>		
Zn <sub>4</sub> O(btbb) <sub>2</sub>	MOF-177	0.427	1.89	4500	5340	126	293	25	46d
Cu(SiF <sub>6</sub> )(4,4'-bpy) <sub>2</sub>		0.86	1.55		1337	106	249	25	112
Zn <sub>3</sub> O(2,7-ndc) <sub>2</sub>		1.04	0.56	1337		125	146	25	113
Cu(GeF <sub>6</sub> )(4,4'-bpy) <sub>2</sub>		0.925	0.458	901	1281	124	144	25	114
Cu <sub>2</sub> (bdeppi)	SNU-50	0.65	1.08	2300	2450	125	120	25	115
Al(OH)(ndc)	DUT-4	0.773	0.68	1308	1996	122	189	25	116
Zn <sub>4</sub> O(ndc) <sub>3</sub>	UTSA-38	0.962	0.61	1090	1690	120 <sup>d</sup>	158	30	117
Cr <sub>3</sub> O(btc) <sub>2</sub> F	MIL-100 (Cr)	0.7	1.1	1900	6170	120	171	30	119
Zn <sub>4</sub> O(btbb) <sub>4/3</sub> (ndc)	MOF-205	0.38	2.16	4460		119	314	25	46d
Zn <sub>4</sub> O(ndc) <sub>3</sub>	IRMOF-8	0.448	1.827	4326		114	254	25	120
Zn <sub>4</sub> O(btbb) <sub>4/3</sub> (ndc)	DUT-6	0.39	2.02	6005		106	271	25	121
Fe <sub>3</sub> O(btc) <sub>2</sub> F	MIL-100 (Fe)	0.7	0.99	2410		117	167	30	43g
Al(OH)(bpdc)	DUT-5	0.634	0.81	1613	2335	113	179	30	117
Cu <sub>2</sub> (bbcdc)	DUT-49	0.311	2.91	5476		113	363	25	48
Zn <sub>4</sub> O(cvb) <sub>3</sub>	SNU-70	0.408	2.17	5290	6100	111	273	25	122
Zn <sub>6</sub> (btbb) <sub>4</sub> (4,4'-bpy) <sub>3</sub>	FJI-1	0.405	1.43	4043	4624	111	273	25	123
Zn(Im) <sub>1.5</sub> (cbim) <sub>0.5</sub>	ZIF-76	0.869	0.57	1340		110	126	30	124
Cu <sub>3</sub> (C <sub>66</sub> H <sub>36</sub> O <sub>12</sub> )	NOTT-119	0.361	2.35	4118		106	294	25	125
Cd(bpydb)		1.21	0.35	346		104	86	25	126
Ni <sub>3</sub> O <sub>2</sub> (btb) <sub>2</sub>	DUT-9	0.358	2.18		6120	101	283	25	127
Cr <sub>3</sub> O(bdc) <sub>3</sub> F	MIL-101 (Cr)	0.44	2.15	4230		101	230	30	119
			1.57	3870		87	197	30	43g
			1.38	2674		82	186	22	43e
			1.303	2693	4492	79	178	30	43b
Zn <sub>4</sub> O(BenzTB) <sub>3/2</sub>	DUT-13	0.385	1.98	6240	5570	96	250	25	128
Zn <sub>4</sub> O(bte) <sub>4/3</sub> (bpdc)	MOF-210	0.25	3.6		10 400	83	331	25	46d
Co <sub>2</sub> (4,4'-bpy) <sub>3</sub> (NO <sub>3</sub> ) <sub>4</sub>		1.36				73	54	25	23
Zn <sub>4</sub> O(bbc) <sub>2</sub>	MOF-200	0.22	3.59	4530	10 400	67	304	25	46d
Cd <sub>2</sub> (azpy) <sub>3</sub> (NO <sub>3</sub> ) <sub>4</sub>		1.54				66	43	25	129
Co <sub>2</sub> (ndc) <sub>2</sub> (dabco)	DUT-8 (Co)	0.67	0.62	1400		52	78	25	102
Zn <sub>2</sub> (ndc) <sub>2</sub> (dabco)	DUT-8 (Zn)	0.68	0.3	710		40	59	25	102
Cu <sub>2</sub> (PF <sub>6</sub> )(NO <sub>3</sub> )(4,4'-bpy) <sub>4</sub> · 1.4PF <sub>6</sub> · 0.6NO <sub>3</sub>		1.057		559		33	31	25	113
Zn <sub>2</sub> (tcpbda)	SNU-30	0.381	0.28	704	770	27	71	25	130
Co(azpy) <sub>2</sub> (NCS) <sub>2</sub>		1.31				19	15	25	129
Co <sub>2</sub> (azpy) <sub>3</sub> (NO <sub>3</sub> ) <sub>4</sub>		1.32				17	13	25	129
Zn <sub>2</sub> (tcpbda)(bpta)		0.459	0.14	308		17	37	25	130
Cu(C <sub>10</sub> H <sub>6</sub> O <sub>2</sub> )(ted) <sub>0.5</sub>			1.08	3129			214 <sup>f</sup>	25	131
Cu(bpdc)(ted) <sub>0.5</sub>			1.27	3265			213 <sup>f</sup>	25	131
Cu(bdc)(ted) <sub>0.5</sub>			0.71	1891			185 <sup>f</sup>	25	131b
VO(bdc)			0.5	1030			137 <sup>f</sup>	30	132
Cu(C <sub>4</sub> H <sub>2</sub> O <sub>4</sub> )(ted) <sub>0.5</sub>	MIL-47 (V)		0.24	606			103 <sup>f</sup>	25	131b







Table 2 (Contd.)

Chemical formula <sup>a</sup>	Common name	$\rho_{\text{cyst}}$ (g cm <sup>-3</sup> )	$V_p$ (cm <sup>3</sup> g <sup>-1</sup> )	Surface area (m <sup>2</sup> g <sup>-1</sup> )		Total CH <sub>4</sub> adsorption <sup>b</sup>		$T$ (°C)	Ref.	
				BET	Langmuir	cm <sup>3</sup> STP cm <sup>-3</sup>	cm <sup>3</sup> STP g <sup>-1</sup>			
Cu(dhbc) <sub>2</sub> (4,4'-bpy)	AX-21 activated carbon	0.49	1.64	320	4880	154	70 <sup>f</sup> 315	35 35	25 25	133 this work
C <sub>25</sub> H <sub>24</sub> B <sub>4</sub> O <sub>8</sub>	COF-102	0.43	1.55	3620	4650	135	313	35	25	134
C <sub>99</sub> H <sub>64</sub> Si <sub>4</sub>	PPN-4	0.284	3.04	6461	10 063	109	384	35	25	135
Na <sub>86</sub> [(AlO <sub>2</sub> ) <sub>86</sub> (SiO <sub>2</sub> ) <sub>106</sub> ]	Zeolite NaX	1.43	0.27			106	74	35.5	25	136
Na <sub>12</sub> [(AlO <sub>2</sub> ) <sub>12</sub> (SiO <sub>2</sub> ) <sub>12</sub> ]	Zeolite 5A	1.48	0.2			104	70	35.5	5	136

<sup>a</sup> adip = 5,5'-(9,10-anthracenediyl)di-isophthalate; azpy = 4,4'-azopyridine; bbc = 4,4',4''-[benzene-1,3,5-triyl-tris(benzene-4,1-diy)]tribenzoate; bbcdc = 9,9'-(1,1'-biphenyl)-4,4'-diyl]bis(9H-carbazole-3,6-dicarboxylate); bdc = 1,4-benzenedicarboxylate; bdeppi = N,N'-bis(3,5-dicarboxyphenyl)pyromellitic diimide; bdi = 5,5'-(buta-1,3-diene-1,4-diy)diisophthalate; bdpp = 3,5-bis(3,5-dicarboxyphenyl)pyridine; BenzTB = N,N,N',N'-benzidine-tetrazine; bbb = 3,3',3'',5,5',5''-benzene-1,3,5-triyl-hexabenzate; bpdcc = biphenyldicarboxylate; bpta = 3,6-di(4-pyridyl)-1,2,4,5-tetrazine; bptc = biphenyl-3,3',5,5'-tetracarboxylate; 4,4'-bpy = 4,4'-bipyridine; bpydb = 4,4'-(4,4'-bipyridine-2,6-diy)di-benzoate; btb = benzene-1,3,5-tribenzoate; btc = 1,3,5-benzenetricarboxylate; bre = 4,4',4''-[benzene-1,3,5-triyl-tris(ethyne-2,1-diy)]tribenzoate; brei = 5,5',5''-benzene-1,3,5-triyl-tris(1-ethynyl-2-isophthalate); bttdc = 9,9',9''-([1,1'-biphenyl]-3,3',5,5'-tetrayl)tetrakis(9H-carbazole-3,6-dicarboxylate); cbIM = *b*-chlorobenzoimidazole; ceb = 4-(2-carboxyethyl)benzoate; cvb = 4-(2-carboxyvinyl)benzoate; dabco = 1,4-diazabicyclo[2.2.2]octane; dceni = 6,6'-dichloro-2,2'-diethoxy-1,1'-binaphthyl-4,4'-di(5-isophthalate); dhbc = 2,5-dihydroxybenzoate; dobbc = 2,5-dioxido-1,4-benzenedicarboxylate; ebdc = 5,5'-(1,2-ethynediyl)-bis(1,3-benzenedicarboxylate); fddi = tetramethyl 5,5'-(9H-flourene-2,7-diy)diisophthalate acid; H<sub>2</sub>tbcpmm = {3,5-bis[(4-carboxyl)phenyl]phenyl}methane; iBu-stpdc = 4,4',4''-(isobutylisilanetriyl)tris-(triphenyl-3,5-dicarboxylate); Im = imidazole; Me-stpdc = 4,4',4''-(methylisilanetriyl)tris-(triphenyl-3,5-dicarboxylate); MeIM = 2-methylimidazole; ndc = 2,6-naphthalenedicarboxylate; 2,7-ndc = 2,7-naphthalenedicarboxylate; 1,4-nddi = 5,5'-naphthalene-1,4-diy]diisophthalate; 2,6-nddi = 5,5'-naphthalene-2,6-diy]diisophthalate; NH<sub>2</sub>-bdc = 2-amino-1,4-benzenedicarboxylate; ntei = 5,5',5''-(4,4',4''-nitro)tris(benzene-4,1-diy)tris(ethyne-2,1-diy)]trisophthalate; OH-stpdc = 4,4',4''-(hydroxylisilanetriyl)tris-(triphenyl-3,5-dicarboxylate); pdjdj = 5,5'-(pyridine-2,5-diy)diisophthalate; ptei = 5,5'-(5'-(4-(3,5-dicarboxyphenyl)ethynyl)phenyl)-1,1',3',1''-terphenyl]-4,4'-diyl]bis(ethyne-2,1-diy)]diisophthalic acid; qpcc = quaterphenyl-3,3''',5,5''',5''''-tetracarboxylate; sbrc = *trans*-stilbene-3,3',5,5'-tetracarboxylate; tcbpa = tris(4-carboxyphenyl)amine; tecpbb = 1,3,5-tris[(1,3-carboxylate-5-(4-(ethynyl)phenyl)butadienyl]-benzene); topbda = N,N,N',N'-tetrakis(4-carboxyphenyl)biphenyl-4,4'-diamine; tdpac = 2,4,6-tris(3,5-dicarboxyphenylamino)-1,3,5-triazine; ted = triethylenediamine; tipb = 1,2,4,5-tetra(5-isophthalate)-benzene; tpic = terphenyl-3,3',5,5'-tetracarboxylate. <sup>b</sup> Values were extrapolated from adsorption isotherms when not explicitly stated in the text or EST. Excess adsorption was converted to total using reported pore volumes and the bulk CH<sub>4</sub> density from the NIST REFPROP database. <sup>c</sup> This is the real, measured density of the pellet. Note that the pellet contains 2% Alox C and 3% graphite as additives. <sup>d</sup> Not specified whether uptake is in terms of excess, total or absolute adsorption. Consequently, values are simply reproduced from original publication and not converted. <sup>e</sup> Pore volume was taken from this work to calculate total adsorption. <sup>f</sup> Structure of framework during CH<sub>4</sub> adsorption is uncertain, and volumetric adsorption cannot be reasonably estimated. Also, it is not specified whether uptake is in terms of excess, total or absolute adsorption.

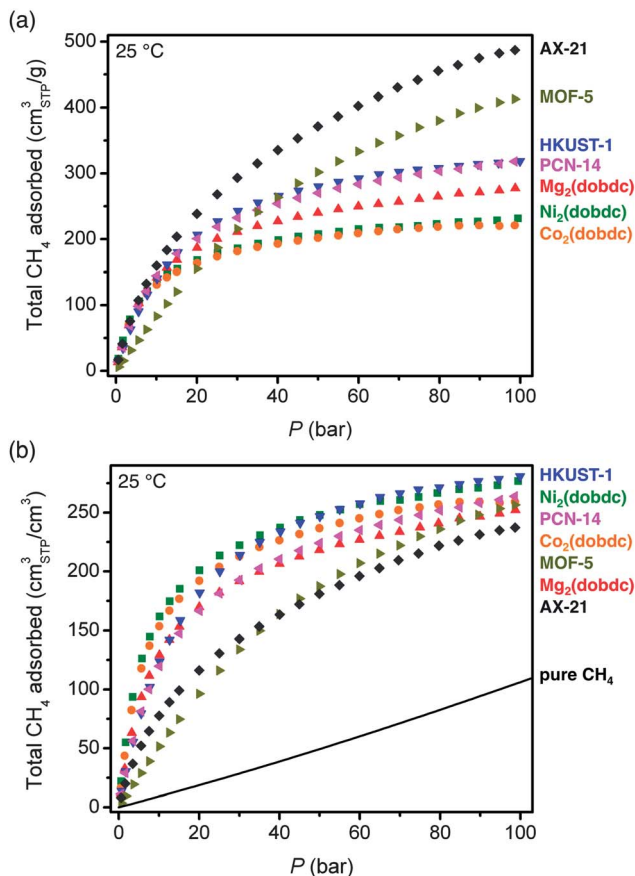


Fig. 3 Total gravimetric (top) and volumetric (bottom)  $\text{CH}_4$  adsorption isotherms at 25 °C. Note that crystallographic densities were used to calculate volumetric adsorption. The solid line corresponds to the volumetric density of pure  $\text{CH}_4$  at 25 °C.

In Fig. 3, the 25 °C high-pressure  $\text{CH}_4$  isotherms of all materials measured in this work are compared in terms of total gravimetric and volumetric adsorption. Of the materials

measured, AX-21 has the highest gravimetric uptake at all pressures. For the metal–organic frameworks, HKUST-1 has the highest gravimetric uptake ( $255 \text{ cm}^3_{\text{STP}} \text{ g}^{-1} = 0.183 \text{ g}_{\text{CH}_4} \text{ g}^{-1}$ ) at 35 bar, but the capacity of MOF-5 is highest at pressures greater than 40 bar. At high pressures, the gravimetric capacity is reasonably well correlated with the gravimetric surface area (Fig. S38<sup>†</sup>), which is consistent with previous observations for both metal–organic frameworks and activated carbons.<sup>7,13,24f,h,61</sup> Indeed, the metal–organic frameworks in Table 2 with the three highest reported gravimetric uptakes at 25 °C and 35 bar all have exceptionally high specific surface areas: DUT-49 with an uptake of  $0.26 \text{ g}_{\text{CH}_4} \text{ g}^{-1}$  and a surface area of  $5476 \text{ m}^2 \text{ g}^{-1}$ , NU-111 with an uptake of  $0.24 \text{ g}_{\text{CH}_4} \text{ g}^{-1}$  and a surface area of  $4930 \text{ m}^2 \text{ g}^{-1}$ , and PCN-68 with an uptake of  $0.24 \text{ g}_{\text{CH}_4} \text{ g}^{-1}$  and a surface area of  $5109 \text{ m}^2 \text{ g}^{-1}$ .<sup>48,50</sup>

In addition to the different  $\text{CH}_4$  capacities of the frameworks studied here, there are important differences in the shapes of their adsorption isotherms. Specifically, AX-21 and MOF-5 have shallower isotherms at low pressures and do not begin to approach saturation until much higher pressures than  $\text{Mg}_2(\text{dobdc})$ , HKUST-1, and PCN-14. This is expected based on the lack of strong adsorption sites in AX-21 and MOF-5, and has important consequences for the amount of  $\text{CH}_4$  that can actually be delivered by each material.

Importantly, as will be discussed in detail below, achieving a high volumetric adsorption capacity is much more critical than a high gravimetric capacity for extending the driving range of a vehicle. While the overall shapes of the volumetric isotherms are similar to the gravimetric ones, the trends in capacity differ significantly. For instance,  $\text{Ni}_2(\text{dobdc})$  and  $\text{Co}_2(\text{dobdc})$  have the highest uptakes at lower pressures, and  $\text{Ni}_2(\text{dobdc})$  and HKUST-1 have the highest total volumetric uptakes at 35 bar: 230 and 225 v/v, respectively. Note that the total volumetric uptake of  $\text{Ni}_2(\text{dobdc})$  is the highest value yet reported for any metal–organic framework at 25 °C and 35 bar. Although PCN-14 has been widely cited as the best existing metal–organic framework

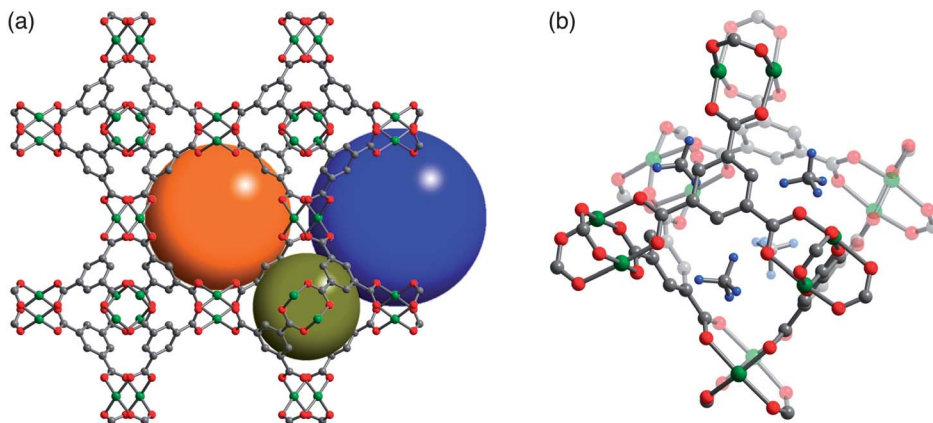


Fig. 4 (a) Crystal structure of HKUST-1 highlighting the three different types of pores in the structure that have diameters of roughly 5 Å (dark yellow), 11 Å (orange), and 13.5 Å (blue). Note that the open coordination site of the exposed  $\text{Cu}^{2+}$  cations is only directed into the 13.5 Å (blue) pores. Atomic coordinates are taken from a desolvated crystal structure at 100 K.<sup>51</sup> (b) Location of adsorbed  $\text{CD}_4$  molecules at the four windows sites of an octahedral cage. The atomic coordinates are taken from a powder neutron diffraction structure with a loading of 1.1  $\text{CD}_4$  per  $\text{Cu}^{2+}$  at 4 K.<sup>44c</sup> Green, gray, red, and light blue spheres represent Cu, C, O, and D atoms, respectively; H atoms have been omitted for clarity.



for volumetric CH<sub>4</sub> storage, Ni<sub>2</sub>(dobdc) and HKUST-1 have significantly higher volumetric capacities at 35 bar and 25 °C.

It is worth noting that in contrast to gravimetric adsorption, the volumetric uptake at 35, 65, or 100 bar, does not correlate with volumetric surface area (Fig. S39†). Indeed, MOF-5 has a volumetric surface area 30% greater than Ni<sub>2</sub>(dobdc), but a volumetric uptake that is lower at all pressures measured here of less than 100 bar. This highlights the importance of the density and strength of specific CH<sub>4</sub> adsorption sites, rather than just surface area and pore volume, for achieving high volumetric capacities.

### Methane adsorption sites in Ni<sub>2</sub>(dobdc) and HKUST-1

While Ni<sub>2</sub>(dobdc) and HKUST-1 have the highest volumetric uptakes of all metal–organic frameworks reported to date (Table 2), they are still well short of the 350 v/v target that is expected to achieve a volumetric energy density similar to that of CNG. In designing a next generation of improved framework materials to meet this target, it is useful to consider the fundamental mechanisms responsible for the high volumetric uptakes of Ni<sub>2</sub>(dobdc) and HKUST-1. Detailed powder X-ray and neutron diffraction experiments have previously been used in several studies to identify the strongest CH<sub>4</sub> adsorption sites in both structures.<sup>42,44</sup> Note that the only structural study of CH<sub>4</sub> in M<sub>2</sub>(dobdc) was for the Mg analogue,<sup>42</sup> but based on the similar adsorption isotherms and previous structural studies with H<sub>2</sub> and CO<sub>2</sub>,<sup>41d-f,i,j,l,m</sup> it is reasonable to expect similar CH<sub>4</sub> binding sites within Ni<sub>2</sub>(dobdc).

In both HKUST-1 and Ni<sub>2</sub>(dobdc), the exposed Cu<sup>2+</sup> and Ni<sup>2+</sup> cations act as strong binding sites that can contribute a maximum of 98 v/v and 172 v/v, respectively, to the total volumetric capacity when one CH<sub>4</sub> is bound to each metal. These are the only strong binding sites expected in Ni<sub>2</sub>(dobdc), and just weaker secondary adsorption sites should be available for CH<sub>4</sub> after the Ni<sup>2+</sup> sites are fully occupied.<sup>42</sup> In contrast, HKUST-1 has additional strong adsorption sites, located in the four windows of each octahedral cage, which are populated at the same time as the Cu<sup>2+</sup> sites,<sup>44</sup> suggesting both adsorption sites have similar CH<sub>4</sub> binding energies (Fig. 4). These window sites bind CH<sub>4</sub> strongly due to several close interactions, in the range 2.7–3.2 Å, between framework O atoms and an adsorbed CH<sub>4</sub> molecule (Fig. S47†).

Significantly, the window sites can contribute an additional 65 v/v to the volumetric capacity of HKUST-1, bringing the total contribution of strong adsorption sites to 163 v/v, just below that of Ni<sub>2</sub>(dobdc) (172 v/v). On the other hand, there is a more pronounced difference in the contribution of strong adsorption sites to the total gravimetric capacity of each material at 144 cm<sup>3</sup><sub>STP</sub> g<sup>-1</sup> and 185 cm<sup>3</sup><sub>STP</sub> g<sup>-1</sup> for Ni<sub>2</sub>(dobdc) and HKUST-1, respectively. Further, while both materials have similar volumetric surface areas (Table S1†), HKUST-1 has a significantly greater gravimetric surface area that can be expected to lead to a higher gravimetric density of weak CH<sub>4</sub> adsorption sites. Taken together, the similar volumetric and different gravimetric capacities of strong and weak adsorption sites can help explain the experimental CH<sub>4</sub> isotherms, wherein both materials have

similar volumetric uptakes at 35 bar, but HKUST-1 has a much higher gravimetric uptake. In order to explain why Ni<sub>2</sub>(dobdc) has a steeper isotherm at lower pressures, it is necessary to also consider differences in the binding energies of the strong adsorption sites of each material.

### Isosteric heats of adsorption

To gain further insight into differences between the seven materials, isosteric heats of adsorption ( $Q_{st}$ ), which represent the average binding energy of an adsorbing molecule at a specific surface coverage, were determined as a function of the amount of CH<sub>4</sub> adsorbed,  $n$ , by using the Clausius–Clapeyron relation (eqn (3)).<sup>52</sup>

$$-Q_{st} = RT^2 \left( \frac{\partial \ln P}{\partial T} \right)_n \quad (3)$$

In order to employ this relation, it is first necessary to fit the high-pressure isotherm data with a mathematical model, such that it is possible to interpolate between measured data points to determine the exact pressures that correspond to the same amount adsorbed at different temperatures. Regardless of the mathematical model used, it is important to remember that the Clausius–Clapeyron equation is fundamentally a thermodynamic relation that describes a phase transition of a gas from a bulk to adsorbed state, and as such, it is based on the absolute amount adsorbed, which includes all gas molecules that experience an attractive potential from the adsorbent surface.<sup>26d</sup> For microporous materials, the total adsorption is often used as an approximation for absolute in heat of adsorption calculations, as most gas molecules inside micropores will have some degree of interaction with the pore surface.<sup>22a,29</sup> In contrast to low-pressure experiments, there is a significant difference between excess and total adsorption at high pressures, and *it is critical that the total adsorption is used for all thermodynamic calculations*,<sup>36</sup> unless the relevant thermodynamic relations have been specifically altered for excess quantities.<sup>26d</sup>

Virial-type equations have been routinely used to fit high-pressure adsorption data for metal–organic frameworks,<sup>53</sup> despite the fact that most virial parameters lack any physical meaning.<sup>54</sup> In contrast, equations that are based on physical models of adsorption, such as the Dubinin–Astakhov (DA)<sup>55</sup> and multi-site Langmuir equations,<sup>56</sup> have been more widely used in analyzing CH<sub>4</sub> isotherms of activated carbons.<sup>57</sup> One major advantage of fitting isotherm data with physically relevant parameters is that it makes extrapolation to temperatures and pressures that were not experimentally measured more meaningful, which is important not only for calculating heats of adsorption but also for process modeling and systems design. Additionally, errors in high-pressure isotherm data can be significant, especially when compared to low-pressure experiments, and leveraging at least some physical constraints on the fitting parameters can help ensure that the resulting isosteric heats are reasonable. Here, single- and dual-site Langmuir models were used to fit the adsorption data of each material at all measured temperatures with one set of parameters (see ESI† for details). Several recent studies have demonstrated the ability



of Langmuir-type equations to successfully model adsorption in metal–organic frameworks, especially those that have well-defined adsorption sites on the pore surface.<sup>36,41*n*-7,58</sup>

The importance of the method used for calculating  $Q_{st}$  can be illustrated by examining the heats of adsorption originally reported for PCN-14, wherein the low-coverage binding enthalpy of  $-30 \text{ kJ mol}^{-1}$  is nearly double the value of  $-18 \text{ kJ mol}^{-1}$  determined in this work (Fig. S37†).<sup>45*a*</sup> It was suggested that this record high heat of adsorption was largely responsible for the high volumetric uptake of PCN-14, but no details of the  $Q_{st}$  calculations were reported. While PCN-14 certainly does exhibit high volumetric uptake, the reported values of  $Q_{st}$ , which influenced several follow-up computational studies,<sup>24*h*,44*c*,45*b*</sup> can hinder efforts to understand the underlying adsorption mechanisms that are responsible and to design improved materials.

For all seven materials evaluated in this work, the isosteric heats of adsorption as a function of the total  $\text{CH}_4$  loading are plotted in Fig. 5. As expected based upon its steep isotherm and high volumetric uptake,  $\text{Ni}_2(\text{dobdc})$  has the highest  $Q_{st}$  at low coverage, followed by  $\text{Co}_2(\text{dobdc}) > \text{Mg}_2(\text{dobdc}) > \text{PCN-14} \sim \text{HKUST-1} > \text{AX-21} > \text{MOF-5}$ . It is interesting to note differences in the shape of  $Q_{st}$  curves as the  $\text{CH}_4$  loading is increased. For example, the  $\text{M}_2(\text{dobdc})$  compounds have relatively constant binding energies at low loadings that begin to decrease as the exposed metal cation sites become populated. On the other hand, PCN-14 and HKUST-1 have heats of adsorption near  $-17 \text{ kJ mol}^{-1}$  regardless of the amount of  $\text{CH}_4$  adsorbed, confirming that the exposed  $\text{Cu}^{2+}$  cations and window adsorption sites in both materials have similar  $\text{CH}_4$  binding strengths. Likewise, MOF-5 exhibits a constant, but much weaker, binding energy of  $-12.3 \text{ kJ mol}^{-1}$ . These differences are consistent with the shapes of the adsorption isotherms, for which the  $\text{M}_2(\text{dobdc})$  compounds have the steepest rises at low pressures, while MOF-5 is the most shallow. Note that the gradual decline in the isosteric heat of adsorption of AX-21 from 15.5 to  $12.4 \text{ kJ mol}^{-1}$  is likely due to the wide distribution of pore sizes present

in the activated carbon, whereby smaller pores will tend to have stronger interactions with  $\text{CH}_4$  than larger pores.

It is important to emphasize that while the single- and dual-site Langmuir models used here describe the experimental adsorption data very well over a wide temperature and pressure range, there may be other models that result in equally good, or in some cases perhaps even better, fits to the data. Some of these models may involve an increase in the isosteric heat of adsorption at high  $\text{CH}_4$  loadings due to the contribution of  $\text{CH}_4 \cdots \text{CH}_4$  interactions at high pressures, as has been reported for several frameworks.<sup>59</sup> Unfortunately, the experimental high-pressure adsorption data is typically not accurate enough to determine reliably whether such an increase actually exists in any of the materials studied here. However, it is worth noting that several studies have clearly shown that using excess adsorption isotherms to calculate  $Q_{st}$  can lead to large increases in  $Q_{st}$  at higher loadings that do not occur when using absolute or total adsorption.<sup>28,36</sup> Moreover, the contribution of  $\text{CH}_4 \cdots \text{CH}_4$  interactions to the overall heat of adsorption has been estimated to be less than  $2 \text{ kJ mol}^{-1}$ , which would be difficult to detect accurately at the high pressures where it would be most influential and the adsorption data is least accurate.<sup>60</sup> Regardless, the differences in isosteric heats of adsorption at pressures most relevant to ANG storage are clear, and these have important consequences for the amount of  $\text{CH}_4$  that can actually be delivered by each material inside a vehicle.

## Usable $\text{CH}_4$ capacity

Comparing the 35 bar  $\text{CH}_4$  capacities of different adsorbents is useful for initial evaluations, but not all of this capacity will be accessible when delivering natural gas to an engine that requires a minimum inlet pressure to operate. As such, the usable  $\text{CH}_4$  capacity is defined as the amount of  $\text{CH}_4$  that can be delivered when decreasing from the filling or adsorption pressure to a specific desorption pressure (Fig. 6a).<sup>28</sup> For ANG storage, the adsorption pressure is usually assumed to be 35 bar, since this is a typical benchmark for the maximum achievable pressure of inexpensive single-stage compressors.<sup>16</sup> While 5 bar is commonly cited as a minimum desorption pressure,<sup>49,61</sup> engines that can operate at inlet pressures as low as 3 bar are available and would allow for a greater usable  $\text{CH}_4$  capacity and increased vehicle driving range. Currently, most natural gas vehicles contain gasoline engines that have been retrofitted to run on natural gas and require inlet pressures of 5 to 10 bar. If the demand for natural gas vehicles increases dramatically, the minimum operating pressure may decrease as engines are built and optimized specifically to burn natural gas. It is important to note that the amount of  $\text{CH}_4$  retained by the adsorbent during desorption can also be reduced by heating, ideally taking advantage of waste heat from the engine.<sup>62</sup>

The volumetric usable  $\text{CH}_4$  capacities of all materials evaluated here are plotted in Fig. 6b for adsorption at 35 bar and  $25^\circ\text{C}$  and desorption at 5 bar and temperatures from 25 to  $145^\circ\text{C}$ . Despite the fact that  $\text{Ni}_2(\text{dobdc})$  has a higher total volumetric uptake at 35 bar, HKUST-1 has the highest usable  $\text{CH}_4$  capacity for all calculated desorption temperatures. This is

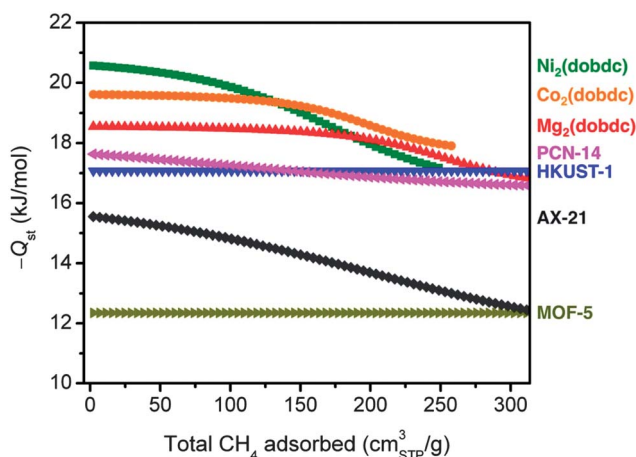


Fig. 5 Isosteric heats of adsorption,  $-Q_{st}$ , at  $25^\circ\text{C}$  as a function of the total amount of  $\text{CH}_4$  adsorbed.





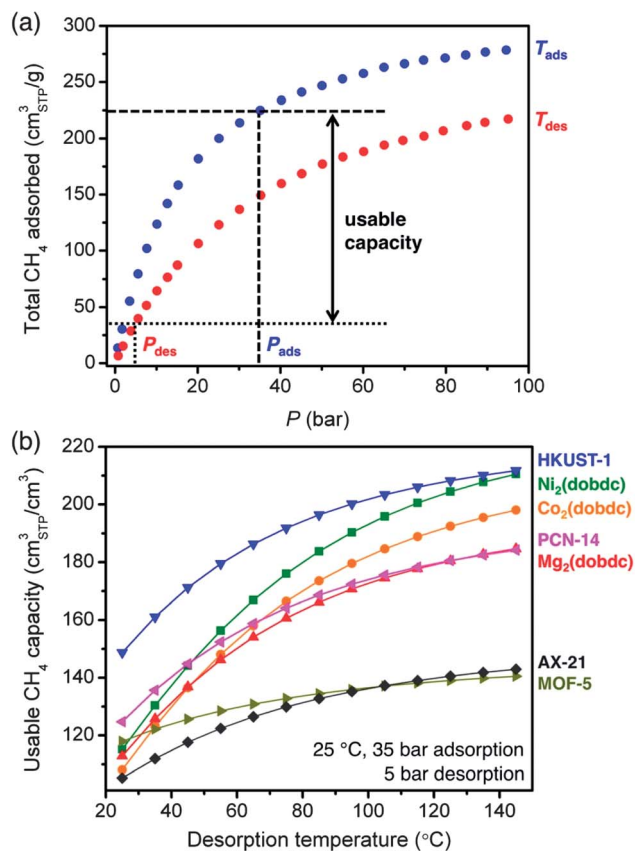


Fig. 6 (a) The usable capacity represents the amount of CH<sub>4</sub> that can be delivered when discharging from a specific adsorption temperature,  $T_{\text{ads}}$ , and pressure,  $P_{\text{ads}}$ , to a desorption temperature,  $T_{\text{des}}$ , and pressure,  $P_{\text{des}}$ . (b) The volumetric usable CH<sub>4</sub> capacity as a function of desorption temperature for adsorption at 25 °C and 35 bar and desorption at 5 bar.

a direct result of the weaker interaction of CH<sub>4</sub> with HKUST-1 than with Ni<sub>2</sub>(dobdc), which results in significantly less CH<sub>4</sub> retained by HKUST-1 at 5 bar. Indeed, the usable CH<sub>4</sub> capacity of Ni<sub>2</sub>(dobdc) is only 115 v/v for desorption at 25 °C, which is just 50% of its 35 bar capacity. In contrast, the usable capacity of HKUST-1 under the same conditions is 149 v/v, which is 66% of its 35 bar capacity.

The gravimetric usable CH<sub>4</sub> capacity is plotted in Fig. S40† for the same adsorption–desorption conditions. In this case, AX-21 has the highest usable capacity at all desorption temperatures, while MOF-5 is the best metal–organic framework for desorption temperatures below 60 °C. Although HKUST-1 exhibits a higher total gravimetric uptake at 35 bar, its usable capacity is below that of MOF-5 unless the desorption temperature is increased. This is due to the weak interaction of MOF-5 with CH<sub>4</sub> (−12 kJ mol<sup>−1</sup>), which results in only a small amount of CH<sub>4</sub> adsorbed at 5 bar. Usable capacity plots as a function of desorption pressure are also given in the ESI† and show similar trends between materials, as is expected since decreasing the desorption pressure has a similar effect to increasing the desorption temperature (Fig. S41–S42†).

Adsorption at lower temperatures or higher pressures can also be considered as a strategy for increasing the usable

capacity (Fig. S43–S46†). Indeed, by decreasing the adsorption temperature to −25 °C, the usable capacity of HKUST-1 reaches 222 v/v for desorption at 5 bar and 25 °C, which is 67% greater than for adsorption at 25 °C. However, a full systems-level analysis is necessary to determine whether the higher costs associated with cooling the fuel and the thermal management of the tank, or with compressing natural gas to higher pressures, would be worth the increase in usable capacity and driving range.

Of all the metal–organic frameworks previously evaluated by others and those studied here, HKUST-1 appears to be the most promising current framework for natural gas storage, as it features one of the highest usable volumetric capacities for CH<sub>4</sub>. A similar conclusion was also reached by others while this manuscript was in preparation,<sup>63</sup> and it is perhaps not surprising that HKUST-1 was chosen by BASF for use in a prototype ANG van in 2007.<sup>64</sup>

### Optimal binding enthalpy

The differences in the usable CH<sub>4</sub> capacities between the materials studied illustrate the importance of both increasing capacity and optimizing binding enthalpy when designing improved adsorbents. If the binding enthalpy is too high, then too much CH<sub>4</sub> will be retained at low pressures, decreasing the usable capacity. On the other hand, if the binding enthalpy is too low, then too little CH<sub>4</sub> will be adsorbed at higher pressures. Using a single-site Langmuir model, it can be shown that the optimal binding enthalpy for CH<sub>4</sub> adsorption at 35 bar and 25 °C and desorption at 5 bar is −17 kJ mol<sup>−1</sup>,<sup>65</sup> exactly equal to that determined for HKUST-1 over the entire pressure range of 5 to 35 bar.

Note that the optimal binding enthalpy is dependant on the exact desorption conditions used. Indeed, Fig. 7 shows the percentage of the saturation capacity that is usable at different binding energies and desorption temperatures. As the desorption

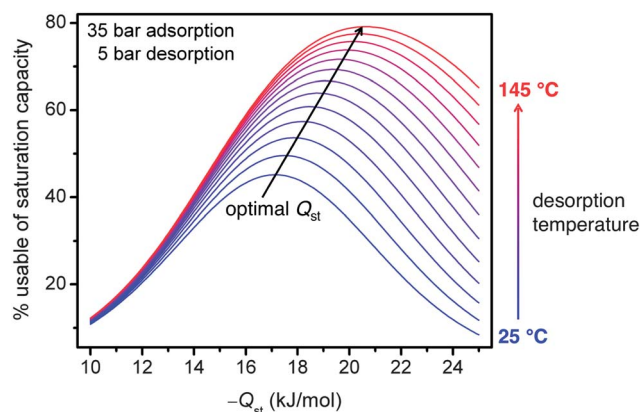


Fig. 7 Assuming a single-site Langmuir isotherm, the percentage of the saturation capacity that is usable is plotted for isosteric heats of adsorption,  $Q_{\text{st}}$ , ranging from −10 to −25 kJ mol<sup>−1</sup> and desorption temperatures from 25 to 145 °C, with adsorption at 35 bar, desorption at 5 bar, and a molar entropy of adsorption of −9.5 R. As the desorption temperature increases, the optimal  $Q_{\text{st}}$  and usable capacity also increase.<sup>65</sup>





temperature is increased, or desorption pressure decreased, the optimal binding enthalpy increases (see ESI† for details). Note that the simple analysis presented here ignores correlations between the adsorption enthalpy and entropy, but these correlations would be expected to lead to even larger increases in the optimal  $Q_{st}$  as the desorption temperature is increased.<sup>66</sup> Regardless, Fig. 7 illustrates the importance of optimizing binding enthalpy and the benefits of using higher desorption temperatures to maximize usable capacity. Nevertheless, employing a material with optimal binding enthalpy is useless if the density of adsorption sites having that enthalpy is small, resulting in a low optimized capacity. Since dramatic improvements in both gravimetric and volumetric capacities are needed to meet the Department of Energy targets at 35 bar and ambient temperature, increasing capacity must be the primary focus of materials development efforts, but these efforts will be most beneficial if the binding enthalpy is near optimal.

### Relative importance of gravimetric and volumetric capacity

It is important to recognize that the acceptability and viability of natural gas vehicles are directly linked to their utility and value to the customer. As indicated, the lower volumetric energy density of compressed natural gas significantly reduces the driving range in comparison to conventional gasoline vehicles and therefore reduces the utility of the vehicle. In designing a next generation of adsorbents for natural gas storage, it is essential to consider the relative importance of improvements in gravimetric *versus* volumetric usable capacity toward increasing the maximum achievable driving range of an ANG vehicle.

In order to make the comparison more informative, the effects of changes in gravimetric and volumetric usable capacity on driving range are considered independently using a few simple assumptions (Fig. 8). In the gravimetric case, a 10 GGE (gallons gasoline equivalent) vehicle is assumed to have an adsorbent

capable of delivering  $0.12 \text{ g}_{\text{CH}_4} \text{ g}^{-1}$ , which is equal to the usable capacity of HKUST-1 for 35 bar adsorption and 5 bar desorption at 25 °C. In order to isolate the effects of changing the usable gravimetric capacity, this analysis assumes a fixed volumetric capacity and changes in gravimetric capacity thus lead to an increase or decrease in the weight of adsorbent required to achieve a 10 GGE energy density ( $2.567 \text{ kg CH}_4$ ).<sup>67</sup> As a general rule, the fuel economy on conventional light-duty vehicles can be improved or reduced by up to 2% per 100 lbs (45 kg) of weight subtracted or added.<sup>68</sup> Since the total amount of natural gas is fixed, changes in the fuel economy are directly proportional to changes in the driving range for this scenario. For example, a 10% improvement in the usable gravimetric capacity of HKUST-1 results in a 19 kg reduction in weight and a 0.8% improvement in fuel economy and driving range.

To isolate the effects of changing usable volumetric capacity, it is assumed that a light-duty vehicle will have a fixed amount of space available for a fuel tank. As a result, there is a roughly 1 : 1 correlation between the usable volumetric capacity of an adsorbent and the expected driving range of a vehicle.

As shown in Fig. 8, improvements in gravimetric capacity have considerably less impact than improvements in volumetric capacity. While increases in gravimetric capacity are still important, similar improvement percentages do not have as significant an impact as volumetric on increasing driving range since the increased weight of the adsorbent material has a minor effect on the fuel economy of the vehicle. Therefore, increasing the usable volumetric  $\text{CH}_4$  capacity is significantly more important than increasing the usable gravimetric capacity for natural gas storage in light-duty vehicles.

These relationships, along with knowledge of the importance of certain vehicle attributes to consumers, such as driving range and cost, are critical for directing adsorbent material improvements and tradeoffs toward the optimal solution for a viable ANG system.

## Adsorbed natural gas system requirements

While working to synthesize a next generation of metal–organic frameworks with improved volumetric and gravimetric capacities, it is also important to consider the complete ANG storage system, as there are several factors that can dramatically affect the ultimate performance of a material when delivering natural gas to an engine. It is worth noting that many of these systems-level issues are not just engineering problems and are fundamentally related to materials properties that can potentially be tuned through synthetic chemistry to improve performance.

### Thermal properties

In an actual ANG system, the heats of adsorption (exothermic) and desorption (endothermic) will likely lead to large temperature changes that both have a negative impact on the usable  $\text{CH}_4$  capacity.<sup>69</sup> Specifically, an adsorbent bed will release heat during refueling and cool during discharge, resulting in less  $\text{CH}_4$  stored during adsorption and more retained during desorption. Faster

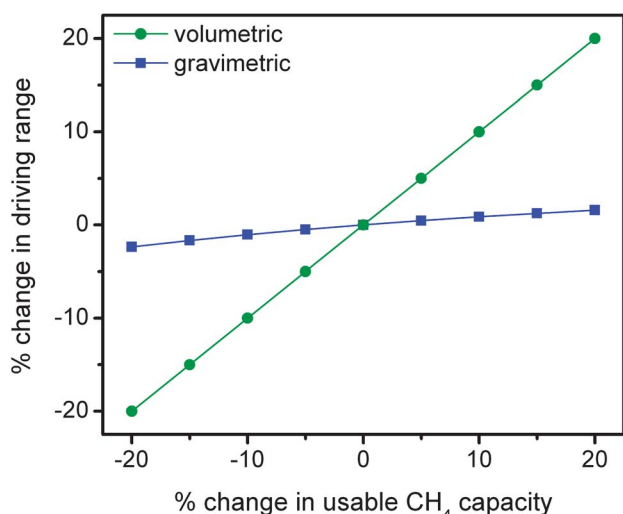


Fig. 8 Effects of changes in gravimetric and volumetric  $\text{CH}_4$  usable capacity on vehicle driving range. To isolate each effect, the gravimetric case assumes a 10 GGE vehicle with a constant volumetric capacity, while the volumetric case assumes a fixed amount of space available for a fuel tank and a constant gravimetric capacity.



refueling and discharge rates, which are often desirable, lead to even greater temperature changes. Indeed, a prototype activated carbon storage tank cooled by as much as 37 °C at a discharge rate typical for a normal driving speed, resulting in a 20% loss in CH<sub>4</sub> capacity compared to isothermal desorption.<sup>69</sup> Various thermal management strategies have been proposed to minimize the impacts of heat flowing in and out of the adsorbent bed, including incorporating a heat exchanger inside the storage tank, changing how natural gas flows inside the tank, and altering the material and geometry of the tank.<sup>13,69,70</sup> While some form of thermal management will ultimately be necessary, all of these engineering solutions involve a significant tradeoff between cost, weight, and available space.

More importantly, all efforts to manage heat flow are highly dependent on the heat capacity and thermal conductivity of the adsorbent. High heat capacities decrease the magnitude of temperature changes resulting from the energy released or consumed during adsorption and desorption, while high thermal conductivities allow heat to dissipate more quickly and permit the use of simpler external or internal temperature control systems. With this in mind, it is worth noting that overcoming thermal management challenges is not just an engineering problem, and there can be a significant contribution from a more fundamental materials synthesis perspective.

While heat capacities have been reported for several metal-organic frameworks,<sup>41a,71</sup> to the best of our knowledge, there have been just two thermal conductivity measurements, both of which were for MOF-5.<sup>72</sup> As is typical of many porous materials, the MOF-5 thermal conductivities were very low at less than 0.32 W m<sup>-1</sup> K<sup>-1</sup> for both a single crystal and packed powder. It is possible to improve the thermal conductivity by incorporating an additive such as graphite, but this will lead to a decrease in both the gravimetric and volumetric CH<sub>4</sub> capacities.<sup>72b</sup> To better understand these tradeoffs, there is a clear need for thermal conductivity and heat capacity measurements on a much wider range of metal-organic frameworks, especially with experiments designed to identify structural and chemical features that are likely to lead to frameworks with higher intrinsic thermal conductivities and heat capacities.

### Mechanical properties

As has been emphasized, the volumetric CH<sub>4</sub> capacity of an adsorbent has a critical impact on the ultimate driving range of an ANG vehicle. Notably, almost all reported volumetric uptakes for metal-organic frameworks, including those in this study, are calculated using the density of a perfect single crystal and represent the maximum possible volumetric capacity. In reality, metal-organic frameworks synthesized on a large enough scale to fill a fuel tank will likely be powders that contain a significant amount of empty space between particles. This interparticle void space results in a much lower density, and consequently a lower volumetric CH<sub>4</sub> capacity, for a bulk powder than that calculated for a single crystal. Indeed, the bulk powder density of MOF-5 was measured at just 0.13 g cm<sup>-3</sup>, 79% less than the single crystal density of 0.621 g cm<sup>-3</sup>.<sup>73d</sup> Note that in addition to decreasing volumetric capacity, low packing densities also lead to lower thermal conductivities.

In order to minimize the losses in capacity and thermal conductivity that result from packing adsorbent particles inside a tank, it will be essential to compact the material in some fashion. Compaction reduces the interparticle void space and increases the bulk density of the powder, but it can also cause partial or complete collapse of framework pores. As a result, materials with higher mechanical stability are desirable, as they are more likely to survive compaction to higher densities without significant losses in porosity. While there have been initial studies on the intrinsic mechanical properties of different metal-organic frameworks, the majority of work has been limited to frameworks that can be synthesized as large single crystals.<sup>74</sup>

Additional research efforts have examined changes in surface area, pore volume, and gas uptake when compacting different metal-organic framework powders, including MOF-5, HKUST-1, and Ni<sub>2</sub>(dobdc), at increasing mechanical pressures.<sup>43c,73</sup> For instance, tablets of HKUST-1 compacted to 66% of its crystallographic density adsorbed just 94 v/v of CH<sub>4</sub> at 35 bar and 30 °C,<sup>43c</sup> highlighting the importance of packing losses on the actual volumetric capacity of an adsorbent. Similarly, a pellet of Ni<sub>2</sub>(dobdc) compacted with 0.1 GPa of pressure adsorbed just 100 v/v of CH<sub>4</sub> at 34 bar and 30 °C,<sup>73c</sup> significantly less than the 230 v/v measured here. These types of compaction studies are certainly useful, but it is difficult to compare the intrinsic mechanical properties of each material based on such measurements, since compaction is affected by particle size and shape in addition to mechanical stability. More importantly, comparisons of the volumetric usable capacity of different materials will be highly dependent on the mechanical stability of the framework and the maximum compaction density that can be achieved. Based on current work, the extent of varying degrees of mechanical stability between different metal-organic frameworks is poorly understood.

With this in mind, efforts to understand fundamental relationships between framework structure and mechanical properties will be extremely valuable in directing synthesis efforts toward robust materials that can be compacted to sufficiently high densities without structural changes that might affect CH<sub>4</sub> adsorption capacities.<sup>75</sup> Equally important will be research toward obtaining finer control over the size and morphology of metal-organic framework particles. In particular, studies on compacting activated carbons have demonstrated that significantly higher packing densities can be achieved when particles of two or more different sizes are mixed and compacted at the same time.<sup>76</sup> To our knowledge, there have not yet been any studies evaluating the effects of the particle size distribution and shape on the achievable packing density for metal-organic frameworks. Note that in addition to evaluating changes in porosity upon compaction, it is also important to consider potential effects on the adsorption and desorption kinetics, as fast kinetics are important for achieving practical refueling and discharge rates in a vehicle.<sup>77</sup>

### Natural gas impurities

Although CH<sub>4</sub> is the largest component, pipeline-quality natural gas contains many other impurities that can affect the long-term stability and capacity of an adsorbent (Table 3).<sup>78</sup> In an ANG vehicle, a guard bed will likely be placed before the storage



Table 3 Example composition of pipeline natural gas (Union Gas)<sup>79</sup>

Component	Mol. %
CH <sub>4</sub>	87–96
C <sub>2</sub> H <sub>6</sub>	1.5–5.1
C3 or greater hydrocarbons	0.1–2.3
C6 or greater hydrocarbons	<0.1
N <sub>2</sub>	0.7–5.6
CO <sub>2</sub>	0.1–1.0
O <sub>2</sub>	<0.1
H <sub>2</sub>	<0.02
H <sub>2</sub> O	<80 mg m <sup>-3</sup>
Sulfur (including odorants)	5.5 mg m <sup>-3</sup>

tank during refueling to minimize exposure to impurities.<sup>20</sup> Still, the adsorbent will inevitably be exposed to at least some level of each impurity throughout its lifetime. Additionally, most guard beds are unlikely to remove a significant amount of the C2 and C3 hydrocarbons that are present in natural gas, and it is unclear how this might affect the usable CH<sub>4</sub> capacity of an adsorbent. Smaller levels of other impurities, especially sulfur-containing compounds, H<sub>2</sub>O, O<sub>2</sub>, and C4 and greater hydrocarbons, may slowly poison CH<sub>4</sub> adsorption sites or degrade the framework over an extended time period. Performing cycling studies in the presence of all expected natural gas impurities will be critical to designing metal–organic frameworks with the long lifetimes necessary for use in a natural gas powered vehicle.

## Conclusions

With some of the highest volumetric and gravimetric CH<sub>4</sub> capacities ever reported, metal–organic frameworks have shown significant potential as adsorbents for natural gas storage. There are still, however, some formidable challenges to overcome before they are likely to find widespread use in natural gas vehicles. Most importantly, substantial increases in the usable volumetric capacity are needed for improving the driving range to levels closer to that of gasoline vehicles. To go beyond just incremental improvements in capacity, completely new design strategies will likely be necessary. For instance, new types of strong binding sites that occupy a small volume but can each polarize multiple CH<sub>4</sub> molecules should dramatically increase the volumetric density of stored CH<sub>4</sub>. Above all, any efforts to minimize the amount of wasted volume inside frameworks that does not contribute to optimally attracting CH<sub>4</sub> molecules, without significantly decreasing porosity, should be beneficial. This includes extra empty space inside large pores, as well as adsorption sites on the pore surface that are too weak or too strong for maximizing the usable capacity.

It is important to emphasize that efforts to design a next generation of high-capacity metal–organic frameworks for natural gas storage must address systems-level factors that will heavily influence the actual performance of a material, including compaction, heat capacity, thermal conductivity, and tolerance to impurities. Studies that address these areas are not only important for determining the practically achievable

usable capacity and lifetime of different materials, but improving our fundamental understanding of the relationship of framework structure and chemical composition with thermal properties, mechanical properties, and long-term stability will also help guide synthetic efforts toward the most useful materials. Ultimately, the cost of the material will also be an important factor in determining the competitiveness of an ANG vehicle. While it is difficult to predict the large-scale cost of organic ligands for which there are currently little demand, basic economic analyses of the best current metal–organic frameworks would be useful for identifying strategies to target materials with the greatest potential for scale-up to the levels required to have an impact in natural gas vehicles.

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